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(54) **ULTRACAPACITOR AND METHOD OF MANUFACTURING THE SAME**

(56) **References Cited**

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**Related U.S. Application Data**

(62) Division of application No. 12/021,491, filed on Jan. 29, 2008, now Pat. No. 8,027,147.

(60) Provisional application No. 60/886,981, filed on Jan. 29, 2007.

(51) **Int. Cl.**  
**H01G 9/00** (2006.01)

(52) **U.S. Cl.**  
USPC ..... **29/25.03**

(58) **Field of Classification Search**  
None  
See application file for complete search history.

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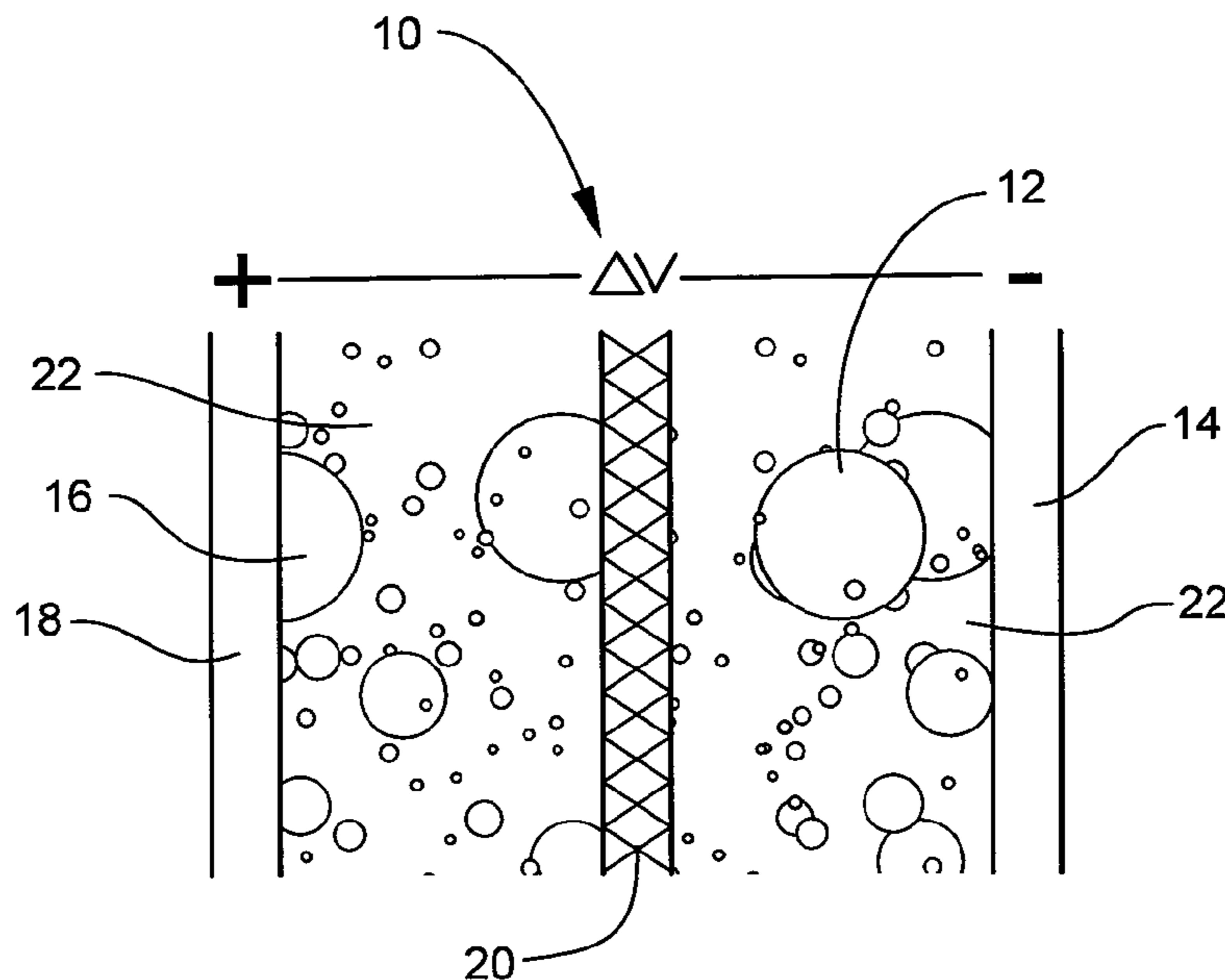
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(57) **ABSTRACT**

A method for producing an ultracapacitor comprises the steps of: providing a negative porous electrode in contact with a negative conducting plate; providing a positive porous electrode in contact with a positive conducting plate; providing an ultracapacitor separator being a microporous material that separates the negative porous electrode from the positive porous electrode; providing an electrolytic solution that impregnates the negative porous electrode, the positive porous electrode, and the ultracapacitor separator; and curing the ultracapacitor at a temperature of at least 200° C.

**8 Claims, 5 Drawing Sheets**



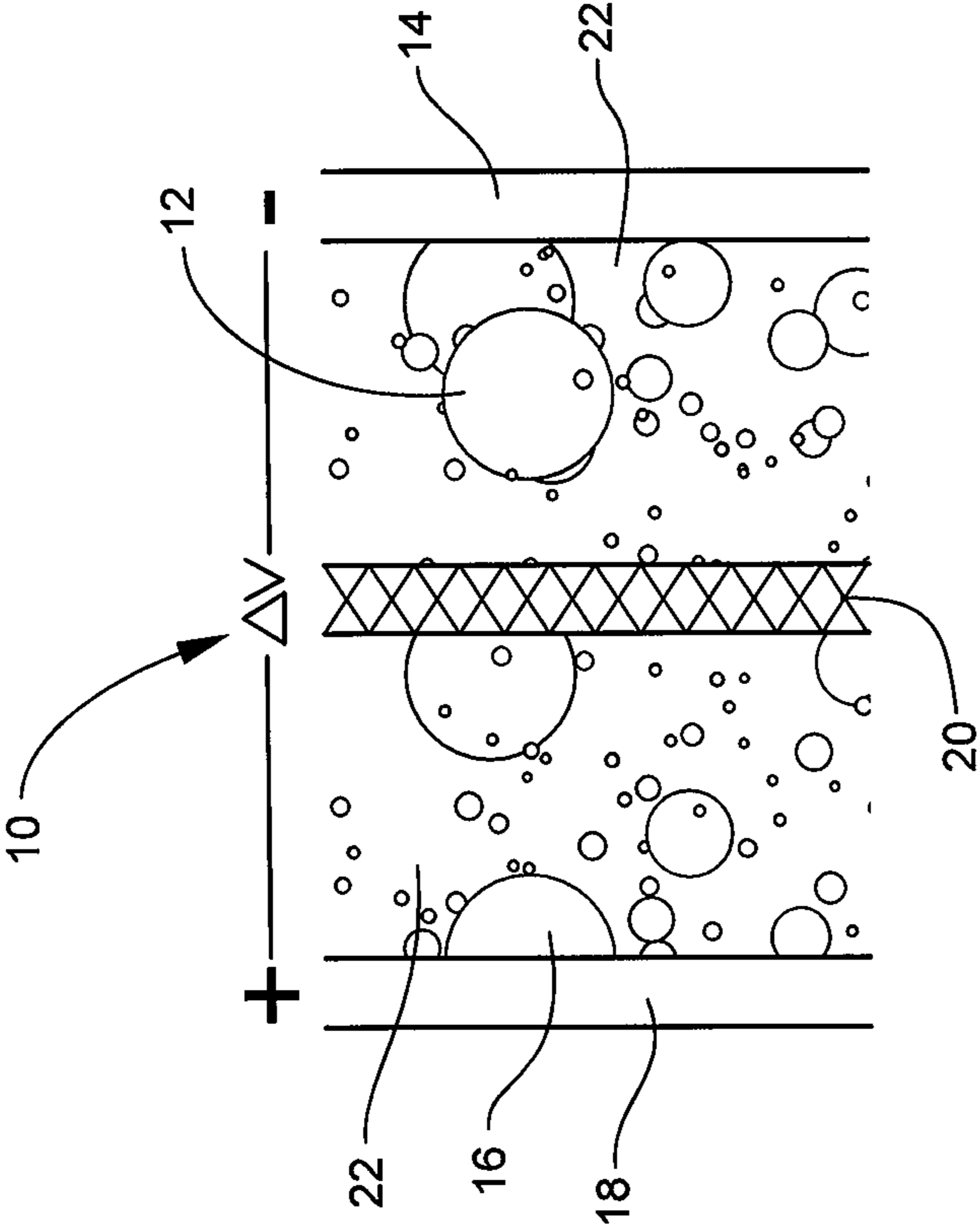


Fig. 1

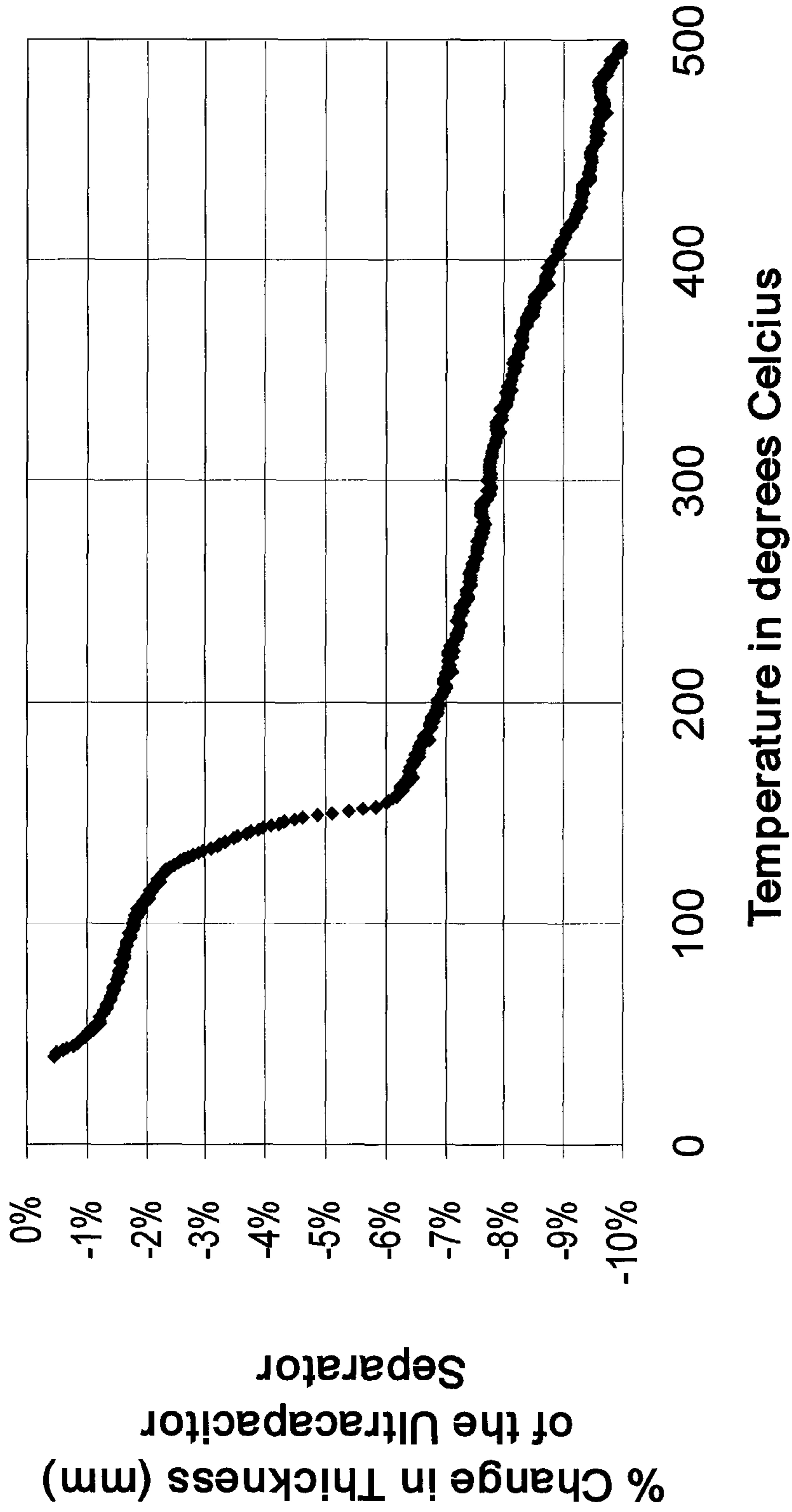


Fig. 2

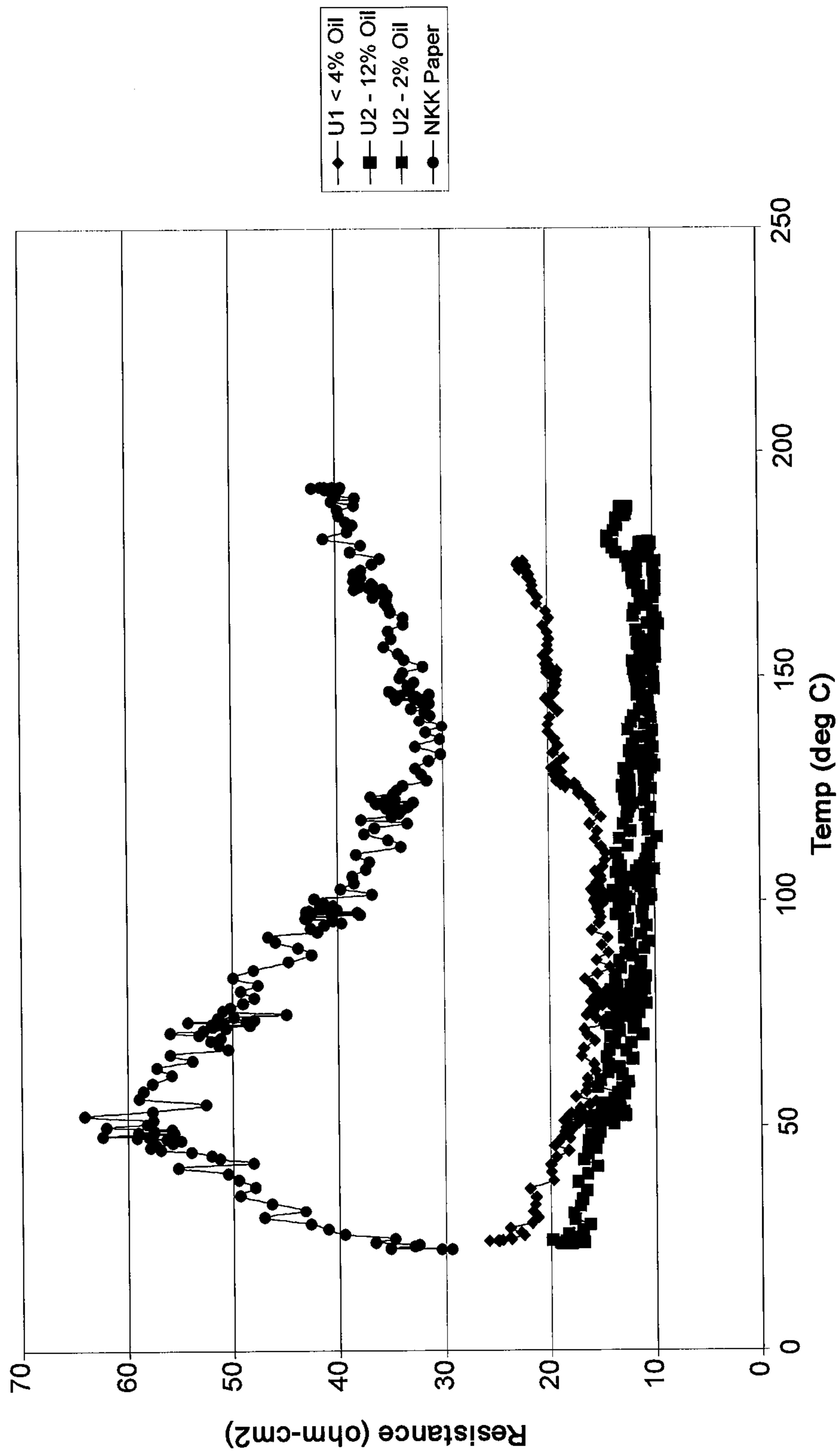


Fig. 3

Hg Porosimetry of Partial Compression of Biaxially Stretched Daramic Membrane

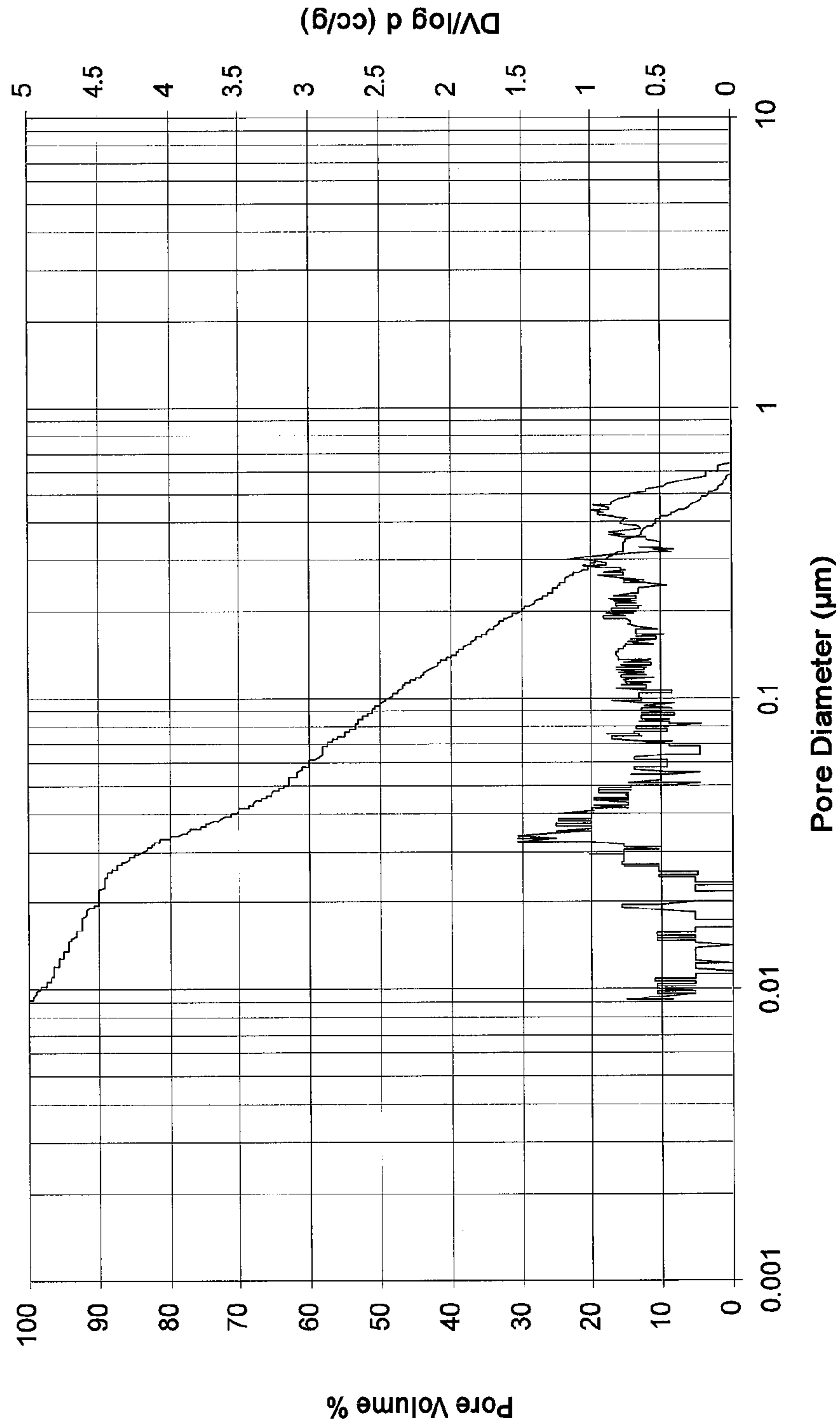


Fig. 4

Hg Porosimetry of Full Compression of Biaxially Stretched Daramic Membrane

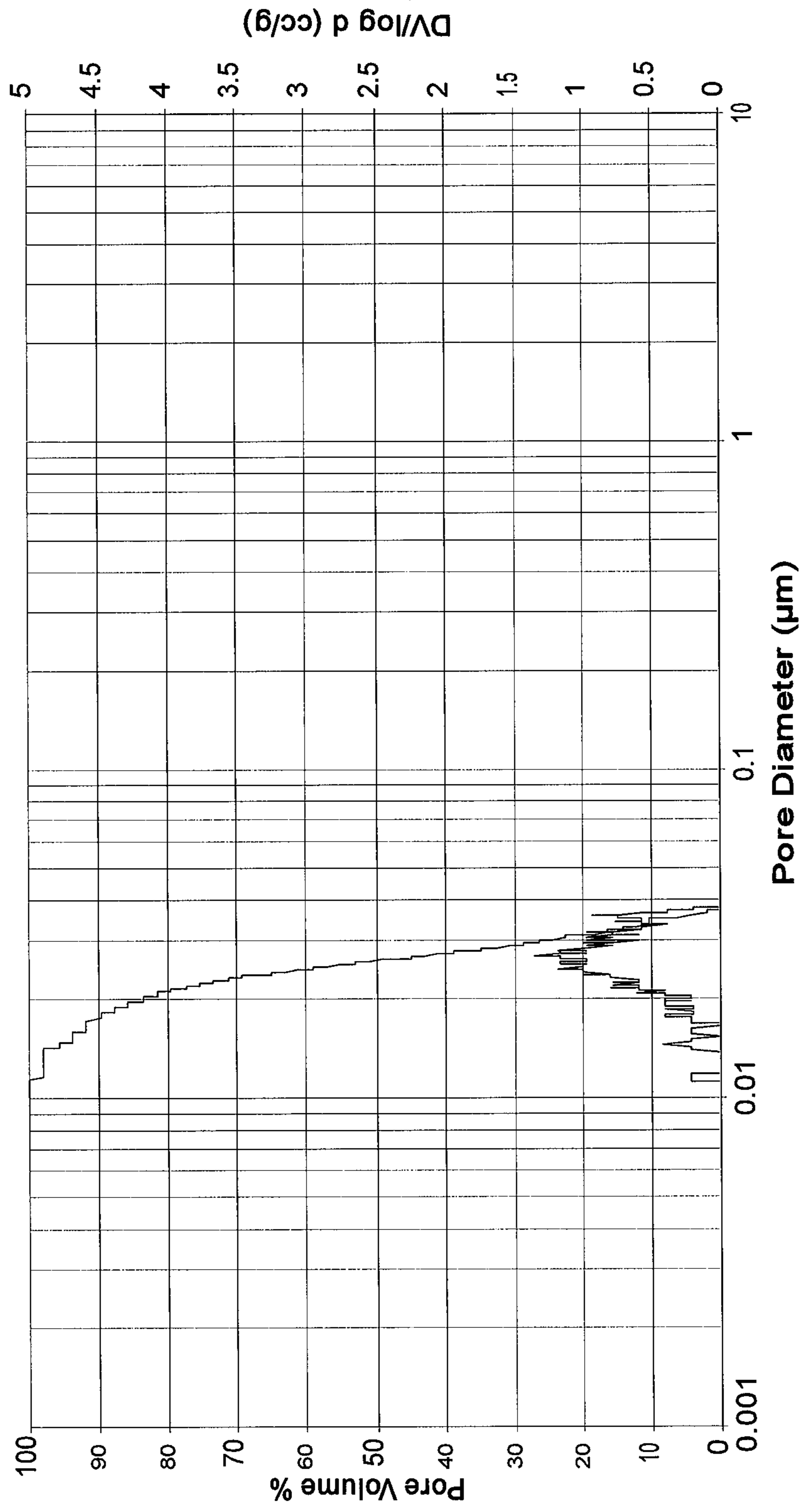


Fig. 5

## ULTRACAPACITOR AND METHOD OF MANUFACTURING THE SAME

### RELATED APPLICATION

This divisional application claims the benefit of application Ser. No. 12/021,491 filed Jan. 29, 2008 now U.S. Pat. No. 8,027,147 which, in turn, claimed the benefit of earlier-filed, co-pending U.S. Provisional application No. 60/886,981 filed Jan. 29, 2007.

### FIELD OF INVENTION

The present application discloses an ultracapacitor with a microporous ultracapacitor separator and a method for making the same.

### BACKGROUND OF THE INVENTION

In general, an ultracapacitor, also known as a supercapacitor or double layer capacitor, is two non-reactive porous plates, or collectors, suspended within an electrolyte, with a voltage potential applied across the collectors. In an individual ultracapacitor cell, the applied potential on the positive electrode attracts the negative ions in the electrolyte, while the potential on the negative electrode attracts the positive ions. A dielectric, or separator, between the two electrodes prevents the charge from moving between the two electrodes while providing minimal resistance to electrolyte ion flow. Currently, ultracapacitors are more expensive than batteries. Consequently, there is a need for separators that are cost effective in order to provide an ultracapacitor that has commercial viability.

In contrast with traditional capacitors, ultracapacitors do not have a conventional separator. They are based on a structure that contains a separator that is an electrical double layer. In an electrical double layer, the effective thickness of the separator is exceedingly thin, and that, combined with the very large surface area, is responsible for their particularly high capacitances in practical sizes. Ultracapacitor separators are typically made of highly porous materials that provide minimal resistance to electrolyte ion movement and that at the same time, provide electronic insulator properties between opposing electrodes.

Various materials have been used as separators in ultracapacitors, including (1) aquagel and resorcinol formaldehyde polymer, (2) polyolefin film, (3) nonwoven polystyrene cloth (4) acrylic resin fibers and (5) nonwoven polyester film. Other materials such as porous polyvinyl chloride, porous polycarbonate membrane and fiberglass paper are suitable as separators for ultracapacitors. Some separator materials such as polyesters, show high ionic resistance in nonaqueous electrolyte because of poor wettability by organic solvents such as propylene carbonates. On the other hand, some of the separator materials demonstrate good features as separators in nonaqueous electrolyte but are too expensive for commercialization.

One problem associated with today's ultracapacitors is they are very sensitive to the electrical resistance of the ultracapacitor cell. The internal electrical resistance of the ultracapacitor cell impacts the performance or energy output. The lower the electrical resistance of the ultracapacitor separator, the better the performance of the cell. For example, large packs (modules) of multiple ultracapacitors which are needed in Hybrid Vehicles create internal heat during operations. Location of the module near heat sources such as the engine or inside the cabin exposes the ultracapacitors to high

heats. The heat generated during operation along with the outside environmental temperature can create a high heat environment which, in turn, exposes the ultracapacitor separator to high heats. High heat increases the electrical resistance of most of the ultracapacitor separators used today. Thus, it is desired to have a robust ultracapacitor separator which can withstand these high temperatures during the life of the ultracapacitor and maintain both the physical and electrical properties of the separator material for the life of the ultracapacitor.

Another problem associated with ultracapacitor cells is moisture. Moisture inside the high surface area carbon electrodes of a ultracapacitor degrades the performance during life by increasing the internal resistance of the cell. Therefore, one must attempt to remove the moisture in order to have an effective ultracapacitor. To drive off the moisture inside the ultracapacitor cell, high temperature curing is required. This process includes heating the ultracapacitor to a high temperature so that the moisture will dry out. This curing process is a function of temperature and time where the higher the curing temperature the less time required to adequately cure the ultracapacitor. Typical ultracapacitor separators begin to increase in electrical resistance in curing temperature above 150° C. for 12 hours. Thus, an ultracapacitor separator which can withstand higher curing temperatures up to 200° C. and maintain its initial properties will allow for higher performance cells as more moisture can be removed. Therefore, in order to save money and speed up the production of an ultracapacitor, there is a need for an ultracapacitor separator material that can be heated to a higher temperature while still substantially maintaining its resistance properties.

The instant invention utilizes a microporous membrane as an ultracapacitor separator. A microporous membrane comprising a very high molecular weight polyolefin and an inert filler material was taught by Larsen, U.S. Pat. No. 3,351,495. The general principles and procedures of U.S. Pat. No. 3,351,495 are incorporated herein by reference. Kono et al., U.S. Pat. No. 4,600,633 teaches a polyethylene superthin film and a process for the production of the same. In this process an ultra high molecular weight polyethylene (herein after UHMWPE) is dissolved in a solvent then extruded to form a gel sheet. The gel sheet then undergoes a first extraction step to remove the solvent. After the first extraction, the sheet is heated and stretched. The stretched sheet then undergoes a second extraction step to remove solvent. The resulting product then undergoes a compression treatment at a temperature of 80° to 140° centigrade. This reference does not use a filler in its UHMWPE. The gel sheet is not calendered prior to solvent extraction. The resulting product is a thin film with a tensile modulus of at least 2000 kg/cm<sup>2</sup> a breaking strength of at least 500 kg/cm<sup>2</sup> and which, is substantially free from pores. In addition, U.S. patent application Ser. No. 11/006,333 to Miller et. al. discloses a microporous material similar to the material used herein, however, this material is not directed for use as an ultracapacitor separator.

The instant invention of an ultracapacitor with a microporous ultracapacitor separator and a method making the same is designed to address the aforementioned problems.

### SUMMARY OF THE INVENTION

The instant invention is directed toward a method for producing an ultracapacitor. The method comprises the steps of: providing a negative porous electrode in contact with a negative conducting plate; providing a positive porous electrode in contact with a positive conducting plate; providing an ultracapacitor separator being a microporous material that sepa-

rates the negative porous electrode from the positive porous electrode; providing an electrolytic solution; and curing the ultracapacitor at a temperature of at least 200° C. The microporous material includes: an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout the microporous material. The filler constitutes from about 5 percent to 95 percent by weight of the microporous material. The microporous material has a network of interconnecting pores communicating throughout the microporous material. The pores constitute at least 25 percent by volume of the microporous material. These pores create a pore distribution where the microporous material has no pores greater in size than 1.0 micrometers and the change in volume divided by log d for the pores of this microporous material is less than 2 cc/g for the entire pore distribution. The electrolytic solution impregnates the negative porous electrode, the positive porous electrode, and the ultracapacitor separator.

#### BRIEF DESCRIPTION OF THE DRAWINGS

For the purpose of illustrating the invention, there is shown in the drawings information about some of the embodiments of the invention; it being understood, however, that this invention is not limited to the precise information shown.

FIG. 1 is a front sectional view of one embodiment of an ultracapacitor utilizing the microporous ultracapacitor separator material of the instant invention;

FIG. 2 is a graph of data obtained using a test called compression thermomechanical analysis (compression TMA) which measures the thickness of an ultracapacitor separator according to the instant invention as a function of temperature to show the amount the material shrinks, melts, deforms when the material is heated to 500° C.;

FIG. 3 is a graph of data which shows the electrical resistance measurements as a function of temperature for both an ultracapacitor separator of the instant invention and a sample of paper which is presently used in ultracapacitor applications to show how the ultracapacitor separator has a lower resistance when heated at a constant heating rate (60° C./min);

FIG. 4 is a graph of data obtained using a mercury Porosimeter which plots pore diameter to pore volume for an ultracapacitor separator made according to the instant invention, where post stretch calendering is performed at moderate pressure;

FIG. 5 is a graph of data obtained using a mercury Porosimeter which plots pore diameter to pore volume for an ultracapacitor separator made according to the instant invention, where post stretch calendering is performed at a higher compression pressure.

#### DETAILED DESCRIPTION OF THE INVENTION

Referring to the drawings, wherein like numerals indicate like elements, there is shown in FIG. 1 one embodiment of an ultracapacitor 10 made according to the method of manufacturing an ultracapacitor according to the instant invention. Ultracapacitor 10 may be any type or size of ultracapacitor. Ultracapacitor 10 may be used alone or in series with one or more other ultracapacitors.

As shown in FIG. 1, ultracapacitor 10 may include a negative porous electrode 12 and a positive porous electrode 16. Negative porous electrode 12 may be in contact with a negative conducting plate 14. Positive porous electrode 16 may be in contact with a positive conducting plate 14. Ultracapacitor separator 20 may separate negative porous electrode 12 from positive porous electrode 16. Negative porous electrode 12,

positive porous electrode 16, and ultracapacitor separator 20 may be impregnated by an electrolytic solution 22.

A method for producing ultracapacitor 10 may comprise the following steps: providing negative porous electrode 12 in contact with negative conducting plate 14; providing positive porous electrode 16 in contact with positive conducting plate 18; providing ultracapacitor separator 20 being a microporous material separating negative porous electrode 12 from positive porous electrode 16; providing electrolytic solution 22 where electrolytic solution 22 may impregnate negative porous electrode 12, positive porous electrode 16, and ultracapacitor separator 20; and curing ultracapacitor 10 at a temperature of at least 200° C.

Ultracapacitor separator 20 may be included in ultracapacitor 10. Ultracapacitor separator 20 may be for separating negative porous electrode 12 from positive porous electrode 16. Ultracapacitor separator 20 may provide minimal resistance to electrolyte ion movement between electrolytic solution 22. Ultracapacitor separator 20 may also provide maximum electronic insulator properties between negative porous electrode 12 and positive porous electrode 16. Ultracapacitor separator 20 may have a change in thickness of less than 8% at a curing temperature of at least 200° C. (see FIG. 2). Ultracapacitor separator 20 may also have a surface resistance of less than 30 ohms/cm<sup>2</sup> at any temperature less than 200° C. (see FIG. 3).

In FIG. 2, a microporous material for ultracapacitor separator 20 was made according to the instant invention and tested using a test called compression thermomechanical analysis (compression TMA). The test involves measuring the thickness of a film sample as a function of temperature. During the experiment, the temperature is increased at a constant heating rate from room temperature until the final desired temperature is reached. In this case, the heating rate which was used was 10° C./min. As shown in FIG. 2, the microporous material shrinks a small amount, less than 8%, at a temperature of at least 200° C. Thus, the microporous material used for ultracapacitor separator 10 can be exposed to high temperatures without substantially deforming, shrinking or melting. These properties of the microporous material shown in FIG. 2 allows for ultracapacitor 10 to be exposed to the step of curing the ultracapacitor 10 at a temperature of at least 200° C., while still substantially maintaining its separator properties, i.e., resistance.

In FIG. 3, a commonly known paper ultracapacitor separator and three microporous materials for ultracapacitor separator 20 were made according to the instant invention and were tested for electrical resistance measurements as a function of temperature. The data was generated from the beginning temperature of the experiment to the final temperature using a constant heating rate. In this case, the heating rate which was used was 60 C/min. This test shows the lower resistance of these three microporous materials at temperatures from 20° C. to 200° C. compared to a commonly used paper separator. According to the results shown in FIG. 3, an ultracapacitor made according to the instant invention will have lower resistance than the prior art, which may result in better performance of ultracapacitor 10.

Ultracapacitor 20 may be made of a microporous material that comprises an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout the microporous material. The filler may constitute from about 5 percent to 95 percent by weight of the microporous material. The microporous material may have a network of interconnecting pores communicating throughout the microporous material, and the pores may constitute at least 25 percent by volume of the microporous material. These pores



may create a pore distribution where the microporous material has no pores greater in size than 1.0 micrometers and the change in volume divided by log d for the pores of this microporous material is less than 2 cc/g for the entire pore distribution.

A method of making the microporous material of ultracapacitor separator **20** may include the following steps: providing an ultrahigh molecular weight polyethylene (herein after UHMWPE); providing a particulate filler; and providing a processing plasticizer where the processing plasticizer is a liquid at room temperature. The UHMWPE, filler and plasticizer are all described in greater detail below. The UHMWPE, filler and plasticizer are mixed together to form a mixture. The mixture is extruded through a die (e.g. slot die or blown film die) to form a sheet. The sheet may be further processed, by casting onto a chilled roller, or calendered, or blown. The cast or calendered sheet is then subjected to an extraction step to partially (or fully) remove the plasticizer and forms thereby a microporous matrix. The matrix comprises UHMWPE, plasticizer if not fully extracted, and the particulate filler distributed throughout the matrix. The filler constitutes from 5 percent to 95 percent by weight of the microporous matrix. The microporous matrix has a network of interconnecting pores communicating throughout the microporous matrix. The pores constitute from 25 percent to 90 percent by volume of the microporous matrix. The microporous matrix is stretched. The stretching process is described in greater detail below. The stretched microporous matrix is not dimensionally stable at elevated temperatures. The stretched microporous matrix is subsequently calendered to produce the final microporous material that is dimensionally stable even at elevated temperatures.

Ultrahigh molecular weight polyethylene (UHMWPE) can be defined as a polyethylene having an intrinsic viscosity of least about 18 deciliters/gram. In many cases the intrinsic viscosity is at least about 19 deciliters/gram. Although there is no particular restriction on the upper limit of the intrinsic viscosity, the intrinsic viscosity is frequently in the range of from about 18 to about 39 deciliters/gram. An intrinsic viscosity in the range of from about 18 to about 32 deciliters/gram is most common.

As used herein and in the claims, intrinsic viscosity is determined by extrapolating to zero concentration the reduced viscosities or the inherent viscosities of several dilute solutions of the UHMWPE where the solvent is freshly distilled decahydronaphthalene to which 0.2 percent by weight, 3,5-di-tert-butyl-4-hydroxyhydrocinnamic acid, neopentane-tetrayl ester [CAS Registry No. 6683-19-8] has been added. The reduced viscosities or the intrinsic viscosities of the UHMWPE are ascertained from relative viscosities obtained at 135° C. using an Ubbelohde No. 1 viscometer in accordance with the general procedures of ASTM D 4020-81, except that several dilute solutions of differing concentration are employed. ASTM D 4020-81 is, in its entirety, incorporated herein by reference.

Sufficient UHMWPE should be present in the matrix to provide its properties to the microporous material for an ultracapacitor separator. Other thermoplastic organic polymers may also be present in the matrix, so long as their presence does not materially affect the properties of the microporous material for an ultracapacitor separator in an adverse manner. The amount of the other thermoplastic polymers which may be present depends upon the nature of such polymers. In general, a greater amount of other thermoplastic organic polymer may be used if the molecular structure contains little branching, few long sidechains, and few bulky side groups, than when there is a large amount of branching, many

long sidechains, or many bulky side groups. For this reason, the exemplary thermoplastic organic polymers that may be mixed with the UHMWPE are low density polyethylene, high density polyethylene, poly(tetrafluoroethylene), polypropylene, copolymers of ethylene, such as ethylene-butene or ethylene-hexene, copolymers of propylene, copolymers of ethylene and acrylic acid, and copolymers of ethylene and methacrylic acid. If desired, all or a portion of the carboxyl groups of carboxyl-containing copolymers may be neutralized with sodium, zinc or the like. Usually at least about 70 percent UHMWPE (or 70 percent UHMWPE and other thermoplastic organic polymers), based on the weight of the matrix, will provide the desired properties to the microporous material for a capacitor separator.

The particulate filler may be in the form of ultimate particles, aggregates of ultimate particles, or a combination of both. In most cases, at least about 90 percent by weight of the filler has gross particle sizes in the range of from about 5 to about 40 micrometers. If the filler used is titanium dioxide (TiO<sub>2</sub>) the gross particle size can range from 0.005 to 45 micrometers. In another embodiment using titanium dioxide (TiO<sub>2</sub>) as a filler, the gross particle size ranges from 0.1 to 5 micrometers. In another case, at least about 90 percent by weight of the filler has a gross particle size in the range of from about 10 to about 30 micrometers. It is expected that filler agglomerates will be reduced in size during processing of the ingredients. Accordingly, the distribution of gross particle sizes in the microporous material for a capacitor separator may be smaller than in the raw filler itself. Particle size is determined by use of a Model TAI Coulter counter (Coulter Electronics, Inc.) according to ASTM C 690-80, but modified by stirring the filler for 10 minutes in Isoton II electrolyte (Curtin Matheson Scientific, Inc.) using a four-blade, 4.445 centimeter diameter propeller stirrer. ASTM C 690-80 is, in its entirety, incorporated herein by reference.

The particulate filler will on average have an ultimate particle size (irrespective of whether or not the ultimate particles are agglomerated) which is less than about 30 micrometer as determined by transmission electron microscopy. Often the average ultimate particle size is less than about 0.05 micrometer. In one embodiment the average ultimate particle size of filler is approximately 20 micrometers (when a precipitated silica is used).

Use of fillers in a polymer matrix is well documented. In general examples of suitable fillers include siliceous fillers, such as: silica, mica, montmorillonite, kaolinite, asbestos, talc, diatomaceous earth, vermiculite, natural and synthetic zeolites, cement, calcium silicate, clay, aluminum silicate, sodium aluminum silicate, aluminum polysilicate, alumina silica gels, and glass particles. In addition to the siliceous fillers other particulate substantially water-insoluble fillers may also be employed. Examples of such optional fillers include carbon black, activated carbon, carbon fibers, charcoal, graphite, titanium oxide, iron oxide, copper oxide, zinc oxide, lead oxide, tungsten, antimony oxide, zirconia, magnesia, alumina, molybdenum disulfide, zinc sulfide, barium sulfate, strontium sulfate, calcium carbonate, and magnesium carbonate.

Silica and the clays are the most useful siliceous fillers. Of the silicas, precipitated silica, silica gel, or fumed silica is most often used.

The particulate filler which has been found to work well is precipitated silica. It is important to distinguish precipitated silica from silica gel, inasmuch as these different materials have different properties. Reference in this regard is made to R. K. Iler, *The Chemistry of Silica*, John Wiley & Sons, New York (1979), Library of Congress Catalog No. QD

181.S6144, the entire disclosure of which is incorporated herein by reference. Note especially pages 15-29, 172-176, 218-233, 364-365, 462-465, 554-564, and 578-579. Silica gel is usually produced commercially at low pH by acidifying an aqueous solution of a soluble metal silicate, typically sodium silicate, with acid. The acid employed is generally a strong mineral acid such as sulfuric acid or hydrochloric acid although carbon dioxide is sometimes used. Inasmuch as there is essentially no difference in density between gel phase and the surrounding liquid phase while the viscosity is low, the gel phase does not settle out, that is to say, it does not precipitate. Silica gel, then, may be described as a non-precipitated, coherent, rigid, three-dimensional network of contiguous particles of colloidal amorphous silica. The state of subdivision ranges from large, solid masses to submicroscopic particles, and the degree of hydration from almost anhydrous silica to soft gelatinous masses containing on the order of 100 parts of water per part of silica by weight, although the highly hydrated forms are only rarely used in the present invention.

Precipitated silica on the other hand, is usually produced commercially by combining an aqueous solution of a soluble metal silicate, ordinarily alkali metal silicate such as sodium silicate, and an acid so that colloidal particles will grow in weakly alkaline solution and be coagulated by the alkali metal ions of the resulting soluble alkali metal salt. Various acids may be used, including the mineral acids, but the preferred material is carbon dioxide. In the absence of a coagulant, silica is not precipitated from solution at any pH. The coagulant used to effect precipitation may be the soluble alkali metal salt produced during formation of the colloidal silica particles, it may be added electrolyte such as a soluble inorganic or organic salt, or it may be a combination of both. Precipitated silica, then, may be described as precipitated aggregates of ultimate particles of colloidal amorphous silica that have not at any point existed as macroscopic gel during the preparation. The sizes of the aggregates and the degree of hydration may vary widely.

Precipitated silica powders differ from silica gels in that they have been pulverized in ordinarily having a more open structure, that is, a higher specific pore volume. However, the specific surface area of precipitated silica as measured by the Brunauer, Emmett, Teller (BET) method using nitrogen as the adsorbate, is often lower than that of silica gel.

Many different precipitated silicas may be employed in the present invention. Precipitated silicas are those obtained by precipitation from an aqueous solution of sodium silicate using a suitable acid such as sulfuric acid or hydrochloric acid. Carbon dioxide can also be used to precipitate the silica. Such precipitated silicas are known and processes for producing them are described in detail in U.S. Pat. No. 2,940,830, the entire disclosure of which is incorporated herein by reference, including the processes for making precipitated silicas and the properties of the products.

In the proceeding process for producing a microporous matrix, extrusion and calendering are facilitated when the substantially water-insoluble filler carries much of the processing plasticizer. The capacity of the filler particles to absorb and hold the processing plasticizer is a function of the surface area of the filler. It is therefore preferred that the filler have a high surface area. High surface area fillers are materials of very small particle size, materials having a high degree of porosity or materials exhibiting both characteristics. Usually the surface area of the filler itself is in the range of from about 20 to about 400 square meters per gram as determined by the Brunauer, Emmett, Teller (BET) method according to ASTM C 819-77 using nitrogen as the adsorbate

but modified by outgassing the system and the sample for one hour at 130° C. Preferably the surface area is in the range of from about 25 to about 350 square meters per gram. ASTM C 819-77 is, in its entirety, incorporated herein by reference. Inasmuch as it is desirable to essentially retain the filler in the microporous matrix sheet, it is preferred that the substantially water-insoluble filler be substantially insoluble in the processing plasticizer and substantially insoluble in the organic extraction liquid when microporous matrix sheet is produced by the above process.

The processing plasticizer is typically a liquid at room temperature and usually it is processing oil such as paraffinic oil, naphthenic oil, or an aromatic oil. Suitable processing oils include those meeting the requirements of ASTM D 2226-82, Types 103 and 104. It has been found that oils which have a pour point of less than 22° C. according to ASTM D 97-66 (reapproved 1978) work well. Oils having a pour point of less than 10° C. also work well. Examples of suitable oils include, but are not limited to, Shellflex® 412 and Shellflex® 371 oil (Shell Oil Co.) which are solvent refined and hydrotreated oils derived from naphthenic crude. ASTM D 2226-82 and ASTM D 97-66 (reapproved 1978) are, in the entirety, incorporated herein by reference. It is expected that other materials, including the phthalate ester plasticizers such as dibutyl phthalate, bis (2-ethylhexyl)phthalate, diisodecyl phthalate, dicyclohexyl phthalate, butyl benzyl phthalate, ditridecyl phthalate and waxes, will function satisfactorily as processing plasticizers. The processing plasticizer has little solvating effect on the thermoplastic organic polymer at 60° C., only a moderate solvating effect at elevated temperatures on the order of about 100° C., and a significant solvating effect at elevated temperatures on the order of about 200° C.

Minor amounts, usually less than about 5 percent by weight, of other materials used in processing such as lubricant, organic extraction liquid, surfactant, water, and the like, may optionally also be present. Yet other materials introduced for particular purposes may optionally be present in the microporous material in small amounts, usually less than about 15 percent by weight. Examples of such materials include antioxidants, ultraviolet light absorbers, flame retardants, reinforcing fibers such as carbon fiber or chopped glass fiber strand, dyes, pigments, and the like. The balance of the microporous material, exclusive of filler and any impregnate applied for one or more special purposes, is essentially the thermoplastic organic polymer and plasticizer (if not fully extracted).

Then the filler, thermoplastic organic polymer powder, processing plasticizer and other additives are mixed until a substantially uniform mixture is obtained. This uniform mixture may also contain other additives such as minor amounts of lubricant and antioxidant. The weight ratio of filler to polymer powder employed in forming the mixture is essentially the same as that of the stretched microporous material to be produced. The ratio of filler to UHMWPE in this mixture is in the range of from about 1:9 to about 15:1 filler to UHMWPE by weight. The particulate filler constitutes from about 5 percent to about 95 percent by weight of that microporous material. Frequently, such filler constitutes from about 45 percent to about 90 percent by weight of the microporous material. From about 55 percent to about 80 percent by weight is used in one of the embodiments of the invention. The ratio of the UHMWPE to the processing plasticizer is 1:30 to 3:2 by weight. Ratio of filler to processing plasticizer is 1:15 to 3:1 by weight.

In the extrusion and calendering process, the mixture, together with additional processing plasticizer, is introduced to the heated barrel of a screw extruder. Attached to the

extruder is a sheeting die. A continuous sheet formed by the die is forwarded without drawing to a pair of heated calender rolls acting cooperatively to form continuous sheet of lesser thickness than the continuous sheet exiting from the die.

The continuous sheet is subjected to an extraction step where processing plasticizer is partially or fully removed there from. The extraction step may include one or more steps. For example, the continuous sheet from the calender then passes to a first extraction zone where the processing plasticizer is substantially removed by extraction with an organic liquid which is a good solvent for the processing plasticizer, a poor solvent for the organic polymer, and more volatile than the processing plasticizer. Usually, but not necessarily, both the processing plasticizer and the organic extraction liquid are substantially immiscible with water. There are many organic extraction liquids that can be used. Examples of suitable organic extraction liquids include but are not limited to hexane, alkanes of varying chain lengths, 1,1,2-trichloroethylene, perchloroethylene, 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2-trichloroethane, methylene chloride, chloroform, isopropyl alcohol, diethyl ether and acetone. The continuous sheet then passes to a second extraction zone where the residual organic extraction liquid is substantially removed by: heat, steam and/or water. The continuous sheet is then passed through a forced air dryer for substantial removal of residual water and remaining residual organic extraction liquid. From the dryer the continuous sheet, which is a microporous matrix, is passed to a take-up roll.

The microporous matrix comprises a filler, UHMWPE, and optional materials in essentially the same weight proportions as those discussed above in respect of the stretched microporous matrix. The matrix might also have some plasticizer if it is not fully extracted. The residual processing plasticizer content is usually less than 20 percent by weight of the microporous matrix and this may be reduced even further by additional extractions using the same or a different organic extraction liquid.

In the microporous matrix, the pores constitute from about 25 to about 90 percent by volume. In many cases, the pores constitute from about 30 to about 80 percent by volume of the microporous matrix. One of the embodiments has from 50 to 75 percent of the volume of the microporous matrix is pores. The porosity of the microporous matrix, expressed as percent by volume. Unless impregnated, the porosity of the stretched microporous matrix is greater than the porosity of the microporous matrix before stretching.

As used herein and in the claims, the porosity (also known as void volume) of the microporous material, expressed as percent by volume, is determined according to the equation:

$$\text{Porosity} = 100[1 - d_1/d_2]$$

where  $d_1$  is the density of the sample which is determined from the sample weight and the sample volume as ascertained from measurements of the sample dimensions and  $d_2$  is the density of the solid portion of the sample which is determined from the sample weight and the volume of the solid portion of the sample. The volume of the solid portion of the sample can be determined using a Quantachrome stereopycnometer (Quantachrome Corp.) in accordance with the accompanying operating manual.

The volume average diameter of the pores of the microporous sheet can be determined by mercury porosimetry using an Autoscan mercury porosimeter (Quantachrome Corp.). Mercury Intrusion/Extrusion is based on forcing mercury (a non-wetting liquid) into a porous structure under tightly controlled pressures. Since mercury does not wet most

substances and will not spontaneously penetrate pores by capillary action, it must be forced into the voids of the sample by applying external pressure. The pressure required to fill the voids is inversely proportional to the size of the pores. Only a small amount of force or pressure is required to fill large voids, whereas much greater pressure is required to fill voids of very small pores.

In operating the porosimeter, a scan is made in the high pressure range (from about 138 kilopascals absolute to about 227 megapascals absolute). If about 2 percent or less of the total intruded volume occurs at the low end (from about 138 to about 250 kilopascals absolute) of the high pressure range, the volume average pore diameter is taken as twice the volume average pore radius determined by the porosimeter. Otherwise, an additional scan is made in the low pressure range (from about 7 to about 165 kilopascals absolute) and the volume average pore diameter is calculated according to the equation:

$$d = 2 \left[ \frac{v_1 r_1}{w_1} + \frac{v_2 r_2}{w_2} \right] / \left[ \frac{v_1}{w_1} + \frac{v_2}{w_2} \right]$$

where  $d$  is the volume average pore diameter,  $v_1$  is the total volume of mercury intruded in the high pressure range,  $v_2$  is the total volume of mercury intruded in the low pressure range,  $r_1$  is the volume average pore radius determined from the high pressure scan,  $r_2$  is the volume average pore radius determined from the low pressure scan,  $w_1$  is the weight of the sample subjected to the high pressure scan, and  $w_2$  is the weight of the sample subjected to the low pressure scan.

Large pores require lower pressures for the mercury to intrude into the pore volume while smaller pores require the higher pressures for intrusion into the pore volumes. In most microporous material, approximately 20% of the pores are smaller than 0.02 micrometers.  $DV/\log d$  represents the change in pore volume with the change in log of pore diameter. Thus in most microporous materials there a large number of pores that have a diameter of approximately 0.016 micrometers, and the peak height is several magnitudes higher than any other peak. In these material, the peak areas and heights represent the relative number of pores at the corresponding log of pore diameter.

The volume average diameter of the pores of the common microporous matrix is usually a distribution from about 0.01 to about 1.0 micrometers. By stretching the precursor material one can obtain pores which are greater than 1 micrometer in size. Depending on the amount of stretch it is possible to obtain pores greater than 20 to 30 micrometers. Then through the subsequent calendering step the pore size can be selectively reduced from the enlarged pore distribution. One example at this modified distribution of the average diameter of the pores is in the range of from about 0.01 to about 0.8 micrometers for the resulting microporous material which is stretched and calendered. In another embodiment the resulting microporous material has a distribution of average diameter of the pores of from about 0.01 to about 0.6 micrometers, as seen in FIG. 4. The volume average diameter of the pores of the microporous matrix is determined by the mercury porosimetry method.

The stretched microporous matrix may be produced by stretching the microporous matrix in at least one stretching direction to a stretch ratio of at least about 1.5. In many cases, the stretch ratio is at least about 1.7. In another embodiment it is at least about 2. Frequently, the stretch ratio is in the range of from about 1.5 to about 15. Often the stretch ratio is in the

range of from about 1.7 to about 10. In another embodiment, the stretch ratio is in the range of from about 2 to about 6. As used herein and in the claims, the stretch ratio is determined by the formula:

$$S=L_2/L_1$$

where S is the stretch ratio,  $L_1$  is the distance between two reference points located on the microporous matrix and on a line parallel to the stretching direction, and  $L_2$  is the distance between the same two reference points located on the stretched microporous material. When the stretching is done in two directions, the stretching in the two directions may be performed either sequentially or simultaneously.

The temperatures at which stretching is accomplished may vary widely. Stretching may be accomplished at about ambient room temperature, but usually elevated temperatures are employed. The microporous matrix may be heated by any of a wide variety of techniques prior to, during, and/or after stretching. Examples of these techniques include radiative heating such as that provided by electrically heated or gas fired infrared heaters, convective heating such as that provided by recirculating hot air, and conductive heating such as that provided by contact with heated rolls. The temperatures which are measured for temperature control purposes may vary according to the apparatus used and personal preference. For example, temperature-measuring devices may be placed to ascertain the temperatures of the surfaces of infrared heaters, the interiors of infrared heaters, the air temperatures of points between the infrared heaters and the microporous matrix, the temperatures of circulating hot air at points within the apparatus, the temperature of hot air entering or leaving the apparatus, the temperatures of the surfaces of rolls used in the stretching process, the temperature of heat transfer fluid entering or leaving such rolls, or film surface temperatures. In general, the temperature or temperatures are controlled such that the microporous matrix is stretched about evenly so that the variations, if any, in film thickness of the stretched microporous matrix are within acceptable limits and so that the amount of stretched microporous matrix outside of those limits is acceptably low. It will be apparent that the temperatures used for control purposes may or may not be close to those of the microporous matrix itself since they depend upon the nature of the apparatus used, the locations of the temperature-measuring devices, and the identities of the substances or objects whose temperatures are being measured.

In view of the locations of the heating devices and the line speeds usually employed during stretching, gradients of varying temperatures may or may not be present through the thickness of the microporous matrix. Also because of such line speeds, it is impracticable to measure these temperature gradients. The presence of gradients of varying temperatures, when they occur, makes it unreasonable to refer to a singular film temperature. Accordingly, film surface temperatures, which can be measured, are best used for characterizing the thermal condition of the microporous matrix. These are ordinarily about the same across the width of the microporous matrix during stretching although they may be intentionally varied, as for example, to compensate for microporous matrix having a wedge-shaped cross-section across the sheet. Film surface temperatures along the length of the sheet may be about the same or they may be different during stretching.

The film surface temperature at which stretching is accomplished may vary widely, but in general they are such that the microporous matrix is stretched about evenly, as explained above. In most cases, the film surface temperatures during stretching are in the range of from about 20° C. to about 220° C. Often such temperatures are in the range of from about 50°

C. to about 200° C. From about 75° C. to about 180° C. is another range in this embodiment.

Stretching may be accomplished in a single step or a plurality of steps as desired. For example, when the microporous matrix is to be stretched in a single direction (uniaxial stretching), the stretching may be accomplished by a single stretching step or a sequence of stretching steps until the desired final stretch ratio is attained. Similarly, when the microporous matrix is to be stretched in two directions (biaxial stretching), the stretching can be conducted by a single biaxial stretching step or a sequence of biaxial stretching steps until the desired final stretch ratios are attained. Biaxial stretching may also be accomplished by a sequence of one or more uniaxial stretching steps in one direction and one or more uniaxial stretching steps in another direction. Biaxial stretching steps where the microporous matrix is stretched simultaneously in two directions and uniaxial stretching steps may be conducted in sequence in any order. Stretching in more than two directions is within contemplation. It may be seen that the various permutations of steps are quite numerous. Other steps, such as cooling, heating, sintering, annealing, reeling, unreeling, and the like, may optionally be included in the overall process as desired.

Various types of stretching apparatus are well known and may be used to accomplish stretching of the microporous matrix according to the present invention. Uniaxial stretching is usually accomplished by stretching between two rollers wherein the second or downstream roller rotates at a greater peripheral speed than the first or upstream roller. Uniaxial stretching can also be accomplished on a standard tentering machine. Biaxial stretching may be accomplished by simultaneously stretching in two different directions on a tentering machine. More commonly, however, biaxial stretching is accomplished by first uniaxially stretching between two differentially rotating rollers as described above, followed by either uniaxially stretching in a different direction using a tenter machine or by biaxially stretching using a tenter machine. The most common type of biaxial stretching is where the two stretching directions are approximately at right angles to each other. In most cases where continuous sheet is being stretched, one stretching direction is at least approximately parallel to the long axis of the sheet (machine direction) and the other stretching direction is at least approximately perpendicular to the machine direction and is in the plane of the sheet (transverse direction).

After the microporous matrix has been stretched either uniaxially or biaxially then the stretched microporous matrix is again calendered. The stretched microporous matrix is forwarded to a pair of heated calender rolls acting cooperatively to form a membrane of lesser thickness than the microporous matrix exiting from the stretching apparatus. By regulating the pressure exerted by these calender rolls along with the temperature, the pore size of the final membrane can be controlled as desired. This allows the manufacturer to adjust the average pore size with a degree of control which heretofore has not been seen. The final pore size will affect other properties such as the Gurley value of the membrane, as well as, improving the dimensional stability of the membrane at temperatures above room temperature of 20° to 25° centigrade.

FIGS. 4-5 provide plots of data collected from mercury porosimetry. FIG. 4 is a graph showing pore diameter in micrometers for a membrane biaxially stretched and subsequently calendered through a gap of 25 micrometers. FIG. 5 is a graph showing pore diameter in micrometers for a membrane biaxially stretched and subsequently calendered at a high compression pressure through a minimal gap. FIGS. 4-5

show that compression substantially changes the pore size distribution which is present in the material. Also, it is possible to adjust the pore size distribution by adjusting the compression conditions.

The final membrane is the result of stretching a precursor material and subsequently compressing it to have at least a 5% reduction in thickness of the stretched precursor material, which is defined above as the microporous matrix. This microporous material consists essentially of (or comprises): an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout the microporous material, where the filler constitutes from about 5 percent to 95 percent by weight of the microporous material. The microporous material has a network of interconnecting pores communicating throughout the microporous material, the pores constituting at least 25 percent by volume of the microporous material. The microporous material has a tensile strength in the machine direction (MD) of greater than 20 N/mm<sup>2</sup>; the microporous material also has a wet out time of less than 180 seconds when silica is used as the filler. It has been observed that this microporous material has an electrical resistance of less than 130 mohm/mm<sup>2</sup>.

An ultracapacitor separator may comprise a microporous material where the microporous material consists essentially of: (or comprises) an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout the microporous material, where the filler constitutes from about 5 percent to 95 percent by weight of the microporous material. The microporous material has a network of interconnecting pores communicating throughout the microporous material, with the pores constituting at least 25 percent by volume of the microporous material. This microporous material has no pores greater in size than 1.0 micrometers; and where change in volume divided by log d for the pores of this microporous material is less than 2 cc/g.

The resulting microporous material which has been both stretched and calendered exhibits shrink in the machine direction of less than 10% and has tensile strength of greater than 25 N/mm<sup>2</sup> in the machine direction (MD).

The microporous material described above can also include a second polymer. The UHMWPE is mixed with a high density (HD) polyethylene to produce a polyolefin mixture, where the polyolefin mixture has at least 50% UHMWPE by weight. The filler used with this polyolefin mixture is in a range of from about 1:9 to about 15:1 filler to polyolefin mixture by weight. The resulting matrix consists essentially of (or comprises) UHMWPE and HD polyethylene and the particulate filler distributed throughout the matrix. This microporous material has a machine direction (MD) tensile strength of greater than 25 N/mm<sup>2</sup>.

With higher compression after the stretch the resulting microporous material consists essentially of: (or comprises) an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout the microporous material, where the filler constitutes from about 5 percent to 95 percent by weight of the microporous material. The microporous material has a network of interconnecting pores communicating throughout the microporous material, with the pores constituting at least 25 percent by volume of the microporous material. Since the compression pressure determines the resulting pore size distribution, the pore structure is highly adjustable. For instance, this microporous material in FIG. 4 has no pores greater in size than 0.50 micrometers. The

median pore size is between or equal to 0.01 and 0.3 micrometers and the pores vary in size by plus or minus 0.2 micrometers.

The resulting microporous material which has been both stretched and calendered exhibits shrink in the machine direction of less than 10% and has tensile strength of greater than 25 N/mm<sup>2</sup> in the machine direction (MD).

The microporous material described above can also include a second polymer. The UHMWPE is mixed with a high density (HD) polyethylene to produce a polyolefin mixture, where the polyolefin mixture has at least 50% UHMWPE by weight. The filler used with this polyolefin mixture is in a range of from about 1:9 to about 15:1 filler to polyolefin mixture by weight. The resulting matrix comprises (or consists essentially of) UHMWPE and HD polyethylene and the particulate filler distributed throughout the matrix. This microporous material has a machine direction (MD) tensile strength of greater than 25 N/mm<sup>2</sup>.

A process for improving the wet out time of an uncoated microporous membrane was developed comprising the steps of: providing an ultrahigh molecular weight polyethylene (UHMWPE); providing a particulate silica filler; providing a processing plasticizer where said processing plasticizer may be a liquid at room temperature. Then mixing UHMWPE, filler and processing plasticizer together to form a mixture, having a weight ratio of filler to UHMWPE of from 1:9 to 15:1 by weight. The mixture is then extruded to form a sheet. The sheet is then processed, where processing is selected from the group consisting of: calendering, casting or blowing. The processed sheet then undergoes an extraction step where all or part of the processing plasticizer is extracted from the sheet to produce a microporous matrix sheet which comprises UHMWPE and the particulate filler. In this matrix the filler is distributed throughout the matrix. The microporous matrix sheet is then calendered to produce a microporous membrane with a reduction in thickness of at least 5%. The resulting microporous membrane typically exhibits a reduction in wet out time of 50% or more over said microporous matrix sheet without the use of any chemical surface coating treatments.

Additionally a process for improving the wet out time of an uncoated microporous membrane comprising the steps of: providing an ultrahigh molecular weight polyethylene (UHMWPE); providing a particulate silica filler; providing a processing plasticizer where said processing plasticizer may be a liquid at room temperature. Then mixing UHMWPE, filler and processing plasticizer together to form a mixture, having a weight ratio of filler to UHMWPE of from 1:9 to 15:1 by weight. The mixture is then extruded to form a sheet. The sheet is then processed, where processing is selected from the group consisting of: calendering, casting or blowing. The processed sheet then undergoes an extraction step where all or part of the processing plasticizer is extracted from the sheet to produce a microporous matrix sheet which comprises UHMWPE and the particulate filler. In this matrix the filler is distributed throughout the matrix. The microporous matrix sheet is then stretched in at least one stretching direction to a stretch ratio of at least about 1.5 to produce a stretched microporous matrix sheet. This stretched microporous matrix sheet is then calendered to produce a microporous membrane with a reduction in thickness of at least 5%. Where the resulting microporous membrane, typically exhibits a reduction in wet out time of 50% or more over the microporous matrix sheet without the use of any chemical surface coating treatments.

## Test Procedures

Thickness—The membrane thickness values are reported in units of micrometers ( $\mu\text{m}$ ) and were measured using ASTM D374.

Puncture Strength—The units of puncture strength are newtons and the test procedure was ASTM D3763.

Tensile Strength—Tensile strength was measured using ASTM D882 and the units are  $\text{N}/\text{mm}^2$ .

Electrical Resistance—The units of electrical resistance are  $\text{mohm}\cdot\text{cm}^2$ .

Shrink Testing—Both MD and TD shrink values were measured using a modified version of ASTM D4802. The samples were cut into 5 inch (12.7 cm) squares and put into an oven for 10 minutes at  $100^\circ\text{C}$ . The units are percentage of change from the original dimension.

Basis Weight—Basis weight was determined using ASTM D3776 and the units are grams per square meter.

Hg porosity—This was measured using Hg intrusion porosimetry.

Gurley—The units are  $\text{sec}/10\text{ cc}$  and were measured by TAPPI T536 method.

Wetout Time—A visual technique whereas a sample is gently placed (not immersed) on the surface of water, and the time (in seconds) it takes for the membrane to begin to darken is called the wetout time.

TABLE 1

Stretched Membrane Characteristics						
Sample #	Net Stretch %	Backweb ( $\mu\text{m}$ )	Puncture (N)	Modulus-MD (MPa)	Tensile-MD ( $\text{N}/\text{mm}^2$ )	ElongationMD %
A-10	300	173	6.7	71.2	11.9	23
A-11	300	173	8.3	69.6	14.1	27
A-12	400	147	9.9	170.8	29.9	21
A-13	400	144	7.9	96.1	18.5	22
A-14	500	124	7.4	261.1	34.3	17
A-15	500	120	7.3	146.3	24.0	19
A-16	300	159	9.9	101.8	23.3	40
A-17	400	150	11.4	149.5	31.3	28
A-18	300 $\times$ 350	80	3.3	23.5	4.6	21
A-19	200 $\times$ 350	106	5.7	27.3	11.2	54

Equipment—Calendering rolls used in these tests were stack rolls having a diameter of 8 inches or 20.3 centimeters.

As can be seen from the Examples which follow, the resulting stretched then calendered microporous material exhibits

improved dimensional stability properties over a membrane which has only been stretched.

## EXAMPLES

Example A is membrane containing the following:

Example A	Polymer UHMWPE	Filler SiO <sub>2</sub>	Plasticizer	Minors	Ratio Filler-Polymer
Extrusion	9.6%	25.0%	64.0%	1.4%	2.6
Extraction	23.5%	61.1%	12.0%	1.4%	2.6

Now taking the material from Example A additional samples were prepared using tenter frame equipment. This equipment allows for both uniaxial and biaxial stretching. The following parameters were used to produce these samples:

45

A-18 and A-19 samples were biaxially stretched and produced using a sequential stretching device. The other samples refer to stretched membranes in the MD direction (uniaxial) only.

TABLE 2

Stretched Membrane Characteristics (Continued)							
Sample #	Modulus-TD (MPa)	Tensile-TD ( $\text{N}/\text{mm}^2$ )	Elongation-TD %	Shrinkage-MD %	Shrinkage-TD %	Basis wt (gsm)	Gurley ( $\text{sec}/100\text{ cc}$ )
A-10	10.6	3.7	204	-3.9	<1	59.5	58.8
A-11	8.6	3.9	229	-3.9	<1	58.7	56.0
A-12	7.1	3.7	303	-11	<1	45.8	119.6
A-13	8.8	3.4	205	-3	<1	47.5	59.4
A-14	6.3	2.8	244	-7	<1	38.3	90.2
A-15	7.4	3.2	219	-2.3	<1	41.7	53.4
A-16	11.6	3.9	234	-10.7	-0.2	55.8	96.3
A-17	8.7	3.4	230	-12.3	-0.3	47.6	86.7
A-18	21.3	6.2	35	-32	-44	15.6	15.4
A-19	19.6	8.3	54	-37	-44	20.5	36.8

TABLE 3

Stretched/Compressed Membrane Conditions and Characteristics							
Sample #	Calender		Temp ° C.	Thickness µm	Puncture N	Tensile	Tensile
	Gap µm	Calender Pressure				MD N/mm2	TD N/mm2
A-16-F	0	Full	110	53.3	9.1	72.9	12.1
A-17-F	0	Full	110	48.3	10.4	86.0	11.5
A-16-M	25	Moderate	110	76.2	9.6	52.6	8.8
A-17-M	25	Moderate	110	71.1	10.5	77.4	10.5
A-16-S	100	Slight	110	149.9	10.1	26.9	4.3
A-17-S	100	Slight	110	142.2	10.8	31.4	3.7
A-16-F	0	Full	135	55.9	10.5	74.8	14.2
A-17-F	0	Full	135	53.3	11.1	90.1	14.2
A-16-M	25	Moderate	135	86.4	10.1	26.3	5.4
A-17-M	25	Moderate	135	78.7	10.9	39.8	5.8
A-16-S	100	Slight	135	157.5	9.6	24.7	4.2
A-17-S	100	Slight	135	149.9	10.8	28.3	4.2
A-18-F	0	Full	121	17.8	4.3	41.6	42.0
A-18-M	20	Moderate	121	22.9	3.3	28.5	28.2
A-19-F	0	Full	121	20.3	8.2	64.9	54.9
A-19-M	20	Moderate	121	30.5	7.0	47.6	34.0

TABLE 4

Stretched/Compressed Membrane Characteristics (Continued)					
Sample #	Elonga- tion - MD %	Elonga- tion - TD %	Shrink- age - MD %	Shrink- age - TD %	Wetout Time sec
A-16-F	47	195	-0.5	0.9	18.0
A-17-F	34	193	-0.5	1.0	18.0
A-16-M	52	222	-2.6	0.1	41.0
A-17-M	39	244	-1.4	0.3	42.0
A-16-S	46	208	-6.5	-0.2	115.0
A-17-S	31	242	-7.0	-0.3	160.0
A-16-F	51	188	-0.1	0.9	20.5
A-17-F	36	221	-0.4	0.8	18.5
A-16-M	46	207	-0.9	0.1	52.0
A-17-M	36	235	-1.3	-0.1	46.5
A-16-S	56	208	-6.5	-0.2	79.5
A-17-S	39	261	-7.0	-0.3	41.0
A-18-F	26	35	-0.8	0.0	4.5
A-18-M	24	50	-3.2	-4.6	9.0
A-19-F	50	47	0.2	0.1	2.5
A-19-M	52	67	-2.4	-1.6	9.0

Wetout times for uncalendered A-16, A-17, A-18 and A-19 were not obtained and found to be much greater than 10 minutes.

From the data presented in these Tables, several advantages can be seen with the present process compared to the prior art. First, the stretched and then calendered films have greatly improved dimensional stability, even at elevated temperatures. The thickness which can be achieved by the stretching process alone is limited and thinner membranes can be achieved by calendering the membrane after stretching. Physical strength is much improved after the calendering of a stretched microporous material. Finally, the calendering process reduces the pore size and various degrees of calendering can be used to adjust to the desired pore size.

The present invention may be embodied in other forms without departing from the spirit and the essential attributes thereof, and, accordingly, reference should be made to the appended claims, rather than to the foregoing specification, as indicated the scope of the invention.

What is claimed is:

1. A method for producing an ultracapacitor comprising the steps of:

providing a negative porous electrode in contact with a negative conducting plate;

providing a positive porous electrode in contact with a positive conducting plate;

providing an ultracapacitor separator separating said negative porous electrode from said positive porous electrode;

providing an electrolytic solution;

said electrolytic solution impregnating said negative porous electrode, said positive porous electrode, and said ultracapacitor separator; and

curing said ultracapacitor at a temperature of at least 200° C.

2. The method of manufacturing an ultracapacitor of claim 1 where said ultracapacitor separator having a change in thickness of less than 8% at a curing temperature of at least 200° C.

3. The method of manufacturing an ultracapacitor of claim 1 where said ultracapacitor separator having a surface resistance of less than 30 ohms/cm<sup>2</sup> at any temperature less than 200° C.

4. The method of manufacturing an ultracapacitor of claim 1 where said ultracapacitor separator including a microporous material comprising:

an ultrahigh molecular weight polyethylene (UHMWPE) and a particulate filler distributed throughout said microporous material;

where said filler constitutes from about 5 percent to 95 percent by weight of said microporous material;

where said microporous material has a network of interconnecting pores communicating throughout said microporous material, said pores constituting at least 25 percent by volume of said microporous material, these pores create a pore distribution;

where said microporous material has no pores greater in size than 1.0 micrometers; and

where change in volume divided by log d for the pores of this microporous material is less than 2 cc/g for the entire pore distribution.

5. The method of manufacturing an ultracapacitor of claim 4, where said microporous material has a machine direction (MD) tensile strength of greater than 25 N/mm<sup>2</sup>.

6. The method of manufacturing an ultracapacitor of claim 4, where said filler is selected from the group consisting essentially of: silica, precipitated silica, silica gel, fumed silica, mica, montmorillonite, kaolinite, asbestos, talc, diatomaceous earth, vermiculite, natural and synthetic zeolites,

cement, calcium silicate, clay, aluminum silicate, sodium aluminum silicate, aluminum polysilicate, alumina silica gels, glass particles, carbon black, activated carbon, carbon fibers, charcoal, graphite, titanium dioxide, lead oxide, tungsten, iron oxide, copper oxide, zinc oxide, antimony oxide, 5 zirconia, magnesia, alumina, molybdenum disulfide, zinc sulfide, barium sulfate, strontium sulfate, calcium carbonate, and magnesium carbonate.

7. The method of manufacturing an ultracapacitor of claim 4 where said UHMWPE is mixed with a high density (HD) 10 polyethylene to produce a polyolefin mixture;

where said polyolefin mixture has at least 50% UHMWPE by weight of said polyolefin mixture; and

where said filler to said polyolefin mixture is in a range of from 1:9 to 15:1 filler to polyolefin mixture by weight 15 and where said matrix comprises UHMWPE and HD polyethylene and said particulate filler distributed throughout said matrix.

8. The method of manufacturing an ultracapacitor of claim 4 where said microporous material being made from a pre- 20 cursor material where said microporous material has a reduction of thickness of 5% or more from said precursor material.

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