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(54) **APPARATUS AND METHOD FOR GAS SEPARATION**

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See application file for complete search history.

(75) Inventors: **Abbas Hassan**, Sugar Land, TX (US);  
**Rayford G. Anthony**, College Station, TX (US); **Aziz Hassan**, Sugar Land, TX (US)

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(73) Assignee: **H R D Corporation**, Houston, TX (US)

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*Primary Examiner* — Duane Smith  
*Assistant Examiner* — Sonji Turner

(74) *Attorney, Agent, or Firm* — Timothy S. Westby; Porter Hedges LLP

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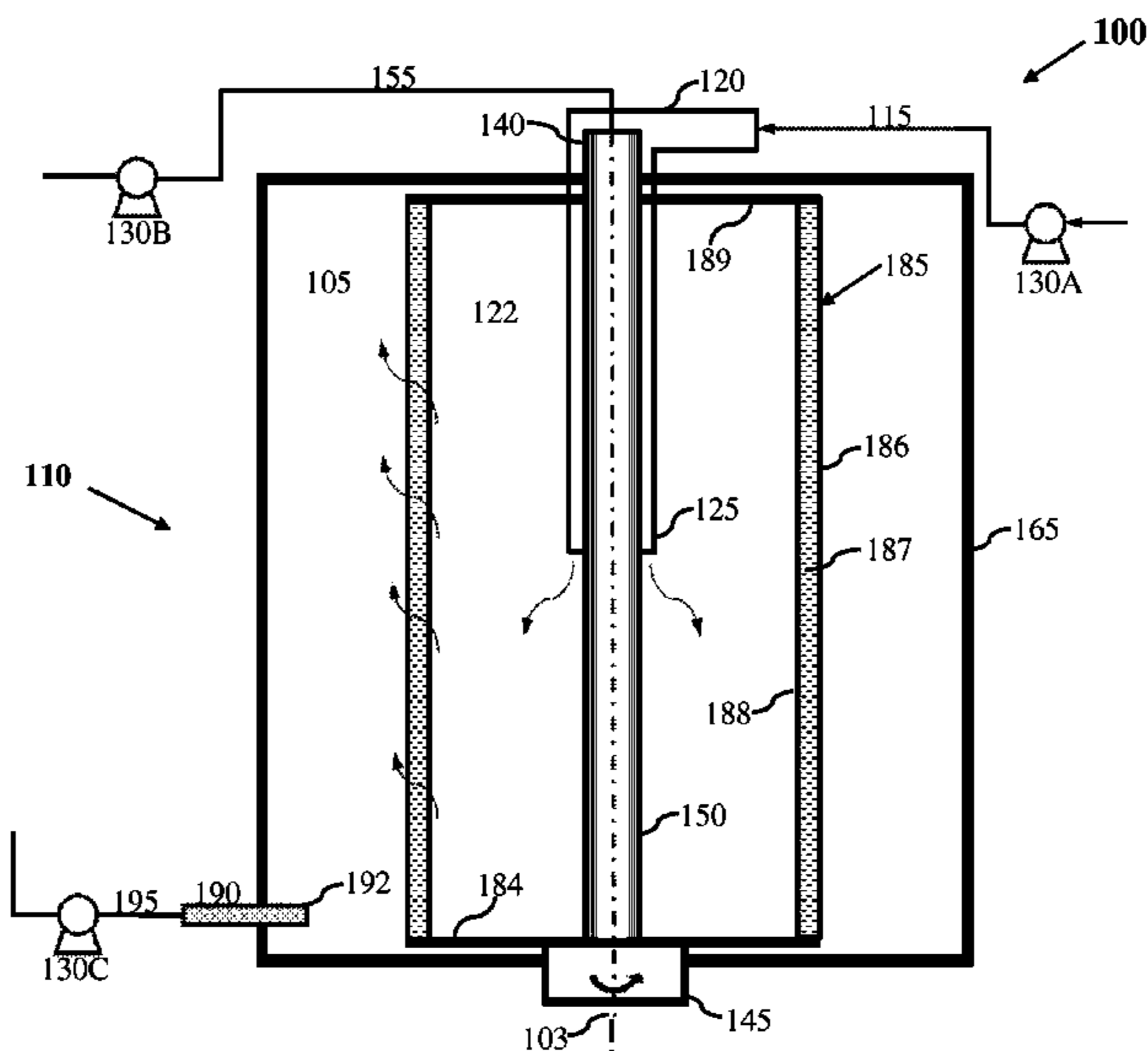
(52) **U.S. Cl.**  
USPC ..... **95/35**; 95/270; 55/400; 55/406; 55/407; 55/401

(57) **ABSTRACT**

Herein disclosed is an apparatus that includes a porous rotor positioned about an axis of rotation and surrounding an interior space wherein the porous rotor comprises sintered metal or ceramic; an outer casing, wherein the outer casing and the porous rotor are separated by an annular space; and a motor configured for rotating the porous rotor about the axis of rotation.

(58) **Field of Classification Search**  
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**18 Claims, 1 Drawing Sheet**



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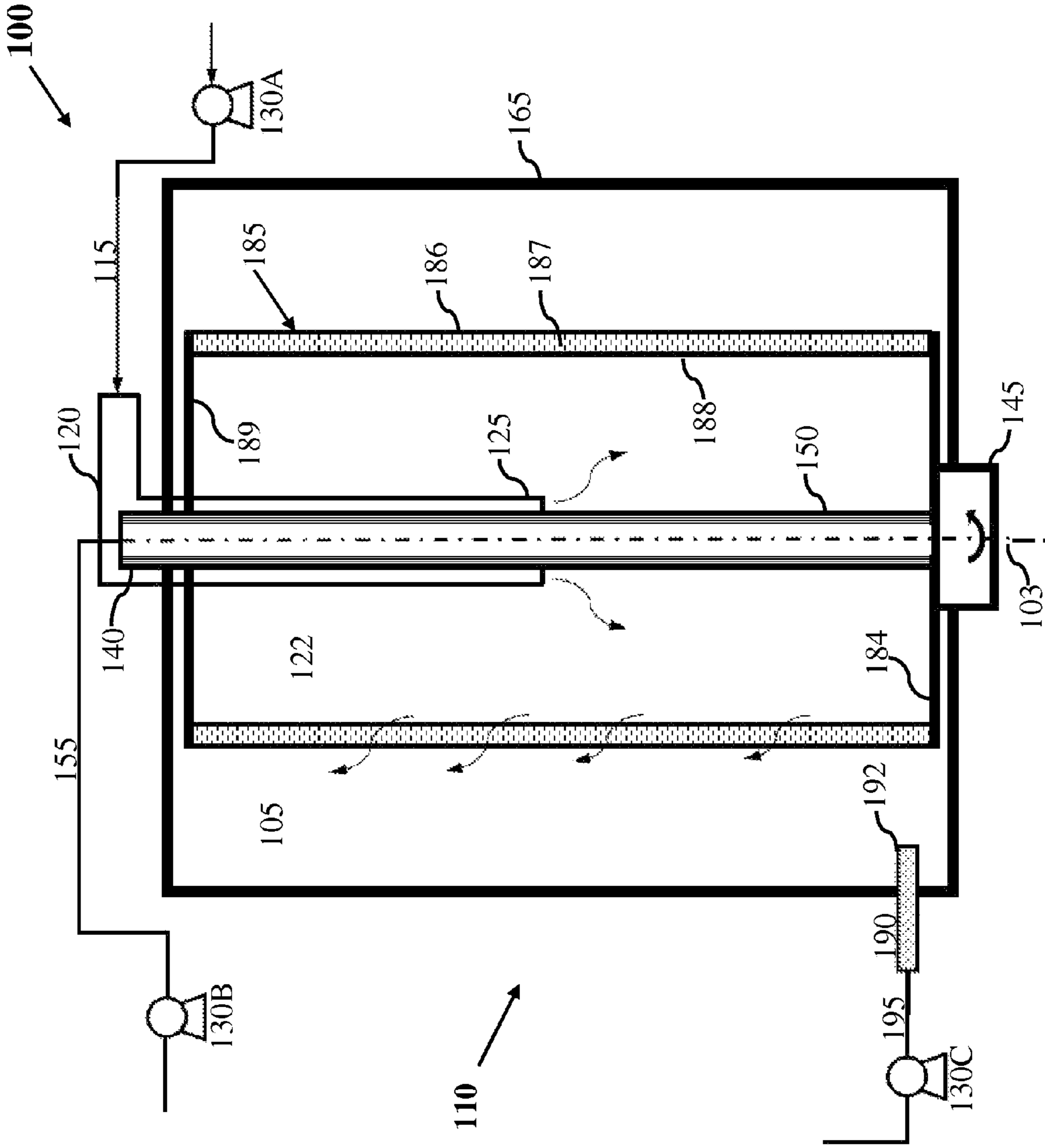
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## APPARATUS AND METHOD FOR GAS SEPARATION

### CROSS-REFERENCE TO RELATED APPLICATIONS

This application is a continuation application of U.S. patent application Ser. No. 12/708,862 (now U.S. Pat. No. 8,277,540), filed Feb. 19, 2010, which application claims the benefit under 35 U.S.C. §119(e) of U.S. Provisional Patent Application Ser. No. 61/154,189 filed Feb. 20, 2009. The disclosure of each application is hereby incorporated herein by reference in entirety for all purposes.

### STATEMENT REGARDING FEDERALLY SPONSORED RESEARCH OR DEVELOPMENT

Not Applicable.

### BACKGROUND OF THE INVENTION

#### 1. Technical Field

The present invention generally relates to the separation of gases. More specifically, the present invention relates to separation of light and heavy components of a feed gas via centrifugation. Even more specifically, in embodiments, the present invention relates to gas separation via centrifugation utilizing a porous rotor.

#### 2. Background of the Invention

Separation of gases, especially gases having similar molecular weights, is a challenging task. Isotope separation is a particularly difficult and energy intensive activity. For example, separating uranium into naturally-occurring uranium-238 from uranium-235. Around 99.284% of naturally-occurring uranium is uranium-238, while about 0.711% is uranium-235, and about 0.0058% is uranium-234. Enriching uranium is difficult because the two isotopes have very nearly identical chemical properties, and are very similar in weight: uranium-235 is only 1.26% lighter than uranium-238. Separation methods, including diffusion techniques and centrifugation, that exploit the slight differences in atomic weights of isotopes have been employed to separate isotopes of uranium and produce depleted uranium consisting mainly of the 238 isotope, and enriched uranium having a higher-than-natural quantity of the uranium-235 isotope.

Diffusion techniques are used to separate similar-molecular weight gases. Gaseous diffusion is a technology used to produce enriched uranium by forcing gaseous uranium hexafluoride through semi-permeable membranes, typically silver-zinc membranes, and separating the different isotopes by difference in diffusion rates. This produces a slight separation between the molecules containing uranium-235 and uranium-238, as uranium-238 is heavier and thus diffuses a bit more slowly than uranium-235. Thermal diffusion applies the transfer of heat across a thin liquid or gas to accomplish isotope separation. The process exploits the fact that the lighter uranium-235 gas molecules will diffuse toward a hot surface, and heavier uranium-238 gas molecules will diffuse toward a cold surface.

Centrifugation is also known for the separation of gases of similar molecular weight. A gas centrifuge is a separating machine specifically developed to separate uranium-235 from uranium-238 by applying forces to the gas mixture by placing material inside a mechanism that rotates the material at high speed. The gas centrifugation process uses a large number of rotating cylinders in series and parallel formations. The rotation of each cylinder creates a strong reactive cen-

trifugal force accelerating molecules based upon mass and causing heavier gas molecules containing uranium-238 to move toward the outside of the cylinder and the lighter gas molecules rich in uranium-235 to collect closer to the center.

Gas centrifugation requires much less energy to achieve similar separation to older gaseous diffusion processes, and thus gas centrifugation has largely replaced gaseous diffusion as an enrichment method. The Zippe centrifuge is an enhancement on the standard gas centrifuge, the primary difference being the use of heat. The bottom of the rotating cylinder is heated, producing convection currents that move the uranium-235 up the cylinder, where it can be collected.

A feature common to all large-scale enrichment schemes is that they employ a number of identical stages to produce successively higher concentrations of uranium-235. Each stage concentrates the product of the previous step further before being sent to the next stage. Similarly, the tailings from each stage are returned to the previous stage for further processing. This sequential enriching system is called a cascade. For example, gas centrifugation is performed with multiple centrifugal runs using cascades of centrifuges.

Another expensive gas separation, for example, is separation of undesired components from methane obtained down-hole. Removal of carbon dioxide and other components from the methane to provide a pipeline-grade methane generally involves the use of very low temperatures and/or amine units. Such units can be costly and their operation time-consuming.

Accordingly, in view of the art, there is a need for efficient and economical apparatus and methods of separating gases. Desirably, the separation is performed in the absence of a large cascade of separation stages and/or in the absence of cooling.

### SUMMARY

Herein disclosed is an apparatus comprising (1) a porous rotor symmetrically positioned about an axis of rotation and surrounding an interior space; (2) an outer casing, wherein the outer casing and the rotor are separated by an annular space; (3) a motor configured for rotating the rotor about the axis of rotation; (4) a feed inlet positioned along the axis of rotation and fluidly connected with the interior space; and (5) a first outlet, wherein the first outlet is fluidly connected with the interior space. In embodiments, the feed inlet of the apparatus extends into the interior space.

A method of separating a feed gas into a first fraction and a second fraction, the method including: introducing the feed gas into an interior space within a rotor of a gas centrifuge, wherein the rotor is permeable to gas and positioned about an axis of rotation; rotating the rotor about the axis of rotation, whereby the heavy molecules of the feed gas are forced toward the rotor; and extracting at least some of the first fraction from within the interior space through a sintered metal tube, and also extracting at least some of the second fraction from within the interior space, wherein the first fraction has an average molecular weight lower than the average molecular weight of the second fraction.

In embodiments, extracting the second fraction from the interior space comprises passing the second fraction through the rotor.

In embodiments, the method includes assisting extraction of the first fraction via application of vacuum.

In embodiments, rotating the rotor about the axis of rotation provides a rotational frequency of at least 7,500 RPM.

In embodiments, the sintered metal tube has an average pore size exclusive of particles above a cutpoint size.

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In embodiments, the rotor includes a porous rotor, and the porous rotor is positioned symmetrically about the axis of rotation.

In aspects, the method may include extracting at least some of the second fraction from within the interior space. In other aspects, extracting the portion of the second fraction from the interior space may include passing the portion of the second fraction through the porous rotor, and wherein extracting at least a portion of the first fraction from within the interior space extracting the portion through a sintered metal tube.

In embodiments, the rotor of the apparatus is substantially tubular. In embodiments, the porous rotor of the apparatus is made from or comprises a selectively-permeable material. In certain embodiments, selectively-permeable material comprises sintered metal or ceramic. In some embodiments, the porous rotor of the apparatus has a diameter in the range of from about 4 to about 12 inches. In some embodiments, the porous rotor of the apparatus has a length in the range of from about 8 to about 20 inches. In certain embodiments, the motor of the apparatus is capable of providing a rotational frequency of the porous rotor of up to at least about 7,500 RPM. In certain embodiments, the apparatus further comprises a second outlet, wherein the second outlet is fluidly connected with the annular space.

Another aspect of the present disclosure includes a system comprising at least one apparatus as described. In certain embodiments, the disclosed system further comprises at least one pump. In some embodiments, the system further comprises a feed inlet line in fluid communication with the feed inlet and a first outlet line fluidly connected with the first outlet, wherein the at least one pump is positioned on the feed inlet line or the first outlet line.

Herein disclosed is also a method of separating a feed gas into a first fraction and a second fraction, wherein the first fraction has an average molecular weight lower than the average molecular weight of the second fraction. The disclosed method comprises: (1) introducing the feed gas into an interior space within a rotor of a gas centrifuge, wherein the rotor is permeable to gas and symmetrically positioned about an axis of rotation; (2) rotating the rotor about the axis of rotation, whereby the heavy molecules of the feed gas are forced toward the rotor; and (3) extracting the first fraction from within the interior space proximal the axis of rotation, leaving the second fraction therein. In some embodiments, rotating the rotor about the axis of rotation provides a rotational frequency of at least 7,500 RPM.

In some embodiments, the method further comprises extracting the second fraction from the interior space. In some cases, extracting the second fraction from the interior space comprises passing the second fraction through the porous rotor and extracting the second fraction from the outside of the rotor. In certain embodiments, extracting the second fraction from the outside of the rotor further comprises assisting extraction of the first fraction via application of vacuum.

In certain embodiments, the porous rotor comprises sintered metal or ceramic. In some embodiments, extracting the first fraction from within the interior space proximal the axis of rotation comprises extracting the first fraction through a sintered metal tube. In certain embodiments, the sintered metal tube has an average pore size exclusive of particles above a cutpoint size. In certain other embodiments, extracting the first fraction through a sintered metal tube further comprises assisting extraction of the first fraction via application of vacuum to the interior space.

These and other embodiments and potential advantages will be apparent in the following detailed description and drawings.

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## BRIEF DESCRIPTION OF THE DRAWINGS

For a more detailed description of the preferred embodiment of the present invention, reference will now be made to the accompanying drawing, wherein:

FIG. 1 is a schematic of a system according to an embodiment of this disclosure.

## NOTATION AND NOMENCLATURE

As used herein, the use of the modifiers “light,” and “heavy” when referring to components or fractions of a gas stream indicate relative weights, i.e. that the “light” component or fraction has a lower molecular weight than the “heavy” component or fraction.

As used herein, the use of the modifiers “large” and “small” when referring to components or fractions of a gas stream indicate relative molecular sizes, i.e. that the “large” component or fraction has a greater molecular size than the “small” component or fraction.

## DETAILED DESCRIPTION

## I. Overview.

Herein disclosed are a system and method of separating a feed gas into a light weight fraction or component and a heavy weight fraction or component. The heavy weight fraction or component has a higher molecular weight than the light weight fraction or component.

Centrifugation relies on the effect of simulating gravity (using reactive centrifugal acceleration) to separate molecules according to their mass, and can be applied to both liquid and gaseous materials. Forces are applied by placing material inside a mechanism (i.e., a centrifuge) that rotates the material at high speed. The conventional gas centrifuge relies on the principles of reactive centrifugal force accelerating molecules based upon mass. As conventionally performed in a cascade of gas centrifuges in series and/or parallel, centrifugation yields separations of components having different molecular weights. According to this disclosure, centrifugation utilizing a sintered material (i.e., a porous rotor and/or a stationary sintered metal tube) allows effective separation by one or a few units, rather than requiring a cascade comprising a large number (up to thousands) of gas centrifuges.

The system and process are similar in theory to reverse osmosis, in which pressure is used to force a solution through a membrane, retaining the solute on one side and allowing the pure solvent to pass to the other side.

## II. System for Gas Separation.

The gas separation system of this disclosure comprises at least one gas centrifuge. The at least one gas centrifuge comprises at least one porous sintered metal rotor or tube. In embodiments, the system comprises at least one porous rotor. The system may further comprise one or more pumps. The gas separation system may further comprise one or more flow control valves. The system may be in electronic communication with a control system for monitoring and controlling flow into and out of the gas centrifuge.

A system for gas separation according to this disclosure will now be described with reference to FIG. 1. FIG. 1 is a schematic of a gas separation system 100 according to an embodiment of this disclosure. Gas separation system 100 comprises gas centrifuge 110, feed pump 130A, first outlet pump 130B, and second outlet pump 130C.

A system of this disclosure comprises at least one gas centrifuge 110. Each of the one or more gas centrifuges of the

disclosed system comprises an outer casing, at least one porous component selected from a porous rotor or a porous outlet tube, at least one feed inlet, and at least two product outlets. In the embodiment of FIG. 1, gas centrifuge **110** comprises outer casing **165**, porous rotor **185**, feed inlet **120**, first fraction outlet **140**, and second product outlet **190**.

Gas centrifuge **110** comprises outer casing **165**. As indicated in FIG. 1, outer casing **165** surrounds rotor **185**. Outer casing **165** may be cylindrical on its outer and/or inner surfaces. Outer casing **165** can be made out of specific materials to prevent harmful materials from hurting users of gas centrifuge **110**. In applications, components of gas centrifuge **110**, such as casing **165**, are made of stainless steel.

Porous Rotor or Stationary Porous Tube.

Each of the one or more gas centrifuges comprises at least one porous component. The porous component may be a porous rotor or a stationary porous tube. In embodiments, the gas separation system comprises a porous rotor. As indicated in the embodiment of FIG. 1, porous rotor **185** is symmetrically positioned within casing **165** about an axis of rotation **103**. Porous rotor **185** is positioned within outer casing **165** such that a clearance or annular space **105** is created between outer wall **186** of porous rotor **185** and the inner surface of outer casing **165**. Rotor **185** surrounds an interior space **122** configured such that the interior space **122** may be evacuated of air prior to use to provide near frictionless rotation when operating. Porous rotor **185** may comprise a selectively permeable or size-exclusion rotor. The rotor may be tubular in shape, e.g. a sintered metal tube. Porous rotor **185** is designed such that it is permeable to gaseous components of a desired size.

In applications, the system comprises a porous tube. For example, in embodiments, first outlet **140** is one end of a stationary porous tube **150**. The walls of stationary porous tube **150** may comprise or contain therein size-exclusion or selectively-permeable material.

The porous component may comprise or contain sintered metal. In embodiments, a porous rotor is made of or contains a selectively permeable cylinder made of any material which can be tailored for the desired pore size and porosity and have the integral strength to withstand the rotation. Suitable porous material may be, for example, ceramic or stainless steel. In embodiments, the porous material comprises 316 stainless steel. In applications, the porosity (density) and average pore size of the porous material is tailored to allow passage of components less than a desired cutpoint size while excluding passage of components having a size greater than the cutpoint size.

The porous material may be sintered metal. In embodiments, the density of the sintered metal is in the range of from about 3 g/cm<sup>3</sup> to about 6 g/cm<sup>3</sup>. In applications, the density of the sintered metal is greater than about 3 g/cm<sup>3</sup>, 3.5 g/cm<sup>3</sup>, 4 g/cm<sup>3</sup>, 4.5 g/cm<sup>3</sup>, 5 g/cm<sup>3</sup>, or 6 g/cm<sup>3</sup>. In applications, the density of the porous material is about 3.5 g/cm<sup>3</sup>, 4 g/cm<sup>3</sup>, 4.5 g/cm<sup>3</sup>, 5 g/cm<sup>3</sup>, or 5.5 g/cm<sup>3</sup>. In embodiments, the average pore size of a selectively permeable porous material is less than about 200 μm, less than about 50 μm, less than about 20 μm, less than about 10 μm, less than about 5 μm, less than about 3 μm, less than about 1 μm, or less than about 0.5 μm. In embodiments, the average pore size is in the range of Angstroms.

In embodiments, the porous material is formed by placing metal powder, e.g. stainless steel powder, in a mold and pressing it under high pressure. In embodiments, pressures of greater than 20,000 psig are utilized to compress the powder and form the porous material. In embodiments, pressures of greater than 50,000 psig are utilized to compress the powder

and form the porous material. In embodiments, pressures of up to 150,000 psig are utilized to compress the powder and form the porous material. Pressing may reduce the thickness of a starting powder by at least 60%. The pressed material may then be calcined in an oven. To avoid shrinkage during formation, the material may be brought to a temperature approaching, but less than, the melt temperature, and cool down may be controlled over a sufficient duration to avoid/minimize shrinkage. Control of temperature during formation of the porous material of the rotor may also hinder the formation of oxides.

The porous material of the rotor may be custom-tailored to provide gas flow paths of a desired tortuosity, porosity (density) and average pore size of the material. For example, a powder may be pressed into a honeycomb structure or wax added and subsequently calcined to remove the honeycomb or wax structure and leave honeycomb- or other patterned tailored paths or voids within the porous material of the rotor. In this manner, the porous rotor may be designed with a desired average pore size and/or flow path.

The porous rotor may have a diameter and length determined to be suitable for a certain application, and the gas centrifuge may have any desired nominal size. As such, the dimensions provided are not meant to be limiting. In applications, porous rotor **185** has a diameter in the range of from about 2 inches to about 12 inches, from about 4 inches to about 10 inches, from about 4 inches to about 8 inches, or from about 4 inches to about 6 inches. Porous rotor **185** may have a vertical length in the range of from about 8 inches to about 20 inches, from about 10 inches to about 17 inches, or from about 12 inches to about 15 inches. The nominal capacity of gas centrifuge **110** may be about 10 gallons, about 5 gallons, or about 1 gallon. The thickness of the sintered material of the rotor may be tailored to provide a desired surface area. In embodiments, rotor **185** comprises sintered material having a thickness of about 1/4-inch, about 1/2-inch, about 3/4-inch, or about 1-inch.

A desired permeability or average pore size of the porous component (e.g., a stationary metal outlet tube **150**) may be obtained by providing a sintered material of a certain pore size (e.g., 30 to 100 μm) and subsequently treating the sintered material with molecular sieve or membrane. The external surfaces of the sintered metal material may be covered with one or more layers of molecular sieve. Suitable molecular sieves include, without limitation, carbon sieves, ALPOS, SAPOS, silicas, titanium silicates, and zeolites. In embodiments, the molecular sieve has a pore size in the range of from 3 angstrom (Å) to about 20 Å (about 0.3 nm to about 2 nm). The coating may be applied via methods similar to methods utilized to prepare catalyst surfaces on monolith and/or honeycomb catalytic converters that are used on automobile mufflers.

Porous rotor **185** may comprise or contain sintered metal. The rotor may be made of or may contain a permeable material. The permeable material may be tailored for a desired pore size and porosity having integral strength to withstand a desired operational rotation. In applications, the rotor comprises carbon fiber.

As mentioned hereinabove, rotor **185** may be porous and may comprise or contain sintered metal. The rotor may be made of or may contain a permeable material. The permeable material may be tailored for a desired pore size and porosity having integral strength to withstand a desired operational rotation. In embodiments, a porous rotor **185** comprises a permeable material **187** is sandwiched between an outer support **186** and an inner support **188**. For example outer wall **186** and inner wall **188** of porous rotor **185** may be a support

material. By positioning the porous material of rotor **185** between supports, increased strength may be provided thereto. Inner and outer supports **186** and **188** may resemble a basket of support material in which the porous material is sandwiched. The inner and outer supports may be configured as a mesh basket (e.g., a stainless steel mesh basket) in which the porous material is sandwiched. The inner and outer supports may be any material known to provide support and through which gas may readily pass. Top **189** and bottom **184** of rotor **185** may be impermeable to gas, or may comprise porous material.

The at least one gas centrifuge of the disclosed system further comprises at least one feed inlet. System **100** of the embodiment of FIG. **1** comprises feed inlet **120**. Feed inlet **120** is configured to introduce feed gas into the interior space **122** defined by porous rotor **185**. One end **125** of feed inlet **120** is in fluid communication with interior space **122** of gas centrifuge **110**. Outlet end **125** of feed inlet **120** is positioned proximal to axis of rotation **103**. Outlet end **125** of feed inlet **120** is positioned between top **189** and bottom **184** of interior space **122**. In embodiments, outlet end **125** of feed inlet **120** is positioned within a lower portion of interior space **122**. In embodiments, outlet end **125** of feed inlet **120** is positioned at or near bottom **184** of interior space **122**. In applications, outlet end **125** of feed inlet **120** is positioned within the upper portion of interior space **122**. In embodiments, outlet end **125** of feed inlet **120** is positioned at or near top **189** of interior space **122**. The other end of feed inlet **120** is configured for introduction of reactant feed gas therein. Feed gas line **115** is fluidly connected with the end of feed inlet **120** outside of interior space **122**.

Each of the one or more gas centrifuges of the disclosed system further comprises at least two outlets configured for removing a light fraction and a heavy fraction respectively from the gas centrifuge. In the embodiment of FIG. **1**, system **100** comprises light fraction or first outlet **140** and heavy fraction or second outlet **190**.

Light fraction outlet **140** is in fluid communication with interior space **122**. In embodiments, light fraction outlet **140** is one end of a porous tube **150**. The porous tube may be stationary or rotating during operation of system **100**. The walls of porous tube **150** extend the entire length of interior space **122**. In applications, the walls of porous tube **150** comprise size-exclusion material as described hereinabove with respect to the porous component. In this manner, for example, the walls of porous tube **150** may be selectively-permeable to gas of a desired size. In embodiments, therefore, first outlet **140** comprises one end of a stationary sintered metal tube extending the entire length of porous rotor **185** along axis **103**. The stationary sintered metal tube may be selectively-permeable to gas molecules having a size below a cutpoint size. For example, the walls of porous tube **150** may be permeable to methane gas and impermeable to carbon dioxide. First or light fraction outlet **140** is in fluid communication with light gas outlet line **155**.

The inner surface of casing **165** and the outer surface **186** of porous rotor **185** create an annular region **105** therebetween. One end **192** of heavy fraction outlet **190** is in fluid communication with annular region **105**. End **192** of product outlet **190** may be vertically positioned anywhere within annular region **105**, for example, towards the top, bottom, or center of annular region **105**. In embodiments, end **192** of second outlet **190** is positioned towards the bottom of annular region **105**. In embodiments, end **192** of product outlet **190** is positioned proximal the inner surface of casing **165**. Alternatively, end **192** of product outlet **190** is positioned distal the inner surface of casing **165**. Alternatively, end **192** of product outlet **190** is

horizontally positioned substantially halfway between the inner surface of casing **165** and outer surface **186** of rotor **185**. Heavy fraction outlet **190** is in fluid communication with heavy fraction outlet line **195**.

In embodiments, inlet and/or outlet ends of feed inlet **120**, first fraction outlet **140**, and/or heavy fraction outlet **190** have a diameter of  $\frac{1}{2}$  inch,  $\frac{3}{4}$  inch, or 1-inch.

The gas centrifuge further comprises a motor coupled to the porous rotor. The motor is capable of providing rotation of the porous rotor about an axis of rotation. Rotation of the rotor applies reactive centrifugal force to the feed gas within the rotor. In the embodiment of FIG. **1**, for example, motor **145** is coupled to porous rotor **185** and is capable of rotating porous rotor **185** about axis of rotation **103**. Motor **145** may be coupled to porous rotor **185** such that porous rotor **185** is rotatable in a clockwise direction or in a counter-clockwise direction. The high speed motor may be capable of rotational frequencies of up to 90,000 RPM. Alternatively, some other means may provide the high rotational frequency. In embodiments, the high speed motor is capable of producing rotational frequencies of at least 5-, 7-, 7.5-, 10-, 15-, 20-, 25-, 30-, 40-, 50-, 60-, 70-, 80-, or 90-thousand revolutions per minute (RPM).

The gas separation system may further comprise one or more flow control valves and/or pumps to control flow thereto and therefrom. One or more pumps may be operable to provide vacuum and/or pressure assist to enhance flow through gas centrifuge **110**. For example, in the embodiment of FIG. **1** gas separation system **100** comprises three pumps, **130A**, **130B**, and **130C**. Feed pump **130A** is positioned on feed inlet line **115** and may serve to force feed gas into gas centrifuge **110** under pressure. First outlet pump **130B** is positioned on product outlet line **155** and is operable to control (assist or minimize) flow of gas via first outlet **140**. For example, first outlet pump **130B** may serve to provide vacuum removal of a light gas fraction from interior space **122**. Second outlet pump **130C** is positioned on second outlet line **195** and is operable to control (assist or minimize) flow of gas via second outlet **190**. Alternatively or additionally, one or more flow control valves may be positioned on feed line **115**, first outlet line **155**, and second outlet line **195** respectively, and may be used to control flow therethrough.

System **100** may be in electronic communication with a control system, including a computer and sensors whereby flow of gas into and out of feed inlet **120**, first outlet **140**, and/or second outlet **190** and/or composition of gas within interior space **122** may be monitored and/or controlled.

Heaters.

It is envisaged that, for certain applications, all or portions of gas centrifuge **110** may be heated to enhance separation of gaseous components. For example, all or portions of outer casing **165** may be heated using apparatus and methods as known in the art. In such applications, second outlet **190** may be desirably positioned within a lower portion of annular space **105** and outlet end **125** of feed inlet **120** may be positioned at or near bottom **184** of interior space **122**, and/or an outlet end of first outlet **140** may be positioned at or near top **189** of interior space **122**.

Two or more gas centrifuges may be configured in series and/or parallel. In embodiments, a first outlet line **155** of a first gas centrifuge is fluidly connected with a feed gas line **115** of a second gas centrifuge. The first gas centrifuge is operable to produce a light gas fraction comprising gas molecules below a first cutpoint size and a second gas centrifuge is operable to produce a second light gas fraction comprising gas components below a second cutpoint size which is less than the first cutpoint size. In embodiments, a second outlet

line 195 of a first gas centrifuge is fluidly connected with a feed inlet line 115 of a second gas centrifuge. In this embodiment, the first gas centrifuge is operable to produce a heavy gas fraction comprising gas molecules above a first cutpoint size and a second gas centrifuge is operable to produce a second heavy gas fraction comprising gas components above a second cutpoint size which is less than the first cutpoint size. In this manner, a feed gas may be fractionated into three or more gas fractions having different average molecular weights.

Outer casing 165 provides an enclosed vessel. Thus, the temperature and pressure within gas centrifuge 110 is adjustable as desired within design limitations. Without limitation, gas centrifuge 110 may be operable at pressures up to at least 15 psig, 500 psig, 1000 psig, or 1455 psig. Gas centrifuge 110 may be operable, without limitation, to temperatures up to 150° C., 200° C., 250° C., 300° C., 400° C., 450° C., 500° C., 550° C., or up to about 600° C.

### III. Method of Gas Separation.

A method of separating light and heavy fractions of a gas according to this disclosure will now be made with reference to FIG. 1. A gaseous feed is introduced via feed line 115 and feed inlet 120 into gas centrifuge 110. The feed gas is introduced via inlet 120 into interior space 122 contained within the walls of rotor 185. In embodiments, the feed gas is introduced at or near the top of interior space 122. In embodiments, the feed gas is introduced at or near the bottom of interior space 122. The feed gas is introduced into interior region 122 proximal axis of rotation 103.

The feed gas is subjected to reactive centrifugal force by motor 145, which causes rotation of rotor 185 about axis of rotation 103. The rotor may be rotated at a rotational frequency of up to 5-, 7-, 7.5-, 10-, 15-, 20-, 25-, 30-, 40-, 50-, 60-, 70-, 80-, or 90-thousand RPM. Reactive centrifugal force pushes heavy molecular weight components of the gas feed toward inner walls 188 of rotor 185, while lower molecular weight components of the feed gas tend toward the center of interior space 122, toward axis of rotation 103. Low molecular weight gas is extracted via first outlet 140 and first outlet line 155. High molecular weight gas is extracted via second outlet 190 and second outlet line 195. Vacuum and/or pressure assist may be provided by first pump 130B and/or second pump 130C to enhance extraction of light gas fraction via first outlet 140 and first outlet line 155 and/or heavy gas fraction via second outlet 190 and second gas outlet line 195. In applications, feed gas is introduced and light gas extracted while the composition of gas within interior space 122 is monitored or calculated based upon the composition of light gas extracted. Once the composition with interior space 122 reaches a desired concentration of heavy gas fraction, heavy gas may be extracted via second outlet 190 and second gas outlet line 195.

As discussed hereinabove, in applications, first outlet 140 is one end of or is in fluid communication with a porous sintered metal tube 150. Porous tube 150 may be made from a selectively-permeable through which only molecules below a desired cutpoint size may pass. In embodiments, feed gas is introduced into interior space 122 and vacuum is provided by first outlet pump 130B to assist in extraction of lower molecular weight gas components via outlet tube 140. Pressure may be applied to annular region 105 via second outlet pump 130C or a suitable valve closed to prevent removal of gas through annular region 105. Light gas is withdrawn from first outlet 140. When the concentration of heavy gas components in interior space 122 exceeds a desired value, introduction of feed is discontinued, extraction of low molecular weight gas completed, and pump 130C operated and/or a suitable valve

opened to provide extraction of heavy gas components through porous rotor 185 and out via annular region 105.

Thus, vacuum and/or pressure assist may be used according to the disclosed method, to extract desired components from gas centrifuge 110.

As gas centrifuge 110 is a closed vessel, surrounded by outer casing 165, the operating temperature and pressure may be selected based on desired performance. In applications, the operating temperature may be in the range of from about 25° C. to about 600° C. In applications, the operating temperature is in the range of from about 100° C. or 150° C. to about 300° C., 400° C., or 500° C. In embodiments, gas separation/fractionation is performed at room temperature. In embodiments, gas separation/fractionation is performed at a temperature within the range of 5° C. to 45° C. In embodiments, gas separation/fractionation is performed at a temperature within the range of 20° C. to 40° C. In embodiments, gas separation/fractionation is performed at a temperature within the range of 25° C. to 35° C. The operational pressure may be a desired pressure within the limits of the design materials. Utilization of high temperatures may allow gas phase separation of feeds which are not gaseous at room temperature.

The gas centrifugation process utilizes a design that provides for gas to constantly flow in and out of the gas centrifuge in certain applications. Unlike most centrifuges which rely on batch processing, the disclosed gas centrifuge permits continuous or semi-continuous processing. In such applications, gas may be continuously or semi-continuously extracted from interior space 122 and/or annular region 105 via first outlet line 155 and second outlet line 195 respectively.

### Serial Operation.

In embodiments of the gas separation method, product gas from a first gas centrifuge is introduced directly into a second gas centrifuge as feed gas thereto. A first gas centrifuge may be operated to remove a first heavy component from a feed gas, a second gas centrifuge operated to remove a second heavy component from the feed gas, etc. In this manner, a feed gas may be fractionated into three or more components or fractions.

### Alternate Design:

In an embodiment, a non-porous rotor is combined with a porous size-exclusion tube 150. Centrifugation will cause high molecular weight molecules to tend toward the inner walls 188 of the non-porous rotor 185, and low molecular weight gas molecules to tend toward the center of interior space 122 coincident axis of rotation 103. Once a concentration of heavy molecular weight gas within interior space 122 exceeds a desired level, introduction of feed may be discontinued and heavy gas may be removed from interior space 122. The concentration of heavy gas in interior space 122 may be determined directly or by calculation of the difference between the inlet gas fed and the light gas removed via first outlet 140 and first gas outlet line 155. A second outlet may be provided to extract heavy gas from within interior space 122. Such a second outlet may extend into interior space 122 symmetrically about axis of rotation 103 and, once within interior space 122, may extend to a position proximal inner wall 188 of rotor 185.

## EXAMPLES

### Example 1

In a specific embodiment, the feed gas continuously introduced into the gas centrifuge comprises dirty methane gas containing carbon dioxide and other gaseous impurities having a molecular weight greater than that of methane. In such



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instances, methane may be removed from interior space **122** via first outlet **140**, while a heavy fraction comprising carbon dioxide and other heavy components is removed from annular region **105**. A size-exclusion outlet tube **150** having walls having a pore size inclusive of methane and exclusive of carbon dioxide and other large molecules may be used to enhance the separation. Vacuum **130B** may be used to assist in withdrawal of methane from the center of interior space **122**. Pressure may be applied to annular space **105** to prevent removal of gas through rotor **185** and annular region **105** until a desired concentration of large molecular weight components, including carbon dioxide, remains within interior space **122**. At this time, introduction of feed gas may be discontinued. Vacuum **130B** may be continued for a time to remove final amounts of low molecular components from interior space **122**. Then, vacuum **130B** may be discontinued, and pump **130C** utilized to extract high molecular weight material through porous rotor **185** and annular region **105**. The light weight fraction may be introduced into a subsequent gas centrifuge and a light component or fraction comprising methane may be separated from a second heavy fraction comprising, for example, nitrogen.

In embodiments, this separation of carbon dioxide from methane gas is performed at ambient temperature. In embodiments, this separation of carbon dioxide from methane gas is performed at a temperature within the range of 5° C. to 45° C. In embodiments, the separation of carbon dioxide from methane gas is performed at a temperature within the range of 20° C. to 40° C. In embodiments, the separation of carbon dioxide from methane gas is performed at a temperature within the range of 25° C. to 35° C. In this manner, pipeline-grade methane may be produced in the absence of cooling and/or in the absence of amine systems.

## Example 2

In an application, first outlet **140** is one end of or is fluidly connected with a porous tube **150** designed with a first cutpoint size. Gas component **1** has a molecular weight below the cutpoint size, while gas components **2** and **3** have sizes above the cutpoint size. In this embodiment, light gas fraction comprising gas component **1** may be removed from interior space **122** via first gas outlet **140**. Heavy gas comprising excluded components **2** and **3** may be extracted from the gas centrifuge via second gas outlet **190**. Heavy gas comprising excluded components **2** and **3** may be subsequently introduced as feed gas into a second gas centrifuge comprising a first outlet **140** comprising a sintered metal tube designed with a second cutpoint size greater than the first cutpoint size. In this manner, gas component **2** may be removed via first outlet **140** and thusly separated from gas component **3**, which may be extracted through porous rotor **185** and annular region **105**. Vacuum and/or pressure assist may be utilized to enhance separation.

## Example 3

In a specific embodiment, the disclosed system and method are utilized to enrich uranium. In such applications, the feed gas continuously introduced into the size-exclusion gas centrifuge comprises gaseous uranium hexafluoride containing uranium-235 and uranium-238. In such instances, light gas component uranium-235 is removed via first outlet **140** and heavy component uranium-238 is extracted via second outlet **190**.

While preferred embodiments of the invention have been shown and described, modifications thereof can be made by

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one skilled in the art without departing from the spirit and teachings of the invention. The embodiments described herein are exemplary only, and are not intended to be limiting. Many variations and modifications of the invention disclosed herein are possible and are within the scope of the invention. Where numerical ranges or limitations are expressly stated, such express ranges or limitations should be understood to include iterative ranges or limitations of like magnitude falling within the expressly stated ranges or limitations (e.g., from about 1 to about 10 includes, 2, 3, 4, etc.; greater than 0.10 includes 0.11, 0.12, 0.13, and so forth). Use of the term “optionally” with respect to any element of a claim is intended to mean that the subject element is required, or alternatively, is not required. Both alternatives are intended to be within the scope of the claim. Use of broader terms such as comprises, includes, having, etc. should be understood to provide support for narrower terms such as consisting of, consisting essentially of, comprised substantially of, and the like.

Accordingly, the scope of protection is not limited by the description set out above but is only limited by the claims which follow, that scope including all equivalents of the subject matter of the claims. Each and every claim is incorporated into the specification as an embodiment of the present invention. Thus, the claims are a further description and are an addition to the preferred embodiments of the present invention. The disclosures of all patents, patent applications, and publications cited herein are hereby incorporated by reference, to the extent they provide exemplary, procedural or other details supplementary to those set forth herein.

What is claimed is:

**1.** A method of separating a feed gas into a first fraction and a second fraction, the method comprising:

introducing the feed gas into a gas centrifuge, wherein the gas centrifuge comprises:

a rotor symmetrically positioned about an axis of rotation, wherein an inner wall of the rotor surrounds an interior space,

a stationary outer casing enclosing the rotor, whereby an annular space is provided between an outer wall of the rotor and the stationary outer casing;

a stationary porous tube centered on the axis of rotation and extending the entire length of the interior space,

wherein the stationary porous tube is fluidly connected with a light gas outlet line at a top thereof; and

a feed gas inlet cylinder extending through a top of and a distance into the rotor, and surrounding a length of the stationary porous tube.

rotating the rotor about the axis of rotation, whereby heavy molecules of the feed gas are forced toward the inner wall of the rotor; and

extracting at least a portion of the first fraction from the interior space through the stationary porous tube, and extracting at least a portion of the second fraction from the interior space,

wherein the first fraction comprises one or more components of the feed gas having a molecular weight below a cutpoint size, and wherein the second fraction comprises one or more components of the feed gas having a molecular weight above the cutpoint size.

**2.** The method of claim **1**, wherein the rotor is permeable to gas, and wherein extracting the second fraction from the interior space further comprises passing the second fraction through the permeable rotor and thus into the annular space.

**3.** The method of claim **1** further comprising assisting extraction of the first fraction via application of vacuum via a pump positioned in the light gas outlet line.

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4. The method of claim 3, wherein rotating the rotor about the axis of rotation provides a rotational frequency of at least 7,500 RPM.

5. The method of claim 1, wherein the stationary porous tube has an average pore size exclusive of particles above the cutpoint size, such that the first fraction can pass there-through, while the second fraction cannot.

6. The method of claim 2, wherein the permeable rotor comprises sintered metal.

7. A method of separating a feed gas into a first fraction and a second fraction, the method comprising:

introducing the feed gas into a gas centrifuge, wherein the gas centrifuge comprises:

a rotor symmetrically positioned about an axis of rotation, wherein an inner wall of the rotor surrounds an interior space,

a stationary outer casing enclosing the rotor, whereby an annular space is provided between an outer wall of the rotor and the stationary outer casing;

a sintered metal tube centered on the axis of rotation and extending the entire length of the rotor, wherein the sintered metal tube is fluidly connected with a light gas outlet line at a top thereof;

a feed gas inlet cylinder extending through a top of and a distance into the rotor, and surrounding a length of the sintered metal tube;

rotating the rotor about the axis of rotation, whereby heavy molecules of the feed gas are forced toward the inner wall of the rotor; and

extracting at least a portion of the first fraction from the interior space, and extracting at least a portion of the second fraction from the interior space;

wherein the first fraction comprises one or more components of the feed gas having a molecular weight below a cutpoint size, and wherein the second fraction comprises one or more components of the feed gas having a molecular weight above the cutpoint size; and wherein extracting the at least a portion of the first fraction from the interior space comprises extracting the at least a portion through the sintered metal tube and out the light gas outlet line.

8. The method of claim 7, wherein the rotor is permeable to gas, and wherein extracting the at least a portion of the second fraction from the interior space further comprises passing the at least a portion of the second fraction through the permeable rotor and into the annular space, and extracting the at least a portion of the second fraction from the annular space via a heavy gas outlet extending through a lower portion of the outer casing and a horizontal distance into the annular space.

9. The method of claim 7, wherein the gas centrifuge further comprises a heavy gas outlet, wherein the heavy gas outlet enters the interior space proximal the axis of rotation, and extends horizontally to a position proximal the inner wall of the rotor, and wherein extracting the at least a portion of the

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second fraction from the interior space further comprises passing the at least a portion of the second fraction through the heavy gas outlet.

10. The method of claim 7, wherein the first fraction comprises uranium-235, and wherein the second fraction comprises uranium-238.

11. The method of claim 2 further comprising extracting the at least a portion of the second fraction from the annular space via a heavy gas outlet extending through a lower portion of the outer casing and a horizontal distance into the annular space.

12. The method of claim 11 further comprising assisting extraction of the second fraction via a pump positioned in the heavy gas outlet.

13. The method of claim 1, wherein the gas centrifuge further comprises a heavy gas outlet, wherein the heavy gas outlet enters the interior space proximal the axis of rotation, and extends horizontally to a position proximal the inner wall of the rotor, and wherein extracting the at least a portion of the second fraction from the interior space further comprises passing the at least a portion of the second fraction through the heavy gas outlet.

14. The method of claim 1 further comprising continuously introducing the feed gas into the gas centrifuge via the feed gas inlet cylinder and extracting the at least a first fraction from the gas centrifuge via the stationary porous tube and the light gas outlet line, while preventing removal of the second fraction; monitoring the composition of the gas within the interior space; and, when the gas within the interior space attains a desired concentration of the second fraction, discontinuing extraction of the first fraction, and extracting the second fraction.

15. The method of claim 14, wherein the rotor is permeable to gas, and wherein extracting the at least a portion of the second fraction from the interior space further comprises passing the at least a portion of the second fraction through the permeable rotor and thus into the annular space, and extracting the at least a portion of the second fraction from the annular space via a heavy gas outlet extending through a lower portion of the outer casing and a horizontal distance into the annular space.

16. The method of claim 15 further comprising assisting extraction of the second fraction via a pump positioned on the heavy gas outlet.

17. The method of claim 14, wherein the gas centrifuge further comprises a heavy gas outlet, wherein the heavy gas outlet enters the interior space proximal the axis of rotation, and extends horizontally to a position proximal the inner wall of the rotor, and wherein extracting the at least a portion of the second fraction from the interior space further comprises passing the at least a portion of the second fraction out the heavy gas outlet.

18. The method of claim 1, wherein the first fraction comprises uranium-235, and wherein the second fraction comprises uranium-238.

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