

US005397441A

United States Patent [19]

Berg

Patent Number: [11]

5,397,441

Date of Patent: [45]

Mar. 14, 1995

[54]	SEPARATION OF ETHYL BENZENE FROM O-XYLENE BY EXTRACTIVE DISTILLATION		[56] References Cited U.S. PATENT DOCUMENTS		
[75]	Inventor:	Lloyd Berg, 1314 S. Third Ave., Bozeman, Mont. 59715	3,105,017 9/1963 Amir et al		
			FOREIGN PATENT DOCUMENTS		
[73]	Assignee:	Lloyd Berg, Bozeman, Mont.	2355793 of 0000 France		
[21]	Appl. No.:	181,016	Primary Examiner-Wilbur Bascomb, Jr.		
			[57] ABSTRACT		
[22]	Filed:	Jan. 14, 1994	Ethyl benzene is difficult to separate from o-xylene by conventional distillation or rectification because of the closeness of their boiling points. Ethyl benzene can be		
[51]	Int. Cl.6	B01D 3/40; C 07C 7/08	readily separated from o-xylene by extractive distilla-		
[52]	U.S. Cl		tion. Effective agents are phenol, cresols, nitrotoluenes		
[50]		; 585/805; 585/808; 585/860; 585/864	and cyclododecanol.		
[58]	Field of Search		1 Claim, No Drawings		

1 Claim, No Drawings

SEPARATION OF ETHYL BENZENE FROM O-XYLENE BY EXTRACTIVE DISTILLATION

FIELD OF THE INVENTION

This invention relates to a method for separating ethyl benzene from o-xylene using certain higher boiling liquids as the agent in extractive distillation.

DESCRIPTION OF PRIOR ART

Extractive distillation is the method of separating close boiling compounds from each other by carrying out the distillation in a multiplate rectification column in the presence of an added liquid or liquid mixture, said 15 liquid(s) having a boiling point higher than the compounds being separated. The extractive agent is introduced near the top of the column and flows downward until it reaches the stillpot or reboiler. Its presence on each plate of the rectification column alters the relative 20 volatility of the close boiling compounds in a direction to make the separation on each plate greater and thus require either fewer plates to effect the same separation or make possible a greater degree of separation with the same number of plates. The extractive agent should boil 25 higher than any of the close boiling liquids being separated and not form minimum azeotropes with them. Usually the extractive agent is introduced a few plates from the top of the column to insure that none of the extractive agent is carried over with the lowest boiling 30 component. This usually requires that the extractive agent boil about twenty Celcius degrees or more higher than the lowest boiling component.

At the bottom of a continuous column, the less volatile components of the close boiling mixtures and the ³⁵ extractive agent are continuously removed from the column. The usual methods of separation of these two components are the use of another rectification column, cooling and phase separation, or solvent extraction.

Extractive distillation typically requires the addition ⁴⁰ of an equal amount to twice as much extractive agent as the ethyl benzene and o-xylene on each plate of the rectification column. The extractive agent should be heated to about the same temperature as the plate into which it is introduced. Thus extractive distillation imposes an additional heat requirement On the column as well as somewhat larger plates. However this is less than the increase occasioned by the additional agents required in azeotropic distillation.

Ethyl benzene boils at 136° C.; o-xylene boils at 145° C. The closeness of their boiling points give them a relative volatility of 1.25. Table 1 shows the relative volatility required to get 99% purity. By straight rectification, 56 actual plates are required for the ethyl benzene—o-xylene separation but with an extractive agent that increases the the relative volatility to 1.6 for example, only 27 actual plates are required.

TABLE 1

	Theoretical and Actual Plates Required vs. Relative Volatility for Ethyl Benzene - o-Xylene Separation					
Relative Volatility	Theoretical Plates Required At Total Reflux, 99% Purity	Actual Plates Required, 75% efficiency				
1.25	42	56				
1.4	27	36				
1.5	23	31				
1.6	20	27				

OBJECTIVE OF THE INVENTION

The object of this invention is to provide a process or method of extractive distillation that will enhance the relative volatility of ethyl benzene from o-xylene in their separation in a rectification column. It is a further object of this invention to identify organic compounds which in addition to the above constraints, are stable, can be separated from o-xylene and recyled to the extractive column and reused with little decomposition.

SUMMARY OF THE INVENTION

The objects of this invention are provided by a process for separating ethyl benzene from o-xylene which entails the use of certain organic compounds as the agent in extractive distillation.

DETAILED DESCRIPTION OF THE INVENTION

I have discovered that certain organic compounds will greatly improve the relative volatility of ethyl benzene to o-xylene and permit the enhanced separation of ethyl benzene from o-xylene by rectification when employed as the agent in extractive distillation. Table 2 lists the compounds that I have found to be effective. They are nitrobenzene, 2-nitrotoluene, 3-nitrotoluene, 4-nitrotoluene, phenol, o-cresol, m-cresol, p-cresol, 3-ethyl phenol, 4-ethyl phenol, 2-isopropyl phenol, 3-isopropyl phenol, o-sec. butyl phenol, o-tert. butyl phenol, 2,4-dimethyl phenol, cyclododecanol, 1-dodecanol and tridecyl alcohol.

TABLE 2

Effective Extractive Distillation Agents				
Compounds	Rel. Vol.	Compounds	Rel. Vol.	
Nitrobenzene	1.45	2-Nitrotoluene	1.45	
3-Nitrotoluene	1.45	4-Nitrotoluene	1.48	
Phenol	1.60	o-Cresol	1.47	
m-Cresol	1.45	p-Cresol	1.42	
3-Ethyl phenol	1.40	4-Ethyl phenol	1.43	
m-p-Cresol	1.50	2-Isopropyl phenol	1.42	
3-Isopropyl phenol	1.38	o-sec. Butyl phenol	1.33	
2,4-Dimethyl phenol	1.45	o-tert. Butyl phenol	1.40	
Cyclododecanol	1.44	1-Dodecanol	1.35	
Tridecyl alcohol	1.40			

THE USEFULNESS OF THE INVENTION

The usefulness or utility of this invention can be demonstrated by referring to the data presented in Tables 1 and 2. All of the successful agents show that ethyl benzene can be separated from o-xylene by means of extractive distillation in a rectification column and that the ease of separation as measured by relative volatility is considerable.

WORKING EXAMPLES

Example 1

Seventy grams of ethyl benzene, 30 grams of o-xylene and 50 grams of phenol were charged to a vapor-liquid equilibrium still and refluxed for ten hours. Analysis indicated a vapor composition of 78.1% ethyl benzene, 21.9% o-xylene; a liquid composition of 68.9% ethyl benzene, 31.1% o-xylene. This is a relative volatility of ethyl benzene to o-xylene of 1.60.

Example 2

Seventy grams of ethyl benzene, 30 grams of o-xylene and 50 grams of cyclododecanol were charged to a

vapor-liquid equilibrium still and refluxed for four hours. Analysis indicated a vapor composition of 75.5% ethyl benzene, 24.5% o-xylene; a liquid composition of 68.1% ethyl benzene, 31.2% o-xylene. This is a relative volatility of 1.44.

I claim:

1. A method for recovering ethyl benzene from a mixture of ethyl benzene and o-xylene which comprises distilling a mixture of ethyl benzene and o-xylene in the presence of about one part of an extractive agent per 10

part of ethyl benzene—o-xylene mixture, recovering the ethyl benzene as overhead product and obtaining the o-xylene and the extractive agent from the stillpot, wherein said extractive agent consists of one material selected from the group consisting of nitrobenzene, 2-nitrotoluene, 3-nitrotoluene, 4-nitrotoluene, cyclododecanol, 1-dodecanol and tridecyl alcohol.

* * * *