

[54] **PROCESS FOR REMOVING SO₂ AND FLY ASH FROM FLUE GAS**

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4,169,714 10/1979 Calvert 55/5
4,220,478 9/1980 Schuff 55/107
4,273,750 6/1981 Hollett et al. 55/262
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Related U.S. Application Data

[63] Continuation of Ser. No. 764,715, Aug. 12, 1985, abandoned.

[51] **Int. Cl.⁵** **B03C 3/00**

[52] **U.S. Cl.** **55/5; 55/107; 423/244**

[58] **Field of Search** **55/5, 107; 423/244 A**

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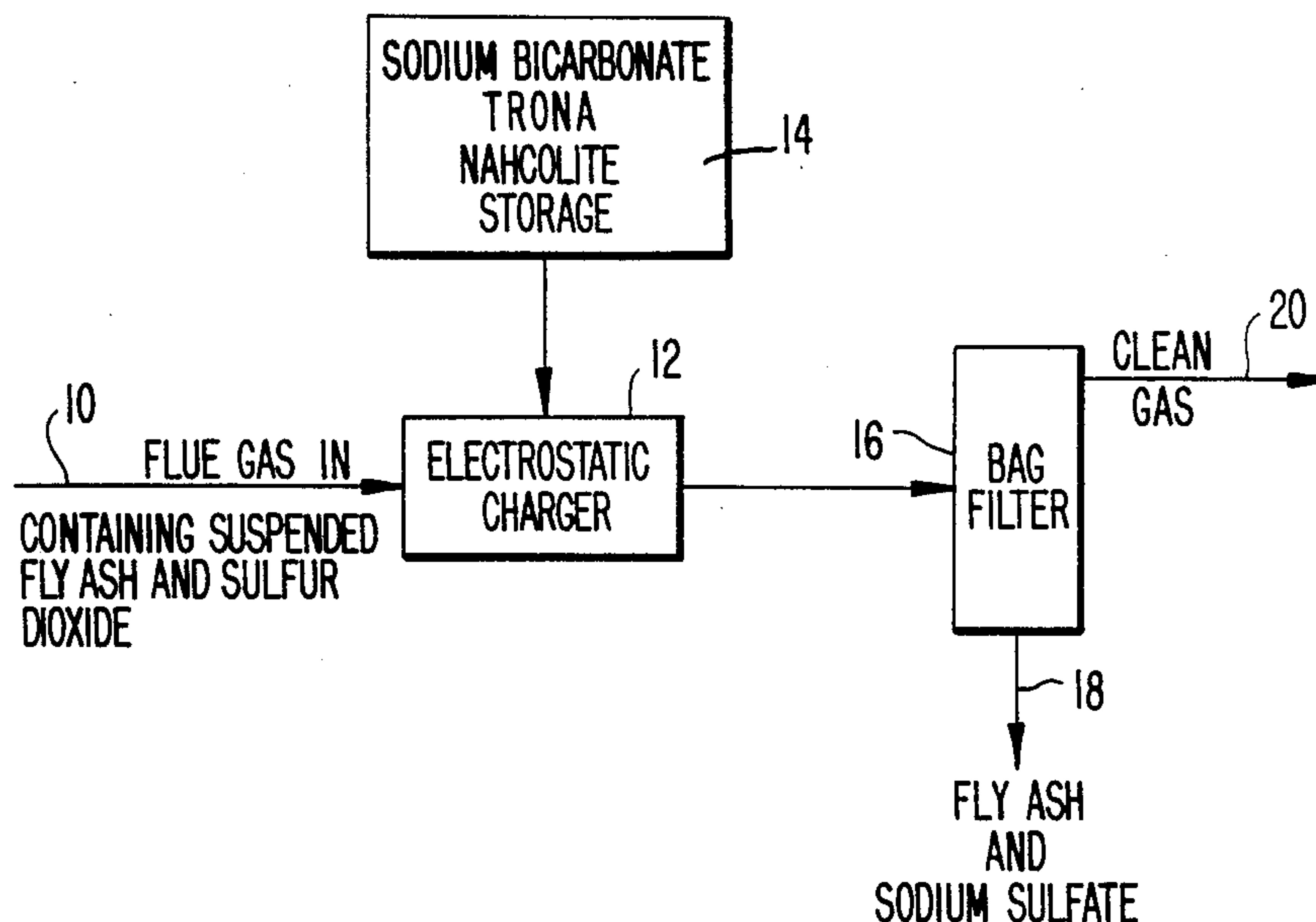
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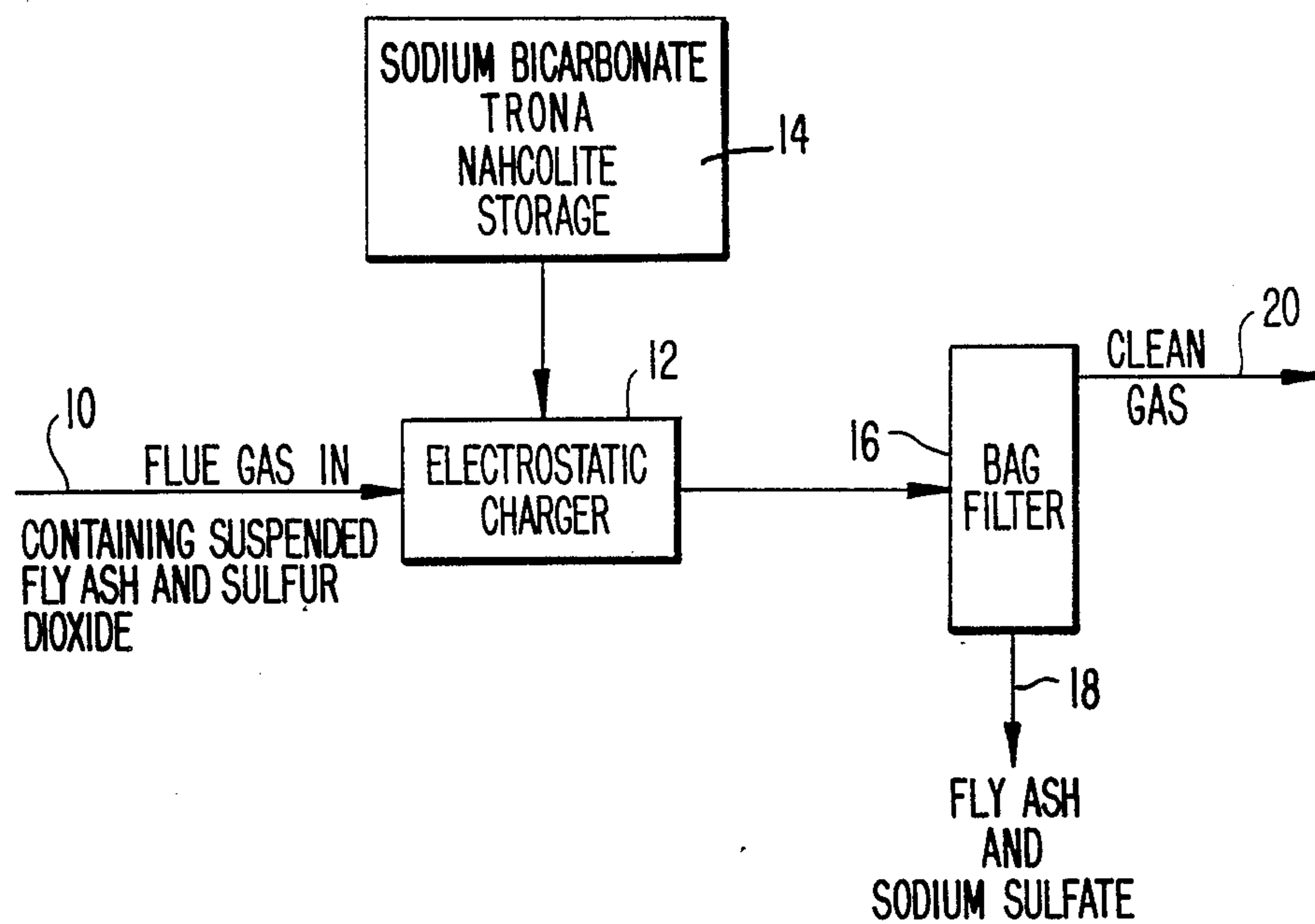
Attorney, Agent, or Firm—Kerkam, Stowell, Kondracki & Clarke

[57] **ABSTRACT**

A process is disclosed for enhanced removal of SO₂ and fly ash from flue gas by directing the flue gas and an SO₂ sorbent through an electrostatic charger and then through a bag filter where electrostatically improved flue gas/sorbent contact occurs and where the suspended fly ash and sodium sulfate are removed and the gas stream is discharged.

4 Claims, 1 Drawing Sheet





PROCESS FOR REMOVING SO₂ AND FLY ASH FROM FLUE GAS

This is a continuation of Application Ser. No. 764,715, filed Aug. 12, 1985, now abandoned.

FIELD OF THE INVENTION

This invention is directed to a process for enhancing the removal of SO₂ and fly ash from flue gases and to such a process wherein the ratio of SO₂ sorbent to SO₂ may be reduced resulting in a substantial saving in the cost of sorbent for plant operation.

BACKGROUND

It is known that the technique of particle charging prior to fabric filtration results in a pressure drop reduction as particle charging prior to fabric filtration produces a charged particle bed on the filter surface which is more open and less densely packed than when non-charged particles are collected. It is also known that SO₂ may be removed from flue gases by certain sorbents such as sodium bicarbonate and Nahcolite.

Examples of prior art are:

Schuff —4,290,786;

Schuff —4,220,478;

Johnstone —2,924,294;

Calvert —4,169,714.

BRIEF SUMMARY OF THE INVENTION

The present invention is based on a process for removing SO₂ and fly ash from flue gases by directing a particulate SO₂ sorbent, such as sodium bicarbonate or Nahcolite, and flue gas containing suspended fly ash and sulfur dioxide through an electrostatic charger and thereafter directing the charged sorbent and flue gas through a bag filter to separate the fly ash and formed sodium sulfate from the flue gas.

BRIEF DESCRIPTION OF THE DRAWING

The drawing is a flow diagram of apparatus for carrying out the process of the invention.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

Referring to the drawing directional arrow 10 represents the flow of flue gas containing suspended fly ash and sulfur dioxide into an electrostatic charger 12 of conventional design. Also directed into the electrostatic charger is particulate SO₂ sorbent preferably sodium

bicarbonate or its naturally occurring form, such as Nahcolite or Trona, from a storage bin 14.

The combined flue gas and SO₂ sorbent are then directed to the bag filter 16 where the electrostatically charged sorbent creates a bed of loosely packed particles. Due to reduced resistance to gas flow, this bed of sorbent can be allowed to increase in depth, resulting in enhanced flue gas contact and enhanced conversion of the SO₂ to sodium sulfate. The discharge from the bag filter 16 is fly ash and sodium sulfate as at 18 and clean gas as at 20. Nahcolite (NaHCO₃) is most often considered as the SO₂ sorbent of choice, and Na₂/S ratio of 1.2 or higher is generally considered to be needed for 90% SO₂ removal. Following the teachings of the present invention reduces the sorbent to SO₂ ratio such that Na₂/S ratio can be lowered to 1.0.

EXAMPLE

Considering a 500 MW power plant using 12,000 BTU/pound, 2% sulfur coal and operating 7,000 hours/year a Na₂/S ratio reduction from 1.2 to 1.0 and assuming a Nahcolite cost of \$75.00 per ton would result in a yearly saving of approximated \$2.4 million. This can be compared to the estimated installation cost of the electrostatic charger of 0.5 million. Preferably the sorbent particles are in the size range of from about 1 micron to about 100 microns.

The electrostatic charger makes use of high voltage corona discharge, such as is utilized in electrostatic precipitators.

I claim:

1. A process for removal of SO₂ and fly ash from flue gas and reducing the ratio of SO₂ sorbent to SO₂ comprising the steps directing a particulate SO₂ sorbent in the size range of from about 1 micron to about 100 microns selected from the group consisting of sodium bicarbonate, Nahcolite and Trona into an electrostatic charger utilizing corona discharge and contacting the flue gas containing suspended fly ash and sulfur dioxide with the SO₂ sorbent; directing the charged sorbent and flue gas to a bag filter; permitting the charged particulate sorbent and fly ash to form a layer on the surface of the bag filter where the SO₂ converts the SO₂ sorbent to sodium sulfate as the flue gas passes through the bag filter.

2. The process as defined in claim 1 wherein the sorbent is sodium bicarbonate.

3. The process as defined in claim 1 wherein the sorbent is Nahcolite.

4. The process as defined in claim 1 wherein the sorbent is Trona.

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