



(19) **United States**

(12) **Patent Application Publication**
Kirk et al.

(10) **Pub. No.: US 2010/0224503 A1**

(43) **Pub. Date: Sep. 9, 2010**

(54) **LOW-ENERGY ELECTROCHEMICAL
HYDROXIDE SYSTEM AND METHOD**

Related U.S. Application Data

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(63) Continuation of application No. 12/375,632, filed on Mar. 5, 2009.

Publication Classification

(51) **Int. Cl.**
C25B 15/08 (2006.01)
C25B 1/02 (2006.01)
C25B 9/10 (2006.01)

(52) **U.S. Cl.** **205/351; 204/242; 204/252**

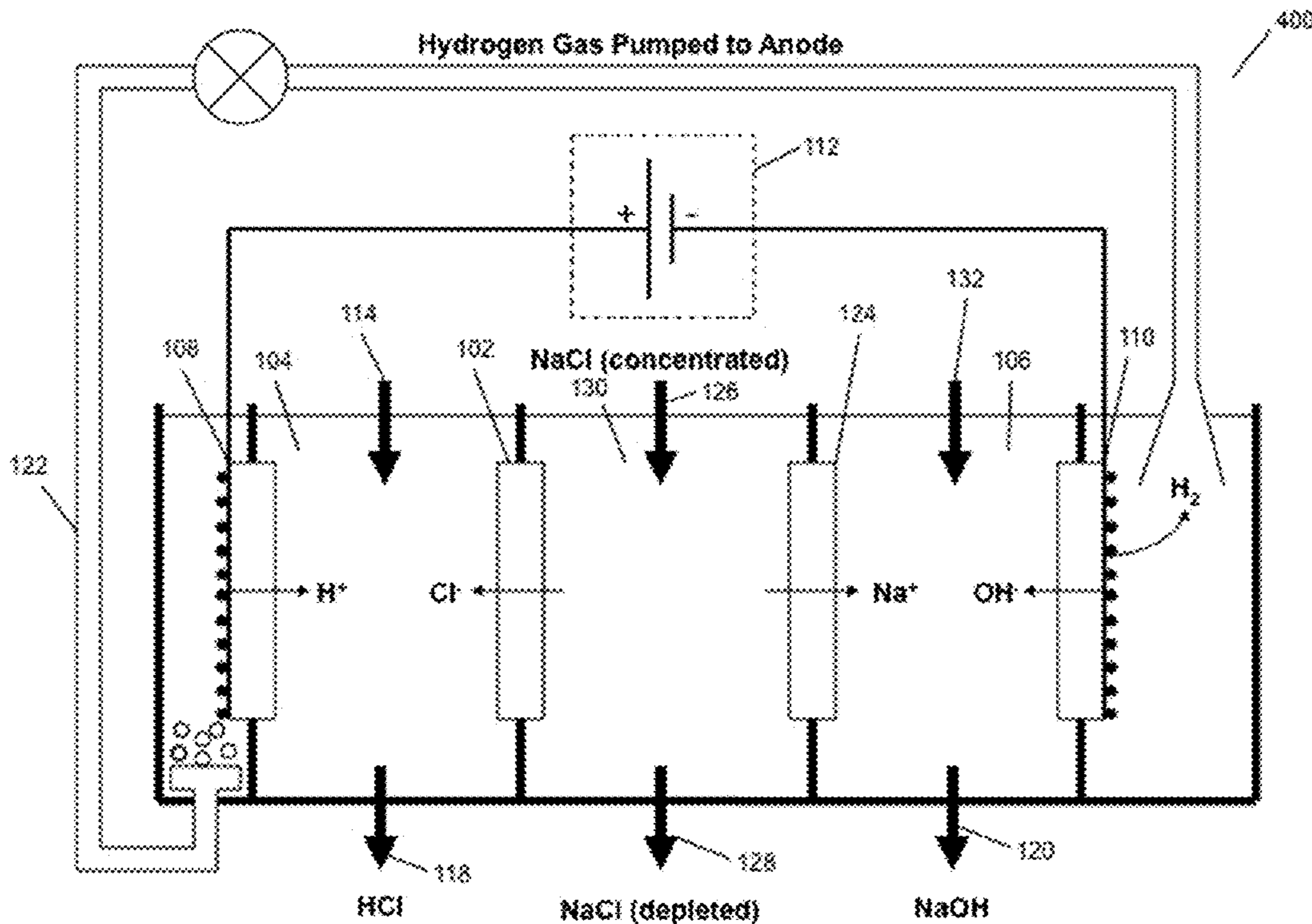
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(57) **ABSTRACT**

A low-energy method and system of forming hydroxide ions in an electrochemical cell. On applying a low voltage across the anode and cathode, hydroxide ions form in the electrolyte containing the cathode, protons form at the anode but a gas e.g. chlorine or oxygen does not form at the anode.

(21) Appl. No.: **12/697,926**

(22) Filed: **Feb. 1, 2010**



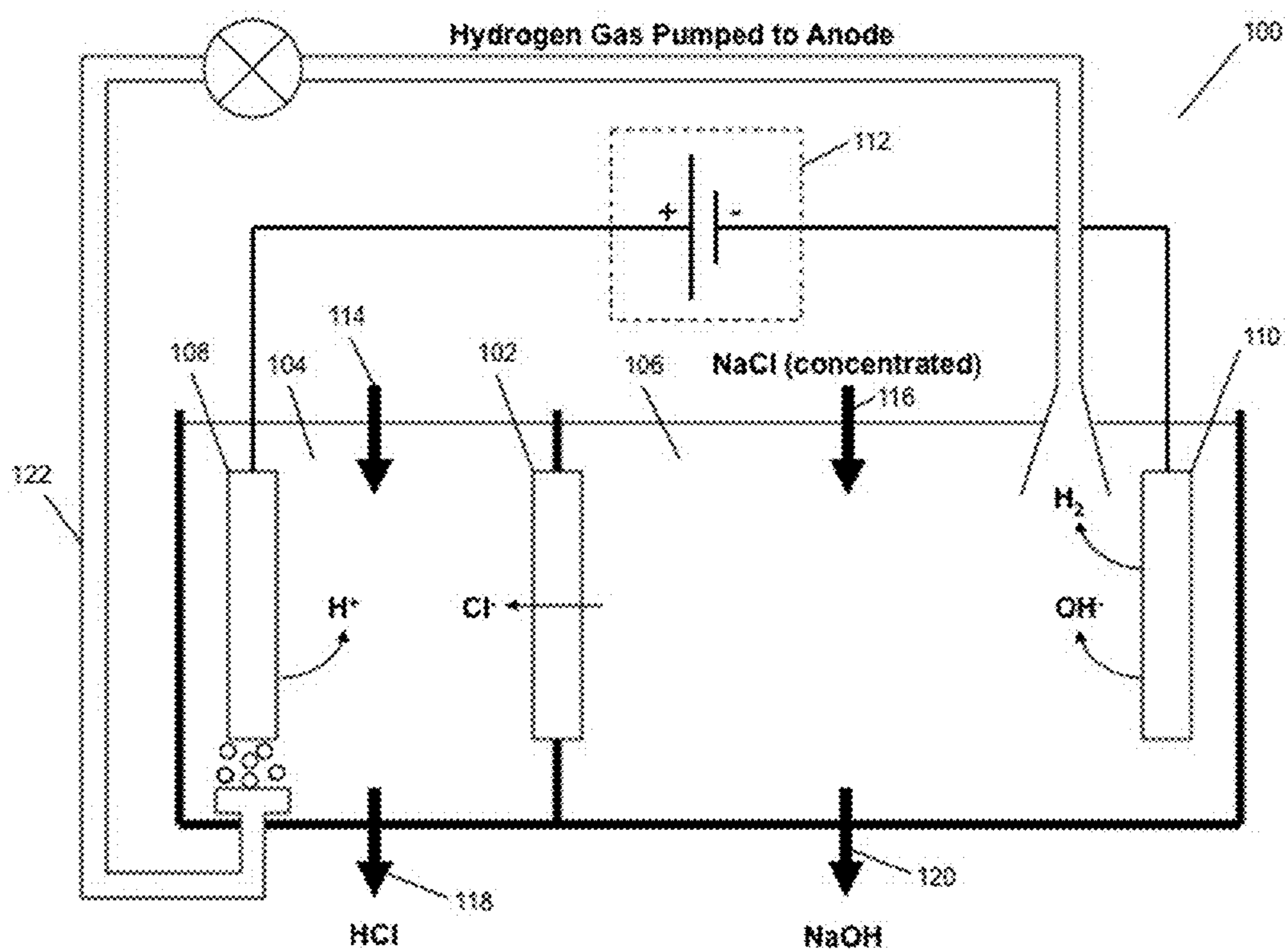


Fig. 1

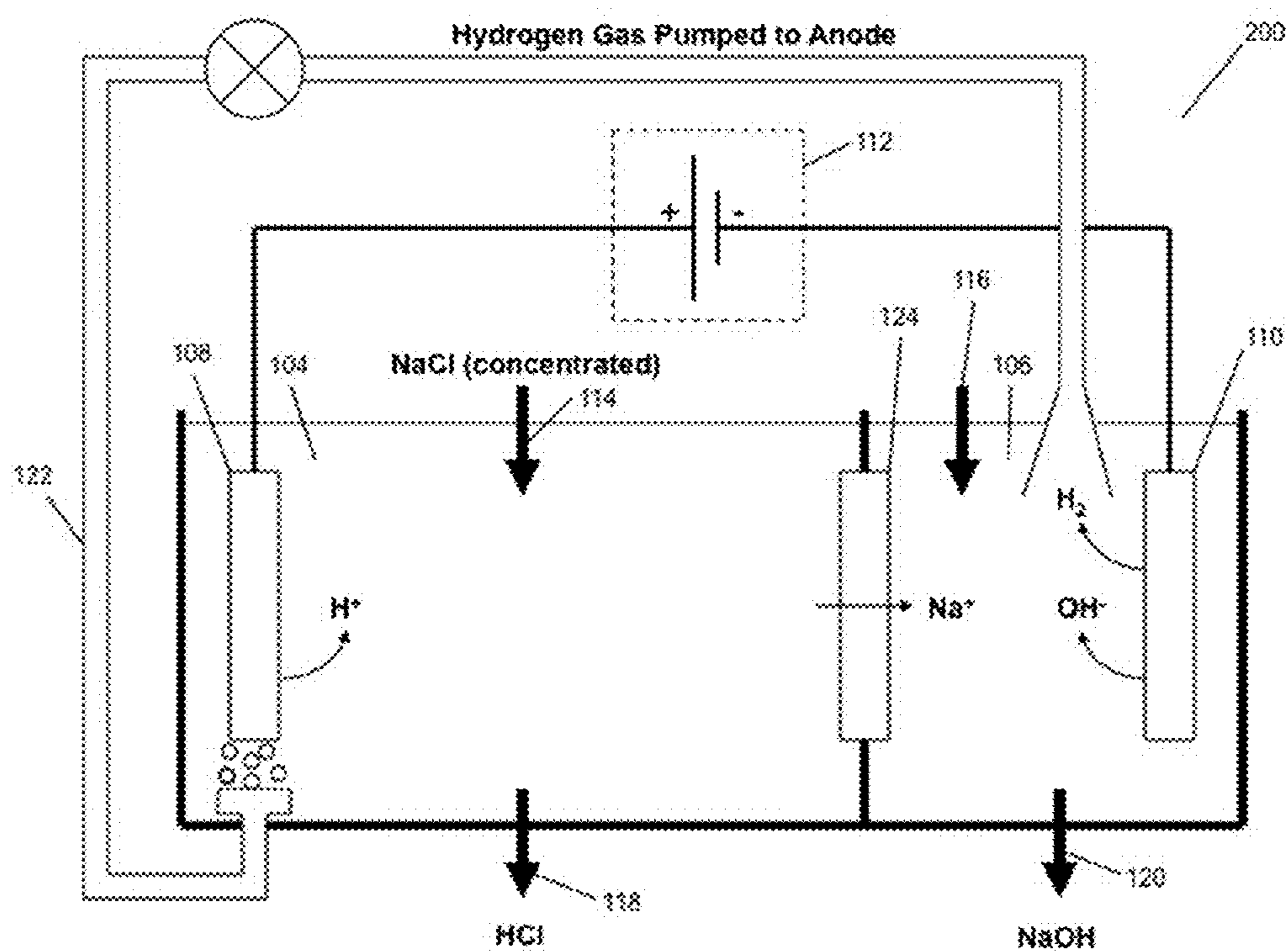


Fig. 2

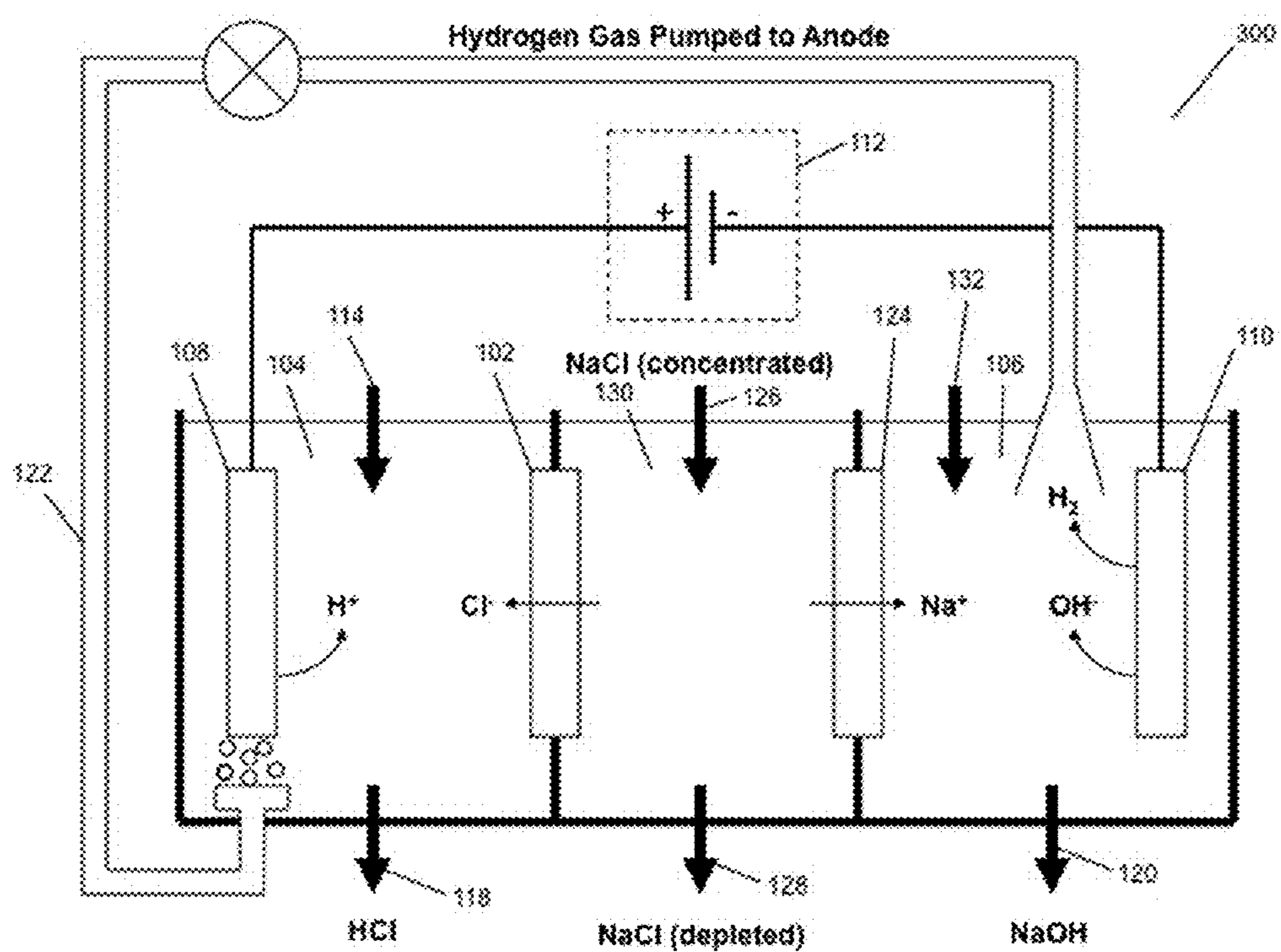


Fig. 3

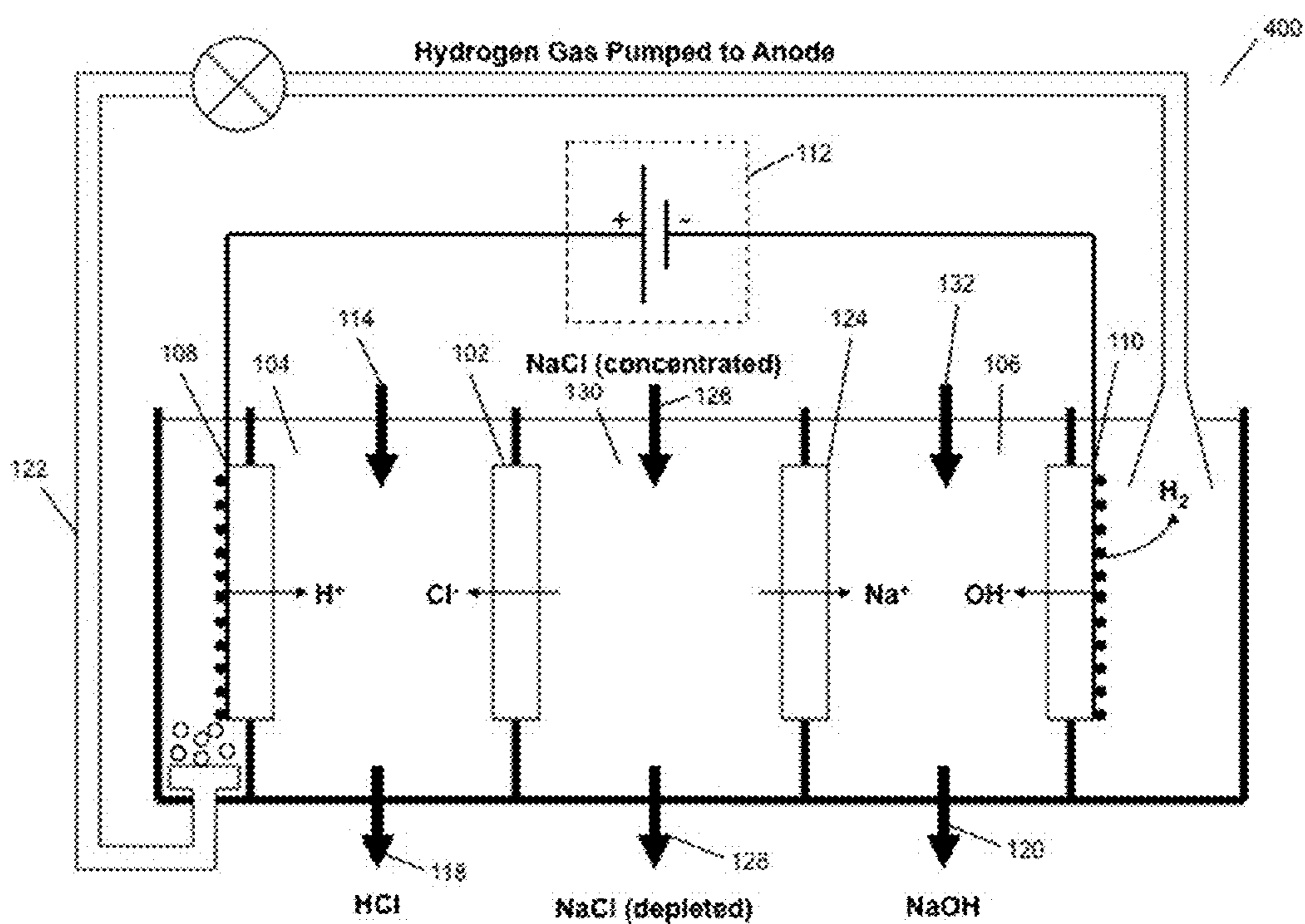


Fig. 4

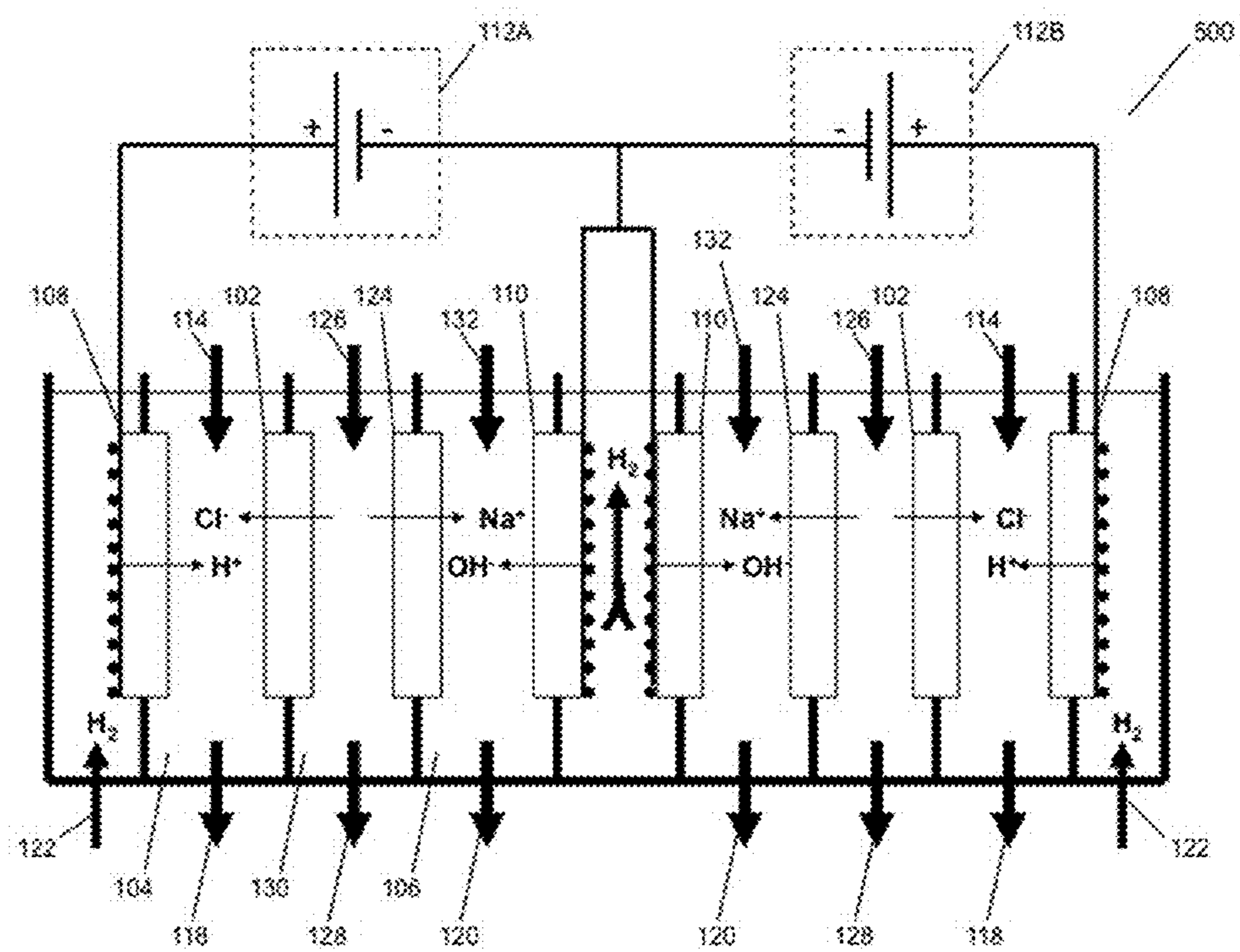


Fig. 5

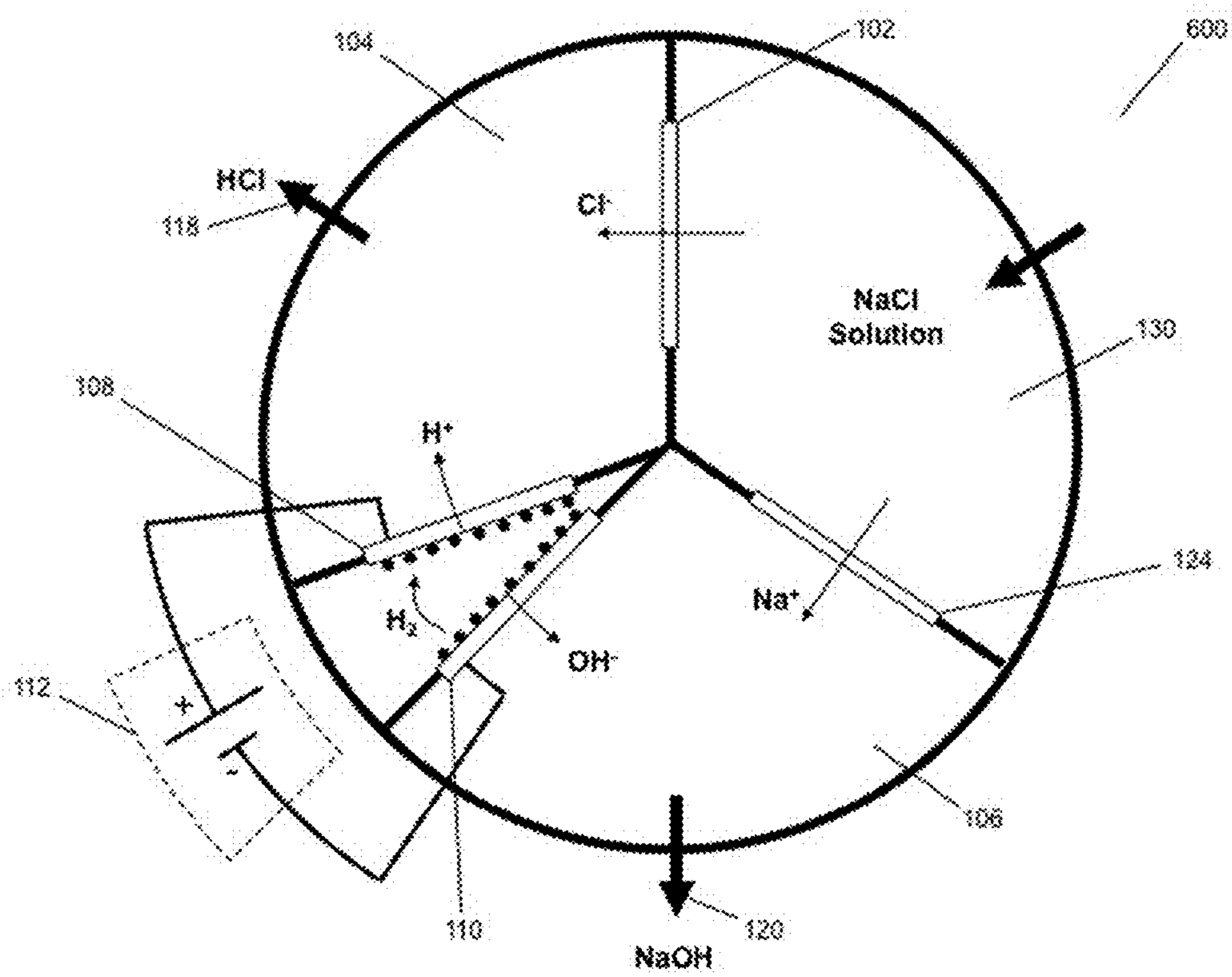


Fig. 6

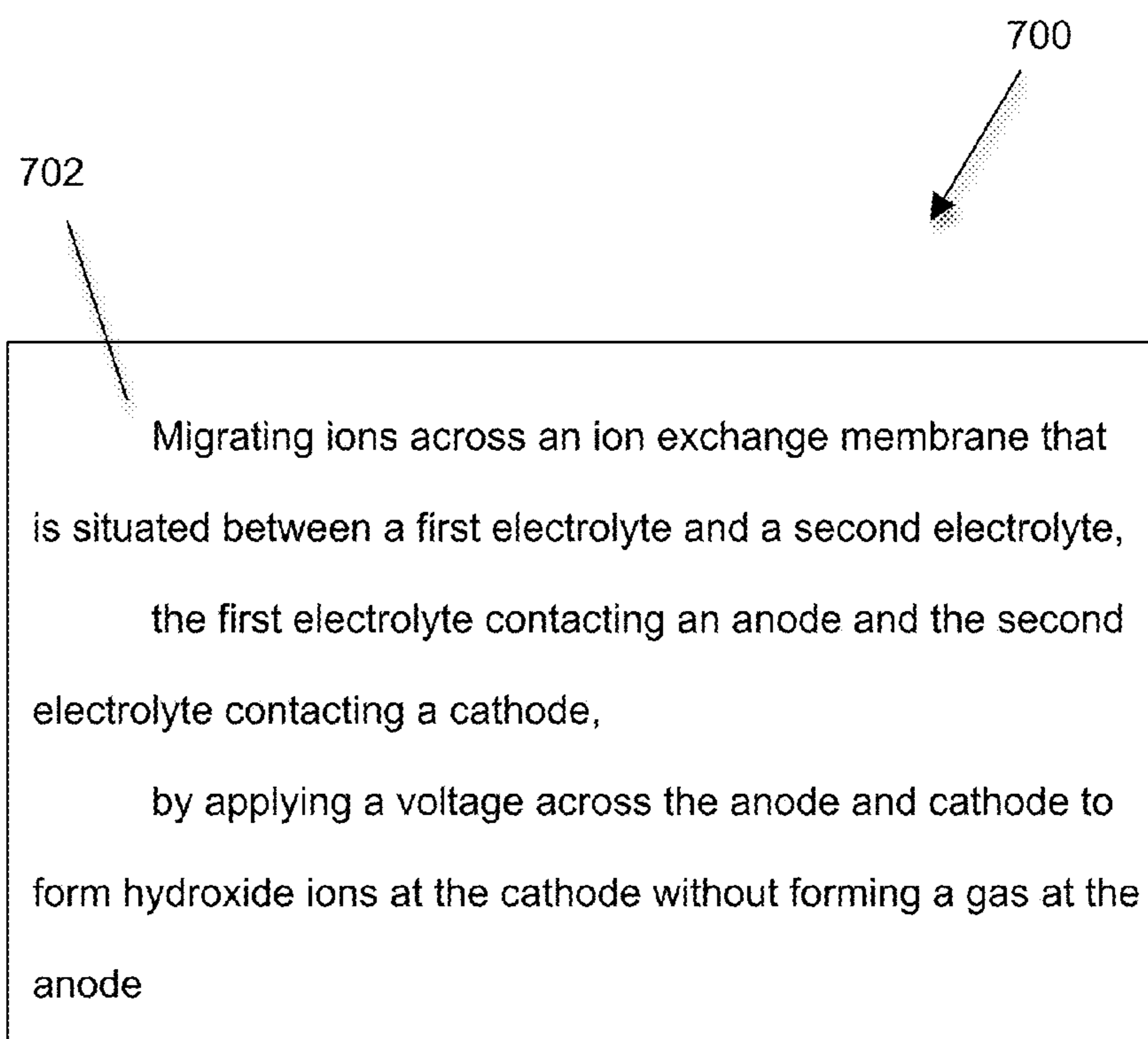


Fig.

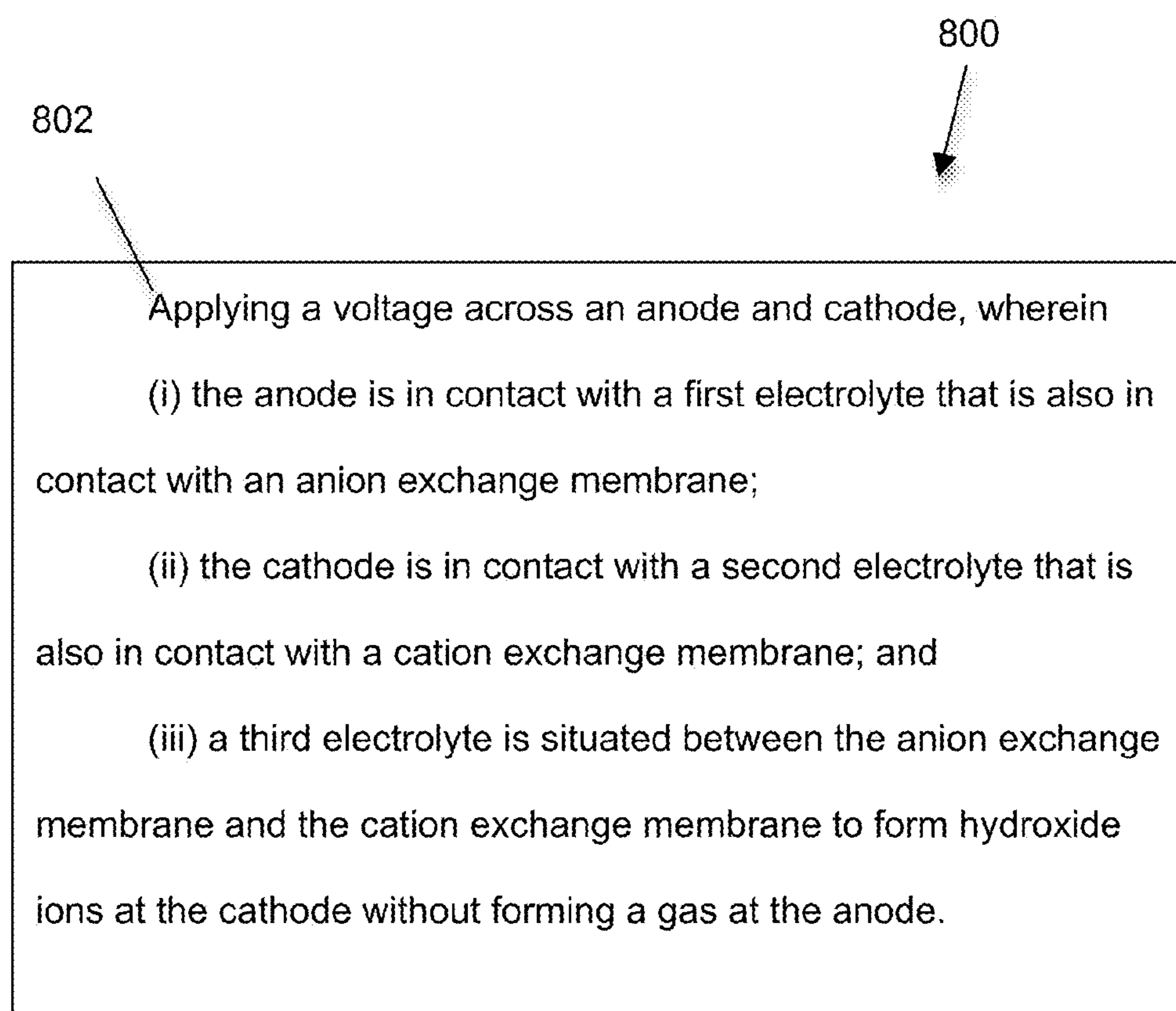


Fig. 8

LOW-ENERGY ELECTROCHEMICAL HYDROXIDE SYSTEM AND METHOD

BACKGROUND

[0001] In many chemical processes a solution of hydroxide ions (OH^-) is required to achieve or modulate a chemical reaction. One way to obtain OH^- in a solution is to dissolve an alkali hydroxide such as sodium hydroxide or magnesium hydroxide in the solution. However, conventional processes for producing hydroxides are very energy intensive, e.g., the chlor-alkali process, and they emit significant amounts of carbon dioxide and other greenhouse gases into the environment.

SUMMARY

[0002] In various embodiments the present invention pertains to a low energy electrochemical system and method of producing OH^- utilizing an ion exchange membrane in an electrochemical cell. The system in one embodiment comprises an anionic or cationic exchange membrane positioned between a first electrolyte and a second electrolyte, the first electrolyte contacting an anode and the second electrolyte contacting a cathode. Suitable electrolytes comprise a salt-water including sodium chloride, seawater, brackish water or freshwater. On applying a low voltage across the anode and cathode, OH^- forms at the cathode and protons form at the anode without a gas, e.g., chlorine or oxygen, forming at the anode. Depending on the electrolytes used, a hydroxide solution, e.g., sodium hydroxide, forms in the second electrolyte in contact with the cathode and an acid, e.g., hydrochloric acid forms in the first electrolyte in contact with the anode. In various embodiments, OH^- forms when a volt of less than 0.1 V is applied across the electrodes.

[0003] In another embodiment the system comprises an electrochemical cell in which an anion exchange membrane separates a first electrolyte from a third electrolyte; a cation exchange membrane separates the third electrolyte from a first electrolyte; an anode is in contact with the first electrolyte; and a cathode is in contact with the second electrolyte. On applying a low voltage across the anode and cathode, OH^- forms at the cathode without a gas, e.g., chlorine or oxygen forming at the anode. Depending on the electrolyte used, a hydroxide solution, e.g., sodium hydroxide, forms in the second electrolyte in contact with the cathode, and an acid, e.g., hydrochloric acid forms in the first electrolyte in contact with the anode. In various embodiments, OH^- forms when a volt of less than 0.1 V is applied across the electrodes.

[0004] In one embodiment the method comprises migrating ions across an ion exchange membrane that is situated between a first electrolyte and a second electrolyte, the first electrolyte contacting an anode and the second electrolyte contacting a cathode, by applying a voltage across the anode and cathode to form hydroxide ions at the cathode without forming a gas, e.g., chlorine or oxygen at the anode. Depending on the electrolyte used, a hydroxide solution, e.g., sodium hydroxide forms in the second electrolyte in contact with the cathode and an acid, e.g., hydrochloric acid forms in the first electrolyte in contact with the anode. In various embodiments, OH^- forms when a volt of less than 0.1 V is applied across the electrodes.

[0005] In another embodiment the method comprises applying a voltage across an anode and cathode, wherein (i) the anode is in contact with a first electrolyte that is also in

contact with an anion exchange membrane; (ii) the cathode is in contact with a second electrolyte that is also in contact with a cation exchange membrane; and (iii) a third electrolyte is situated between the anion exchange membrane and the cation exchange membrane to form hydroxide ions at the cathode without forming a gas e.g., chlorine or oxygen at the anode. By the method OH^- forms at the cathode in contact the second electrolyte without a gas e.g., chlorine or oxygen at the anode. Depending on the electrolyte used, a hydroxide solution, e.g. sodium hydroxide, forms in the second electrolyte in contact with the cathode, and an acid, e.g., hydrochloric acid forms in the first electrolyte in contact with the anode. In various embodiments, OH^- forms when a volt of less than 0.1 V is applied across the electrodes.

[0006] In various configurations, the system and method are adapted for batch, semi-batch or continuous flows. Depending on the electrolytes used, the system is adaptable to form OH^- in solution, e.g., sodium hydroxide at the cathode, or an acidic solution, e.g., hydrochloric acid at the anode without forming a gas e.g., chlorine or oxygen at the anode. In various embodiments, the solution comprising OH^- can be used to sequester CO_2 by contacting the solution with CO_2 and precipitating alkaline earth metal carbonates, e.g., calcium and magnesium carbonates and bicarbonates from a solution comprising alkaline earth metal ions as described U.S. Provisional Patent Application Ser. No. 60/931,657 filed on May 24, 2007; U.S. Provisional Patent Application Ser. No. 60/937,786 filed on Jun. 28, 2007; U.S. Provisional Patent Application 61/017,419, filed on Dec. 28, 2007; U.S. Provisional Patent Application Ser. No. 61/017,371, filed on Dec. 28, 2007; and U.S. Provisional Patent Application Ser. No. 61/081,299, filed on Jul. 16, 2008, herein incorporated by reference. The precipitated carbonates, in various embodiments, are useable as building products, e.g., cements, as described in United States patent applications herein incorporated by reference. Similarly, the system and method are adaptable for desalinating water as described in United States patent applications herein incorporated by reference.

BRIEF DESCRIPTION OF THE DRAWINGS

[0007] The following drawings illustrate the present system and method by way of examples and not limitations. The methods and systems may be better understood by reference to one or more of these drawings in combination with the description herein:

[0008] FIG. 1 is an illustration of an embodiment of the present system.

[0009] FIG. 2 is an illustration of an embodiment of the present system.

[0010] FIG. 3 is an illustration of an embodiment of the present system.

[0011] FIG. 4 is an illustration of an embodiment of the present system.

[0012] FIG. 5 is an illustration of an embodiment of the present system.

[0013] FIG. 6 is an illustration of an embodiment of the present system.

[0014] FIG. 7 is a flow chart of an embodiment of the present method.

[0015] FIG. 8 is a flow chart of an embodiment of the present method.

DETAILED DESCRIPTION

[0016] Before the present methods and systems are described in detail, it is to be understood that this invention is not limited to particular embodiments described and illustrated herein, and as such may vary. It is also to be understood that the terminology used herein is for the purpose of describing particular embodiments only, and is not intended to be limiting, since the scope of the present invention will be limited only by the appended claims.

[0017] Where a range of values is provided, it is to be understood that each intervening value, to the tenth of the unit of the lower limit unless the context clearly dictates otherwise, between the upper and lower limit of that range and any other stated or intervening value in that stated range, is encompassed within the invention. The upper and lower limits of these smaller ranges may independently be included in the smaller ranges and are also encompassed within the invention, subject to any specifically excluded limit in the stated range. Where the stated range includes one or both of the limits, ranges excluding either or both of those included limits are also included in the invention.

[0018] Ranges are presented herein at times with numerical values being preceded by the term "about." The term "about" is used herein to provide literal support for the exact number that it precedes, as well as a number that is near to or approximately the number that the term precedes. In determining whether a number is near to or approximately a specifically recited number, the near or approximating unrecited number may be a number that, in the context in which it is presented, provides the substantial equivalent of the specifically recited number.

[0019] Unless defined otherwise, all technical and scientific terms used herein have the same meaning as commonly understood by one of ordinary skill in the art to which this invention belongs. Although any methods, systems and materials similar or equivalent to those described herein can also be used in the practice or testing of the present invention, representative illustrative methods, systems and materials are herein described.

[0020] All publications and patents cited in this specification are herein incorporated by reference as if each individual publication or patent were specifically and individually indicated to be incorporated by reference and are incorporated herein by reference to disclose and describe the methods and/or materials in connection with which the publications are cited. The citation of any publication is for its disclosure prior to the filing date and should not be construed as an admission that the present invention is not entitled to antedate such publication by virtue of prior invention. Further, the dates of publication provided may be different from the actual publication dates that may need to be independently confirmed.

[0021] As used herein and in the appended claims, the singular forms "a," "an," and "the" include plural references unless the context clearly dictates otherwise. Also, the claims may be drafted to exclude any optional element. As such, this statement is intended to serve as antecedent basis for use of such exclusive terminology as "solely," "only" and the like in connection with the recitation of claim elements, or use of a "negative" limitation. Additionally, the term "reservoir" as used herein refers to an enclosure for holding a liquid such as a vessel, tank, chamber or bag.

[0022] As will be apparent to those of skill in the art, each of the embodiments described and illustrated herein has dis-

crete components and features which may be readily separated from or combined with the features of any of the other several embodiments without departing from the scope or spirit of the present invention. Any recited method can be carried out in the order of events recited or in any possible logical order.

[0023] In the description herein, the invention will be described for convenience in terms of production of hydroxide. It will be appreciated that in some embodiments hydroxide may not be produced, e.g., in embodiments where the pH of the electrolyte solution in contact with the cathode, as described herein, is kept constant or even decreases, there is no net production of hydroxide ions and can even be a decrease in hydroxide ion production. This can occur, e.g., in embodiments in which CO₂ is introduced into the second electrolyte solution, as described further herein.

[0024] The present invention in various embodiments is directed to a low voltage electrochemical system and method for forming OH⁻ in a solution, e.g., a saltwater solution, utilizing ion exchange membranes. On applying a voltage across a cathode and an anode, OH⁻ forms in solution in the electrolyte contacted with the cathode, protons form in the solution contacted with the anode, and a gas e.g., chlorine or oxygen is not formed at the anode. Hydroxide ions are formed where the voltage applied across the anode and cathode is less than 2.8, 2.7, 2.5, 2.4, 2.3, 2.2, 2.1, 2.0, 1.9, 1.8, 1.7, 1.6, 1.5, 1.4, 1.3, 1.2, 1.1, 1.0, 0.9, 0.8, 0.7, 0.6, 0.5, 0.4, 0.3, 0.2, or 0.1 V.

[0025] In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 2.5 V without the formation of gas at the anode. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 2.2V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 2.0V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 1.5 V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 1.0V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.8 V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.7V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.6V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.5V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.4V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.3V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.2V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.1V. In certain embodiments hydroxide ions are formed where the voltage applied across the anode and cathode is less than 0.05V. In various embodiments an acidic solution, e.g., hydrochloric acid is formed in the electrolyte in contact with the anode.

[0026] With reference to FIGS. 1-6, in various embodiments the present system is adaptable for batch and continuous processes as described herein. Referring to FIGS. 1 and 2, in one embodiment the system comprises an electrochemical

system including an ion exchange membrane (102, 124) separating a first electrolyte (104) from a second electrolyte (106), the first electrolyte contacting an anode (108) and the second electrolyte contacting a cathode (110). As used herein, "ion exchange membrane" includes membranes that are selectively permeable to one ion, or one type of ion (e.g., anions, or monovalent anions, or cations, or monovalent cations). In the system as illustrated in FIG. 1, on applying a voltage across the anode and cathode, hydroxide ions form in the electrolyte contacting the cathode, protons form in the electrolyte contacting the anode without a gas e.g., chlorine or oxygen forming at the anode. In the illustration of FIG. 1, an anion exchange membrane (102) is utilized; in FIG. 2, a cation exchange membrane (124) is utilized.

[0027] In the embodiment illustrated in FIG. 1, first electrolyte (104) comprises an aqueous salt solution such as a saltwater, e.g., seawater, freshwater, brine, brackish water or the like. In various embodiments, second electrolyte (106) comprises a concentrated solution of sodium chloride; in other embodiments, second electrolyte may comprise saltwater. In the embodiment of FIG. 2, the first electrolyte (104) comprises a concentrated solution of sodium chloride, and second electrolyte (106) comprises an aqueous solution such as a saltwater, e.g., seawater, freshwater, brine, brackish water or the like. In an alternative embodiment, first electrolyte may comprise a saltwater.

[0028] In various embodiments, anion exchange membrane (102) and/or cation exchange membrane (124) are any ion exchange membranes suitable for use in an acidic and/or basic electrolytic solution temperatures in the range from about 0° C. to about 100° C., such as conventional ion exchange membranes well-known in the art, or any suitable ion exchange membrane. Suitable anion exchange membranes are available from PCA GmbH of Germany, e.g., an anion exchange membrane identified as PCSA-250-250 can be used; similarly, a cation exchange membrane identified as PCSK 250-250 available from PCA GmbH can be used. As will be appreciated, in the system the ion exchange membranes are positioned to prevent mixing of the first and second electrolytes.

[0029] With reference to FIGS. 1 and 2, in various embodiments the electrochemical system (100, 200) includes first electrolyte inlet port (114) for inputting first electrolyte (104) into the system and second electrolyte inlet port (116) for inputting second electrolyte (106) into the system. The cell includes outlet port (118) for draining first electrolyte from the system, and outlet port (120) for draining second electrolyte from the system. As will be appreciated by one ordinarily skilled, the inlet and outlet ports are adaptable for various flow protocols including batch flow, semi-batch flow, or continuous flow. In alternative embodiments, the system includes a conduit, e.g., a duct (122) for directing hydrogen gas to the anode; in various embodiments the gas comprises hydrogen formed at the cathode (110); other sources of hydrogen gas can be used.

[0030] As illustrated in FIGS. 1 and 2, the first electrolyte (104) contacts the anode (108) and ion exchange membrane (102, 124) on a first side; and the second electrolyte contacts the cathode (106) and the ion exchange membrane at an opposed side to complete an electrical circuit that includes conventional voltage/current regulator (112). The current/voltage regulator is adaptable to increase or decrease the current or voltage across the cathode and anode as desired.

[0031] With reference to FIG. 1, in an exemplary and non-limiting example using anion exchange membrane (102) and a concentrated solution of sodium chloride as the second electrolyte (116), upon applying a low voltage across the cathode (110) and anode (108), hydroxide ions are produced in the second electrolyte and hydrogen gas forms at the cathode (110), while protons form in the first electrolyte solution that is in contact with the anode (108) but a gas, e.g., chlorine or oxygen does not form at the anode (108). Where second electrolyte (106) comprises sodium chloride, chloride ions migrate into the first electrolyte (104) from the second electrolyte (106) through the anion exchange membrane (102), and protons form in the electrolyte in contact with the anode (108).

[0032] As can be appreciated by one ordinarily skilled in the art, and with reference to FIG. 1, in second electrolyte (106) as hydroxide ions form in the electrolyte in contact with the cathode (110) and enter into the second electrolyte (106), and as chloride ions migrate from the second electrolyte into the first electrolyte (104), an aqueous solution of sodium hydroxide will form in second electrolyte (106). Depending on the rate of introduction and/or removal of second electrolyte from the system, the pH of the second electrolyte is adjusted, e.g., increases, decreases or does not change. Similarly, with reference to FIG. 1, as protons form in the solution in contact with the anode and enter into the first electrolyte (104), the pH of the first electrolyte will adjust depending on rate of introduction and/or removal of first electrolyte from the system. Also, as chloride ions migrate to the first electrolyte from the second electrolyte across the anion exchange membrane, hydrochloric acid will form in the first electrolyte.

[0033] With reference to FIG. 2, in another exemplary and non-limiting embodiment, where a cation membrane (124) is used and concentrated solution of sodium chloride is used as the first electrolyte, upon applying a voltage across the cathode (110) and anode (108), hydroxide ions form in the second electrolyte and hydrogen gas forms at the cathode (110), protons form in the first electrolyte in contact with the anode but a gas, e.g., chlorine or oxygen does not form at the anode (108). Where first electrolyte (104) comprises sodium chloride, sodium ions migrate from the first electrolyte (104) to the second electrolyte (106) through the cation exchange membrane (124).

[0034] As can be appreciated by one ordinarily skilled in the art, and with reference to FIG. 2, in second electrolyte (106) as hydroxide ions form in the electrolyte in contact with the cathode (110) and enter into solution and with the migration of sodium ions into the second electrolyte, an aqueous solution of sodium hydroxide will form in second electrolyte (106). Depending on the rate of introduction and/or removal of second electrolyte from the system, the pH of the second electrolyte is adjusted, e.g., increases, decreases or does not change. Similarly, with reference to FIG. 2, as protons form in the electrolyte in contact with the anode and enter into solution, the pH of the first electrolyte will adjust depending on rate of introduction and/or removal of first electrolyte from the system, i.e., the pH of the first electrolyte may increase, decrease or does not change. Also, as sodium ions migrate from the first electrolyte across the cation exchange membrane to the second electrolyte, hydrochloric acid will form in the first electrolyte due to the presence of protons and chloride ions in the first electrolyte.

[0035] With reference to FIGS. 1 and 2, depending the flow of electrolytes in the system and the electrolytes used, e.g.

saltwater, when a voltage is applied across the anode (108) and cathode (110) OH^- will form in the in the second electrolyte (106), and consequently cause the pH of the second electrolyte to be adjusted. In one embodiment, when a voltage of about 0.1 V or less, 0.2 V or less, 0.4V or less, 0.6 V or less, 0.8 V or less, 1.0V or less, 1.5V or less, or 2.0V or less, e.g., when a voltage of 0.8V or less is applied across the anode and cathode, the pH of the second electrolyte solution is increased; in another embodiment, when a voltage of 0.01 to 2.5 V, or 0.01V to 2.0V, or 0.1V to 2.0V, or 0.1V to 1.5V, or 0.1 V to 1.0V, or 0.1V to 0.8V, or 0.1V to 0.6V, or 0.1V to 0.4V, or 0.1V to 0.2V, or 0.01V to 1.5V, or 0.01 V to 1.0V, or 0.01V to 0.8V, or 0.01V to 0.6V, or 0.01V to 0.4V, or 0.01V to 0.2V, or 0.01V to 0.1V, e.g., when a voltage of 0.1V to 2.0V is applied across the anode and cathode the pH of the second electrolyte increased; in yet another embodiment, when a voltage of about 0.1 to 1 V is applied across the anode and cathode the pH of the second electrolyte solution increased. Similar results are achievable with voltages of 0.1 to 0.8V; 0.1 to 0.7 V; 0.1 to 0.6 V; 0.1 to 0.5 V; 0.1 to 0.4 V; and 0.1 to 0.3 V across the electrodes.

[0036] Exemplary results achieved with the present system are summarized in Table 1.

TABLE 1

LOW ENERGY ELECTROCHEMICAL METHOD AND SYSTEM					
Volt across Electrodes	Membrane Type	Average Current	Initial pH Anode and Cathode	Final pH Anode	Final pH Cathode
0.4	Anion	1.45	6.624	4.790	9.609
0.6	Anion	1.27	6.624	4.643	9.779
0.4	Anion	0.81	6.624	4.896	9.458
0.6	Anion	0.90	6.624	4.596	9.393
1.0	Anion	1.49	6.624	4.677	9.974
0.6	Cation	2.07	6.624	4.444	10.140
0.6	Cation	16.0	6.624	3.381	11.171
1.0	Cation	24.7	6.624	3.245	11.328
1.0	Cation	14.0	6.624	3.237	10.901
0.6	Cation and Anion	6.22	6.624	3.888	10.717
1.0	Cation and Anion	17.6	6.624	3.115	11.066

With reference to Table 1, using saltwater as the first electrolyte and a sodium chloride as the second electrolyte, a process and method in accordance with the present invention as illustrated in FIG. 1, 2, or 3 was used to adjust the pH in the first and second electrolytes. By the method and system, NaOH was produced in the second electrolyte (106), and HCl in the first electrolyte (104) at a low operating voltage across the electrodes; it will be appreciated by those of ordinary skill in the art that the voltages may be adjusted up or down from these exemplary voltages; the minimum theoretical voltage is 0 or very close to 0, but to achieve a useful rate of production of hydroxide, a practical lower limit may be in some embodiments 0.001V or 0.01V, or 0.1 V, depending on the desired time for hydroxide production and/or pH adjustment, volume of second electrolyte solution, and other factors apparent to those of ordinary skill; i.e., in some embodiments the systems and methods are capable of producing hydroxide at voltages as low as 0.001V, or 0.01 V, or 0.1V, and can also produce hydroxide at higher voltages if more rapid production is desired, e.g., at 0.2-2.0V; in some embodiments the hydroxide is produced with no gas formation at the anode, e.g., no formation of oxygen or chlorine.

[0037] The system used included two 250 mL compartments separated by an anion exchange membrane in one embodiment, and a cation membrane in another embodiment. In both compartments a 0.5M NaCl 18M Ω aqueous solutions (28 g/L of NaCl was solvated with de-ionized water) was used. Both the anode and cathode comprised a 10 cm by 5 cm 45 mesh Pt gauze. In the anode compartment H_2 gas was sparged under the Pt electrode, and the two electrodes were held at a voltage bias as indicated in Table 1 e.g., 0.4, 0.6 V and 1.0 V, for 30 minutes. The pH of the electrolyte in contact with the anode before applying the voltage was 6.624. The cathode compartment where the hydroxide formation occurred was stirred at 600 rpm. As set forth in Table 1, significant changes in the pH in the cathode and anode compartment were achieved.

[0038] In these examples, and in various embodiments of the invention, a pH difference of more than 0.5, 1, 1.5, 2, 2.5, 3, 3.5, 4, 4.5, 5, 5.5, 6, 6.5, 7, 7.5, 8.0, 8.5, 9.0, 9.5, 10.0, 10.5, 11.0, 11.5, or 12.0 pH units may be produced in a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membrane, when a voltage of 1.0V or less, or 0.9V or less, or 0.8V or less, or 0.7 or less, or 0.6V or less, or 0.5V or less, or 0.4V or less, or 0.3V or less, or 0.2V or less, or 0.1V or less, or 0.05V or less, is applied across the anode and cathode.

[0039] For example, in particular embodiments the invention provides a system that is capable of producing a pH difference of more than 0.5 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 0.05V or less is applied across the anode and cathode. In some embodiments the invention provides a system that is capable of producing a pH difference of more than 1.0 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 0.1V or less is applied across the anode and cathode. In some embodiments the invention provides a system that is capable of producing a pH difference of more than 2.0 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 0.2V or less is applied across the anode and cathode.

[0040] In some embodiments the invention provides a system that is capable of producing a pH difference of more than 4.0 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 0.4V or less is applied across the anode and cathode. In some embodiments the invention provides a system that is capable of producing a pH difference of more than 6 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two

electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 0.6V or less is applied across the anode and cathode. In some embodiments the invention provides a system that is capable of producing a pH difference of more than 8 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more exchange membranes, when a voltage of 0.8V or less is applied across the anode and cathode. In particular embodiments the invention provides a system that is capable of producing a pH difference of more than 8 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 1.0 V or less is applied across the anode and cathode. In some embodiments the invention provides a system that is capable of producing a pH difference of more than 10 pH units between a first electrolyte solution and a second electrolyte solution where the first electrolyte solution contacts an anode and the second electrolyte solution contacts a cathode, and the two electrolyte solutions are separated, e.g., by one or more ion exchange membranes, when a voltage of 1.2V or less is applied across the anode and cathode.

[0041] It will be appreciated that the voltage need not be kept constant and that the voltage applied across the anode and the cathode may be very low, e.g., 0.05V or less, when the two electrolytes are the same pH or close in pH, and that the voltage may be increased as needed as the pH difference increases. In this way, the desired pH difference or production of hydroxide ions may be achieved with the minimum average voltage. Thus in some embodiments described in the previous paragraph, the average voltage may be less than 80%, 70%, 60%, or less than 50% of the voltages given in the previous paragraph for particular embodiments.

[0042] In various embodiments and with reference to FIGS. 1-2, hydrogen gas formed at the cathode (110) is directed to the anode (108). Without being bound to any theory, it is believed that the gas is adsorbed and/or absorbed into the anode and subsequently forms protons at the anode.

[0043] In some embodiments, one or more of the electrolyte solutions is depleted in divalent cations, e.g., in magnesium or calcium, during parts of the process where the electrolyte is in contact with the ion exchange membrane (or membranes, see embodiments described below in which more than one membrane is used). This is done to prevent scaling of the membrane, if necessary for that particular membrane. Thus, in some embodiments the total concentration of divalent cations in the electrolyte solutions when they are in contact with the ion exchange membrane or membranes for any appreciable time is less than 0.06 mol/kg solution, or less than 0.06 mol/kg solution, or less than 0.04 mol/kg solution, or less than 0.02 mol/kg solution, or less than 0.01 mol/kg solution, or less than 0.005 mol/kg solution, or less than 0.001 mol/kg solution, or less than 0.0005 mol/kg solution, or less than 0.0001 mol/kg solution, or less than 0.00005 mol/kg solution.

[0044] In another embodiment as illustrated in FIG. 3, the present system (300) includes an electrolytic cell comprising an anode (108) contacting a first electrolyte (104); an anion exchange membrane (102) separating the first electrolyte

from a third electrolyte (130); a second electrolyte contacting a cathode (110), and a cation exchange membrane (124) separating the second electrolyte from the third electrolyte. As can be appreciated, the ion exchange membranes are positioned in the system to prevent mixing of the first and second electrolytes. A current/voltage regulator (112) is adaptable to increase or decrease the current or voltage across the cathode and anode in the system as desired. On applying a voltage across the anode and cathode, hydroxide ions form in the solution in contact with the cathode without a gas e.g., oxygen or chlorine forming at the anode. As with the system of FIGS. 1 and 2, the system of FIG. 3 is adaptable for batch, semi-batch and continuous operation.

[0045] In system illustrated in FIG. 3, as with the systems of FIGS. 1-2, the first electrolyte (104), second electrolyte (106) and third electrolyte (130) in various embodiments comprise e.g., saltwater including seawater, freshwater, brine, or brackish water or the like. In one embodiment the third electrolyte (130) comprise substantially a solution of a sodium chloride.

[0046] In various embodiments, anion exchange membrane (102) and cation exchange membrane (124) of FIG. 3 are any suitable ion exchange membranes suitable for use in an acidic and/or basic solution at operating temperatures in an aqueous solution in the range from about 0° C. to about 100° C., or higher depending on the pressure in the system such as conventional ion exchange membranes well-known in the art, or any suitable ion exchange membrane. Suitable anion exchange membranes are available from PCA GmbH of Germany, e.g., an anion membrane identified as PCSA-250-250 can be used; similarly, a cation membrane identified as PCSK 250-250 available from PCA GmbH can be used.

[0047] With reference to FIG. 3, in various embodiments, the electrochemical cell includes first electrolyte inlet port (114) adaptable for inputting first electrolyte (104) into the system; second electrolyte inlet port (116) for inputting second electrolyte (106) into the system; and third inlet port (126) for inputting third electrolyte into the system. Additionally, the cell includes first outlet port (118) for draining first electrolyte; second outlet port (120) for draining second electrolyte; and third outlet port (128) for draining third electrolyte. As will be appreciated by one ordinarily skilled, the inlet and outlet ports are adaptable for various flow protocols including batch flow, semi-batch flow, or continuous flow. In alternative embodiments, the system includes a conduit, e.g., a duct (122) for directing gas to the anode; in various embodiments the gas comprises hydrogen formed at the cathode (110).

[0048] With reference to FIG. 3, upon applying a voltage across the cathode (110) and anode (108), hydroxide ions form in the electrolyte in contact with the cathode (110), protons form in the electrolyte in contact with the anode and gas, e.g., chlorine or oxygen does not form at the anode (108). Where third electrolyte (130) comprises sodium chloride, chloride ions migrate into the first electrolyte (104) from the third electrolyte (130) through the anion exchange membrane (102); sodium ions migrate to the second electrolyte (106) from the third electrolyte (130); protons form at the anode (104); and hydrogen gas forms at the cathode (110).

[0049] As can be appreciated by one ordinarily skilled in the art, and with reference to FIG. 3 as hydroxide ions form in the electrolyte in contact with the cathode (110) and enter into the third electrolyte concurrent with migration of sodium ions from the third electrolyte (130) into the second electrolyte (106), an aqueous solution of sodium hydroxide will form in

second electrolyte (106). Depending on the voltage applied across the system and the flow rate of the second electrolyte through the system, the pH of the solution will be adjusted. In one embodiment, when a voltage of about 0.1 V or less, 0.2 V or less, or 0.3V or less, or 0.4V or less, or 0.5V or less, or 0.6V or less, or 0.7V or less, or 0.8V or less, or 0.9V or less, or 01.0V or less, or 01.2V or less, or 01.4V or less, or 1.6V or less, or 01.8V or less, or 2.0V or less, or 02.2V or less is applied across the anode and cathode, the pH of the second electrolyte solution is increased; in another embodiment, when a voltage of 0.01 to 2.5 V, or 0.01V to 2.0V, or 0.1V to 2.0V, or 0.1V to 1.5V, or 0.1 V to 1.0V, or 0.1V to 0.8V, or 0.1V to 0.6V, or 0.1V to 0.4V, or 0.1V to 0.2V, or 0.01V to 1.5V, or 0.01 V to 1.0V, or 0.01V to 0.8V, or 0.01V to 0.6V, or 0.01V to 0.4V, or 0.01V to 0.2V, or 0.01V to 0.1V, e.g., when a voltage of 0.1V to 2.0V is applied across the anode and cathode the pH of the second electrolyte is increased; in yet another embodiment, when a voltage of about 0.1.0 to 1 V is applied across the anode and cathode the pH of the second electrolyte solution increased. Similar results are achievable with voltages of 0.1 to 0.8 V; 0.1 to 0.7 V; 0.1 to 0.6 V; 0.1 to 0.5 V; 0.1 to 0.4 V; and 0.1 to 0.3 V across the electrodes. In one embodiment, a volt of about 0.6 volt or less is applied across the anode and cathode; in another embodiment, a volt of about 0.1 to 0.6 volt or less is applied across the anode and cathode; in yet another embodiment, a voltage of about 0.1 to 1 volt or less is applied across the anode and cathode.

[0050] As will be appreciated and with reference to FIG. 3, in first electrolyte (104) as proton form in the electrolyte in contact with the anode (108) and enter into the solution concurrent with migration of chloride ions from the third electrolyte (130) to the first electrolyte (104), increasingly an acidic solution will form in first electrolyte (104). Depending on the voltage applied across the system and the flow rate of the second electrolyte through the system, the pH of the solution will be adjusted as noted above.

[0051] As with the embodiments of FIGS. 1 and 2 and as is illustrated in FIG. 3, optionally hydrogen gas formed at the cathode (110) is directed to the anode (108). Without being bound to any theory, it is believed that hydrogen gas is adsorbed and/or absorbed into the anode and subsequently forms protons at the anode in contact with the first electrolyte (104). Also, in various embodiments as illustrated in FIGS. 1-3, a gas such as oxygen or chlorine does not form at the anode (108). Accordingly, as can be appreciated, with the formation of protons at the anode and migration of chlorine into the first electrolyte, hydrochloric acid is obtained in the first electrolyte (104).

[0052] With reference to FIG. 4, which illustrates a variation of the embodiment of FIG. 3, a cation exchange membrane is in contact with the anode (108) on one surface, and in contact with the first electrolyte (104) at an opposed surface. In this configuration, as will be appreciated by one ordinarily skilled in the art, H^+ formed at or near the anode will migrate into the first electrolyte through the cation exchange membrane to cause the pH of the first electrolyte to be adjusted as discussed with reference to the system of FIG. 3. Similarly, at the cathode (110), an anion exchange membrane is in contact with the cathode (110) on one surface, and in contact with the second electrolyte (106) at an opposed surface. In this configuration, as will be appreciated by one ordinarily skilled in the art, OH^- formed at or near the anode will migrate into the first electrolyte to cause the pH of the second electrolyte to be adjusted as discussed with reference to the system of FIG. 3.

Optionally, as illustrated in FIG. 4, the hydrogen gas formed at the cathode (110) can be redirected to the anode (108) without contacting the second (106) or first (104) electrolyte.

[0053] FIG. 5 illustrates a variation of the invention where at least two of the systems of FIG. 4 are configured to operate together. As can be appreciated and with reference to FIG. 5, as hydroxide ions form at the cathode (110) and enter into second electrolyte (106) and with the migration of sodium ions into the second electrolyte from the third electrolyte (130), an aqueous solution of sodium hydroxide will form in second electrolyte (106). Depending on the rate of addition and/or removal of electrolytes from the system, the pH of the second electrolyte is adjusted, e.g., increases, decreases or does not change. Also with reference to FIG. 5, in first electrolyte (104) as proton form at the anode (108) and enter into the solution concurrent with migration of chloride ions from the third electrolyte (130) to the first electrolyte (104), increasingly an acidic solution will form in first electrolyte (104).

[0054] FIG. 6 illustrates a variation of the system of FIG. 3 arranged for continuous or semi-continuous flow. With reference to FIG. 6, upon applying a low voltage across the cathode (110) and anode (108), hydroxide ions form at the cathode (110), protons form at the anode and gas, e.g., chlorine or oxygen does not form at the anode (108). Where third electrolyte (130) comprises sodium chloride, chloride ions migrate into the first electrolyte (104) from the third electrolyte (130) through the anion exchange membrane (102); sodium ions migrate to the second electrolyte (106) from the third electrolyte (130) through the cation exchange membrane (124); protons form at the anode (104); and hydrogen gas forms at the cathode (110). In first electrolyte (104) as proton form at the anode (108) and enter into the solution concurrent with migration of chloride ions from the third electrolyte (130) to the first electrolyte (104), increasingly an acidic solution will form in first electrolyte (104). Depending on the voltage applied across the system and the flow rate of the second electrolyte through the system, the pH of the solution will be adjusted.

[0055] With reference to FIGS. 1, 2 and 7 the present method in one embodiment (700) comprises a step (702) of migrating ions across an ion exchange membrane (102) that is situated between a first electrolyte (104) and a second electrolyte (106), the first electrolyte contacting an anode (108) and the second electrolyte contacting a cathode (110), by applying a voltage across the anode and cathode to form hydroxide ions at the cathode without forming a gas at the anode. As described with reference to FIGS. 1-2, as hydroxide ions form at the anode (110) and enter in to the second electrolyte (106) concurrent with migration of chloride ions from the second electrolyte, an aqueous solution of sodium hydroxide will form in second electrolyte (106). Consequently, depending on the voltage applied across the system and the flow rate of the second electrolyte (106) through the system, the pH of the second electrolyte is adjusted. Also, with the formation of protons in the first electrolyte, an acid solution will form in the first electrolyte as a result of migration of chloride ions into the first electrolyte as discussed with reference to the system of FIGS. 1 and 2.

[0056] In one embodiment, when a volt of about 0.6 volt or less is applied across the anode and cathode, the pH of the second electrolyte solution increased; in another embodiment, when a volt of about 0.1 to 0.6 volt or less is applied across the anode and cathode the pH of the second electrolyte

increased; in yet another embodiment, when a voltage of about 0.1 to 1 volt or less is applied across the anode and cathode the pH of the second electrolyte solution increased. Other exemplary results achieved in accordance with the present system are summarized in Table 1.

[0057] With reference to FIGS. 3-6 and 8, in one embodiment the present method (800) comprises a step (802) of applying a voltage across an anode (108) and cathode (110), wherein: (i) the anode is in contact with a first electrolyte (104) that is also in contact with an anion exchange membrane (102); (ii) the cathode is in contact with a second electrolyte (106) that is also in contact with a cation exchange membrane; and

(iii) a third electrolyte (130) is situated between the anion exchange membrane and the cation exchange membrane to form hydroxide ions at the cathode without forming a gas at the anode. As described with reference to the system of FIGS. 3-6 above, as hydroxide ions from the cathode (110) and enter in to the second electrolyte (106) concurrent with migration of sodium ions into the second electrolyte from the third electrolyte, an aqueous solution of sodium hydroxide will form in second electrolyte (106). Consequently, depending on the voltage applied across the system and the flow rate of the second electrolyte (106) through the system, the pH of the second electrolyte is adjusted. Also, with the formation of protons in the first electrolyte and the migration of chloride ions into the first electrolyte from the third electrolyte, an acid solution will form in the first electrolyte.

[0058] In all embodiments described herein, optionally, CO₂ is dissolved into the second electrolyte solution; as protons are removed from the second electrolyte solution more CO₂ may be dissolved in the form of bicarbonate and/or carbonate ions; depending on the pH of the second electrolyte the balance is shifted toward bicarbonate or toward carbonate, as is well understood in the art. In these embodiments the pH of the second electrolyte solution may decrease, remain the same, or increase, depending on the rate of removal of protons compared to rate of introduction of CO₂. It will be appreciated that no hydroxide need form in these embodiments, or that hydroxide may not form during one period but form during another period. Optionally, another electrochemical system as described herein may be used to produce concentrated hydroxide, which, when added to the second electrolyte containing the dissolved CO₂, causes the formation of a precipitate of carbonate and/or bicarbonate compounds such as calcium carbonate or magnesium carbonate and/or their bicarbonates. In some embodiments, divalent cations such as magnesium and/or calcium are present in certain solutions used in the process, and/or are added. The precipitated carbonate compound can be used as cements and building material as described in United States patent applications incorporated herein by reference.

[0059] In an optional step, the acidified first electrolyte solution 104 is utilized to dissolve a calcium and/or magnesium rich mineral, such as mafic mineral including serpentine or olivine, for precipitating carbonates and bicarbonates as described above. For example, the acidified stream can be employed to dissolve calcium and/or magnesium rich minerals such as serpentine and olivine to create the electrolyte solution that can be charged with bicarbonate ions and then made sufficiently basic to precipitate carbonate compounds. Such precipitation reactions and the use of the precipitates in cements are described in the United States patent applications incorporated by herein by reference.

[0060] In alternative embodiments, rather than precipitating carbonates, the carbonate and bicarbonate solution is disposed of in a location where it will be stable for extended periods of time. For example, the carbonate/bicarbonate electrolyte solution can be pumped to an ocean depth where the temperature and pressure are sufficient to keep the solution stable over at least the time periods set forth above.

[0061] Although the foregoing invention has been described in some detail by way of illustration and example for purposes of clarity of understanding, it is readily apparent to those of ordinary skill in the art in light of the teachings of this invention that certain changes and modifications may be made thereto without departing from the spirit or scope of the appended claims.

[0062] Accordingly, the preceding merely illustrates the principles of the invention. It will be appreciated that those skilled in the art will be able to devise various arrangements, which, although not explicitly described or shown herein, embody the principles of the invention, and are included within its spirit and scope. Furthermore, all examples and conditional language recited herein are principally intended to aid the reader in understanding the principles of the invention and the concepts contributed by the inventors to furthering the art, and are to be construed as being without limitation to such specifically recited examples and conditions. Moreover, all statements herein reciting principles, aspects, and embodiments of the invention as well as specific examples thereof, are intended to encompass both structural and functional equivalents thereof. Additionally, it is intended that such equivalents include both currently known equivalents and equivalents developed in the future, i.e., any elements developed that perform the same function, regardless of structure. The scope of the present invention, therefore, is not intended to be limited to the exemplary embodiments shown and described herein. Rather, the scope and spirit of present invention is embodied by the appended claims.

1.-20. (canceled)

21. A carbonate precipitating system comprising:

an electrochemical system comprising an anion exchange membrane separating an anode electrolyte that is in contact with an anode from an intermediate electrolyte; and a cation exchange membrane separating a cathode electrolyte that is in contact with a cathode from the intermediate electrolyte; wherein the cathode is configured to produce a hydroxide in the cathode electrolyte on application of a voltage across the anode and cathode; and wherein

the electrochemical system is operably connected to a reactor configured to mix the cathode electrolyte and a source of waste gas mixed to produce a precipitate comprising a hydroxide and/or a carbonate and/or a bicarbonate.

22. The carbonate precipitating system of claim 21, wherein the reactor is configured to mix the cathode electrolyte and the waste gas with a salt water.

23. The carbonate precipitating system of claim 22, wherein the source of waste gas comprises carbon dioxide from a cement production process, a power generating facility, or a carbon combustion process.

24. The precipitating system of claim 23, wherein the voltage is less than 2.8 V.

25. The carbonate precipitating system of claim 24, wherein the salt water comprises divalent cations.

26. The carbonate precipitating system of claim **25**, wherein the precipitate comprises calcium an/or magnesium.

27. The carbonate precipitating system of claim **26**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to absorb hydrogen gas and produce protons without producing a gas.

28. The carbonate precipitating system of claim **26**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode electrolyte is configured to produce a gas.

29. The carbonate precipitating system of claim **28**, wherein the anode electrolyte comprises hydrochloric acid and the cathode electrolyte comprises sodium hydroxide and/or sodium carbonate and/or sodium bicarbonate.

30. The carbonate precipitating system of claim **29**, comprising a third electrolyte separated from the cathode electrolyte and the anode electrolyte by one or more ion exchange membranes.

31. The carbonate precipitating system of claim **30**, configured to migrate anions from the third electrolyte through an anion exchange membrane into the anode electrolyte, and migrate cations through a cation exchange membrane into the cathode electrolyte.

32. A CO₂ sequestration system comprising:

an electrochemical system comprising an anode contacting an anode electrolyte and a cathode contacting a cathode electrolyte, wherein the cathode is configured to produce a hydroxide in the cathode electrolyte with a voltage applied across the anode and cathode; and

a source of industrial waste gas, wherein the source of waste gas comprises a cement production process that emits carbon dioxide, and wherein the electrochemical system and the source of waste gas are operably integrated such that carbon dioxide from the source of waste gas is absorbed into the cathode electrolyte.

33. The CO₂ sequestration system of claim **32**, wherein the source of waste gas comprises a power generating facility or a carbon combustion process.

34. The CO₂ sequestration system of claim **33**, wherein the cathode electrolyte comprises bicarbonates and/or carbonates.

35. The CO₂ sequestration system of claim **34**, wherein the carbonates and/or bicarbonates comprise calcium and/or magnesium.

36. The CO₂ sequestration system of claim **35**, wherein the voltage is less than 2.8 V.

37. The CO₂ sequestration system of claim **36**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to absorb hydrogen gas and produce protons without producing a gas.

38. The CO₂ sequestration system of claim **37**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode electrolyte is configured to produce a gas.

39. The CO₂ sequestration system of claim **37**, wherein the anode electrolyte comprises hydrochloric acid and the cathode electrolyte comprises sodium hydroxide and/or sodium carbonate and/or sodium bicarbonate.

40. The CO₂ sequestration system of claim **39**, comprising a third electrolyte separated from the cathode electrolyte and the anode electrolyte by one or more ion exchange membranes.

41. A method comprising:

producing hydroxide ions in a cathode electrolyte by applying a voltage across a cathode in contact with the cathode electrolyte and an anode in contact with an anode electrolyte; and

mixing the cathode electrolyte with an industrial waste gas such that carbon dioxide in the waste gas is absorbed into the cathode electrolyte.

42. The method of claim **41**, wherein the source of waste gas comprises a cement production process, a power generation facility or a carbon combustion process.

43. The method of claim **42**, wherein the carbon dioxide is derived from calcining limestone.

44. The method of claim **43**, comprising producing bicarbonates and/or carbonates in the cathode electrolyte.

45. The method of claim **44**, wherein the carbonates and/or bicarbonates comprises calcium and/or magnesium.

46. The method of claim **45**, wherein the voltage is less than 2.8 V.

47. The method of claim **46**, comprising producing hydroxide ions and hydrogen gas at the cathode, and absorbing hydrogen gas at the anode and producing protons without producing a gas at the anode.

48. The method of claim **47**, comprising producing hydroxide ions and hydrogen gas at the cathode, and a gas at the anode.

49. A system comprising:

an electrochemical system configured with an anode contacting an anode electrolyte a cathode contacting a cathode electrolyte to produce hydroxide ions in the cathode electrolyte with a voltage applied across the anode and cathode; and

an absorber operably integrated with the electrochemical system and configured to sequester carbon dioxide from a waste gas by mixing the cathode electrolyte with the waste gas and a salt water.

50. The system of claim **49**, wherein the salt water comprises a brine, seawater or brackish water.

51. The system of claim **50**, wherein the salt water comprises divalent cations.

52. The system of claim **51**, wherein the waste gas comprises waste gases of a cement production process, a power generating facility, or a carbon combustion process.

53. The system of claim **53**, wherein the cathode electrolyte comprises a hydroxide and/or a bicarbonate and/or a carbonate.

54. The system of claim **54**, wherein the carbonate and/or bicarbonate comprise calcium and/or magnesium.

55. The system of claim **55**, wherein the voltage is less than 2.8 V.

56. The system of claim **55**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to absorb hydrogen gas and produce protons without producing a gas.

57. The system of claim **55**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to produce a gas.

58. The system of claim **56**, wherein the anode electrolyte comprises hydrochloric acid and the cathode electrolyte comprises sodium hydroxide and/or sodium carbonate and/or sodium bicarbonate.

59. The system of claim **58**, comprising a third electrolyte separated from the cathode electrolyte and anode electrolyte by one or more ion exchange membranes.

- 60.** A method comprising:
 configuring an electrochemical system to produce a hydroxide in a cathode electrolyte by contacting an anode with an anode electrolyte and a cathode with a cathode electrolyte and applying a voltage across the anode and cathode; and
 sequestering carbon dioxide from a waste gas by mixing the cathode electrolyte with a salt water and the waste gas.
- 61.** The method of claim **60**, wherein the salt water comprises a brine, seawater or brackish water.
- 62.** The method of claim **61**, wherein the salt water comprises divalent cations.
- 63.** The method of claim **62**, wherein the waste gas comprises waste gases from a cement production process, a power generating facility, or a carbon combustion process.
- 64.** The method of claim **63**, comprising producing a hydroxide and/or a bicarbonate and/or a carbonate in the cathode electrolyte.
- 65.** The method of claim **64**, wherein the carbonates and/or bicarbonates comprises calcium and/or magnesium.
- 66.** The method of claim **65**, wherein the voltage is less than 2.8 V.
- 67.** The method of claim **66**, comprising producing hydroxide ions and hydrogen gas at the cathode, and absorbing hydrogen gas at the anode and producing protons without producing a gas at the anode.
- 68.** The method of claim **66**, comprising producing hydroxide ions and hydrogen gas at the cathode, and a gas at the anode.
- 69.** An integrated system comprising:
 an electrochemical system comprising an anode contacting an anode electrolyte and a cathode contacting a cathode electrolyte, and configured to produce hydroxide ions in the cathode electrolyte and an acid in the anode electrolyte with an applied voltage across the anode and cathode; and
 a mineral-dissolution system operably integrated with the anode electrolyte and configured to produce cations by dissolving a mineral with the acid.
- 70.** The integrated system of claim **69**, wherein the acid comprises hydrochloric acid.
- 71.** The integrated system of claim **70**, wherein the mineral comprises a mafic mineral.
- 72.** The integrated system of claim **71**, wherein the cations comprise calcium ions and/or magnesium ions.
- 73.** The integrated system of claim **72**, wherein the voltage is less than 2.8 V.
- 74.** The integrated system of claim **73**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to absorb hydrogen gas and produce protons without producing a gas.
- 75.** The integrated system of claim **73**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas and the anode electrolyte is configured to produce a gas.
- 76.** A method comprising:
 producing hydroxide ions in a cathode electrolyte in contact with a cathode and an acid in an anode electrolyte in contact with an anode with an applied voltage across the anode and cathode; and
 produce cations by dissolving a mineral with the acid in a mineral-dissolution system.
- 77.** The method of claim **76**, wherein the acid comprises hydrochloric acid.
- 78.** The method of claim **77**, wherein the mineral comprises a mafic mineral.
- 79.** The method of claim **78**, wherein the cations comprise calcium ions and/or magnesium ions.
- 80.** The method of claim **79**, wherein the voltage is less than 2.8 V.
- 81.** The method of claim **80**, comprising producing hydroxide ions and hydrogen gas at the cathode, and absorbing absorb hydrogen gas at the anode and produce protons without producing a gas.
- 82.** The method of claim **80**, comprising producing hydroxide ions and hydrogen gas at the cathode and a gas at the anode.
- 83.** A precipitating system comprising:
 an electrochemical system comprising an anode contacting an anode electrolyte, a cathode contacting a cathode electrolyte and configured to produce hydroxide ions in the cathode electrolyte and an acid in the anode electrolyte with an applied voltage across the anode and cathode; wherein
 the electrochemical system is operable connected to a precipitator that is configured to produce a cementitious composition by mixing the cathode electrolyte with a salt solution and a waste gas comprising carbon dioxide.
- 84.** The precipitating system of claim **83**, wherein the cementitious composition comprises a carbonate and/or a bicarbonate.
- 85.** The precipitating system of claim **84**, wherein the cementitious composition comprises calcium and/or magnesium.
- 86.** The precipitating system of claim **85**, wherein the cathode electrolyte comprises carbonate ions and/or bicarbonate ions.
- 87.** The precipitating system of claim **86**, wherein the source of the waste gas comprises a cement production process, a power generating facility, or a carbon combustion process.
- 88.** The precipitating system of claim **87**, wherein the voltage is less than 2.8 V.
- 89.** The precipitating system of claim **88**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas, and the anode is configured to absorb hydrogen gas and produce protons without producing a gas.
- 90.** The precipitating system of claim **88**, wherein the cathode is configured to produced hydroxide ions and hydrogen gas and the anode configured to produce a gas.
- 91.** The precipitating system of claim **90**, wherein the anode electrolyte comprises hydrochloric acid and the cathode electrolyte comprises sodium hydroxide and/or sodium carbonate and/or sodium bicarbonate.
- 92.** The precipitating system of claim **91**, comprising a third electrolyte separated from the cathode electrolyte and the anode electrolyte by one or more ion exchange membranes.
- 93.** A method comprising:
 configuring an electrochemical system with an anode contacting an anode electrolyte and a cathode contacting a cathode electrolyte, to produce hydroxide ions in the cathode electrolyte with an applied voltage across the anode and cathode; and
 producing a cementitious composition by mixing the cathode electrolyte with a salt solution and a waste gas comprising carbon dioxide in a precipitator operably connected to the cathode electrolyte.

94. The method of claim **93**, wherein the cathode electrolyte comprises carbonate ions and/or bicarbonate ions.

95. The method of claim **94**, wherein the cementitious composition comprises a carbonate and/or a bicarbonate.

96. The method of claim **95**, wherein the cementitious composition comprises calcium and/or magnesium.

97. The method of claim **96**, wherein the source of the waste gas comprises a cement production process, a power generating facility, or a carbon combustion process.

98. The method of claim **97**, wherein the voltage is less than 2.8 V.

99. The method of claim **98**, comprising producing hydroxide ions and hydrogen gas at the cathode, and absorbing hydrogen gas and producing protons at the anode without producing a gas at the anode.

100. The method of claim **99**, comprising producing hydroxide ions and hydrogen gas at the cathode and a gas at the anode.

101. A system comprising an industrial plant and an electrochemical system configured to absorb a waste gas generated by the industrial plant into a cathode electrolyte of the electrochemical system.

102. The system of claim **101**, wherein the industrial plant comprises a power generating plant, a cement producing plant or an ore smelting plant.

103. The system of claim **102**, wherein the waste gas comprises carbon dioxide and combustion gases and wherein the electrochemical system is configured to produce an alkaline solution in the cathode electrolyte without generating a gas at an anode in the electrochemical system.

104. The system of claim **103**, wherein the alkaline solution comprises a hydroxide and/or a bicarbonate and/or a carbonate.

105. The system of claim **104**, wherein the hydroxide and/or a bicarbonate and/or a carbonate comprises calcium and/or magnesium.

106. The system of claim **105**, wherein the electrochemical system is configured to produce hydrogen gas at the cathode and consume hydrogen gas at the anode and produce protons in an anode electrolyte in contact with the anode.

107. The system of claim **106**, wherein the alkaline solution is produced with a voltage of less than 2.8 V across the anode and cathode.

108. The system of claim **107**, further comprising a gas absorber operably connected to the electrochemical system and configured to precipitate a carbonate and/or a bicarbonate by mixing the cathode electrolyte and the waste gas.

109. The system of claim **108**, further comprising a mineral-dissolution system operably connected to the electrochemical system and configured to dissolve a material comprising divalent cations with the anode electrolyte.

110. A method comprising:

absorbing a waste gas from an industrial plant into a cathode electrolyte in an electrochemical system and producing a hydroxide and/or a bicarbonate and/or a carbonate in the cathode electrolyte.

111. The method of claim **110**, wherein the industrial plant comprises a power generating plant, a cement producing plant or an ore smelting plant.

112. The method of claim **111**, wherein the hydroxide and/or a bicarbonate and/or a carbonate comprises calcium and/or magnesium.

113. The method of claim **112**, wherein the hydroxide and/or a bicarbonate and/or a carbonate comprises calcium and/or magnesium.

114. The method of claim **113**, wherein the waste gas comprises carbon dioxide and combustion gases.

115. The method of claim **114**, comprising producing hydrogen gas and hydroxide ions at the cathode and consuming a hydrogen and producing protons at the anode without producing a gas at the anode of the electrochemical system by applying a voltage across the cathode and anode.

116. The method of claim **115**, comprising directing hydrogen gas produced at the cathode to the anode.

117. The method of claim **116**, wherein the voltage is less than 2.8 V.

118. The method of claim **117**, comprising producing an acid in the anode electrolyte in contact with the anode and producing a divalent cation solution by dissolving a material with the acid.

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