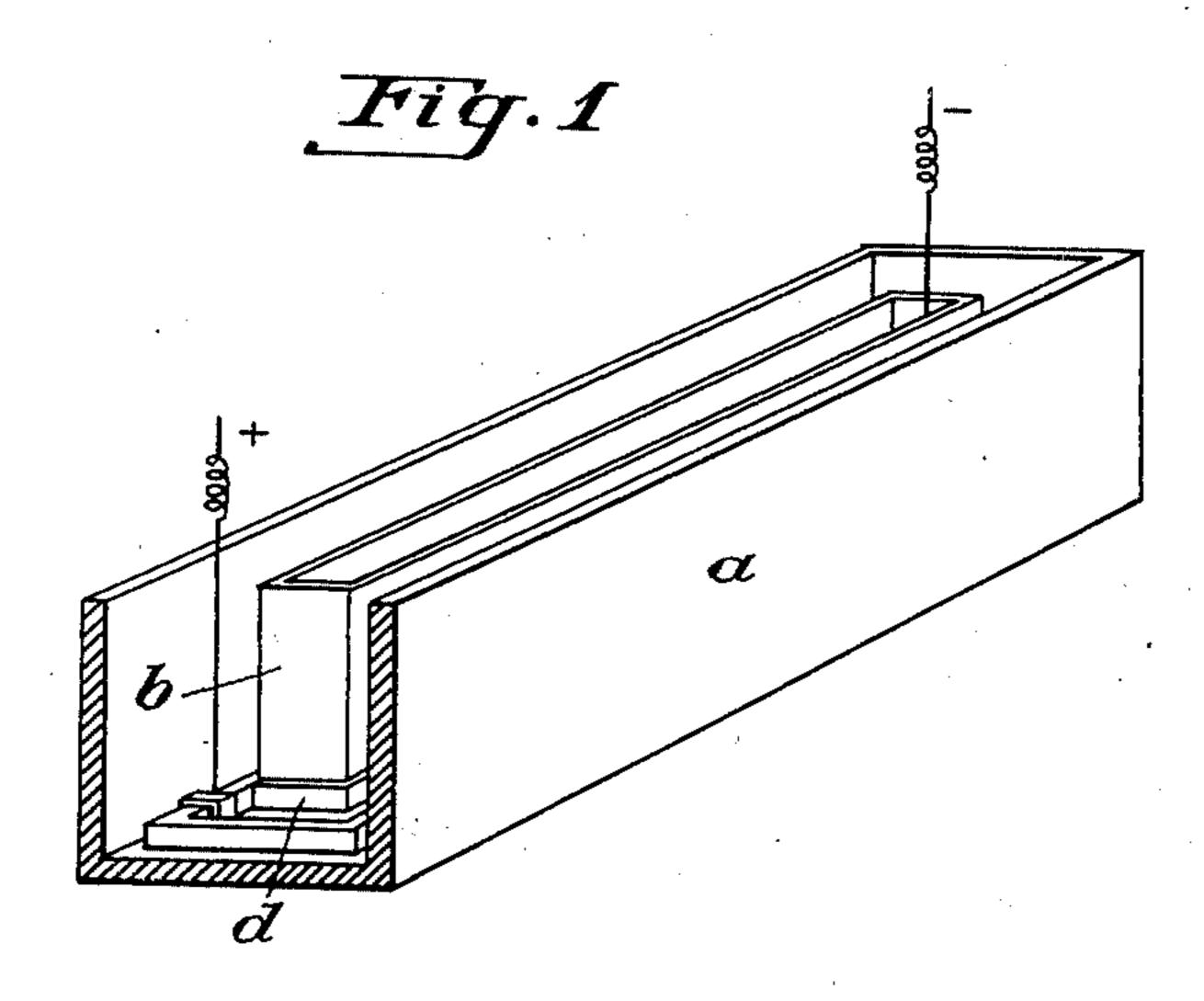
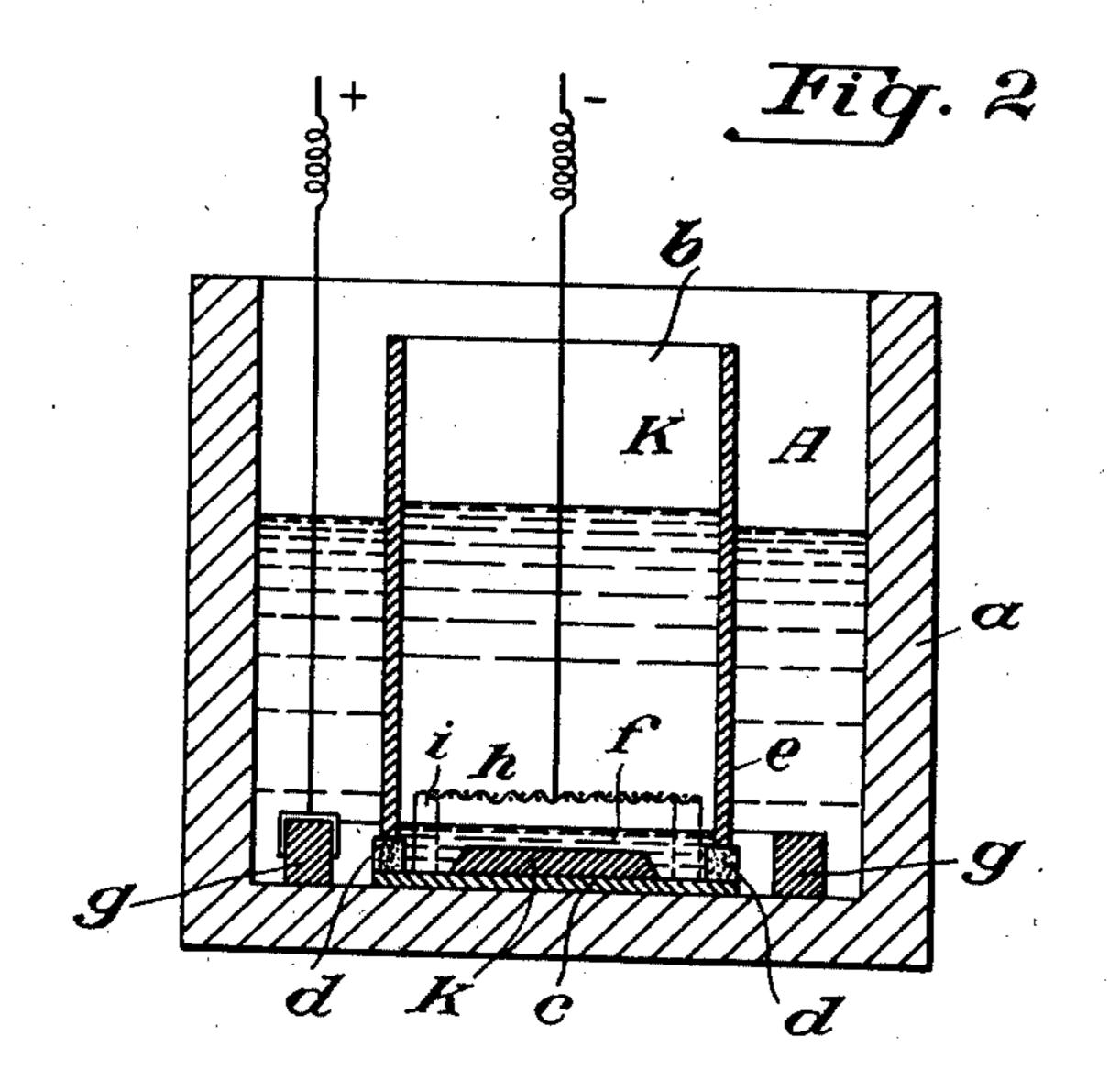
ELECTROLYTIC CELL OF THE MERCURY TYPE
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Inventors:
Victor Engelhardt
and Nicolaus Schönfeldt

by their Attorney

UNITED STATES PATENT OFFICE

VICTOR ENGELHARDT AND NIKOLAUS SCHÖNFELDT, OF BERLIN-CHARLOTTENBURG, GERMANY, ASSIGNORS TO SIEMENS & HALSKE, AKTIENGESELLSCHAFT, OF SIEMENSSTADT NEAR BERLIN, GERMANY, A CORPORATION OF GERMANY

ELECTROLYTIC CELL OF THE MERCURY TYPE

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Our invention relates to electrolytic cells, and more particularly electrolytic cells for the electrolysis of alkali or alkaline earth metal halides by the mercury process.

The hitherto employed electrolytic cells for the electrolysis of alkaline metal halides according to the mercury process require generally considerable quantities of mercury or constant supervision and attendance.

The object of our invention is to provide a cell in which these drawbacks are effectively eliminated. Our improved cell requires only a very small quantity of mercury and no constant supervision and thus ensures a 15 particularly high economy. We attain this end in view by designing only a portion of the vertical partition dividing the anode series of the elements and 2 the reciprocal compartment from the cathode compartment value of the overpotential of the metal. adjacent to the bottom of the electrolyser as 20 a porous diaphragm. The preferably rigid deliberations it has been found advan- 70 diaphragm need only be very low, for instance a few millimetres high. The diaphragm which at the same time serves as a 25 meable portion of the partition is advan- than its speed of formation. In this way 75 tageously designed as a closed circular ring, we attain the result that an oxidation of the or as polygon and the mercury is arranged mercury is rendered entirely impossible in 30 located at the outside of the diaphragm. art processes. The height of the mercury is chosen slightly — In carrying out our improved process the higher than the height of the diaphragm. metal selected in accordance with the re-The anode is preferably also slightly higher than the diaphragm. The mercury itself or 35 a special metal body located above the mercury may be employed as cathode. This special cathode may also be electrically con-

40 a high degree upon the choice of the metal respective plant, a corresponding metal coat-90 used in its manufacture. It has already ing is electrolytically deposited, for instance been suggested to accelerate the decomposi- a coating of cadmium with or without applition of the amalgam by employing specially cation of one or more intermediate layers. selected substances, such as vanadium, In the drawing affixed to our specificamolybdenum or tungsten, as well as high- tion and forming part thereof one embodi
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variably used such metals or alloys which accelerated the decomposition of the amalgam as much as possible. This has the advanting. 1, tage, it is true, that such processes could in tion, and

themselves be carried through continuously with comparatively small quantities of mercury, but in practice the serious drawback arises that, in consequence of the strong action of the metal employed, an oxidation 55 of the mercury is liable to occur and thus cause a considerable disturbance of the process.

The object of our invention is to eliminate this drawback and thus to render the process much more reliable. Numerous experiments and thorough researches have shown that the speed of decomposition of the amalgam can be considered as a function of two values, viz. 1 the distance of the respective 65 metal from the mercury in the electromotive

On the basis of these experiments and tageous to employ such a metal connected to the negative pole of the source of current that the speed of decomposition of the amalsupport for the considerably larger imper- gam is equal to or better still a little less on the inside of the ring or polygon. The our improved process and that the operation anode, which may be of similar shape, is is rendered much more reliable than in prior

quired output of the plant can be connected to the mercury cathode through a suitable resistance. The metal is, for instance, em- 85 ployed in the form of wire netting supported upon feet of graphite. The wire netting or nected to the mercury. The satisfactory gauze may preferably consist of iron wire operation of the improved cell depends to upon which, according to the output of the

resistance alloys. These known processes in- ment of our invention, an electrolytic cell, is illustrated by way of example.

In the drawing shows:

Fig. 1, a perspective view, partly in sec-

Fig. 2, a cross-section through our improved cell.

Like parts are indicated by like letters of reference in both figures of the drawing.

Referring to the drawing a is an oblong, rectangular tank, vat or the like constructed of concrete, slate, impregnated wood or any other suitable material, into which is placed a likewise rectangular smaller vessel 10 b. The vessel b serves as a cathode comably constructed of a single material, the 15 vessel b is composed or built up of a plurality of different parts. On a bottom plate o is placed the diaphragm d of only a few millimetres height which in its turn carries or supports the considerably higher imper-20 meable partition e. The said three parts c, d and e are preferably combined into a single structure. At the inner side of the diaphragm d there is arranged a quantity of mercury f and at the outer side of the claims. 25 diaphragm there is located the anode g. The anode g are slightly greater than that of the diaphragm d. In the example illustrated a framework h the feet i which consist of 30 graphite, for example, rest upon the bottom 35 by placing a cathode secured in position ment covering the entire porous portion of 100 ment A there is introduced in the usual 40 manner the solution of the alkali halide and into the cathode compartment K preferably

In order to obtain a decomposition speed adapted to the output of the plant for the 45 amalgams forming cathodically, by paying attention to the above considerations, a suitable metal may be chosen, for example, cadmium.

pure water.

Preferably a coating of cadmium is elec-50 trolytically deposited upon a netting of iron wire. The thus prepared wire gauze h is provided with feet of graphite i and placed on the bottom of the receptacle b. The graphite members g then serve simultaneous-55 ly as leads to the mercury cathode d.

If desired the rate of decomposition of the amalgam which occurs when employing a certain metal may be controlled by varying the resistance located between the metal 60 gauze h and the mercury cathode f, in the example illustrated the resistance of the rods of graphite i. This may, for instance, be effected by impregnating or coating the rods of graphite i with a liquid insulating agent, 65 such as a suitable varnish. The resistance

may also be omitted altogether so that the mercury is then in bipolar connection.

As diaphragms porous plates of sufficient strength to resist chemical actions are used, for instance plates of chromic oxide, alu- 70 minum oxide, infusorial earth (Kieselguhr), vulcanite and the like.

It is also possible to arrange displacement bodies k in the mercury whereby a further substantial saving in mercury can be 75 partment while the remaining space in the effected. For this purpose the bottom of the electrolyser a is utilized as anode compart- vessel b may be provided with suitable proment. Unlike the tank a, which is prefer-jections, for instance. The mercury may then be arranged in the shape of a ring, for example. As numerous tests extending over 80 a long time have shown our improved cell works very economically and entirely free from any objections although only a very small quantity of mercury is required.

It will be understood that structural 85 modifications and changes may be made without departing from the spirit of our invention and the scope of the appended

We claim as our invention:

heights of the quantity of mercury f and the 1. In an electrolytic cell for the electrolysis of alkalis or alkaline-earths of the halogens according to the mercury process, in combination, an anode compartment, a cathode compartment, a partition dividing said 95 c of the inner vessel b and this dip into the anode compartment from said cathode commercury f, serving as leads for the supply of partment only the portion of which adjacurrent to the mercury cathode. A bipolar cent to the bottom of the electrolyser is connection to the mercury f may be effected porous, mercury within the cathode compartmerely by a suspension or by resting upon said partition, and a cathode located above non-conducting blocks at some distance the mercury, which is electrically connected above the mercury. Into the anode compart- to the mercury through high-ohmic resistances.

> 2. In a cell for the electrolytic decom- 105 position of alkaline metal halides, a containing vessel forming an anode compartment, an interior cathode compartment resting on the bottom of said containing vessel, the walls of said cathode compartment being 110 impermeable for the greater part of their height but having a narrow, porous, horizontal section adjacent the said bottom of said containing vessel.

> 3. The electrolyte cell of claim 2 in which 115 the porous, horizontal section of the cathode compartment is annular and has a height of the order of a few millimeters.

> 4. The electrolytic cell of claim 2 in which the cathode compartment is filled with mer- 120 cury to a height just above the said porous, horizontal section.

> 5. The electrolytic cell of claim 2 in which the anode rests on the bottom of said containing vessel, the said anode extending to 125 a height somewhat above that of the said porous, horizontal section of said cathode compartment.

> 6. In a cell for the electrolytic decomposition of alkaline metal halides, a cathode 130

compartment containing a shallow layer of mercury amalgam and a metal cathode, the said amalgam and the said cathode being electrically connected by a resistance element whose resistance is capable of being varied, whereby the rate of decomposition of the amalgam may be controlled.

7. The electrolytic cell of claim 2 wherein the cathode compartment contains a shal-10 low layer of mercury and displacement members in the bottom of said compartment of size sufficient to effect a substantial sav-

ing in mercury.

8. The structure of claim 2 in which a 15 cathode is employed in said cathode compartment, said cathode being free from metallic connection with the amalgam in the

cathode compartment.

9. In a cell for the electrolytic decompo-20 sition of alkaline metal halides by formation and subsequent decomposition of an alkaline metal amalgam, a cathode comprising a wire

gauze coated with cadmium.

10. In a cell for the electrolytic decompo-25 sition of alkaline metal halides by the formation and subsequent decomposition of an alkaline metal amalgam, a cathode having a composition comprising cadmium.

In testimony whereof we affix our sig-

30 natures.

VICTOR ENGELHARDT. NIKOLAUS SCHÖNFELDT.