UNITED STATES PATENT OFFICE

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PROCESS OF PRODUCING TETRA ALKYL LEAD

No Drawing.

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This invention relates to the manufacture of tetra alkyl lead and more particularly to an improvement in the process of producing

tetra ethyl lead.

Several methods have been known for the recovery of tetra ethyl lead from the metallic lead sludges always present after its formaconsisted principally of low temperature, taken as limitations thereof. high vacuum distillation, steam distillation, Example I.—A mixture of tetra ethyl lead tures not much above 125° C.

ticular object of our invention is to increase ployed. the yield of tetra alkyl lead. A further object of our invention is an improvement in these may be lower than 200° C. and even as the distillation of tetra alkyl lead from the high as 400° C. 35 sludges present. Other objects will appear hereinafter.

high temperature steam, and particularly ten parts of water. The tetra ethyl lead and steam superheated to temperatures between 200° C. and 300° C., is employed in the step of distillation, instead of the ordinary saturated steam, and that tetra alkyl lead may

dropped into a still which is previously heated and maintained at a temperature approximately 200 to 300° C. Operating the process in this way results in a mixture of tetra alkyl lead and water flash-distilling out of the 55 still.

The following examples illustrate pretion by the reaction of ethyl halides with the ferred embodiments of our invention, but it sodium alloys of lead. These methods have is to be understood that these are not to be

and extraction with organic solvents. The and lead sludge such as is obtained by the latter, however, is objectionable because the interaction between lead mono-sodium alloy removal of the solvents is necessary, and this and ethyl chloride is mixed with approxiis difficult and expensive. Also, vacuum dis- mately 10 times its weight of water. This 65 tillation presents many difficulties and dan- mixture is then brought to a boil by the apgers. When steam distillation is employed plication of external heat by the use of a it has been the practice to use low-pressure steam jacket for large scale operation or on saturated steam, the temperature of which a small scale, by direct gas flame. When is approximately not above 110-115° C. the mixture is boiling the external heat is re- 70 The literature on this subject discloses that moved and steam, superheated to 200-300° tetra ethyl lead will decompose at tempera- C. is introduced through orifices in the bottom of the still. Distillation by this proce-An object of our invention is to overcome dure is generally complete in two to three the difficulties heretofore experienced in the hours. The tetra ethyl lead is recovered 75 recovery of tetra ethyl lead from the metallic from the water fraction of the distillate in sludges inherently present in such processes. the usual manner and the yield obtained will A further object of our invention is to im- be approximately between three per cent and prove generally on the process of manufac- four per cent higher than it would have been turing tetra alkyl lead compounds. A par- had ordinary saturated steam been em- 80

While we prefer the temperatures specified,

Example II.—An iron still is provided 85 with an oil bath or other baths capable of These objects are accomplished by the fol-being raised to 300° C. The temperature of lowing invention in which we have found the bath is elevated until the internal temthat tetra alkyl lead and particularly tetra perature of the still reaches approximately ethyl lead, can be distilled from the sludges 275° C. There is then run into the still at 90 formed in the process of manufacture, with such a rate that the temperature does not an increased completeness of removal as is fall below 200° C. a mixture of one part of indicated by increases in yield, provided that lead sludge containing tetra ethyl lead and water immediately flash off the lead sludge 95 and are recovered in the usual fashion. The tetra ethyl lead is separated from the water fraction in the normal manner and the yield also be recovered without decomposition if will be found to be from three per cent to a mixture of the sludge and water is slowly four per cent higher than could have been obwith ordinary saturated steam.

Similar improved results may be obtained by flash-distilling in like manner other tetra 5 alkyl lead compounds such as tetra methyl

lead and tetra butyl lead, etc.

As many apparently widely different embodiments of this invention may be made without departing from the spirit thereof, 10 it is to be understood that we do not limit ourselves to the foregoing examples or descriptions except as indicated in the following patent claims.

We claim:

1. In the process of producing tetra alkyl lead by the interaction of alkyl halides and a lead sodium alloy, the step of removing the tetra alkyl lead from the metallic lead sludge present which comprises steam distilling the 20 mixture with superhoated steam heated to a temperature of from about 200° C. to about 400° C.

2. In the process of recovering tetra alkyl lead from metallic lead sludge which com-25 prises contacting the mixture with superheated steam at a temperature of between

200° C. and 300° C.

3. In the process of recovering tetra ethyl lead from metallic lead sludge which comprises steam distilling the mixture with superheated steam at a temperature of between 200° C. and 300° C.

4. In the process of recovering tetra alkyl lead from metallic lead sludge which comprises flash-distilling the mixture at a temperature of from about 200° C. to about

400° C.

5. In the process of recovering tetra ethyl lead from metallic lead sludge which comprises flash-distilling the mixture at a temperature of from about 200° C. to about 400° C.

6. The process of recovering tetra alkyl lead from metallic lead sludge which comprises mixing the sludge with water, raising the temperature of a still to from 200° C. to 300° C. and gradually introducing the mixture of the sludge and water into the heated still while maintaining the still at such tem-

peratures.

7. The process of recovering tetra ethyl lead from metallic lead sludge which comprises mixing the sludge with water, maintaining the temperature of a still at approximately from 200° C. to 300° C. and gradually contacting the mixture of the sludge and water with the heated surfaces of the still.

8. The process of recovering tetra alkyl lead from metallic lead sludge which comprises distilling the mixture in the presence of water at a temperature above that at which the tetra alkyl lead will decompose in the absence of water at atmospheric pressure.

9. The process of recovering tetra alkyl

tained by the distillation of a like sample lead from metallic lead sludge which comprises distilling the mixture in the presence of water at a temperature of from about 200° C. to about 400° C.

In testimony whereof we affix our signa- 70

tures. MARION G. AMICK. FREDERICK B. DOWNING. ALFRED E. PARMELEE.

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