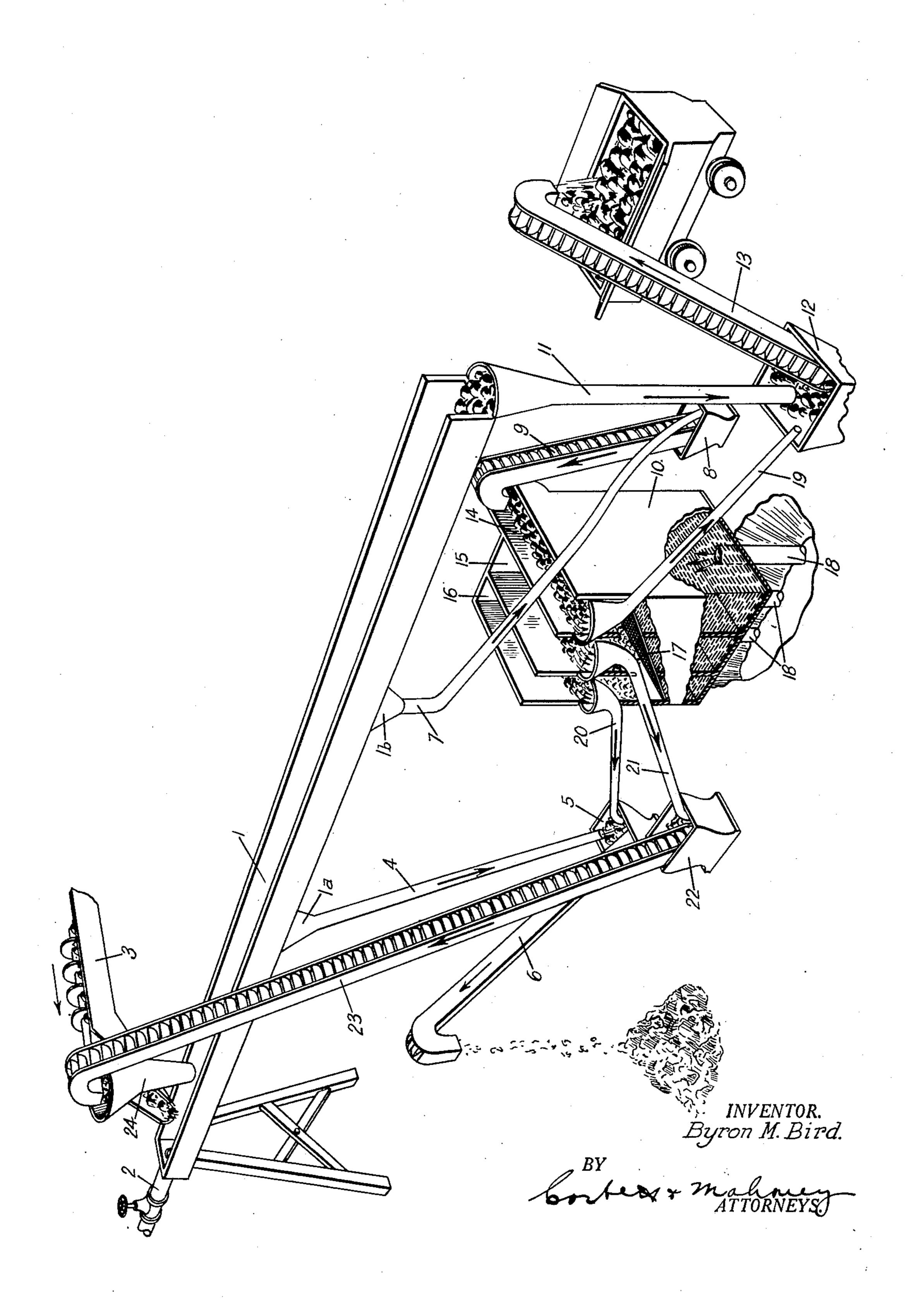
PROCESS OF SEPARATING COAL AND OTHER MINERALS
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My invention relates to process of separating coal and other minerals. It has to do primarily with the provision of a novel process of such a nature that separation of the 3 minerals may be effected with a minimum amount of apparatus and in a minimum length of time. It is particularly applicable to the treatment of minerals where the components of high density are relatively in-

10 frangible.

Wet processess for effecting separation according to differences in specific gravity may be roughly divided into several broad classes. One of these classes involves the use of hori-15 zontally flowing currents of water or other fluids serving as a vehicle for conducting the material and effecting separation thereof. Another class involves the use of vertical currents of water passing upwardly through the 20 material to bring about separation of the products.

In those processes which use horizontally flowing currents of fluid to effect separation, the material arranges itself in superimposed 25 layers. In the main, the lower and intermediate layers or strata contain a larger proportion of the material of higher specific gravity while the upper layers mainly contain the particles of lower specific gravity. ³⁰ In the extreme upper layer, this separation is ordinarily complete. In the intermediate and lower layers, however, the separation according to specific gravity is usually incomplete.

Normally, the bottom layers contain coarser particles of comparatively high specific gravity. Between these coarser particles are interstices or voids which, under the normal operation with the usual type of feed become filled with finer material with an undesirably large percentage of particles of low specific gravity. In other words, these finer particles

of low specific gravity move downwardly into these voids and in a measure nullify the sep- of finer particles of high specific gravity aration according to specific gravity. Thus, than is found in the feed being treated. This in the use of sloping launders, in an effort to added charge of material supplies an incomplete the separation of the product of creased proportion of fine particles of high highest density, it has been customary to re- specific gravity which will gravitate into the

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For example, in the treatment of coal by this process, the feed is delivered into the upper end of a launder at approximately the same point as the fluid and stratifies while flowing down the launder, with the denser 55 material such as slate et cetera near the bottom of the launder and the material of less specific gravity, such as coal in the upper layers for ultimate delivery over the end of the launder. The general tendency is to-60 ward separation but the coarser particles of high specific gravity which normally stratify close to the bottom of the launder have interstices or voids between them which become filled with finer material of low specific 65 gravity such as fine coal. Because this percentage of coal that finds its way into the interstices in the lower strata of the bed of the launder is normally quite large, it is ordinarily necessary to re-treat these lower 70 strata several times. This is usually accomplished by withdrawing the bottom strata from the primary launder and re-treating them in one or more separate launders and in the same launder. Even these retreatment 75 steps are often found to be not fully effective.

One of the objects of this invention is to avoid this necessity for re-treatment of the product or, at least, to reduce to a minimum any re-treating action which must be effected. 80

Another object of this invention is, by avoiding or minimizing the necessity for this re-treatment, to reduce the length of the process and the amount of apparatus necessary in performing such process.

Another object of this invention is to effect a more complete separation of the components of low specific gravity from the components of high specific gravity.

My invention contemplates adding to the 90 normal feed, which is supplied in the horizontally flowing current process, a charge of material which contains a higher percentage sort to re-treatment of the product several interstices or voids between the coarser particles of high specific gravity adjacent the

to prevent the entrance thereinto of fine par- designated 4, conveys the refuse downwardly ticles of low specific gravity which it is desir- into a boot 5 from which it is delivered by 5 bed. In other words, by the introduction of this increased proportion of fine particles of high specific gravity and the subsequent pas- which it may be delivered by means of an sage of these fine particles of high specific elevator 9 to a vertical current classifier 10. per layers and thus are grouped with the coarser materials of low specific gravity.

One way in which I may use my process contemplates the taking of a middling from 15 a horizontally flowing current apparatus and delivering it to a vertical current apparatus suitable for making three products. In this vertical current apparatus, the charge delivered thereto may be separated to produce 20 a product consisting of small particles of low specific gravity, a product consisting of coarse particles of high specific gravity, and a product consisting mainly of fine particles of high specific gravity together with any coarse particles of low specific gravity, if any are present in the product that was received by the vertical current apparatus.

The last product, that is, the product consisting mainly of fine particles of high spe-30 cific gravity is then fed back into the horizontally flowing current apparatus. The preponderating quantity of fine particles of high specific gravity which make up this product will fill up the interstices or voids in the low-35 er and intermediate strata of the bed and thus crowd the fine particles of low specific gravity up into the upper layers, thereafter making the separation of the feed according to specific gravity more complete and either rendering re-treatment unnecessary or greatly reducing the amount of re-treatment re-

quired under prior art conditions.

One type of apparatus which I may use in the performance of my process is shown diagrammatically in the accompanying drawing wherein similar characters of reference designate corresponding parts and wherein:

The figure is a perspective view diagrammatically representing the combination of a sloping launder and a vertical current classifier together with the various separating pipes and conveying units complemental

thereto. In the drawing, which illustrates the separation of coal, a launder of the sloping type is shown at 1 and is adapted to be fed with water at its upper end through the medium of a valve-controlled pipe 2. In the separation of coal, the material to be treated may be fed into this launder by a screw convey-

er 3. The trough 1 is provided in its base with suitable devices 1a and 1b for withdrawing products therefrom. A pipe is connected to

bottom of the bed and fill these voids so as each one of these devices. One such pipe, able to crowd into the upper layers of the means of an elevator 6 to a refuse storage pile. Another such pipe, designated 7, con- 70 veys a middling down into a boot 8 from gravity into the voids, the fine materials of A third pipe 11 located at the lower end of 10 low specific gravity are crowded into the up- the launder conveys the washed coal into a 75 boot 12 from which elevator 13 delivers it to a car or other location.

The water from the elevator boots 5, 8 and 12 as well as from the other elevator boot to be subsequently described can be returned to 80 the launder and classifier by any means used

in the industry.

The vertical current classifier 10 may be of any conventional form but it is preferably of such construction as to produce three prod- 85 ucts. As shown, it comprises three compartments designated 14, 15 and 16, each equipped with perforations 17 in the screen plate and pipes 18 for delivering water upwardly thereto.

In the treatment of the middling product in the classifier, I preferably use an uprising current of water sufficiently swift to barely keep the mass of particles, with the exception of the lowermost strata in a mo- 95 bile condition which is generally referred to in ore dressing or coal preparation as a condition of "teeter". This results in a substantially complete separation with the coarsest particles of highest specific gravity 100 in the lowermost layer and with the fine particles of lowest specific gravity in the uppermost layer. In the intermediate layer, the separation according to specific gravity is incomplete but this product of the classifier 105 is composed mainly of fine particles of high specific gravity together with such coarser particles of low specific gravity as may have been contained in the middling product delivered to the classifier.

The fine product of low specific gravity from the classifier is delivered from the compartment 14 into a pipe 19 which in turn delivers it to the boot 12. The coarse product of high specific gravity as delivered from 115 the compartment 16 into a pipe 20 which in

turn delivers it into the boot 5. The intermediate product of the classifier being mainly composed of smaller particles of high specific gravity with such coarser 120 particles of low specific gravity as may have been delivered with the middling charge to the classifier is delivered into a pipe 21 which in turn delivers it into boot 22. This constitutes the prepared charge. It is conducted 125 by means of an elevator 23 upwardly to a point above the trough 1 and delivered into this trough 1 adjacent the upper end thereof through the medium of a chute 24.

It will be seen from this description that 130

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the intermediate strata or middling from the one to be rejected. Such valuable materent classifier and there separated. Then the intermediate strata from the vertical cur-5 rent classifier, being composed mainly of fine particles of high specific gravity together with some larger particles of low specific gravity are delivered back into the trough 1 with the result that the fine particles of high 10 specific gravity shortly find their way into the interstices or voids in the lower and intermediate layers of the materials therein so the stratification of the material by substanthat, in the subsequent treating operation, the fine particles of low specific gravity are 15 crowded upwardly into the upper layers in the trough and delivered in greater proportion to the end of the trough. Any coarser particles of low specific gravity which have entered the launder as a part of this charge 20 from the classifier will, of course, normally flow over the end of the primary launder.

In the operation of my process by the use of the apparatus shown in the drawing, the treating operation will be started by deliv-25 ering the feed to the trough 1 by means of the conveyer 3 and at the same time delivering water or other fluid to this trough through the pipe 2. At the beginning of the operation withdrawing device 1a will usually be closed and the refuse and middlings will be drawn out through the withdrawing device 1b and delivered by pipe 7 and elevator 9 to the classifier. The washed coal will pass over the end of the trough and down pipe 11 into

35 boot 12.

The material delivered to the classifier will be treated in the manner described and the intermediate product thereof will pass into the boot 22 and be delivered by elevator 23 40 and chute 24 to the upper end of the trough 1. This intermediate product is mainly composed of smaller particles of high specific gravity. These smaller particles of high specific gravity will thereupon find their way into the interstices or voids in the lower and intermediate layers of the bed of material in the trough so that treatment from then on will result in the crowding of the finer particles of low specific gravity up into the upper 50 layers in the trough.

As a bed of material of high specific gravity and relatively free from fine particles of low specific gravity forms in the launder, withdrawing device 1a is gradually opened 55 and the entire system is rendered operative. In this manner, the formation of the proper bed with the desired high percentage of fine particles of high specific gravity may be obtained in a minimum length of time and may be maintained throughout the continu-

ous operation of the apparatus.

It will be readily understood that the process is substantially identical in application to minerals where the valuable material to be saved is of higher specific gravity than

trough 1 are conducted into the vertical cur- rial will be recovered from draw 1a and from pipe 20. The middling product of the classifier containing small particles of high specific gravity to fill the voids in the bottom 70 of the launder will serve to crowd fine gangue particles up into the upper layers and so to

keep the concentrates up to grade.

It will be apparent that my process is not limited to the particular methods and appa- 75 ratus shown and described. For example, tially horizontal flow may be effected by the use of air instead of liquid or by various other means. Various types of hindered-settling \$0 classifiers or jigs may be used to prepare the charge or it may be separately prepared. The charge may also be prepared by use of a two deck screen, the top screen which is of relatively coarse mesh removing the coarse §5 material of high specific gravity and the bottom screen, which is of relatively finer mesh, removing the fine material of low specific gravity, while the oversize of the bottom screen returns to the feed of the launder. 90 Likewise, other devices for effecting classification may be selected.

Having thus described my invention, what

I claim is:

1. The process of separating composite 95 minerals comprising subjecting said minerals to a substantially horizontal flow and thereby stratifying the components of said minerals according to densities, supplying to the stream of minerals a quantity of material 100 whose particles are of specific gravity equaling that of the lower strata of the stream and are of a size smaller than the average particle size of the minerals sufficient to substantially fill the voids in the lower strata of the mineral 105 stream, and separating the strata thereby formed.

2. The process of separating composite minerals comprising subjecting composite minerals whose constituents of high specific 110 gravity are infrangible relatively to those constituents of lesser specific gravity to a substantially horizontal flow and thereby stratifying the components of said minerals according to densities, supplying to the stream of 115 minerals a quantity of material whose particles are of specific gravity equaling that of the lower strata of the stream and are of a size smaller than the average particle size of the minerals to fill voids in the lower strata 120 of the mineral stream, and separating the strata thereby formed.

3. The process of separating composite minerals comprising subjecting said minerals to a substantially horizontal flow and thereby 125 stratifying the components of said minerals according to densities, supplying to the stream of minerals a quantity of material whose particles are of specific gravity equaling that of the lower strata of the stream and 130

are of a size smaller than the average particle size of the minerals to fill voids in the lower strata of the mineral stream, and separating

the strata thereby formed.

4. The process of separating composite minerals comprising subjecting said minerals to a substantially horizontal flow and thereby stratifying the components of said minerals according to densities, supplying to the stream 10 of minerals a quantity of material whose particles are mainly of specific gravity higher than that of the top strata of the stream and of specific gravity lower than that of the bot-sity than those of the top strata of the stream, tom strata of the stream and are of a size subjecting such product to upward currents 15 smaller than the average particle size of the of water sufficiently swift to create in the par- 80 minerals to fill voids in the lower strata of the ticles of such product substantially a condimineral stream, and separating the strata tion of "teeter" and removing from such thereby formed.

20 minerals comprising subjecting said minerals those of the top strata of the stream and are 85 with fluid to a substantially horizontal flow of a size smaller than the average particle and thereby stratifying the components of size of the lower strata of the stream, returnsaid minerals according to densities, supply- ing such middling product to the norizontal ing to the stream of minerals a quantity of flow and then effecting stratification thereof 25 material whose particles are of specific grav- with the stream, and separating the strata 90 ity equaling that of the lower strata of the thereby formed. stream and are of a size smaller than the average particle size of the minerals to fill voids in minerals comprising, first, subjecting said

30 separating the strata thereby formed.

6. The process of separating composite minerals comprising subjecting said minerals to a substantially horizontal flow and thereby stratifying the components of said minerals are of specific gravity equaling that of the lower strata of the stream and are of a size smaller than the average particle size of the 40 minerals, introducing such material to fill voids in the lower strata of the mineral stream, and separating the strata thereby formed.

7. The process of separating composite 45 minerals comprising subjecting said minerals to a substantially horizontal flow and thereby stratifying the components of said minerals according to densities, separating from such stratified material an intermediate prod-50 uct whose particles are of specific gravity higher than that of the top strata of the stream and are of a size smaller than the average particle size of the minerals, introducing such material to fill voids in the lower 55 strata of the mineral stream, and separating the strata thereby formed.

8. The process of separating composite minerals comprising subjecting said minerals to a substantially horizontal flow and thereco by stratifying the components of said minerals according to densities, withdrawing an in- horizontal flow. termediate portion of the said stratified material, selecting from said portion a middling signature. containing particles of a specific gravity 65 higher than that of the top strata of the

stream and of a size smaller than the average particle size of the minerals, supplying such middling to the mineral stream to fill voids in the lower strata of the mineral stream, and separating the strata thereby formed.

9. The process of separating composite minerals which comprises subjecting said minerals to a substantially horizontal flow and thereby stratifying the components of said minerals according to densities, separat- 75 ing from such stratified material a product whose particles are mainly of a higher denproduct a middling product whose particles 5. The process of separating composite are mainly of specific gravity higher than

10. The process of separating composite the lower strata of the mineral stream, and mineral to a substantially horizontal flow and thereby stratifying the components of said 95 minerals according to densities, second, separating from such stratified material a product of low specific gravity and a product of high and intermediate densities, removing 25 according to densities, separating from such from the latter a material whose particles of 100 stratified material a material whose particles high specific gravity are of a size smaller than the average particle size of the minerals in the lower strata of the horizontal flow, also removing therefrom a portion composed mainly of small particles of low specific 105 gravity, third, introducing the material containing small particles of high density into the horizontal flow and stratifying it therewith and adding the separated small particles of low specific gravity to the product of low 110 specific gravity from the horizontal flow, thereafter separating from the horizontal flow a product of low specific gravity and a product of intermediate density, removing from the latter a middling whose particles 115 of high specific gravity are of a size smaller than the average particle size of the minerals in the lower strata of the horizontal flow and also removing a portion composed mainly of small particles of low specific gravity, intro- 120 ducing the material containing small particles of high density into the horizontal flow and stratifying it therewith, and mixing the small particles of low specific gravity with the particle of low specific gravity from the 125

In testimony whereof, I hereby affix my

BYRON M. BIRD.