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Kamire et al.

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(54) **ELECTROCHEMICAL CARBON DIOXIDE CONVERTER AND LIQUID REGENERATOR**

B01D 2252/30 (2013.01); *B01D 2256/10* (2013.01); *B01D 2256/12* (2013.01); (Continued)

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CPC Y02P 20/151; Y02C 20/40; Y02E 60/36; B01D 53/326; B01D 2257/108; B01D 2257/502; B01D 2256/16; B01D 2252/30; B01D 2256/20; B01D 2257/504; B01D 53/1475; B01D 2256/12; B01D 2256/10; (Continued)

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(*) Notice: Subject to any disclaimer, the term of this patent is extended or adjusted under 35 U.S.C. 154(b) by 120 days.

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Related U.S. Application Data

(60) Division of application No. 15/985,475, filed on May 21, 2018, now Pat. No. 10,941,497, which is a (Continued)

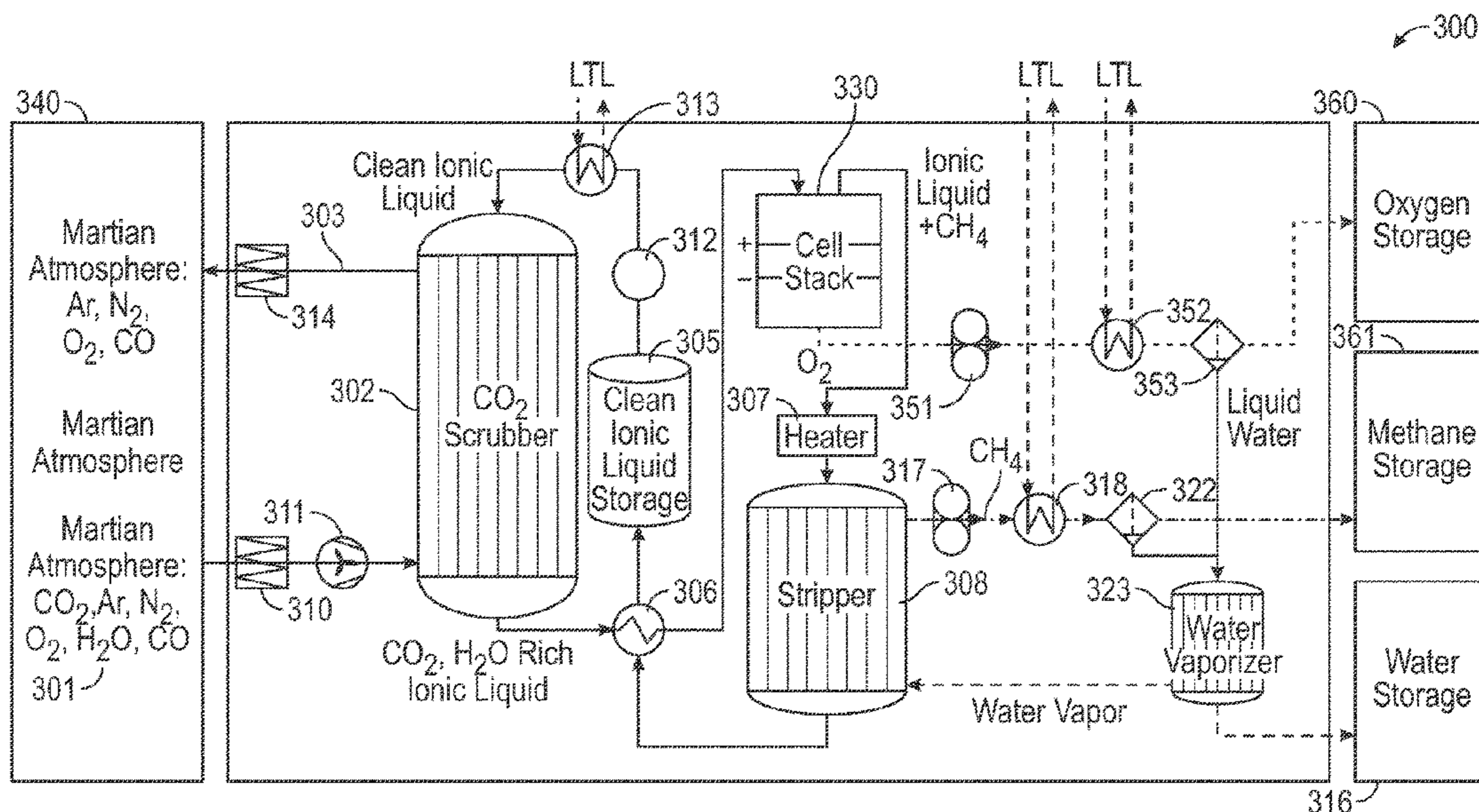
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(57) **ABSTRACT**
A carbon dioxide conversion system for an environment includes a first gas-liquid contactor-separator downstream of the environment; an electrochemical conversion cell downstream of the first gas-liquid contactor-separator; and a cleaned ionic liquid storage intermediate the first gas-liquid contactor-separator and the electrochemical conversion cell.

7 Claims, 9 Drawing Sheets



Related U.S. Application Data

continuation-in-part of application No. 15/896,150, filed on Feb. 14, 2018, now Pat. No. 11,123,685, and a continuation-in-part of application No. 15/896,156, filed on Feb. 14, 2018, now Pat. No. 10,688,435.

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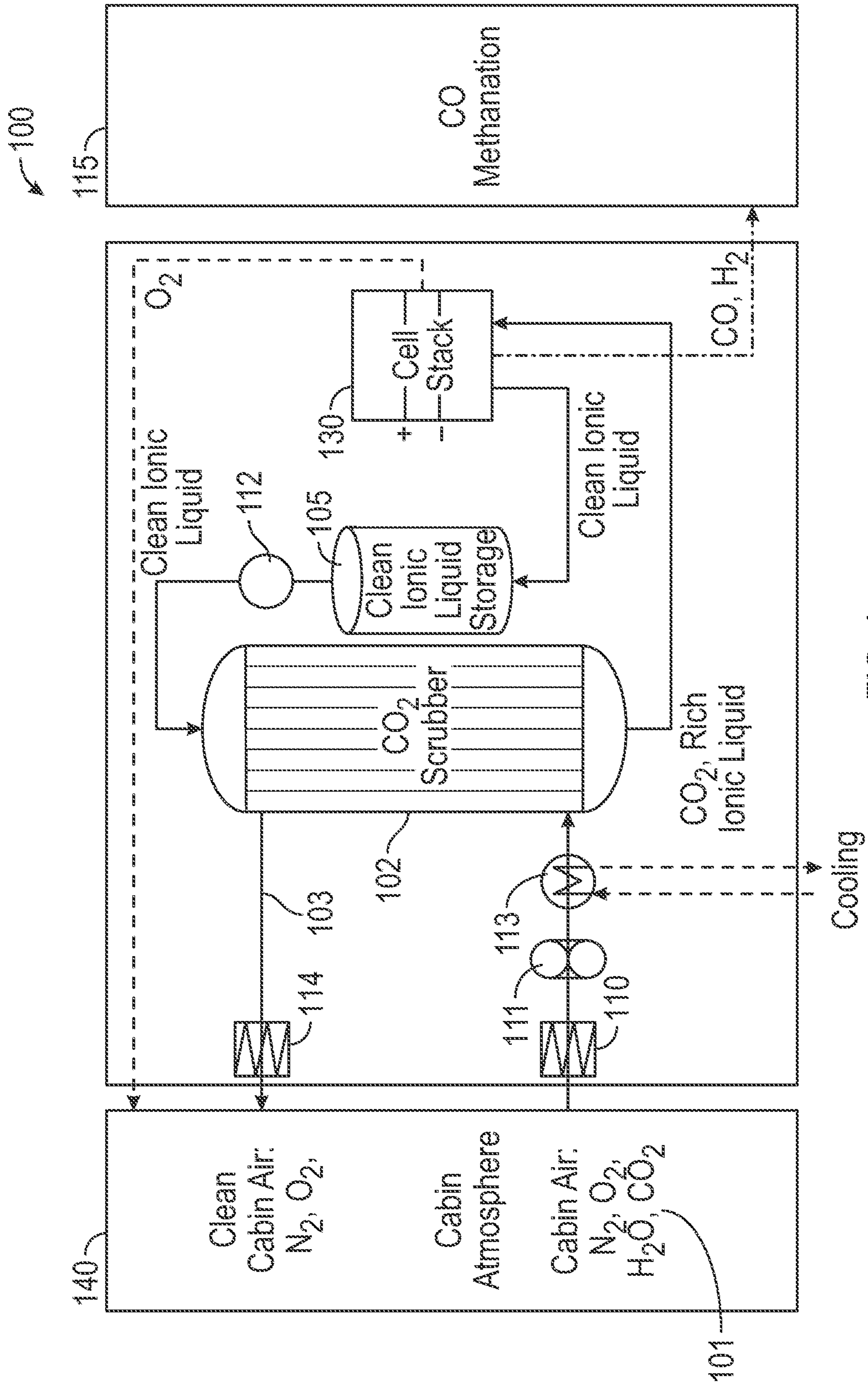
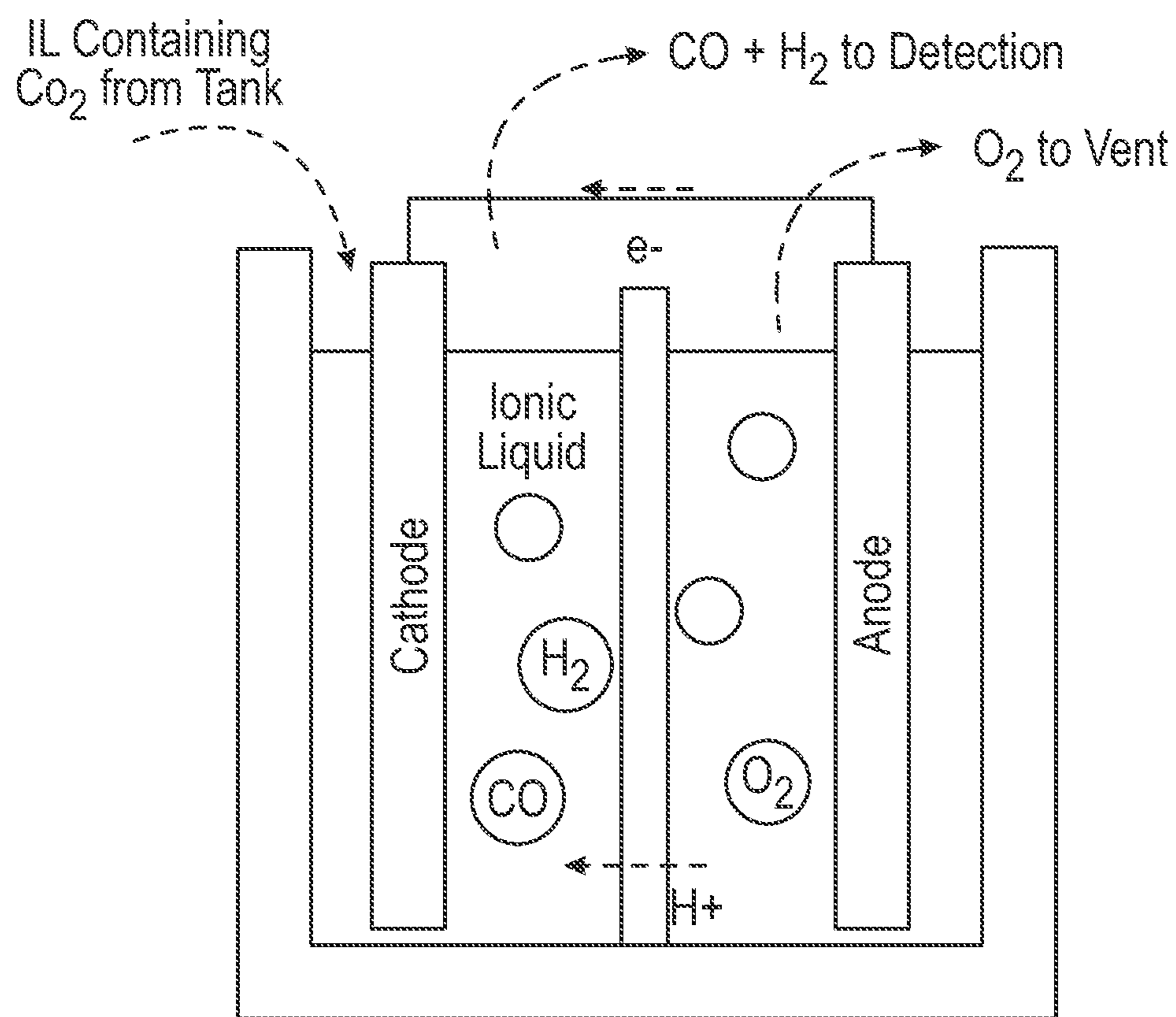


FIG. 1



Electrochemical Conversion

FIG. 1A

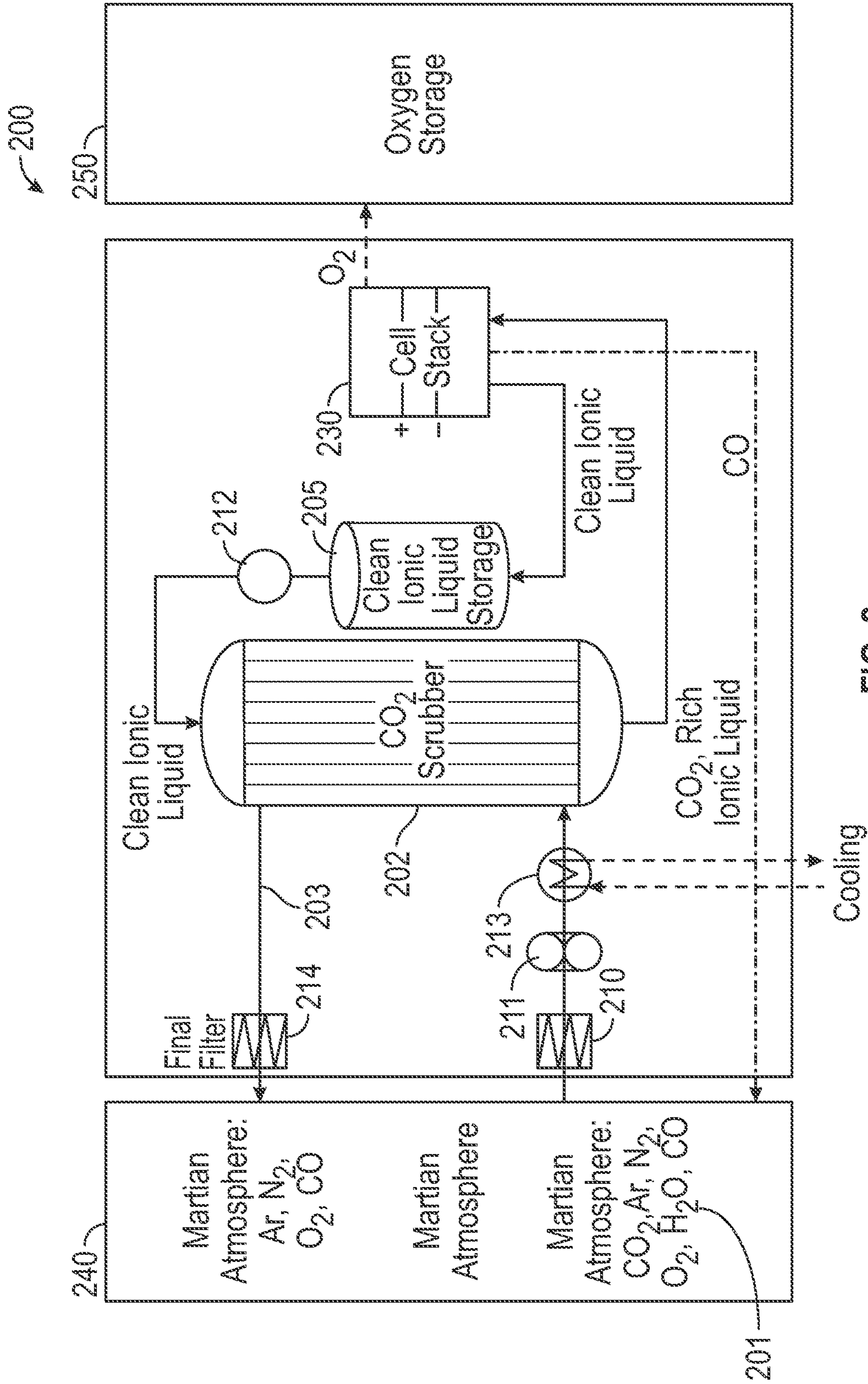


FIG. 2

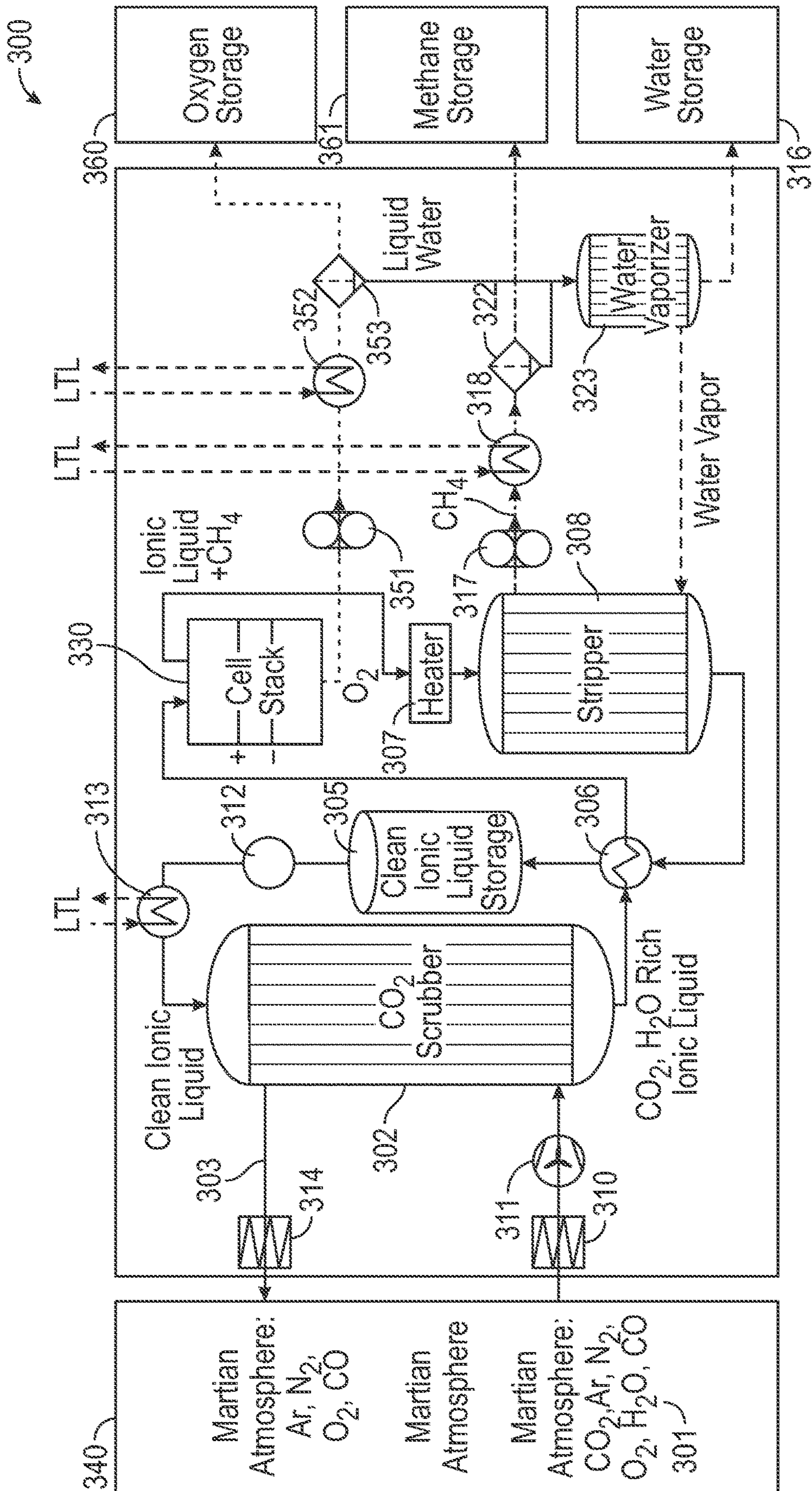


FIG. 3A

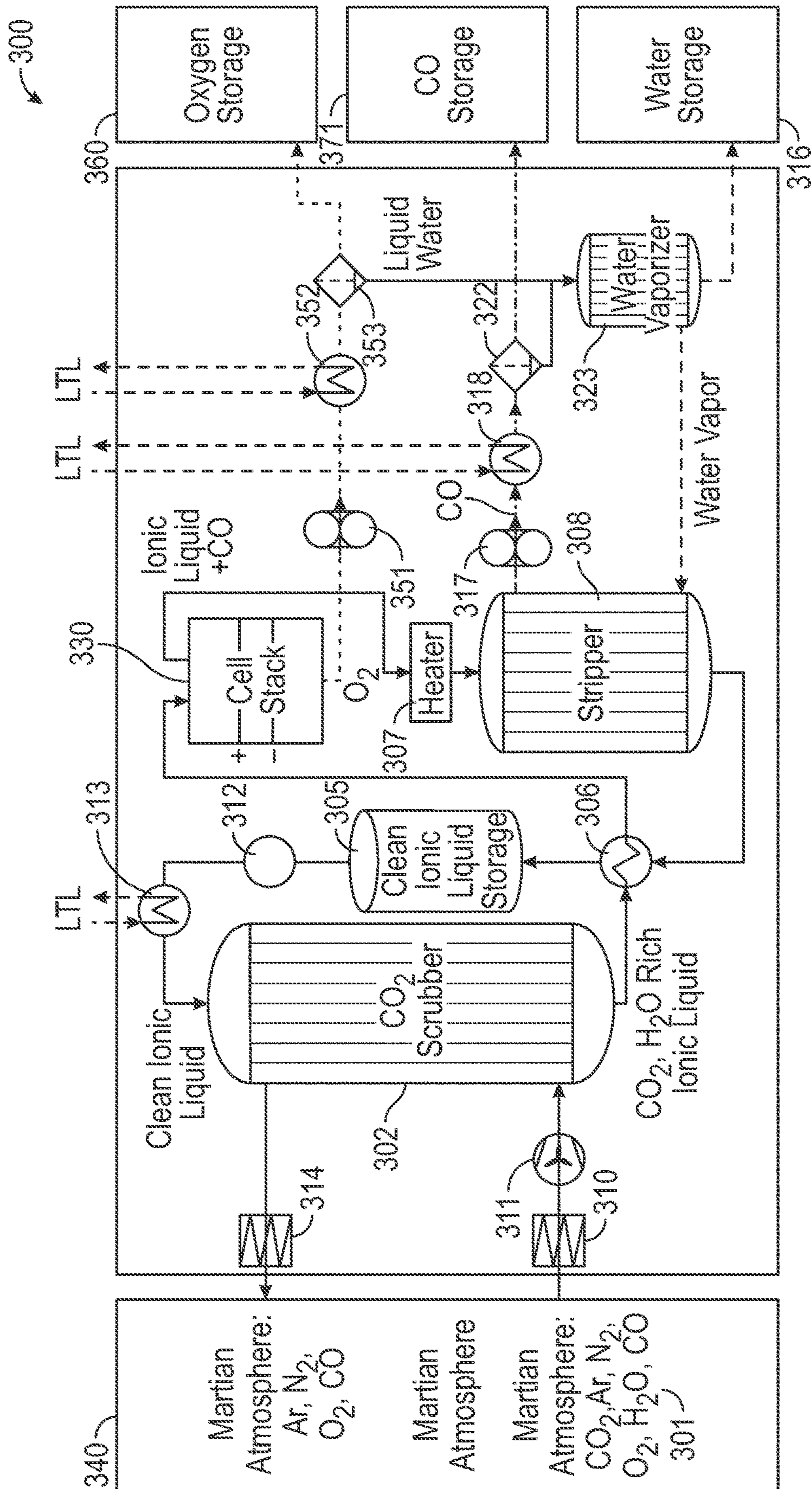


FIG. 3B

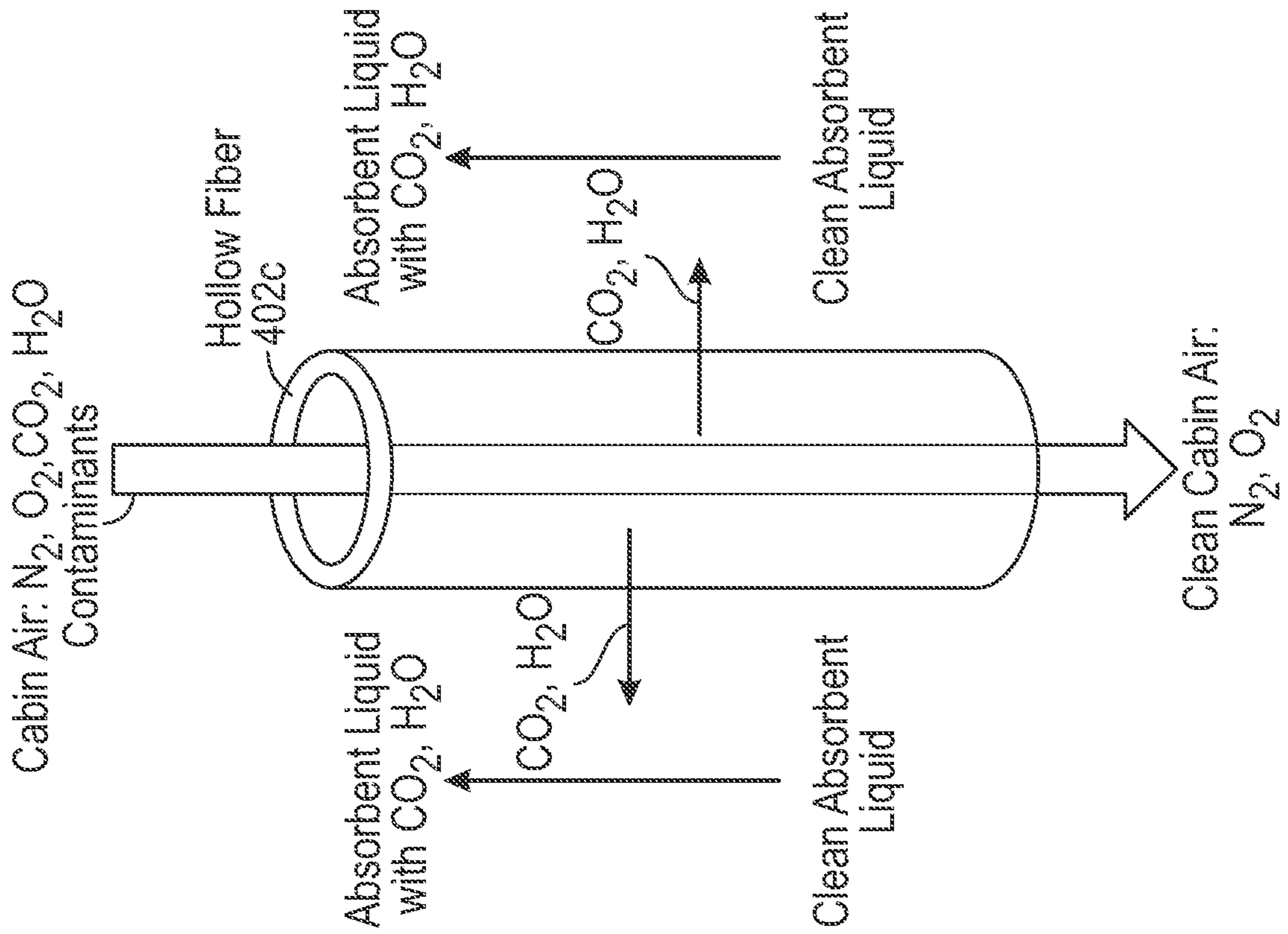


FIG. 4B

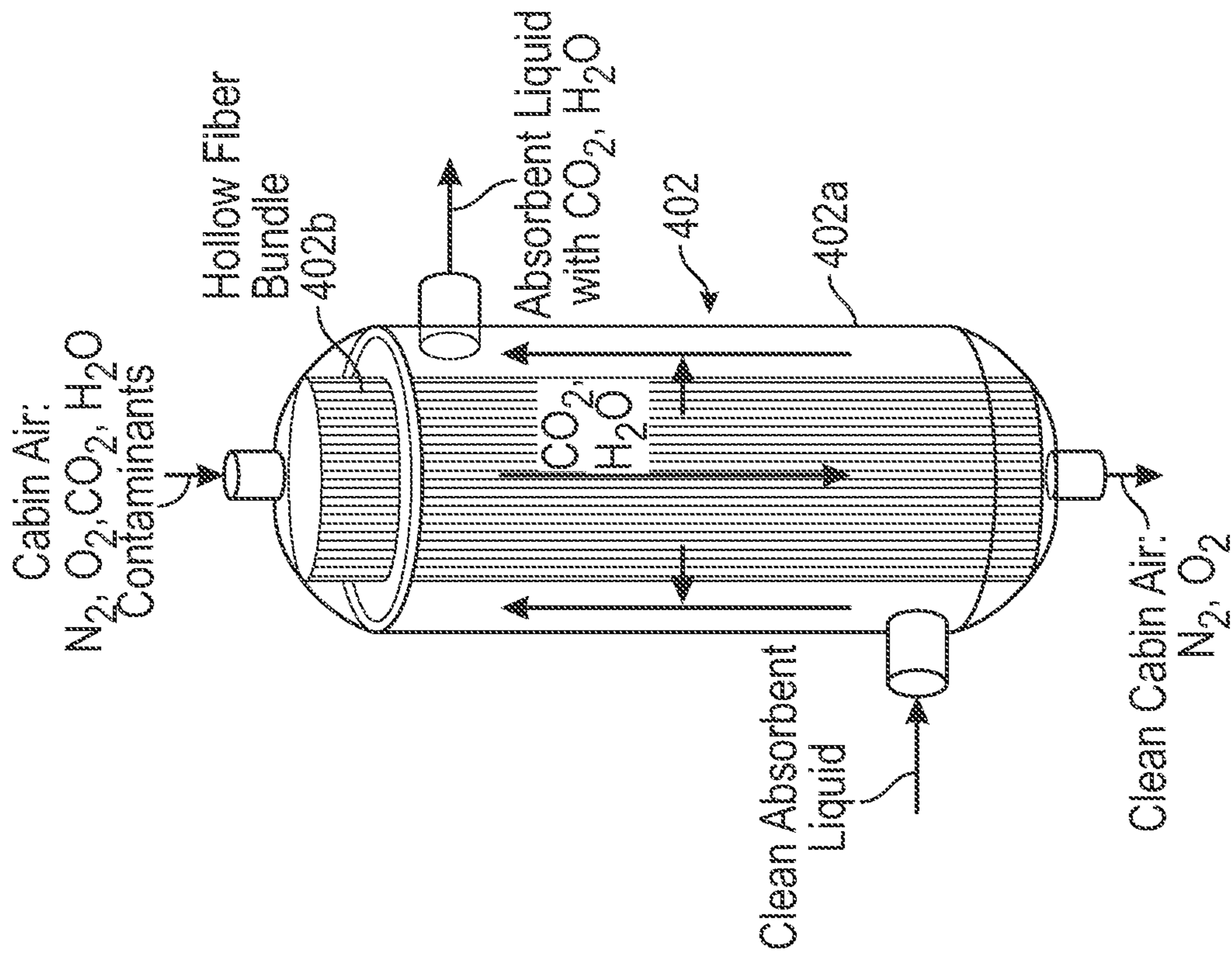


FIG. 4A

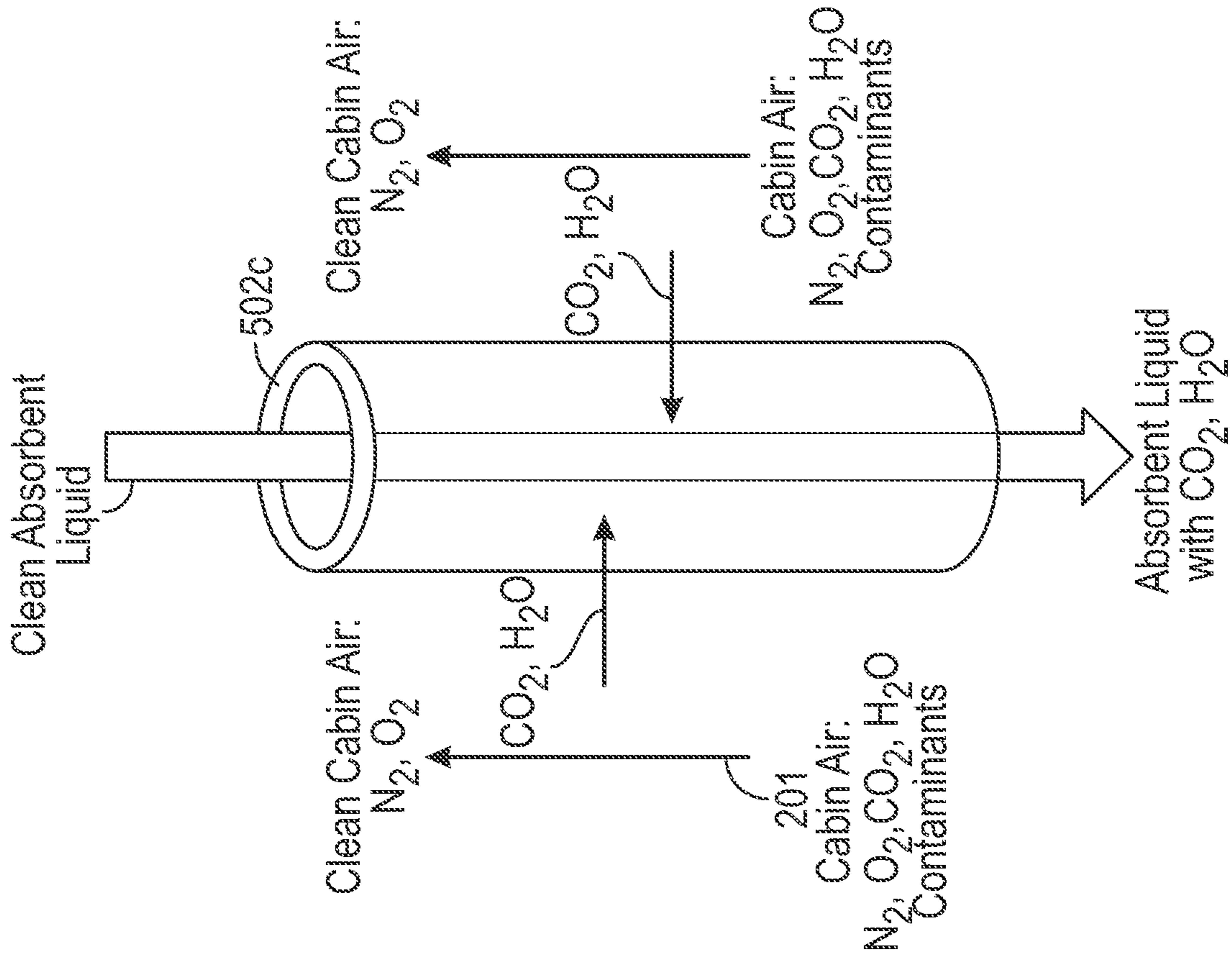


FIG. 5B

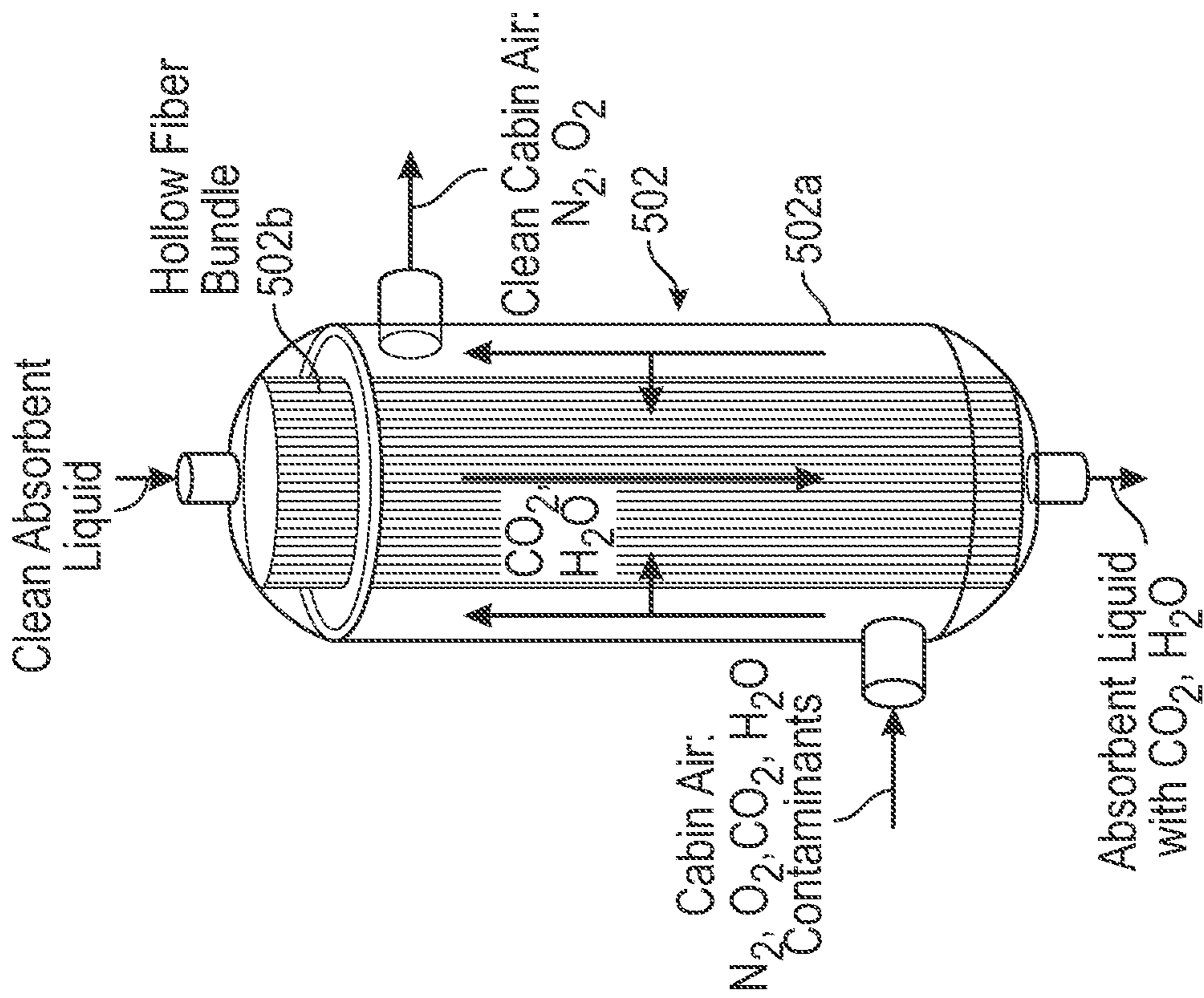


FIG. 5A

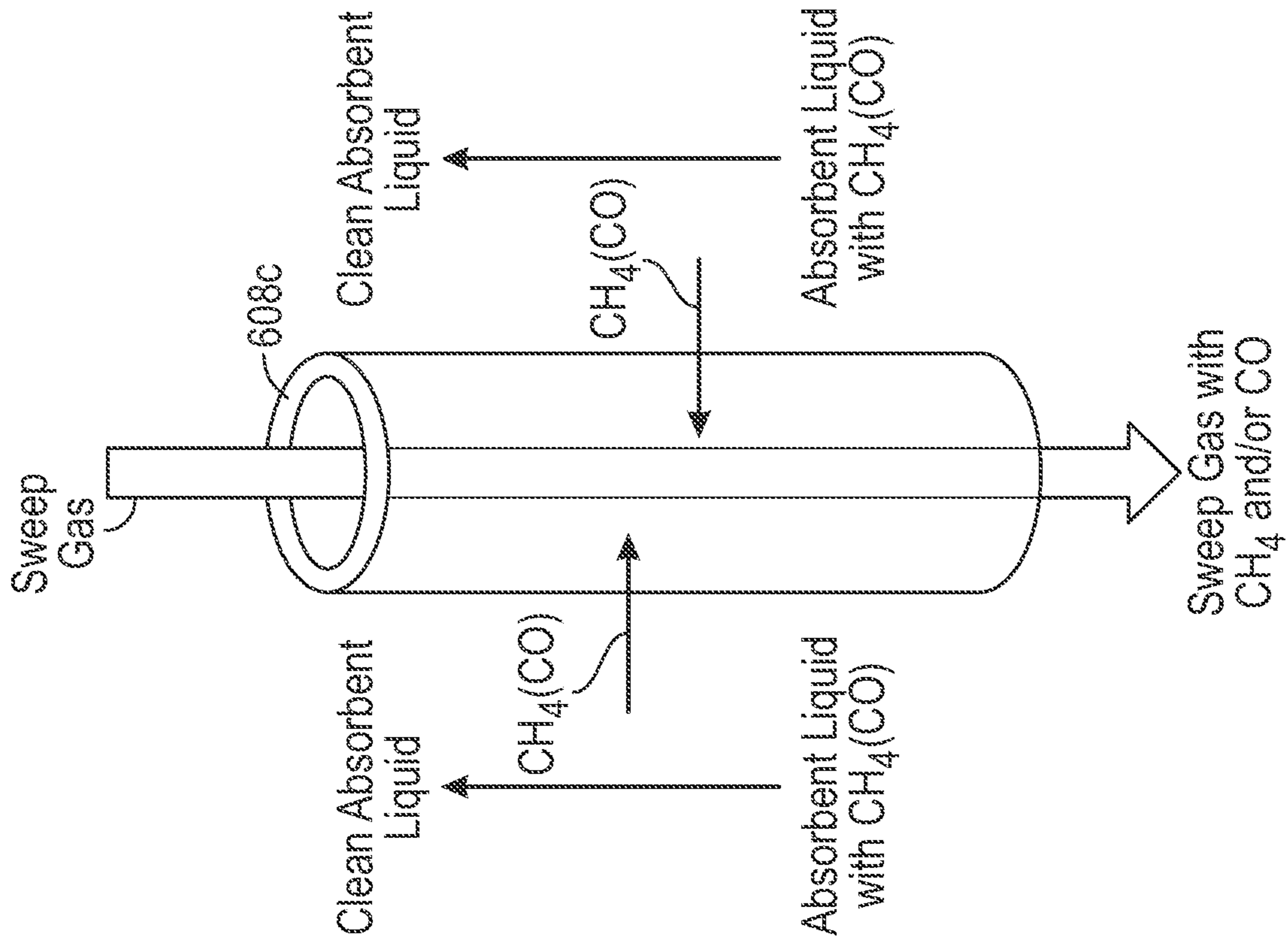


FIG. 6B

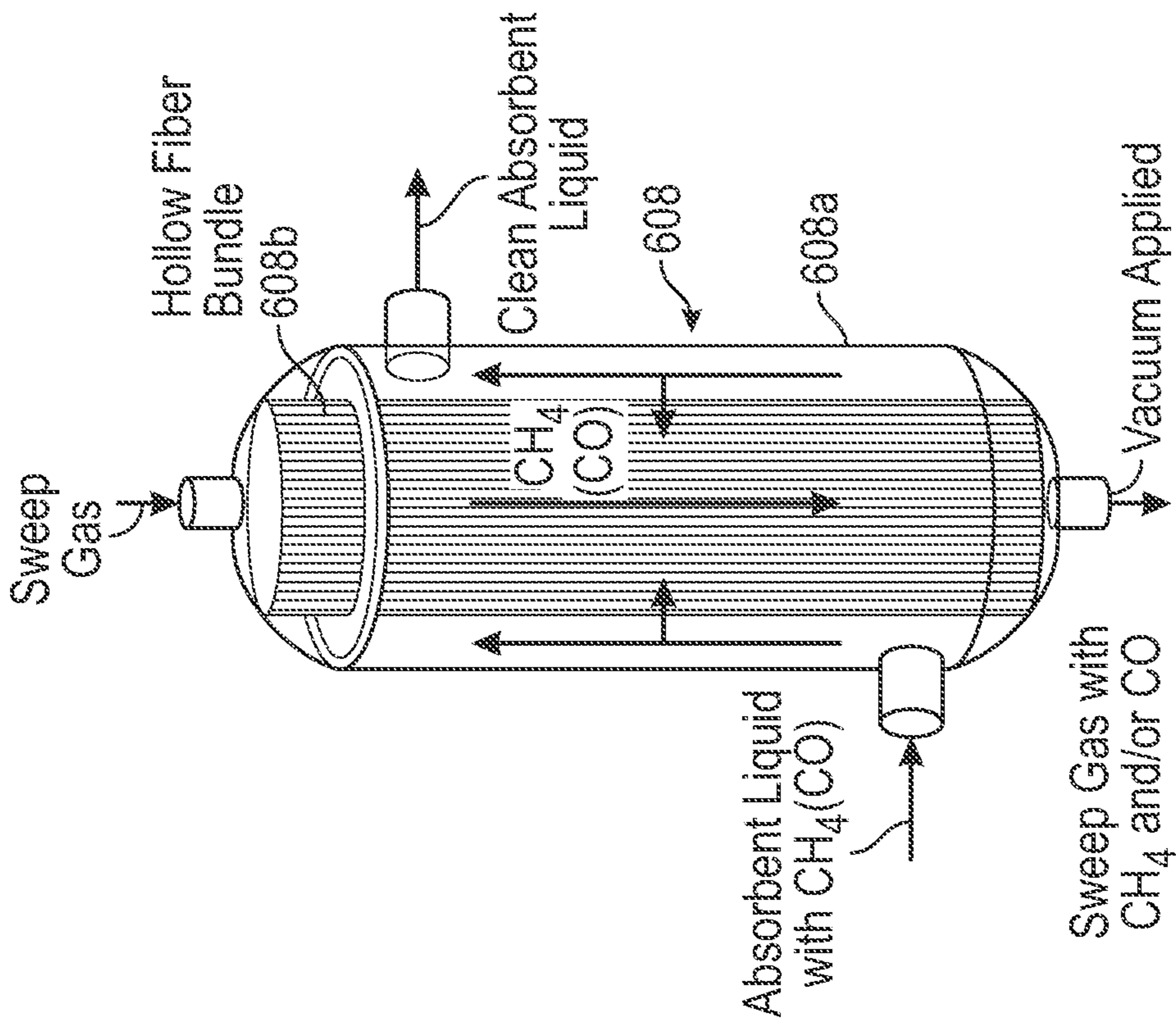


FIG. 6A

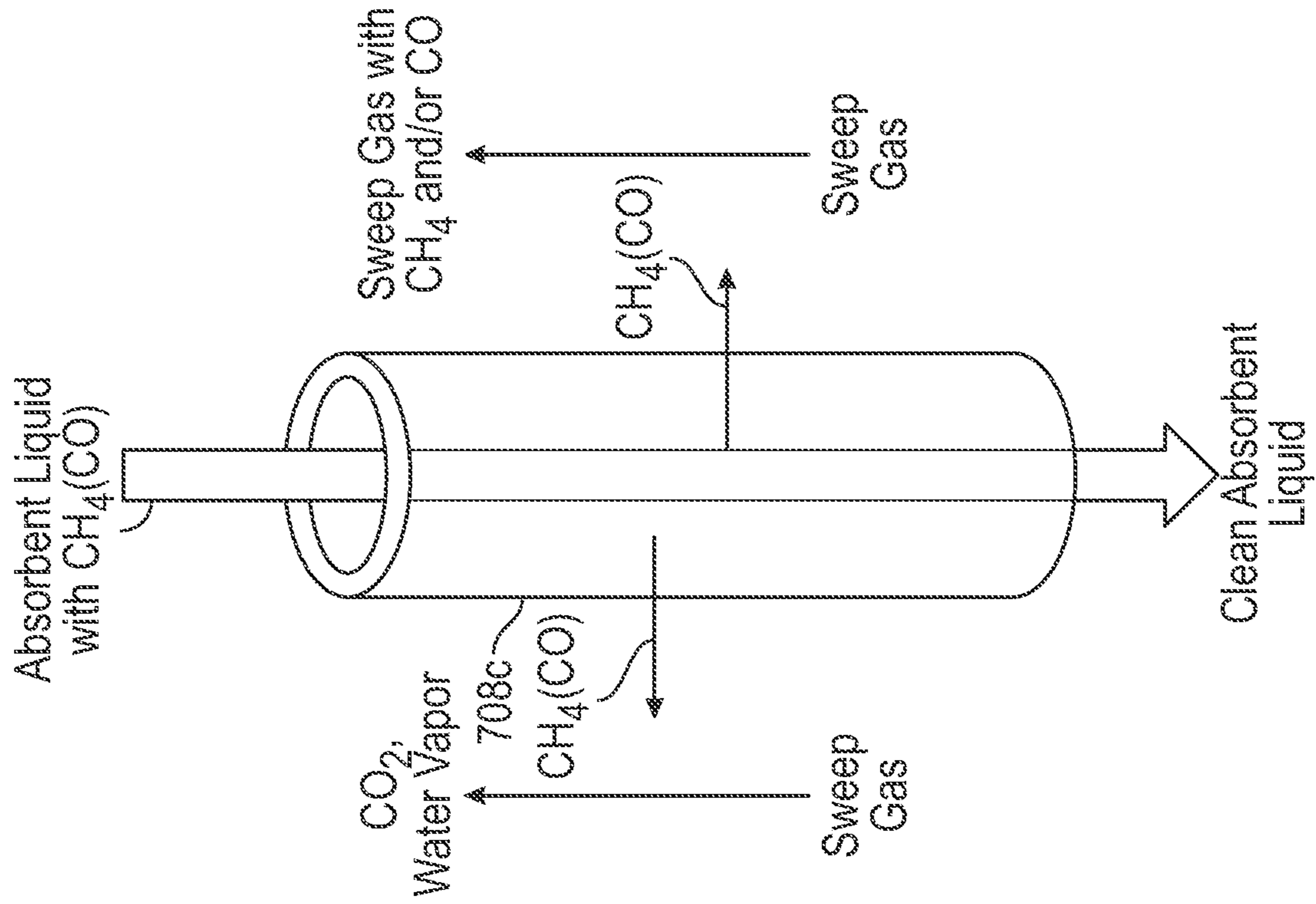


FIG. 7B

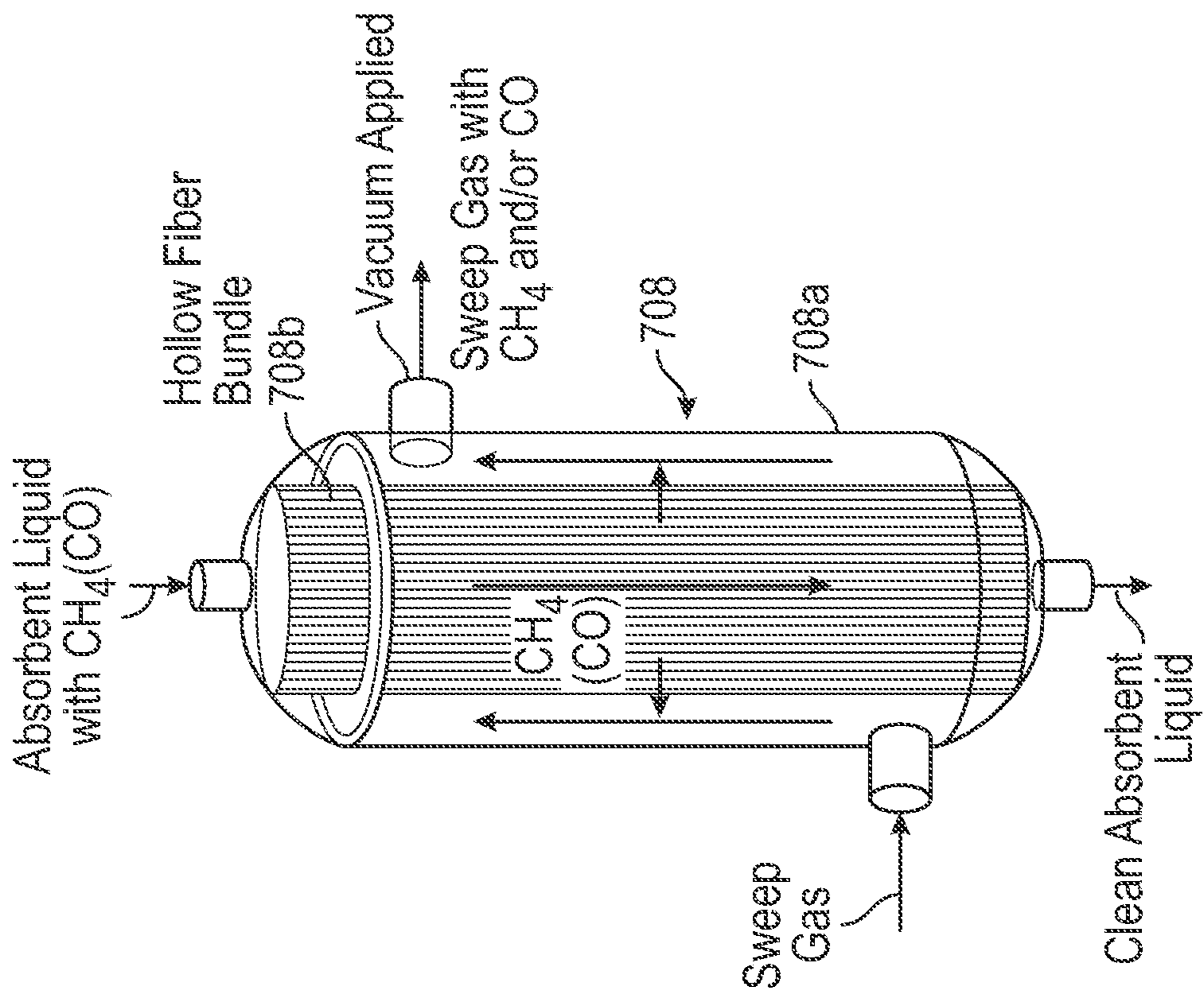


FIG. 7A

ELECTROCHEMICAL CARBON DIOXIDE CONVERTER AND LIQUID REGENERATOR

CROSS-REFERENCE TO RELATED APPLICATIONS

This application is a divisional application of U.S. patent application Ser. No. 15/985,475, filed May 21, 2018, which claims the benefit of and priority to U.S. patent application Ser. No. 15/896,150, filed Feb. 14, 2018, and which claims the benefit of U.S. provisional application Ser. No. 62/463,921, filed Feb. 27, 2017; and U.S. patent application Ser. No. 15/896,156, filed Feb. 14, 2018 and which claims the benefit of U.S. provisional application Ser. No. 62/463,921, filed Feb. 27, 2017; all of which are incorporated herein by reference.

BACKGROUND OF THE INVENTION

The present invention generally relates to carbon dioxide conversion and, more particularly, to apparatus and methods of carbon dioxide conversion employing gas-liquid contact and separation and electrochemical cells.

Long duration human space travel, such as to Mars, will require a life support system capable of recovering oxygen (O₂) in high yield from carbon dioxide (CO₂) exhaled by astronauts. The technological challenge falls only after spacecraft weight and susceptibility to radiation as a hurdle to long term habitation in space. On the International Space Station, CO₂ is removed from the cabin by adsorption to solid sorbents. These are heavy and cannot be replaced or serviced in space. Accidental water exposure results in adsorbed water that is difficult to remove. In addition, a high regeneration temperature is required for CO₂ desorption from the solid sorbents for downstream reaction with hydrogen (H₂) in a Sabatier reactor to produce water. O₂ is recovered from water via electrolysis. This is a very complicated system with many opportunities for failure and a maximum O₂ yield of 50%.

Establishing an environment for human use on the planet Mars will require a source for oxygen for respiration and for propulsion. In addition to recovering oxygen from exhaled carbon dioxide, it may be useful to convert carbon dioxide from the Martian atmosphere into oxygen. The Martian atmosphere has an average pressure of 600 Pa (0.087 psi), and an average temperature of -55 degrees C. It has a composition comprising 96% CO₂, 1.9% argon, and 1.9% nitrogen.

As can be seen, there is a need for improved apparatus and methods to remove carbon dioxide from a supply gas and convert it into oxygen in environments such as deep space vehicles.

SUMMARY OF THE INVENTION

In one aspect of the present invention, a carbon dioxide conversion system for an environment comprises a first gas-liquid contactor-separator downstream of the environment; an electrochemical conversion cell downstream of the first gas-liquid contactor-separator; and an ionic liquid storage intermediate the first gas-liquid contactor-separator and the electrochemical conversion cell.

In a further aspect of the present invention, a carbon dioxide conversion system for an environment closed to ambient air or gas comprises a scrubber downstream of the environment; an electrochemical conversion cell downstream of the scrubber; and an ionic liquid storage interme-

diating the scrubber and the electrochemical conversion cell; wherein the scrubber is configured to receive contaminated air from the environment, receive cleaned liquid absorbent from the ionic liquid storage, and discharge cleaned air to the environment; and wherein the cell stack is configured to discharge oxygen to the environment.

In another aspect of the present invention, a carbon dioxide conversion system for an environment open to ambient air or gas comprises a scrubber downstream of the environment; an electrochemical conversion cell downstream of the scrubber; and an ionic liquid storage intermediate the scrubber and the electrochemical conversion cell; wherein the scrubber is configured to receive contaminated air from the environment, receive cleaned liquid absorbent from the ionic liquid storage, and discharge at least one of Ar, N₂, and CO to the environment; and wherein the cell stack is configured to discharge at least one of O₂, CO, and CH₄ not to be returned to the environment.

These and other features, aspects and advantages of the present invention will become better understood with reference to the following drawings, description and claims.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a schematic diagram of a carbon dioxide conversion system according to an embodiment of the present invention;

FIG. 1A is a schematic diagram of an electrochemical conversion cell in a carbon dioxide conversion system according to an embodiment of the present invention;

FIG. 2 is a schematic diagram of a carbon dioxide conversion system according to another embodiment of the present invention;

FIGS. 3A-3B are schematic diagrams of a carbon dioxide conversion system according to a further embodiment of the present invention;

FIGS. 4A-4B are side views of a scrubber according to an embodiment of the present invention;

FIGS. 5A-5B are side views of a scrubber according to another embodiment of the present invention;

FIGS. 6A-6B are side views of a stripper according to an embodiment of the present invention;

FIGS. 7A-7B are side views of a stripper according to another embodiment of the present invention.

DETAILED DESCRIPTION OF THE INVENTION

The following detailed description is of the best currently contemplated modes of carrying out the invention. The description is not to be taken in a limiting sense, but is made merely for the purpose of illustrating the general principles of the invention, since the scope of the invention is best defined by the appended claims.

Various inventive features are described below that can each be used independently of one another or in combination with other features. However, any single inventive feature may not address any of the problems discussed above or may only address one of the problems discussed above. Further, one or more of the problems discussed above may not be fully addressed by any of the features described below.

Broadly, the present invention can be integrated into environments such as spacecraft used in long-duration missions, specifically, space stations and spacecraft and habitats used in and beyond low earth orbit, as the invention, particularly gas-liquid separation, operates independent of gravity.

The present invention generally provides a Carbon Dioxide Removal by Ionic Liquid Sorbent (CDRILS) system wherein ionic liquids (ILs) can act as liquid CO₂ sorbents. In contrast to solid sorbents, liquid CO₂ sorbents can be more easily exchanged in space, while continuous flow processing has the potential to afford a more robust system and a lower overall mass. Select ILs have high capacities for CO₂, chemical and electrochemical stabilities, compatibilities with humidity in the gas stream, and negligible vapor pressures. The capacity of IL for both CO₂ and water allows for dual function CO₂ and humidity removal, while the chemical stability of both 1-butyl-3-methylimidazolium acetate (BMIM Ac) and 1-ethyl-3-methylimidazolium acetate (EMIM Ac) makes repeated absorption/desorption, temperature cycling, and electrochemical cycling possible. The lack of vapor pressure makes ILs particularly suited to the closed environments in space where any risk of air contamination or loss of liquids by evaporation outside the environment must be avoided. The CDRILS hollow fiber scrubber membranes provide high surface area for CO₂ sorption into the ILs. A subsequent stripper membrane removes the CO₂ at lower temperatures than those required for solid sorbents and regenerates the IL for recirculation to the scrubber.

The CDRILS system of the present invention can produce a CO₂-loaded IL and water mixture following the scrubber. The CO₂ Electrolysis in Ionic Liquid (CEIL) of the current invention can electrochemically convert the CO₂ and water directly to O₂ and reduced carbon species such as carbon monoxide (CO), methane (CH₄), and/or other products using IL as the electrolyte solution. The O₂ and reduced carbon products are easier to strip from the IL than CO₂.

When the CDRILS and CEIL systems are used for life support, production of O₂ and CO increases the maximum possible O₂ yield from CO₂ from 50% to 67%, when followed by a reactor configured for carbon monoxide methanation similar to a Sabatier reactor for carbon dioxide methanation. The reduced carbon species or further reduced products of the reactor may be transformed further to recover additional valuable products, or they can be used as fuels.

Additionally, the present invention could be used for In-situ Resource Utilization (ISRU) if the CO₂ source is the Mars atmosphere. If the desired target of ISRU is life support, CO₂ can be electrolyzed to CO and O₂. If the target is fuel generation for propulsion, CO₂ and water can be electrolyzed to CO, H₂, and/or methane (CH₄) and O₂. CO and H₂ would be further converted to CH₄ at a second catalyst, or electrochemically generated CH₄ could be utilized directly. The O₂ product would be stored for use when burning the fuel.

The present invention also enables water electrolysis to H₂ and O₂ in the same cell as CO₂ transformation. Water electrolysis in the same electrolysis cell(s) could eliminate the need for the current O₂ generation cell stack.

The invention uses a hollow fiber-based contactor for CO₂ and water removal from the cabin air or Mars atmosphere. The IL mixed with water is flowed through either the lumen or the shell of the hollow fiber module, while the cabin air or Mars atmosphere is flowed countercurrent through either the shell or the lumen respectively. The CO₂-loaded IL and water mixture is continuously flowed through the cathode compartment of an electrochemical conversion cell. The cathode compartment is separated from the anion compartment by an ion exchange membrane or porous separator. The anode compartment contains either a CO₂-free IL solution or an aqueous solution. A voltage is

applied between the two electrodes to reduce CO₂ and water to reduced carbon species and H₂ and hydroxide at the cathode and oxidize water or hydroxide to O₂ at the anode. Additional cells can be stacked to provide the appropriate scaling for the necessary O₂ generation rate.

The O₂-laden liquid from the anode is then flowed to a stripper or centrifugal separator for O₂ separation, which can then be sent to the cabin or stored. The liquid is recycled to the anode compartment. The product-laden liquid from the cathode is flowed to a hollow fiber stripper. The liquid is flowed through the lumen or shell, while low pressure on the other side of the fiber strips the products and water from the IL to recover the mixture required for the scrubber inlet. The products are flowed to the methanation catalyst for water and methane production.

U.S. patent application entitled "Apparatus and Methods for Enhancing Gas-Liquid Contact/Separation" filed Feb. 1, 2017, Ser. No. 15/422,170; U.S. patent application entitled "Ionic Liquid CO₂ Scrubber for Spacecraft" filed Feb. 1, 2017, Ser. No. 15/422,166; U.S. patent application entitled "Hollow Fiber Membrane Contactor Scrubber/Stripper for Cabin Carbon Dioxide and Humidity Control" filed Feb. 14, 2018, Ser. No. 15/896,150; and U.S. patent application entitled "Dual Stripper with Water Sweep Gas" filed Feb. 14, 2018, Ser. No. 15/896,156, are incorporated herein by reference as though fully set forth herein.

Herein, the term "absorbent" is intended to generally include absorbents and/or adsorbents.

"Used liquid absorbent" means "clean liquid absorbent" that has absorbed carbon dioxide.

"Cleaned liquid absorbent" means liquid absorbent that is substantially free of absorbed carbon dioxide.

"Regenerated liquid absorbent" means used liquid absorbent that has undergone desorption of carbon dioxide.

"Cleaned gas" means gas that has an insubstantial amount of carbon dioxide and/or H₂O. "Cleaned gas" has a carbon dioxide and/or H₂O concentration less than that of the gas from the environment to be cleaned.

FIG. 1 is a schematic diagram of an exemplary carbon dioxide conversion system (i.e., closed-loop air revitalization system) **100** that may be employed in a space-based system. A "closed-loop air revitalization system" is intended to mean a system which recovers valuable resources from waste products, such as recovering valuable oxygen from waste carbon dioxide. The system **100** may include one or more gas-liquid contactor-separators to effectuate removal of carbon dioxide. However, the system **100** is not limited to the contactor-separators described below.

The carbon dioxide conversion system **100** may receive a contaminated air **101** from an enclosed environment **140** suitable for human occupants, such as a spacecraft cabin. Thus, the environment **140** can be configured to be closed to, or sealed from, ambient air or gas. The contaminated air or gas **101** may include one or more gas/vapor contaminants such as N₂, CO₂, and/or H₂O.

The air or gas **101** may flow into a first gas-liquid contactor-separator (i.e., scrubber) **102**. In embodiments, the contaminated air **101** may, before entering the scrubber **102**, be filtered for dust and particulates, via a filter **110**, as well as being forced, via a fan or compressor **111**, into the scrubber **102**. In some embodiments, the contaminated air **101** may exit the fan **111** and enter a cooler **113** before entering the scrubber **102**.

Concurrently with, or sequentially with, the scrubber **102** receiving the contaminated air **101**, cleaned liquid absorbent may be pumped, via a pump **112**, into the scrubber **102**, from a cleaned liquid absorbent storage **105**. In embodiments, the

liquid absorbent may be one or more ionic liquids described below. In the scrubber **102**, the cleaned ionic liquid(s) may absorb contaminants, such as CO₂, from the contaminated air **101**.

From the scrubber-separator **102**, cleaned air **103** may optionally flow through a filter **114**, to capture any leaked ionic liquid and/or produce a further cleaned air that can flow back to the environment **140** to be conditioned. In embodiments, the cleaned air **103** may have a gas contaminant(s) concentration, and/or H₂O concentration, lower than that of the contaminated air **101**.

Also from the scrubber-separator **102**, used liquid absorbent may exit. The used liquid absorbent may flow into an electrochemical conversion cell **130** or, in embodiments, a plurality of electrochemical conversions cells. In embodiments, the plurality of cells may be in a stack configuration.

FIG. **1A** schematically depicts an exemplary electrochemical conversion cell **130**. The cell **130** may have an anode, cathode and an ionic membrane therebetween, all of which are in a bath of ionic liquid. The half reaction at the anode that generates oxygen is either $2\text{H}_2\text{O} \rightarrow \text{O}_2 + 4\text{H}^+ + 4\text{e}^-$ or $4\text{OH}^- \rightarrow 2\text{H}_2\text{O} + 4\text{e}^- + \text{O}_2$, depending on the pH. Multiple reactions are proposed to occur at the cathode. These include production of hydrogen: $2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2$ or $2\text{H}_2\text{O} + 2\text{e}^- \rightarrow 2\text{OH}^- + \text{H}_2$, and production of carbon monoxide: $\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{CO} + \text{H}_2\text{O}$ or $2\text{H}_2\text{O} + 2\text{CO}_2 + 4\text{e}^- \rightarrow 2\text{CO} + 4\text{OH}^-$. Under some circumstances, and depending on the cathode material, methane may also be generated: $\text{CO}_2 + 8\text{H}^+ + 8\text{e}^- \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$ or $6\text{H}_2\text{O} + \text{CO}_2 + 8\text{e}^- \rightarrow \text{CH}_4 + 8\text{OH}^-$.

The cell **130** can receive a used ionic liquid having CO₂. The cell **130** can discharge O₂ to the environment **140**. Concurrently with, or sequentially with, the O₂ discharge, the cell **130** may discharge cleaned ionic liquid to the ionic liquid storage **105**. Concurrently with, or sequentially with, the O₂ and cleaned ionic liquid discharge, the cell **130** may discharge CO and/or H₂ to a CO methanation reactor **115**. The CO methanation reactor functions by reacting the carbon monoxide with hydrogen to convert it to methane and water. The water, in turn, may be electrolyzed to generate hydrogen and oxygen, forming a closed-loop air revitalization system.

As noted above, the electrochemical conversion cell **130** may be present in the form of a stack of cells. Such a stack may be as described in Fry, A. J., *Electrochemical Processing, Organic*. In *Kirk-Othmer Encyclopedia of Chemical Technology*, John Wiley & Sons, Inc.: 2000, FIG. 10, which is incorporated herein in its entirety.

FIG. **2** is a schematic diagram of another exemplary embodiment of the present invention. FIG. **2** is similar to that described in relation to FIG. **1**. Accordingly, reference numbers in FIG. **2** correspond to like reference numbers in FIG. **1**.

However, in the exemplary embodiment of FIG. **2**, a carbon dioxide conversion system **200** is provided in the context of an environment **240** open to ambient air or gas—such as a Martian atmosphere—as opposed to the closed environment **140** of FIG. **1**. In this exemplary instance, the environment **240** is the Martian atmosphere. From the Martian atmosphere **240**, feed gas **201** to the system may include CO₂, Ar, N₂, O₂, H₂O, CO, and/or other gases present in the Martian atmosphere **240**.

In FIG. **2**, a scrubber **202** may separate CO₂ from the feed gas **201** and discharge a cleaned gas **203** that contains less CO₂ than feed gas **201** to the Martian atmosphere **240**. The discharged gas **203** may include Ar, N₂, O₂, CO, and/or other gases present in the Martian atmosphere **240** or

produced by the conversion cell(s) **230**. An electrochemical conversion cell(s) **230** (or cell stack) may discharge CO into the Martian atmosphere **240**, rather than being sent to a CO methanation reactor **115** as in FIG. **1**. Also, O₂ discharged from the conversion cell(s) **230** can be sent to an oxygen storage unit **250** for eventual use by human occupants in a space craft or habitat, for example. This is in contrast to O₂ being sent from the conversion cell **130** to the cabin **140** in FIG. **1**.

FIG. **3A** is a schematic diagram of another exemplary embodiment of the present invention. FIG. **3A** is similar to that described in relation to FIG. **2**. Accordingly, reference numbers in FIG. **3A** correspond to like reference numbers in FIG. **2**.

However, in the embodiment of FIG. **3A**, a cooler **313** may be intermediate a pump **312** and a scrubber **302**, whereas there is no similar cooler in FIG. **2**. A heat exchanger **306** may be intermediate the scrubber **302**, a clean ionic liquid storage **305**, an electrochemical conversion cell(s) **330** (or cell stack), and a second gas-liquid contactor-separator (i.e., stripper) **308**. In the embodiment of FIG. **2**, there is no similar heater or stripper.

Accordingly, in the embodiment of FIG. **3A**, the scrubber **302** may discharge a used liquid absorbent having CO₂ and H₂O, for example. That used liquid absorbent can be received by the heat exchanger **306** and then discharged to the conversion cell(s) **330**. Concurrently with, or sequentially with, the foregoing, the heat exchanger **306** may receive cleaned liquid absorbent from the stripper **308** and discharge the same to the clean ionic liquid storage **305**. Thus, cleaned liquid absorbent can be pumped into the scrubber **302** where CO₂ is separated from the feed gas **301**, and discharge cleaned gas **303** containing Ar, N₂, O₂, CO, and/or other gases present in the Martian atmosphere **340** or produced by the conversion cell(s) **330** may be discharged into the Martian atmosphere.

The electrochemical conversion cell(s) **330**, upon receiving the ionic liquid with CO₂ and H₂O from the scrubber **302** and performing electrochemical conversions, may discharge ionic liquid with CH₄ to a heater **307**, and the same may then flow to the stripper **308**. CH₄ may exist in the discharged ionic liquid as a result of the characteristics of the cathode and solubility of CH₄ in the ionic liquid. The stripper **308** may remove CH₄ from the ionic liquid to thereby discharge cleaned ionic liquid that can flow into the ionic liquid storage **305**. The CH₄ removed by the stripper **308** may be discharged to a pump **317**, a condenser **318**, and a water extractor **322** for receipt by a methane storage **361**. The system may also be operated without heater **307**, stripper **308**, and pump **317**, where gaseous products of the conversion cell(s) **330** cathode are discharged to condenser **318** if solubility of CH₄ in the ionic liquid is low. Stored methane may then be used as fuel in a space craft, for example.

Concurrently with, or sequentially with, the conversion cell(s) **330** discharging ionic liquid with CH₄, the conversion cell(s) **330** may also discharge O₂ through a pump **351**, a condenser **352**, and a water extractor **353** for receipt by an oxygen storage **360**. Stored oxygen may then be used by human occupants in a space craft, for example.

From the water extractor **353**, liquid water may flow to a water vaporizer **323**. Discharged liquid water therefrom may be received in a water storage **316**, while discharged water vapor therefrom may flow to the stripper **308** wherein the water vapor can be used as a sweep gas.

FIG. **3B** is a schematic diagram of another exemplary embodiment of the present invention. FIG. **3B** is similar to

that described in relation to FIG. 3A. Accordingly, reference numbers in FIG. 3B correspond to like reference numbers in FIG. 3A.

The embodiment of FIG. 3B is largely the same as the embodiment of FIG. 3A. However, in FIG. 3B, the electrochemical conversion cell(s) 330 discharges ionic liquid with CO rather than with CH₄ as in FIG. 3A. Thus, the stripper 308 discharges CO rather than CH₄. And the discharged CO is received by a CO storage 371 for eventual use by human occupants in a space craft or habitat, for example.

The invention could also be used in several other configurations.

In one embodiment, the anode compartment contains ionic liquid and/or an aqueous electrolyte solution. O₂ is recovered through a gas diffusion electrode directly as O₂ in FIGS. 3A and 3B, or by passing the solution from the anode compartment through a stripper, pump, compressor, and water extractor as in methane and CO FIGS. 3A and 3B.

In this embodiment, the anode compartment does not contain an IL or aqueous solution separate from the solution in the cathode compartment. Instead, water or hydroxide passes through the ion exchange membrane or porous separator from the cathode compartment and is electrolyzed on the anode surface to O₂. This removes the need for O₂ separation from an electrolyte solution. O₂ is recovered as in O₂ in FIGS. 3A and 3B.

In CO₂ removal applications where closed-loop O₂ recovery is unnecessary (e.g., aircraft, submarines), electrochemical H₂ and CO fuel production could be targeted. The O₂, H₂, and CO products could be collected for use in fuel cells.

FIGS. 4A-4B depict an exemplary embodiment of a scrubber 402 that may be employed in the carbon dioxide conversion system 100, for example. In FIG. 4A, the scrubber 402 may include a cylindrical housing 402a that encloses a hollow fiber bundle 402b. CO₂-rich gas may enter the housing 402a at one end thereof and CO₂-lean gas may exit at an opposite end thereof. Regenerated or cleaned liquid absorbent may enter the housing 402a at one side thereof, and used liquid absorbent with carbon dioxide may exit the housing 402a at an opposite side thereof. In this embodiment, regenerated or cleaned absorbent liquid flows counter (i.e., opposite) to the gas flow. Moreover, the counter flow causes carbon dioxide to flow from the gas out of the hollow fiber bundle 402b into the liquid.

FIG. 4B depicts the same flows as in FIG. 4A, but in the context of a single hollow fiber 402c that can be part of the hollow fiber bundle 402b.

FIGS. 5A-5B depict another exemplary embodiment of a scrubber 502 that may be employed in the carbon dioxide conversion system 100, for example. As in FIG. 4A, in FIG. 5A, the scrubber 502 may include a cylindrical housing 502a that encloses a hollow fiber bundle 502b. However, CO₂-rich gas may enter the housing 502a at one side thereof and CO₂-lean gas may exit at an opposite side thereof. Regenerated or cleaned absorbent liquid may enter the housing 502a at one end thereof, and used absorbent liquid with carbon dioxide may exit the housing 502a at an opposite end thereof. As in FIG. 4A, in this embodiment, cleaned absorbent liquid flows counter (i.e., opposite) to the gas flow. However, the counter flow causes carbon dioxide to flow from the gas into the liquid in the hollow fiber bundle 502b.

FIG. 5B depicts the same flows as in FIG. 5A, but in the context of a single hollow fiber 502c that can be part of the hollow fiber bundle 502b.

FIGS. 6A-6B depict an exemplary embodiment of a stripper 608 that may be employed in the carbon dioxide

conversion system 300, for example. In FIG. 6A, the stripper 608 may include a cylindrical housing 608a that encloses a hollow fiber bundle 608b. Sweep gas may enter the housing 608a at one end thereof and contaminants (CO₂, H₂O, CH₄, and/or CO) may exit at an opposite end thereof. Used absorbent liquid with contaminants may enter the housing 608a at one side thereof, and regenerated or clean absorbent liquid may exit the housing 608a at an opposite side thereof. In this embodiment, used absorbent liquid with contaminants flows counter (i.e., opposite) to the sweep gas flow. Moreover, the counter flow causes contaminants to flow from the liquid into the gas in the hollow fiber bundle 608b.

FIG. 6B depicts the same flows as in FIG. 6A, but in the context of a single hollow fiber 608c that can be part of the hollow fiber bundle 608b.

FIGS. 7A-7B depict another exemplary embodiment of a stripper 708 that may be employed in the carbon dioxide conversion system 300, for example. As in FIG. 6A, in FIG. 7A, the stripper 708 may include a cylindrical housing 782a that encloses a hollow fiber bundle 708b. However, sweep gas may enter the housing 708a at one side thereof and contaminants may exit at an opposite side thereof. Used absorbent liquid with contaminants may enter the housing 708a at one end thereof, and regenerated or clean absorbent liquid may exit the housing 708a at an opposite end thereof. As in FIG. 6A, in this embodiment, sweep gas flows counter (i.e., opposite) to the used absorbent liquid with contaminants flow. However, the counter flow causes contaminants to flow from the liquid out from the hollow fiber bundle 708b into the gas.

FIG. 7B depicts the same flows as in FIG. 7A, but in the context of a single hollow fiber 708c that can be part of the hollow fiber bundle 708b.

According to the present invention, the liquid absorbent can meet a demanding set of criteria. The liquid can be safe and nontoxic to humans, and may not contaminate the purified air with odors or organic vapors. It may absorb carbon dioxide at the partial pressure expected during the mission, and may not lose performance when simultaneously absorbing water. It may also be regenerable without the use of space vacuum, so as not to lose CO₂ and water to space, and regenerable without using excessive temperatures or power. The liquid may be durable and last without deterioration for the life of the mission. Since the liquid also serves as the electrolyte in the electrochemical cell, it may have appreciable electrical conductivity, and it may be stable with respect to electrochemical oxidation or reduction within the potential window for the process.

The liquid absorbent can be one or more ionic liquids. They are salts, generally comprised of an anion and organic cation, which are liquid at their temperature of use. Because they are salts, they have effectively zero vapor pressure, thus eliminating odors and reducing the likelihood of contaminating the purified air. Also, because they are salts, they have good electrical conductivity. They are generally nontoxic and have sufficient stability to resist deterioration. Ionic liquids generally contain relatively large organic cations (quaternary ammonium or phosphonium compounds) and any of a variety of anions, both of which can be tailored to obtain desired characteristics. Ionic liquids can both physically dissolve carbon dioxide and have specific chemical interactions with it. Interactions of some ionic liquids with carbon dioxide and electrode surfaces favor electrochemical conversion of carbon dioxide into specific products. As a class, almost every ionic liquid is water soluble and hygroscopic, meaning that they will absorb moisture from the air, but due to their negligible volatility, the water can be

removed by evaporation either by elevating the temperature or reducing the water partial pressure. Because a very large number of ionic liquids exist, and both the cation and the anion can be tailored to obtain desired characteristics, this class of compounds has flexibility as the liquid absorbent and electrolyte for a carbon dioxide removal and conversion system.

Ionic liquids suitable for use in this invention comprise those with melting points below 20° C., low vapor pressure, and with capacity for carbon dioxide, at 30° C. and in the presence of 3.8 torr carbon dioxide partial pressure, of >0.3 wt %. Examples of such ionic liquids include 1-ethyl-3-methylimidazolium acetate, 1-ethyl-3-methylimidazolium trifluoroacetate, 1-butyl-3-methylimidazolium acetate, tributylmethylphosphonium acetate, triethylmethylphosphonium acetate etc. These ionic liquids are hygroscopic and can absorb water as well and carbon dioxide. Therefore, the effective working fluid can, in many cases, comprise a mixture of the ionic liquids specified and water. It may, under some circumstances, be useful to add water to the ionic liquid before contacting with carbon dioxide. This can reduce the carbon dioxide capacity but also reduce the viscosity.

1-butyl-3-methylimidazolium acetate (BMIM Ac) has a high CO₂ capacity and well understood physical properties. BMIM Ac satisfies the basic requirements for an absorbent in a manned vehicle. It is not a hazardous substance or mixture, and has no hazards not otherwise classified. The pH of an aqueous solution is 6.1, and the autoignition temperature is 435° C. The compound is a clear, somewhat viscous liquid, and can be handled readily. The surface tension is similar to that for a polar organic solvent, and the density is similar to that for water. The onset for thermal degradation sets the upper temperature limit for processing, and is comfortably higher than the temperature needed for desorption. The viscosity for this ionic liquid is higher than that of water, but can be reduced by raising either the temperature or water content. In normal use, the ionic liquid absorbs both CO₂ and water, and therefore the viscosity values vary in the presence of water. Viscosity plays a role in determining mass transfer rates for CO₂ adsorption and desorption. Control of viscosity can therefore reduce the weight and volume of the contactor-separator.

According to the present invention, a significant increase in O₂ recovery could be a game-changer for NASA and commercial interests pursuing travel to Mars or space habitation. Electrochemical technology may significantly decrease the amount of O₂ (and/or water) that will be required to be brought on each mission. This saves both

space on the vessel and launch weight. In addition, the present invention may require less power than alternative CO₂ conversion technologies for recovery of the same amount of O₂.

It should be understood, of course, that the foregoing relates to exemplary embodiments of the invention and that modifications may be made without departing from the spirit and scope of the invention as set forth in the following claims.

We claim:

1. A carbon dioxide conversion system for an environment that is ambient gas, comprising:
 - a scrubber downstream of the environment;
 - an electrochemical conversion cell downstream of the scrubber;
 - an ionic liquid storage intermediate the scrubber and the electrochemical conversion cell;
 - a stripper intermediate the electrochemical conversion cell and the ionic liquid storage, wherein:
 - the scrubber is configured to receive gas containing carbon dioxide from the environment, receive cleaned liquid absorbent from the ionic liquid storage, and discharge at least one of Ar, N₂, and CO to the environment, and
 - the stripper is configured to (i) use water vapor as a sweep gas, (ii) discharge cleaned liquid absorbent to the ionic liquid storage, and (iii) discharge methane to a methane storage.
2. The system of claim 1, further comprising a water vaporizer upstream of the stripper.
3. The system of claim 1, wherein the electrochemical conversion cell is configured to discharge O₂ to an oxygen storage.
4. The system of claim 3, further comprising:
 - a water extractor disposed intermediate the electrochemical conversion cell and the oxygen storage, the water extractor configured to extract water from the oxygen.
5. The system of claim 4, further comprising:
 - a water vaporizer downstream of the water extractor and configured to discharge (i) liquid water to a water storage and (ii) water vapor to the stripper.
6. The system of claim 1, wherein the scrubber is further configured to discharge used liquid absorbent having CO₂ and H₂O.
7. The system of claim 1, further comprising a heater disposed intermediate the electrochemical conversion cell and the stripper.

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