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(54) **SULFUR DIOXIDE SCRUBBING SYSTEM AND PROCESS FOR PRODUCING POTASSIUM PRODUCTS**

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(58) **Field of Classification Search**

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(57) **ABSTRACT**

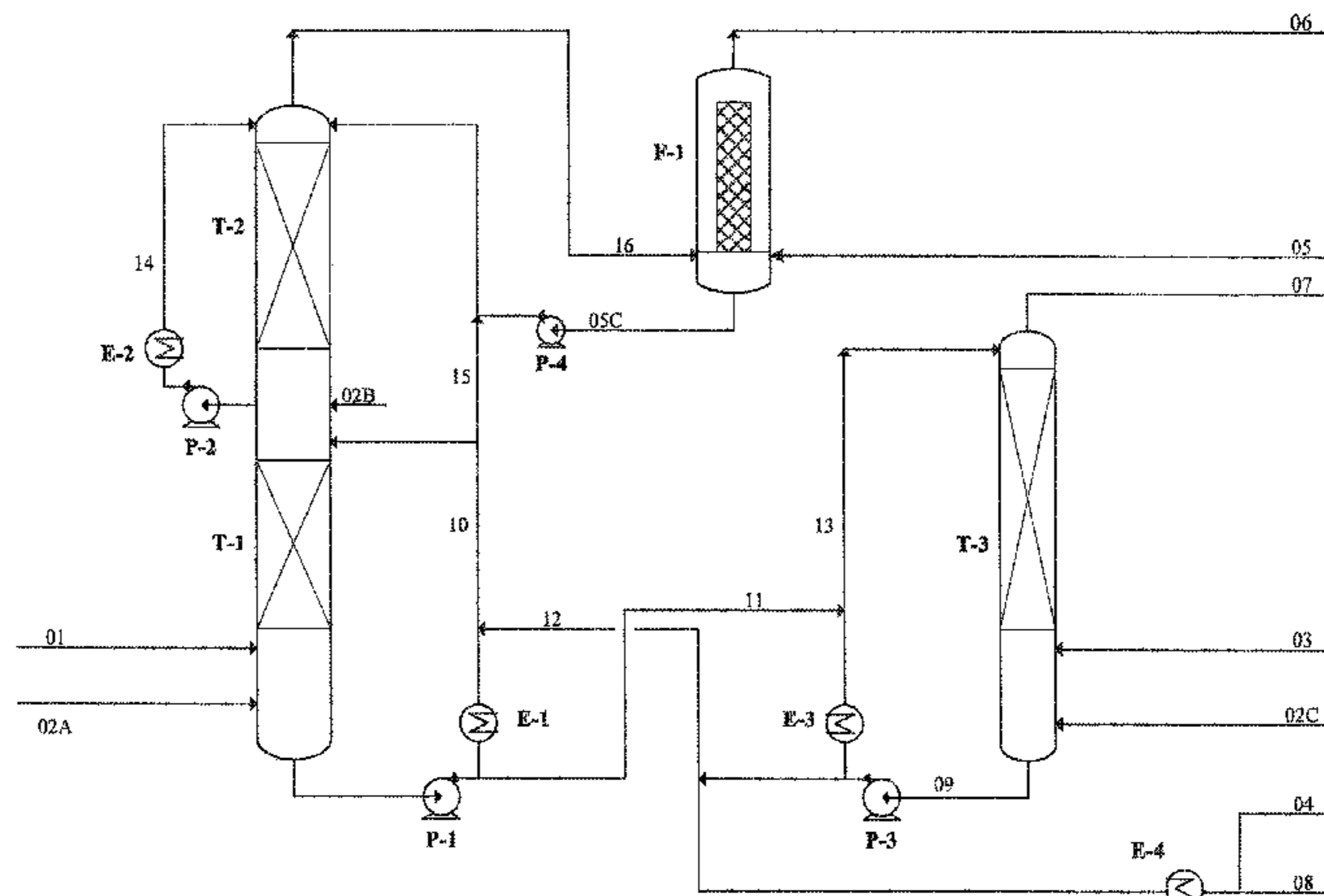
The invention relates to a process for preparing potassium thiosulfate, potassium sulfite or potassium bisulfite comprising the following steps:

Step (1a): providing a potassium hydroxide or potassium carbonate solution for neutralizing acid forming components such as dissolving SO₂ or H₂S;

Step (1b): providing an SO₂ contacting solution, containing at least some potassium sulfite or potassium bisulfite or potassium thiosulfate;

Step (2): providing SO₂ gas;

(Continued)



Step (3): reacting these to absorb the SO₂ gas and to form an intermediate reaction mixture comprising potassium sulfite, or potassium bisulfite or a mixture thereof, and optionally recovering the potassium sulfite, or potassium bisulfite or a mixture thereof, and/or optionally using steps 4 and 5;
 Step (4): adding sulfur or sulfide containing compound containing sulfur having the oxidation state of 0, -2 or of between 0 and -2 to the reaction mixture and optionally potassium hydroxide or potassium carbonate, and reacting the mixture under suitable conditions to form potassium thiosulfate; and
 Step (5): recovering the potassium thiosulfate, and optionally concentrating the potassium thiosulfate.

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22 Claims, 2 Drawing Sheets

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B01D 53/14 (2006.01)
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(58) **Field of Classification Search**
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 See application file for complete search history.

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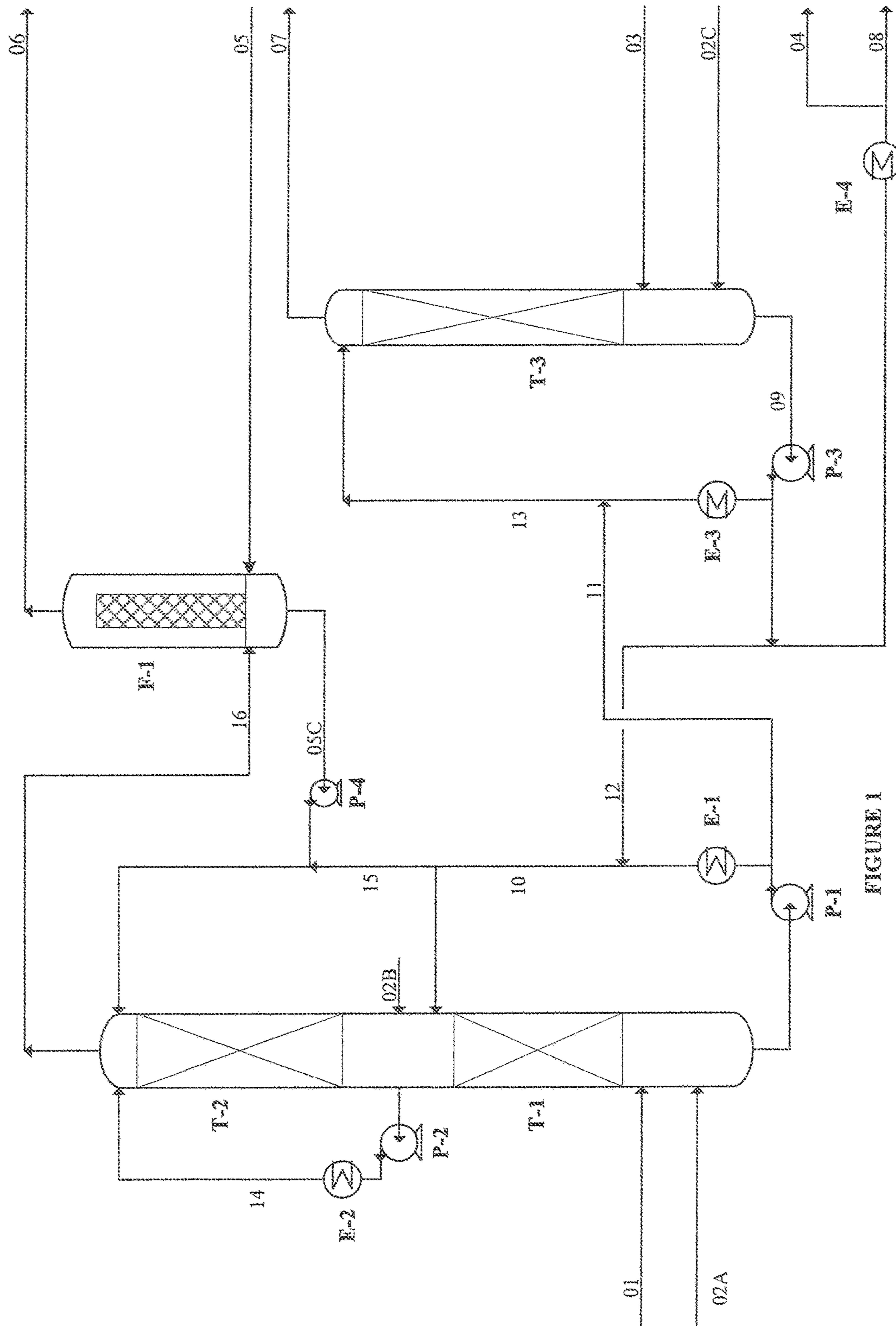


FIGURE 1

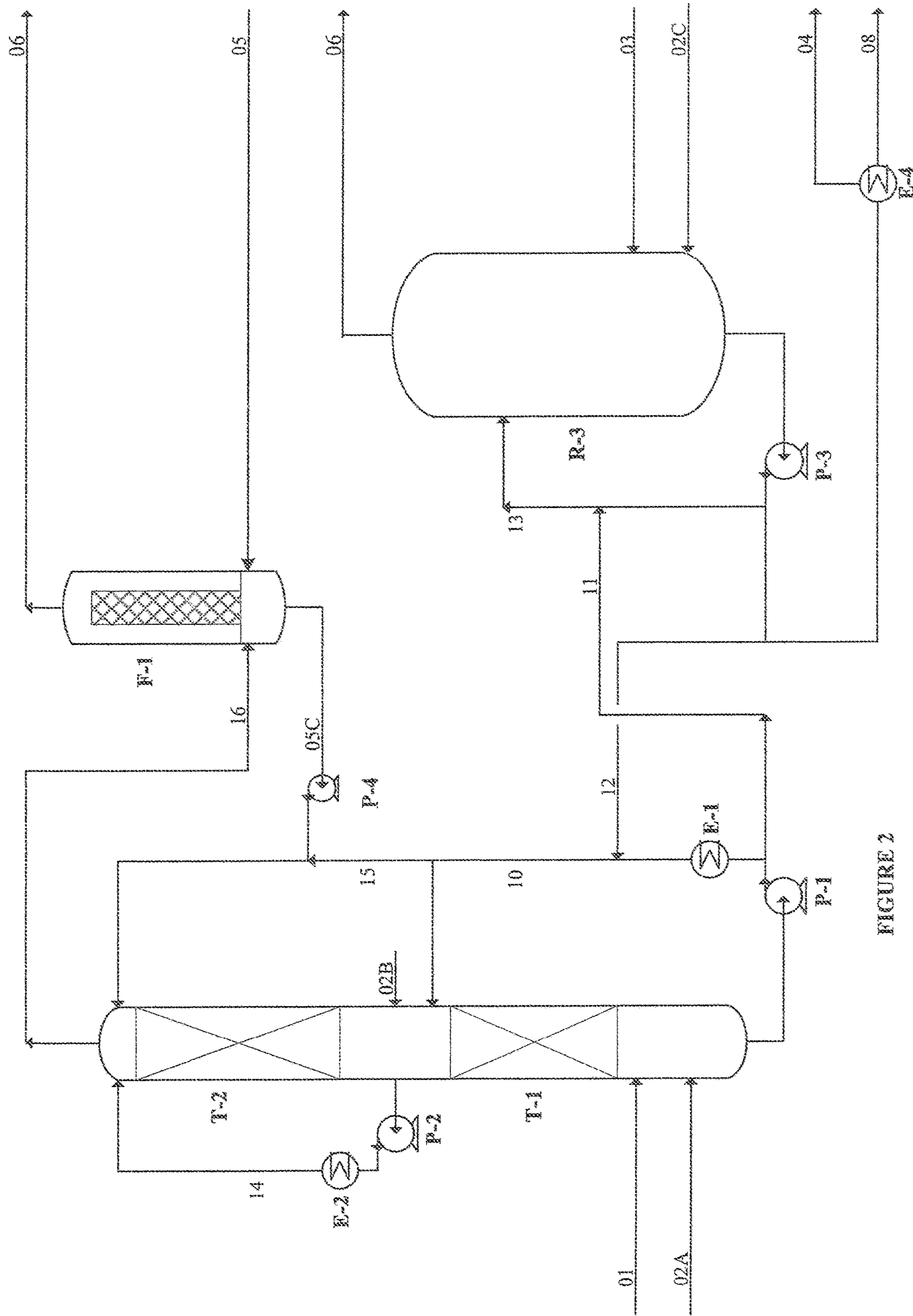


FIGURE 2

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SULFUR DIOXIDE SCRUBBING SYSTEM AND PROCESS FOR PRODUCING POTASSIUM PRODUCTS

CROSS-REFERENCE TO RELATED APPLICATIONS

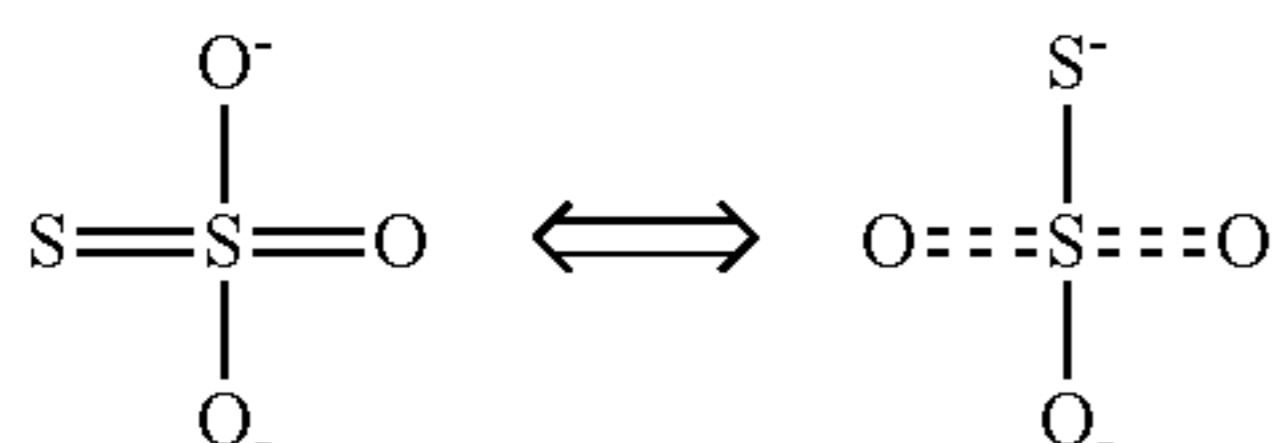
This application is a continuation of U.S. nonprovisional application Ser. No. 15/380,702 filed on Dec. 15, 2016, now U.S. Pat. No. 10,005,667, which claims priority to U.S. provisional application No. 62/273,389 filed on Dec. 30, 2015, both of which are hereby incorporated herein by reference for all that they each disclose.

FIELD OF THE INVENTION

The present invention relates to a process for the preparation of potassium thiosulfate, or potassium sulfites and/or potassium bisulfites.

BACKGROUND OF THE INVENTION

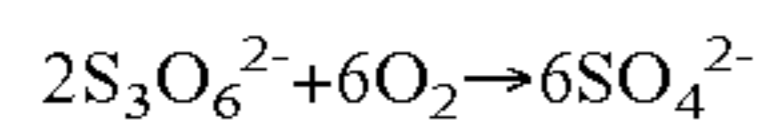
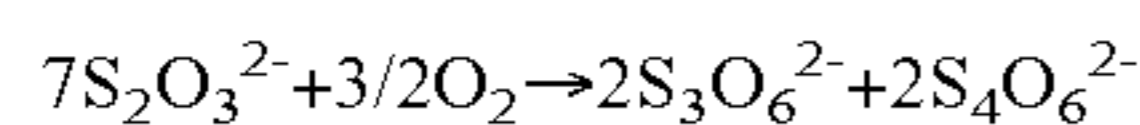
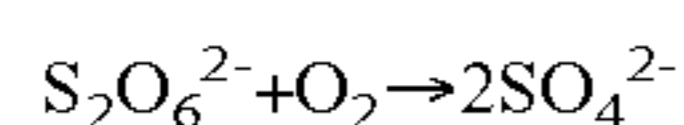
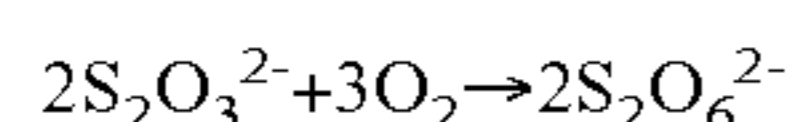
The thiosulfate ion, $S_2O_3^{2-}$, is a structural analogue of the SO_4^{2-} ion in which one oxygen atom is replaced by one S atom. However, the two sulfur atoms in $S_2O_3^{2-}$ are not equivalent. One of the S atoms is a sulfide-like sulfur atom that gives the thiosulfate its reducing properties and complexing abilities.



Thiosulfates are used in leather tanning, paper and textile manufacturing, flue-gas desulfurization, cement additives, dechlorination, ozone and hydrogen peroxide quenching, coating stabilizers, as an agricultural fertilizer, as a leaching agent in mining, and so on.

Due to these complex-forming abilities with metals, thiosulfate compounds have also been used in commercial applications such as photography, waste treatment and water treatment applications.

Thiosulfates do however readily oxidize to dithionates, trithionates, tetrathionates, and finally to sulfates:



Due to this transformation, thiosulfates are used as fertilizers in combination with cations such as ammonium, potassium, magnesium and calcium. The ammonium, alkali metal and alkaline earth thiosulfates are soluble in water. Water solubilities of thiosulfates decrease from ammonium to alkali metals to alkaline earth thiosulfates.

Potassium (K) is a primary plant nutrient. Potassium is associated with movement of water, nutrients, and carbohydrates in plant tissue. If potassium is deficient or not supplied in adequate amounts, growth is stunted and yields are reduced. Potassium stimulates early growth, increases

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protein production, improves the efficiency of water use, is vital for stand persistence in cold weather, and improves resistance to disease and insects.

Potassium thiosulfate fertilizer contains the highest percentage of potassium in liquid form, compared to other sources of potassium such as potassium chloride (KCl), potassium nitrate (KNO_3), and potassium sulfate (K_2SO_4). In addition, it combines potassium with sulfur (17%) which is also an essential plant nutrient.

It is contemplated that potassium thiosulfate could be produced by several alternative routes such as:

I. Reaction of S and SO_3^{2-} in neutral or alkaline medium

II. Reaction of S^{2-} and SO_3^{2-} (via SO_2 and HSO_3^{2-})

III. Oxidation of Potassium Hydrosulfide (KSH)

IV. Ion Exchange reaction between alkaline thiosulfates and potassium chloride or nitrate

V. Salt exchange between alkaline thiosulfates and Potassium Chloride or Nitrate

VI. Oxidation of Potassium Polysulfide

However, some of these alternatives present serious difficulties or disadvantages. Route I and II are longer processes and require the use of sulfur dioxide SO_2 . Both these routes are described when the scrubbing of the air pollutant sulfur dioxide is an objective. Route III requires handling of potassium hydrosulfide as a raw material which is not favorable due to a hydrogen sulfide environment. Routes IV and V suffer from the drawback that ion exchange and salt exchange require expensive raw materials and equipment, and also require a step of final stripping due to the need for working with dilute solutions. The prior art has been unsuccessful producing high purity potassium thiosulfate via Route VI with low byproducts. Thiosulfates, in general, are susceptible to further conversion to sulfite and sulfate under adverse temperature, and pressure.

SUMMARY OF THE INVENTION

Described herein are processes, preferably continuous, for the preparation of potassium thiosulfate in relatively high concentration with relatively low amounts of soluble or solid byproducts. The process may be used to produce a substantially clear solution having a relatively high percentage of potassium, and almost neutral pH, making it very suitable as a chlorine-free liquid fertilizer, for example as a foliar fertilizer, starter fertilizer, in furrow fertilizer and the like, and optionally in combination with other fertilizers.

Also described herein are processes, preferably continuous, for the preparation of potassium sulfite, potassium bisulfite or mixtures thereof as a substantially clear solution having a relatively high percentage of potassium and almost neutral pH, making it suitable as a liquid fertilizer, for example as a foliar fertilizer, in furrow fertilizer and the like.

Generally, the process of the present invention provides a method for preparing potassium thiosulfate, comprising the following steps:

Step (1a): providing a potassium hydroxide or potassium carbonate solution for neutralizing acid forming components;

Step (1b): providing a SO_2 contacting solution, comprising or containing at least some potassium sulfite or potassium bisulfite or potassium thiosulfate;

Step (2): providing sulfur dioxide gas;

Step (3): reacting these to absorb the SO_2 gas and to form a reaction mixture comprising potassium sulfite, potassium bisulfite or mixtures thereof, which may be sulfite rich potassium thiosulfate;

Step (4): adding sulfur or sulfide containing compound containing sulfur having the oxidation state of 0, -2 or of between 0 and -2 to the reaction mixture and optionally potassium hydroxide or potassium carbonate, and reacting the mixture under suitable conditions to form potassium thiosulfate; and

Step (5): recovering the potassium thiosulfate and, optionally concentrating the potassium thiosulfate.

Furthermore, the present invention provides a process for preparing potassium sulfite, potassium bisulfite or a mixture thereof, comprising the following steps:

Step (1a): providing a potassium hydroxide or potassium carbonate solution for neutralizing-acid forming components;

Step (1b): providing a SO₂ contacting solution, comprising at least potassium sulfite;

Step (2): providing sulfur dioxide gas; and

Step (3): reacting these to form a reaction mixture comprising potassium sulfite, or potassium bisulfite or a mixture thereof, and recovering the potassium sulfite, or potassium bisulfite or a mixture thereof.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a schematic representation of a process according to an embodiment of the invention.

FIG. 2 is a schematic representation of a process according to yet another embodiment of the invention.

DETAILED DESCRIPTION OF THE INVENTION

It is an object of the present invention to provide a method for production of potassium thiosulfate by reaction of an intermediate with a sulfite/bisulfite composition wherein relatively inexpensive raw materials, such as sulfur, water, sulfur dioxide and hydrogen sulfide gas are used, and wherein relatively high purity potassium thiosulfate can be obtained. Potassium hydroxide, potassium carbonate, potassium polysulfide, potassium sulfide or potassium bisulfide are other raw materials that may be used in this approach.

It is another objective of the present invention to produce a concentrated potassium thiosulfate solution.

It is still another objective of this invention to produce potassium thiosulfate with relatively low residual contamination from byproducts, in particular soluble or solid byproducts.

It is still another objective of the present invention to produce potassium thiosulfate by a continuous operation approach.

It is still another objective of the present invention to produce potassium thiosulfate by using waste gas, such as hydrogen sulfide, and converting the waste gas to sulfur or sulfur dioxide or for direct absorption for this operation.

It is still another objective of the present invention to use sulfur dioxide as pristine gas by burning sulfur with oxygen or by using sulfur dioxide from waste tail gas operations or coke operations or flue gas containing sulfur dioxide.

It is still another objective of the present invention to provide a method which allows production of a stable potassium thiosulfate product of close to neutral pH, and with a shelf life sufficient for commercial use.

One or more of the objectives as described above are obtained with the processes as described below. Also, one or more of said objectives are obtained with the apparatus as described below.

One or more of the objectives as described above are obtained with the process according to the present invention, describing (preferably continuous) processes for the preparation of potassium thiosulfate in relatively high concentration with relatively low amount of soluble contaminants such as sulfite, and sulfate.

In a preferred embodiment, controlling process parameters such as mole ratio of the raw materials, pH, temperature, concentration and composition of the intermediate potassium sulfite/bisulfite can result in a preferred clear solution with a high percentage of potassium in liquid form. The liquid may have an almost neutral pH, which makes this suitable as a liquid fertilizer, such as a foliar fertilizer. The potassium thiosulfate may be used as such, or in admixture with other compatible fertilizers, micronutrients, additives, and/or the like.

One or more of the objectives as described above are obtained with the processes according to the present invention describing preparation of potassium thiosulfate from an intermediate rich in sulfite and preferably under appropriate conditions, and using preferred mole ratios of raw materials, producing a liquid solution of potassium thiosulfate in relatively high concentration with relatively low amounts of solid or soluble byproducts.

Generally, the process for preparing potassium thiosulfate of the present invention comprises the following steps:

Step (1a): providing a potassium hydroxide or potassium carbonate solution for neutralizing acid forming components;

Step (1b): providing a SO₂ contacting solution, comprising or containing at least some potassium sulfite or potassium thiosulfate;

Step (2): providing sulfur dioxide gas;

Step (3): reacting these (i.e., the potassium hydroxide or potassium carbonate, the SO₂ contacting solution and the SO₂ gas) to form a reaction mixture comprised of potassium sulfite, or potassium bisulfite or a mixture thereof. (The reaction mixture may be sulfite rich potassium thiosulfate);

Step (4): adding (i) sulfur and/or (ii) hydrogen sulfide and/or (iii) potassium polysulfide and/or (iv) potassium sulfide and/or (v) potassium bisulfide to the reaction mixture, and reacting the mixture under suitable conditions to form potassium thiosulfate; and

Step (5): recovering the potassium thiosulfate and optionally concentrating the potassium thiosulfate.

Recovering the potassium thiosulfate means separating the potassium thiosulfate from the process to obtain a product that can be stored, transported and sold.

The process for preparing potassium thiosulfate provides a preferably continuous non-regenerative sulfur dioxide scrubbing system and process for the production of potassium products including potassium thiosulfate.

The above described process steps 1-3 can also be used to provide potassium sulfite, or potassium bisulfite or a mixture thereof. Recovering said potassium sulfite, or potassium bisulfite or a mixture thereof means separating said product from the process to obtain a product that can be stored, transported and sold.

The SO₂ provided in the process may originate from any source, which includes for example: burning sulfur with oxygen; sulfur dioxide from tail gas, coke operations, or by converting hydrogen sulfide to sulfur dioxide, or from flue gas of other processes containing SO₂.

In addition to producing potassium products, the SO₂ gas scrubbing and absorption system may be utilized as a Tail Gas Treating Unit (TGTU) or as a Flue Gas Desulfurization

(FGD) system for emissions control by treating and cleaning gas streams containing acidic sulfur components and other acidic gas components before being discharged to atmosphere.

In one embodiment, the present invention utilized as a Flue Gas Desulfurization (FGD) and/or Tail Gas Treating Unit (TGTU) relates to a continuous process and recovery system for the recovery of sulfur dioxide (SO₂) contained in combustion gas streams for the purpose of limiting SO₂ gas emissions and for the purpose of producing products containing sulfur and potassium.

The SO₂ which is reacted is not regenerated as SO₂, but is recovered as potassium sulfite/bisulfite mixture, and/or potassium thiosulfate, solution products containing sulfur and potassium; these products can be used as agricultural fertilizers, or can be used for other purposes.

The process may include control of SO₂ gas generation and production to control production rate of products to meet market demand and to control O₂, SO₃ and NO_x concentrations in SO₂ gas for low sulfate generation and low vent stack gas emissions.

The process may include additional process steps for removal of excess water in a SO₂ gas Quench Tower and/or in an evaporator/concentrator, preferably at the end of the process, such as for example an evaporator/concentrator to concentrate the potassium thiosulfate if necessary.

Small amounts of sulfate as SO₃ generated in combustion processes producing SO₂ gas may be partially removed along with excess water in the SO₂ gas Quench Tower as dilute sulfuric acid; the sulfuric acid may then be utilized in other process equipment such as pH control of cooling tower or may be neutralized and discharged as waste water.

Further sulfate removal from potassium sulfite, or potassium bisulfite or a mixture thereof and/or potassium thiosulfate products, if necessary, may be done in the product filtration step of the process, to remove solid crystals of potassium sulfate which have low solution solubility in the concentrated potassium sulfite, or potassium bisulfite or a mixture thereof solution and/or potassium thiosulfate product solution.

With proper design and control of the combustion system and the SO₂ recovery system, it is possible to limit oxidation of SO₂ and sulfite in the SO₂ recovered products resulting in products low in sulfate. The SO₂ gas stream contaminants which may be either wholly or partially eliminated or removed include but are not limited to: O₂, SO₃, NO_x, HCl, H₂O and fly ash.

Potassium hydroxide or another base-potassium source like potassium carbonate is used (step 1a) as the alkaline feed for process reactions, pH control and the source of potassium for the process and potassium products produced. Potassium hydroxide is the preferred alkaline feed and source of potassium for the process.

The potassium base is used for neutralizing acid forming components such as SO₂ or H₂S.

The potassium base is preferably used as a solution, such as for example 0.1 Molar to 13.5 Molar solution. Preferably, the solution has a concentration of about 5 to 13.5 Molar. Optionally, a base-potassium source solution is formed by combining dry or solid potassium hydroxide or potassium carbonate with water. The dry or solid potassium hydroxide or potassium carbonate may be in any suitable form, such as beads, flakes or pellets.

Either a solution of potassium sulfite, or potassium bisulfite or a mixture thereof or a potassium thiosulfate solution (or a mixture comprising potassium thiosulfate with potassium sulfite and/or potassium bisulfite) may be utilized

as the primary SO₂ scrubbing solution (step 1b) in a SO₂ absorber to scrub and absorb SO₂ from a gas stream containing SO₂ to produce scrubbing solution containing potassium sulfite/bisulfite.

The primary SO₂ scrubbing solution is typically a concentrated recirculating solution of potassium sulfite, or potassium bisulfite or a mixture thereof formed from the addition of SO₂, potassium hydroxide and dilute potassium sulfite, or potassium bisulfite or a mixture thereof or water from other process streams.

Alternatively, concentrated potassium thiosulfate from a downstream reactor may be recycled to the absorption tower if the hot SO₂ gas is used to evaporate excess water, or in the case there is excess alkalinity in the potassium thiosulfate in the downstream reactor which can be carried forward to the absorption tower, or in the case where reduced oxidation to sulfate is desired.

A secondary SO₂ scrubbing step in 2nd Stage SO₂ Scrubber may be utilized for additional SO₂ absorption and recovery. Optionally, a final gas treating step using fiber bed gas filters may be utilized to filter out sulfur containing particulates, for additional control of vent stack gas emissions.

In one embodiment, where dilute solution of potassium sulfite, or potassium bisulfite or a mixture thereof from other places in the process is added to the primary SO₂ scrubbing solution, a concentrated solution of potassium sulfite, or potassium bisulfite or a mixture thereof is obtained. This concentrated solution of potassium sulfite, or potassium bisulfite or a mixture thereof may be marketed as the potassium product or may be further processed to produce the potassium thiosulfate product.

The total potassium salt concentration of this concentrated solution of potassium sulfite, or potassium bisulfite or a mixture thereof is preferably about 35-41 wt % potassium sulfite, potassium bisulfite and potassium sulfate, even more preferably about 38-40 wt % total salt solution concentration. The pH preferably is between about 7 to about 8.5.

In another embodiment, a potassium thiosulfate solution may be utilized as the primary SO₂ scrubbing solution to scrub and absorb SO₂, thereby producing a sulfite rich potassium thiosulfate solution that may be further processed to produce potassium thiosulfate product solution that is low in sulfite and sulfate content. This sulfite rich potassium thiosulfate solution contains potassium sulfite, potassium bisulfite and potassium thiosulfate; the relative amount of potassium sulfite and potassium bisulfite being dependent on the pH.

The process may include process steps for reacting intermediary products of potassium sulfite, or potassium bisulfite or a mixture thereof or sulfite rich potassium thiosulfate in a sulfur reactor, H₂S gas contactor/reactor, or potassium polysulfide, sulfide, or hydrosulfide reactor to produce potassium thiosulfate that is low in sulfite.

In one embodiment (embodiment i), sulfur may be added to the process in a sulfur reactor for the purpose of converting the SO₂ recovery product (the potassium sulfite, or potassium bisulfite or a mixture thereof product obtained after step 3) to potassium thiosulfate product.

In another embodiment (embodiment ii), sulfur may also be added as H₂S from H₂S acid gas streams and H₂S from hydrocarbon gas streams typically generated in oil refineries and gas plants. The H₂S component in these gas streams may be contacted, absorbed and reacted to also produce the potassium thiosulfate product. When contacting, absorbing and reacting H₂S contained in hydrocarbon gas streams, the

present invention may be utilized as a replacement for amine units typically used for H₂S removal and recovery.

In a further embodiment, sulfur is provided as a sulfide, as in embodiment (iii) a potassium polysulfide; embodiment (iv) potassium sulfide; or embodiment (v) potassium bisulfide, wherein any of these sulfur compounds is contacted with the solution of potassium sulfite, or potassium bisulfite or a mixture thereof or a potassium thiosulfate solution containing sulfite, for reaction of the polysulfide, sulfide or bisulfide with sulfite to form additional thiosulfate.

Generally, the conversion of sulfite/bisulfite intermediate (i.e., the potassium sulfite, or potassium bisulfite or a mixture thereof) to produce the potassium thiosulfate product takes place at near atmospheric pressure in a sulfur reactor or in an H₂S contactor at H₂S containing gas pressure, or in a liquid-liquid reactor, as the sulfide generally is liquid.

Additional sulfur may also be added to a sulfur/sulfide burner, to increase SO₂ production.

The potassium thiosulfate product is particularly suitable as a chlorine-free potassium plant nutrient with a very high potassium concentration in liquid form which can be applied through all types of irrigation systems with no plugging of the drip lines. The liquid could also be converted to form crystalline solid potassium thiosulfate. However, the potassium thiosulfate preferably is used in liquid form.

The potassium product obtained with the process as described above preferably is a fertilizer product, and more preferably a liquid fertilizer product.

The present invention provides a process for preparing a highly concentrated solution of potassium thiosulfate (K₂S₂O₃), of which the amount generally is about 40-56 wt %, preferably about 48-56 wt % and most preferably about 50-56 wt %.

The thiosulfate can be of relatively high purity, and the amount of products other than potassium thiosulfate and water is about 5 wt % or less, preferably about 2 wt % or less. Particular impurities are preferably as follows: generally, the amount of sulfate is about 1 wt % or less (measured as potassium sulfate), preferably, about 0.8 wt % or less, and even more preferable about 0.4 wt % or less. Generally, sulfite is present in an amount of about 1 wt % or less, preferably about 0.7 wt % or less (measured as potassium sulfite). Generally, sodium is present in an amount of about 1 wt % or less.

Preferably, the process is performed in such a way that the described products of such good quality can be obtained.

The relatively low amount of other products allows the potassium thiosulfate to have a good storage stability. The preferred storage stability is at least half a year or more, preferably 1 year or more, and even more preferably 2 years or more at ambient temperature. Storage stable means that the liquid remains clear, i.e., no crystals or deposition is visible with the naked eye.

Preferably, the intermediate, sulfite/bisulfite mixture is formed at such a pH that the composition of intermediates favors a high amount of sulfite presence. In one embodiment, the intermediate potassium sulfite/bisulfite is provided at a high pH, which maximizes SO₂ absorption but is low enough to prevent the absorption of carbon dioxide, if present in these SO₂ waste gas streams.

The high amount of sulfur and potassium in both the intermediary potassium sulfite, or potassium bisulfite or a mixture thereof and in the potassium thiosulfate product is controlled by controlling the solution concentrations. The solution concentrations are controlled by controlling the water content of the product solutions. The water content of the product solutions is controlled by controlling one or

more of three process control variables. One is direct control of water addition to the process. The second is removal of water from the process by condensing water out of the SO₂ gas stream. The amount of total sulfur, calculated as potassium sulfite, in the potassium sulfite, or potassium bisulfite or a mixture thereof or sulfite rich potassium thiosulfate solution, which is withdrawn from the scrubbing section for reaction with sulfur or sulfide, is generally between about 20 wt % and 41 wt %, preferably between about 30 wt % and 41 wt %. The third process control variable to control water content is concentration by evaporation/boiling of water out of the products. Concentrating would preferably be done on the final potassium thiosulfate product but may also be done on the potassium sulfite, or potassium bisulfite or a mixture thereof product.

This non-regenerative SO₂ absorption and recovery system is less complex and less costly to build and operate than other, regenerative SO₂ recovery processes or other TGTU's such as SCOT units. This is because there is no need for processing to regenerate SO₂ or the SO₂ absorption agent used to absorb SO₂, or for conversion to H₂S for amine absorption, regeneration and recycle as is done in SCOT TGTU's. Both SO₂ and potassium absorption agent are incorporated into sulfur and potassium containing products that have market value primarily as agricultural fertilizers, preferably liquid fertilizer, such as preferably a fertilizer for foliar spray.

DESCRIPTION OF FURTHER PREFERRED EMBODIMENTS OF THE INVENTION

FIG. 1 is a schematic process scheme according to the process of the present invention.

FIG. 2 is another schematic process scheme according to the present invention.

The schemes set forth in FIGS. 1 and 2 will be referred to in the detailed description below. The lines and unit numbers have the following meaning, while same numbers in FIGS. 1 and 2 have the same meaning:

Processing Units are denoted with the following numbers in the two schemes:

T1: Scrubber of SO₂ containing gas

T2: Second scrubber of SO₂ containing gas, coming from T1

T3: packed absorber tower for potassium bisulfite reaction with polysulfide, sulfide, hydrosulfide, sulfur or H₂S

F1: fiber bed Gas Filter

R3: Sulfur reactor for reaction of liquid sulfur with potassium bisulfite/potassium thiosulfate

E1, E2, E3, E4: Heat exchangers

P1, P2, P3, P4: Pumps

The following lines numbers represent piping as follows in both schemes:

01: SO₂ containing gas

02A, 02C, 02C: potassium hydroxide or potassium carbonate solution

03: elemental sulfur feed or H₂S feed gas or polysulfide or sulfide or hydrosulfide stream

04: evaporated water stream

05: water feed

05C: process water from F1

06: vent stack gas stream

07: CO₂ vented from the reactor

08: concentrated potassium thiosulfate or potassium bisulfite

09: potassium thiosulfate solution

10: potassium bisulfite or potassium thiosulfate-SO₂ absorption solution

11: mixture of potassium sulfite and potassium bisulfite solution

12: potassium bisulfite or potassium thiosulfate-SO₂ absorption solution

13: recycle stream in H₂S absorption

14: recycle stream for SO₂ absorption

15: potassium bisulfite or potassium thiosulfate-SO₂ absorption solution

16: vent stack gas stream

The preferred embodiment of the invention involves a multi-step process for converting sulfur dioxide into the final potassium thiosulfate product.

An optional preliminary step involves pretreating the sulfur dioxide combustion gas feed stream in a Quench Tower to cool the gas, condense out excess water and remove some of the other acidic gas components such as sulfuric and hydrochloric acid.

The first steps involve absorption and reaction of the sulfur dioxide gas component from the combustion gas stream (step 2) into a solution containing potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate (step 1b), while utilizing potassium hydroxide or potassium carbonate as the alkaline absorption agent (step 1a) to provide a potassium sulfite, or potassium bisulfite or a mixture thereof product (step 3).

The next step (step 4) involves reaction of the sulfite (SO₃²⁻), that may be present in the form of bisulfite (HSO₃⁻), with either sulfur, hydrogen sulfide, potassium polysulfide, potassium sulfide or potassium hydrosulfide as an alternative source of sulfur.

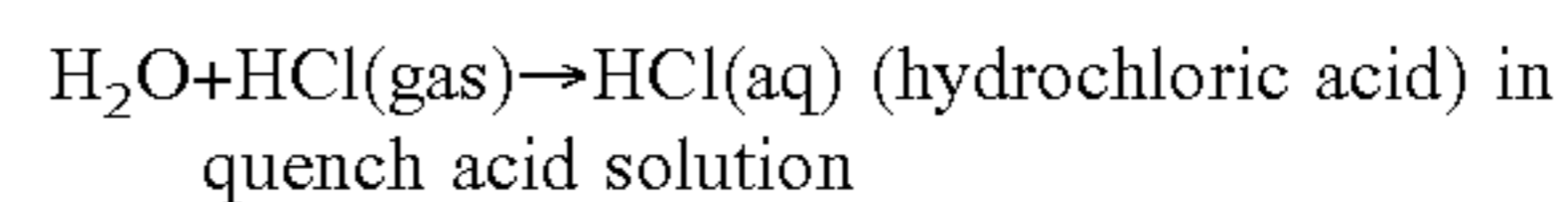
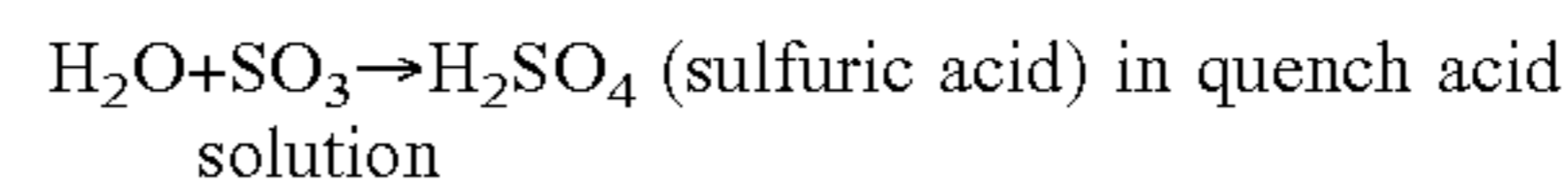
The reaction product formed is potassium thiosulfate (K₂S₂O₃), as described in step 5. Potassium thiosulfate is a highly water soluble potassium salt containing two sulfur atoms, making potassium thiosulfate solution high in sulfur content. Optionally, the potassium thiosulfate solution can be concentrated by boiling or evaporating excess water out of solution to produce a concentrated potassium thiosulfate solution or dry potassium thiosulfate product.

The SO₂ feed gas formed upstream of the potassium thiosulfate process may be from several different sources including but not limited to (i) incineration of Claus off-gas from refinery and gas plant sulfur recovery units (SRUs), (ii) incineration of sulfur bearing solids, liquids or gasses including H₂S/Acid Gas streams, (iii) SO₂ streams from regenerative SO₂ recovery processes, (iv) pure or concentrated SO₂ from other SO₂ generation processes and (v) SO₂ in flue gas from another combustion or incineration process. The total available quantity of SO₂ in the SO₂ feed gas sets the amount of potassium thiosulfate product that may be produced.

In a preferred embodiment, additional sulfur bearing feeds may be added to the upstream combustion process for the purpose of controlling and increasing production rate to meet market demand for the potassium thiosulfate and or potassium sulfite, or potassium bisulfite or a mixture thereof products produced. Preferably, the combustion process is carried out in incineration and waste heat recovery process equipment that controls and limits the amount of excess oxygen in the SO₂ gas stream (01). Limiting excess oxygen reduces further oxidation of SO₂ and the absorbed SO₂ as sulfite to sulfate.

Preferably, in a preliminary process step, SO₂ is pretreated. In such pretreatment, the SO₂ feed gas is cooled and excess water is condensed. Furthermore, preferably, the SO₂ is scrubbed to remove acidic and or particulate components

from the hot SO₂ combustion gas. Although this process step is preferred, it is not a process requirement. In case such step is applied, this is preferably done in a Quench Tower utilizing the dilute acid solution formed from the condensation of water vapor present in the SO₂ feed gas along with acid components that may also be present.

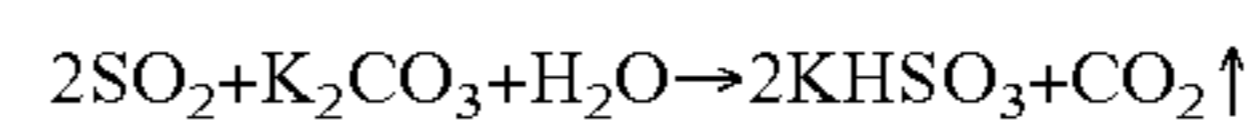
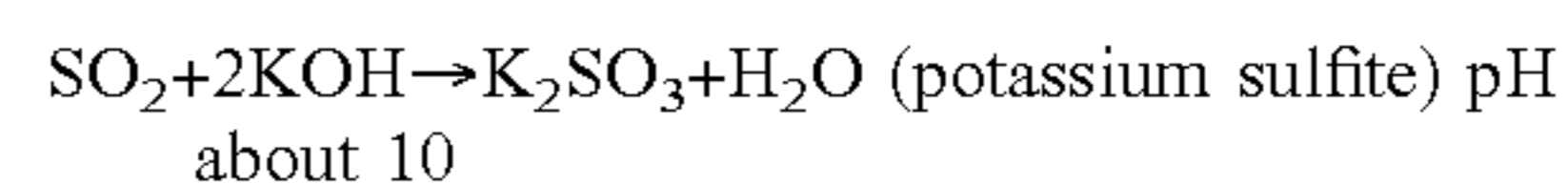
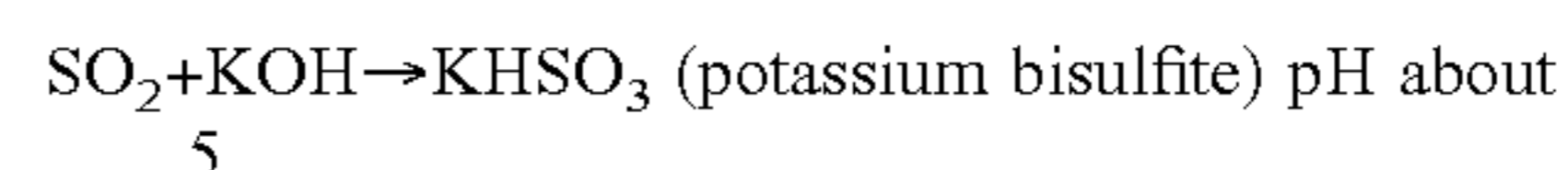


The Quench Tower typically utilizes a circulation pump to circulate the dilute acid solution through a heat exchanger and to the gas/liquid contact zone inside the Quench Tower in order to contact, scrub and cool the SO₂ feed gas. The Quench Tower may alternatively be any kind of gas/liquid contacting process equipment including but not limited to spray, packed or tray tower, venture scrubber, inline spray or inline static mixer. As explained, the process objective is to cool the hot SO₂ combustion gas, condense excess water and to scrub gas for acidic gas components such as sulfuric and hydrochloric acids which would add undesirable components to the final potassium thiosulfate and or potassium sulfite, or potassium bisulfite or a mixture thereof product. In cases where there is little or no excess water vapor in the SO₂ feed gas to be condensed, process water may be added. Process water may also be added to dilute acid concentration in Quench Tower to limit corrosion.

Preferably the SO₂ gas is cooled to about 50° C. (120° F.) or less but higher temperatures may be acceptable depending on the desired distribution and balance of water in the process. The dilute acid formed may be utilized for its acid content in another application or it may be neutralized and disposed of as waste water. The SO₂ in the SO₂ feed gas is slightly soluble in the dilute acid formed and represents a very minor loss of SO₂ to the rest of the process. If desired this minor amount of SO₂ can be recovered from the dilute acid using a stripping process for SO₂ recovery.

For SO₂ feed gas formed from combustion of a concentrated sulfur source such as elemental sulfur there is very little or no water vapor formed and no water would be condensed in the Quench Tower. In this case water may be added if cooling and scrubbing is desired. The Quench Tower may also incorporate gas filters to further remove acid fume particles. In any case, the quench operation may be omitted in favor of downstream process alternatives for cooling and removal of excess water and contaminants.

The next process step recovers the SO₂ component from the SO₂ gas stream (01) to form a solution composed of a mixture of potassium sulfite and potassium bisulfite solution (11) referred to as potassium sulfite, or potassium bisulfite or a mixture thereof. The ratio of sulfite to bisulfite depends on solution pH controlled by the addition of potassium hydroxide or potassium carbonate from stream (02A).



The pH of the solution of potassium sulfite, or potassium bisulfite or a mixture thereof may be controlled over a broad range from about pH 5 to about pH 10 with potassium hydroxide but has preferably a pH of between about 7-9, and more preferably, a pH between about 8.0-8.5 to enhance SO₂

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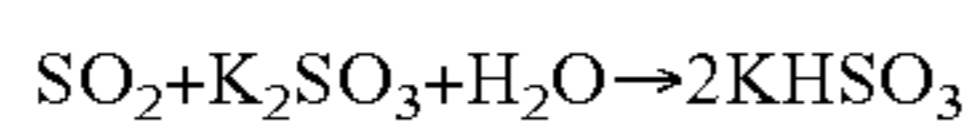
absorption efficiency, reject CO₂ absorption and increase solution solubility. If no CO₂ is present a pH of up to about 10 may be controlled for maximum solution concentration allowing potassium thiosulfate production with sulfur reaction in R-3 as concentrated potassium thiosulfate without the use of evaporator, E-4.

If potassium carbonate is used the pH preferably is limited to less than about 9, more preferably less than about 8.5 to enable disengagement of CO₂ from the carbonate in solution. There is however the ability to disengage some remaining CO₂, if any, in the third and fourth process steps.

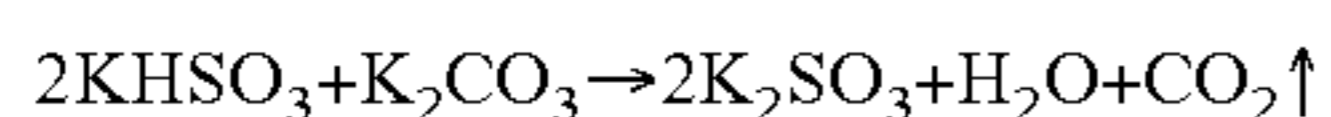
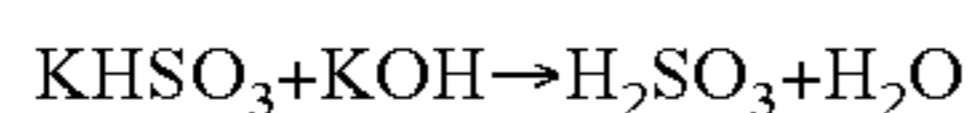
The SO₂ gas is contacted by the solution of potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution in the SO₂ Absorber (T-1) where gas/liquid contact results in the absorption and reaction of SO₂ from the SO₂ gas stream. T-1 typically utilizes a circulation pump, P1 to circulate the potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution through a heat exchanger E-1 and to the gas/liquid contact zone in order to contact and absorb SO₂ from the SO₂ feed gas stream (01).

The SO₂ Absorber may alternatively be any kind of gas/liquid contacting process equipment including but not limited to spray, packed, tray or bubble tower, venture scrubber, inline spray or inline static mixer.

Both the absorption and reaction of SO₂ with solution of potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution produces heat which is removed by the SO₂ Absorber Cooler (E-1). The reaction is primarily with the more alkaline potassium sulfite component in the potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution to form additional potassium bisulfite at a lower solution pH:



The solution of potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution pH is controlled with the addition of potassium hydroxide or potassium carbonate from stream (2A) which adds alkalinity back into the potassium sulfite, or potassium bisulfite or a mixture thereof solution to form more potassium sulfite:



Cooling may be controlled to operate T-1 at any process temperature from about 10-95° C. (50-200° F.) depending on chosen process objectives.

Preferably temperatures are controlled to about 60° C. (140° F.) or less to limit water vapor in vented gas stream. Limiting water vapor in gas reduces the steam plume (condensed water vapor) in the final vent gas that is typically discharged to atmosphere through a vent stack. If steam plume formation from warm water vapor saturated vent gas mixing with cooler atmospheric air is not an environmental issue then, higher T-1 operating temperatures may be utilized in order to allow excess water to leave the process with the vent gas. This can eliminate the use of a Quench Tower for excess water removal and even eliminate the need for E-1 and E-2 cooling requirements. In this case process temperature is controlled by cooling from natural evaporation of water as water vapor from the solution of potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate solution. This would also help to produce a more concentrated solution potassium sulfite, or potassium bisulfite or a mixture thereof or potassium thiosulfate with sulfite solution.

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To the solution of potassium sulfite, or potassium bisulfite or a mixture thereof (or potassium thiosulfate with sulfite) in T-1 process water from stream (05) can be added to the process which feeds forward to T-2 and then to T-1. T-1 may be any suitable process equipment for gas/liquid contacting but is preferably a contacting spray or packed bed tower.

The addition of a second stage gas contactor, SO₂ Scrubber (T-2) may be required for extended contacting of the SO₂ gas stream for additional SO₂ recovery and removal. This allows for very low loss of SO₂ with vent gas so very low SO₂ emissions are obtained in the vent gas discharged to atmosphere. T-2 operates as a gas/liquid contactor in the same manner as T-1.

In one embodiment, the scrubbing solution is a dilute or weak potassium sulfite, or potassium bisulfite or a mixture thereof solution. The solution pH may be controlled with the addition of potassium hydroxide or carbonate from stream (02B) over a broad range of pH from about 5-10 but preferably about 7-9 and more preferably about 8.0-8.5 to enhance SO₂ absorption efficiency and reject CO₂ absorption. The dilute solution of potassium sulfite, or potassium bisulfite or a mixture thereof generated passes to and becomes part of T-1 potassium sulfite, or potassium bisulfite or a mixture thereof solution. The produced T-1 potassium sulfite, or potassium bisulfite or a mixture thereof solution is considered an intermediate product that undergoes further processing in the third process step to become potassium thiosulfate. However, potassium sulfite, or potassium bisulfite or a mixture thereof may also be taken off from the process as a separate product.

In another embodiment, the scrubbing solution contains potassium thiosulfate, and optionally some potassium sulfite, or potassium bisulfite or a mixture thereof. The pH preferences as described in the former paragraph apply equally.

In a further embodiment, a last process operation of the step to recover SO₂ and clean the gas before discharge to atmosphere is to filter the gas through fiber bed Gas Filter (F-1). This Gas Filter has proven to be useful in addition to gas contacting in the Quench Tower, T-1 and T-2 because of some residual submicron acid fume particles remaining in the gas stream that are not absorbed into solution. This dilute acid collected by the Gas Filter may be fed forward with process water as shown in the schemes 1 and 2, or may alternatively be drawn off separately for use as dilute acid or neutralized for waste water disposal.

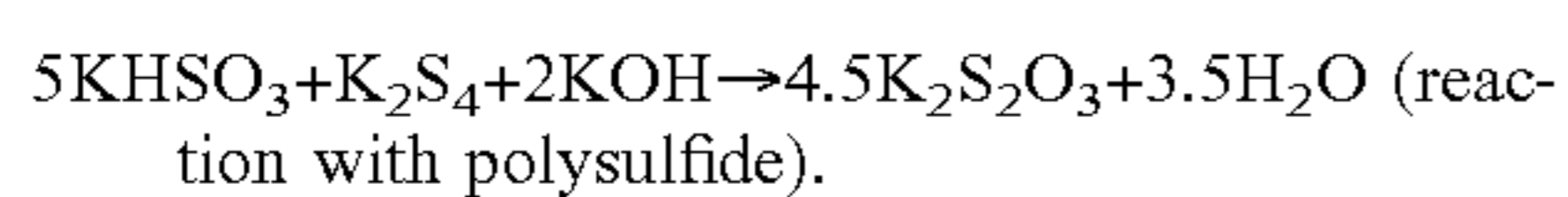
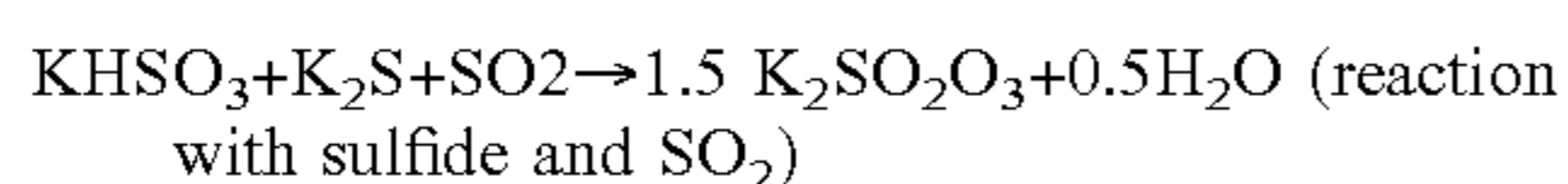
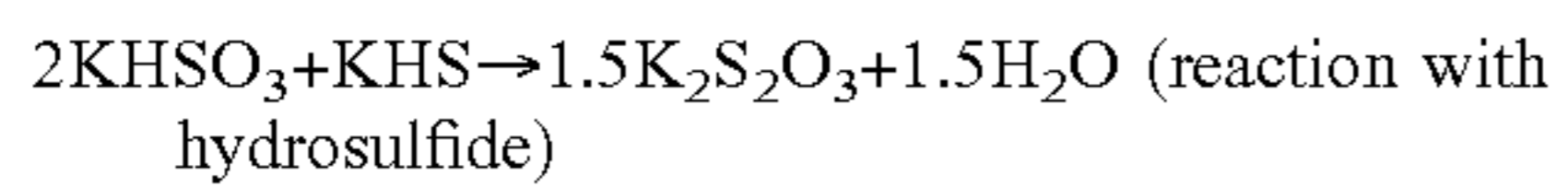
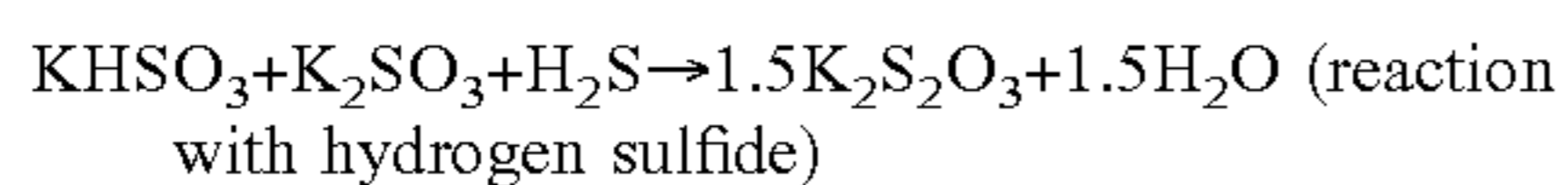
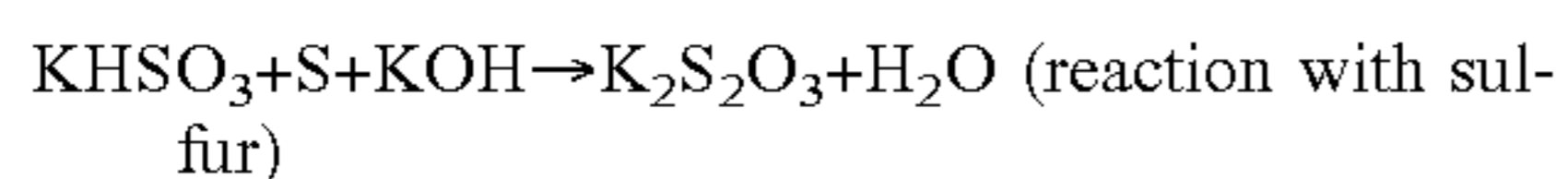
The next process step (step 4) involves conversion of potassium sulfite, or potassium bisulfite or a mixture thereof (which may also be sulfite rich potassium thiosulfate) produced in the SO₂ absorption process step, to potassium thiosulfate, by way of reaction with additional sulfur.

The additional sulfur may be elemental sulfur having a chemical valence of 0. The additional sulfur may also be hydrogen sulfide sulfur having a chemical valence of -2 as a gas or as a liquid in a potassium-based solution as potassium sulfide and or potassium hydrosulfide. The additional sulfur may also be a mixture of elemental and hydrogen sulfide sulfur with potassium hydroxide as potassium polysulfide, which may have an average valence between 0 and -2.

Additional potassium hydroxide or potassium carbonate may be added as required to maintain potassium thiosulfate reaction product pH and in the case where potassium thiosulfate reaction product has elevated pH with excess KOH from reaction with potassium sulfide the potassium thiosulfate can be recirculated to T-1 for reaction with SO₂ to lower pH and consume excess KOH.

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The chemical reactions to produce potassium thiosulfate may be represented by the chemical equations:



In one embodiment (embodiment i), in this process step (step 4) potassium sulfite, or potassium bisulfite or a mixture thereof or sulfite rich potassium thiosulfate is reacted with additional elemental sulfur. This step can be carried out in any process equipment that promotes contacting of reaction mixture with elemental sulfur. The potassium thiosulfate/sulfur reactor (R-3) is preferably a Continuously Stirred Tank Reactor (CSTR).

The elemental sulfur feed, stream (03) may be either solid or liquid/molten sulfur but preferably molten so that the stirring action in the reactor breaks up the molten sulfur feed as it cools to form small solid sulfur particles. The small sulfur particles advantageously have a large total surface area available for reaction with the potassium thiosulfate solution in the reactor.

The reaction mixture is primarily potassium thiosulfate solution that contains sulfite from the potassium sulfite, or potassium bisulfite or a mixture thereof feed stream (11) into the potassium thiosulfate/sulfur reactor (R-3). The reaction taking place is between the sulfite component supplied by the potassium sulfite, or potassium bisulfite or a mixture thereof and elemental sulfur in the potassium thiosulfate solution to produce additional potassium thiosulfate. The accumulating potassium thiosulfate is preferably taken off on a continuous basis from the continuous process but the reaction could be done on a batch basis if desired.

Preferably the sulfur is suspended in the reacting solution with stirring action in the CSTR. Alternatively the sulfur may be reacted in a fluidized bed reactor where the sulfur is in suspension in the reacting potassium thiosulfate solution by means of a circulation pump or updraft impeller or impellers. Also alternatively the sulfur may be in a static bed where the reacting potassium thiosulfate solution is circulated through the bed.

The reaction may be carried out at any temperature but the reaction is slow and faster reaction is favored at higher temperatures. Preferably the reaction temperature is controlled with heating coils to between about 70 and about 105° C., and more preferably about 93-99° C. (200 to 210° F.) for optimum reaction rates with solid sulfur particles and to limit R-3 to low or atmospheric reactor pressure. Higher reactor temperatures may also be employed but at temperatures above about 121° C. (250° F.), sulfur is in the molten/liquid state and higher reactor pressure and higher stirring agitation is required to keep molten sulfur disbursed into small droplets.

The reaction pH is controlled to neutral or slightly alkaline with the addition of potassium hydroxide or potassium carbonate, stream (02C). If potassium carbonate is used or if any residual carbonate is present from the potassium bisulfite produced, there will be CO₂ vented from the reactor

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in stream (07). The pH generally is between about 5 and about 9, preferably between about 6 and about 8.

In another embodiment of this step 4 (embodiment ii), this process step is done with hydrogen sulfide gas, and is carried out in any process equipment that promotes gas-liquid contacting for the absorption and reaction of H₂S gas with the potassium thiosulfate plus potassium sulfite, or potassium bisulfite or a mixture thereof reaction mixture.

Preferably the absorption solution is primarily a potassium thiosulfate solution or sulfite rich potassium thiosulfate solution containing some sulfite from potassium sulfite, or potassium bisulfite or a mixture thereof addition, this solution preferably is controlled to neutral or slightly alkaline pH. Reaction temperature is controlled with process cooling preferably above about 50° C. (120° F.) to minimize condensation of hydrocarbons and preferably below about 82° C. (180° F.) to limit moisture in unabsorbed T-3 vent gas. The pH generally is between about 5 and about 9, preferably between about 6 and about 8.

Preferably the absorption and reaction of H₂S gas is carried out in a packed absorber tower referred to as the Hydrogen Sulfide Absorber Tower (T-3) in FIG. 1. The H₂S feed gas stream (03) may consist of 100% H₂S gas to gas streams containing less than 1% H₂S. Preferably the H₂S gas stream is a concentrated H₂S gas stream containing 50% or more H₂S and is referred to as acid gas in gas plants and refineries coming off amine units used to remove H₂S from hydrocarbon streams. The absorption and reaction is selective for H₂S and rejects CO₂ and hydrocarbons that may be in the H₂S, acid gas feed stream (03) to T-3.

This embodiment of the process, step 4, for selectively absorbing and reaction of H₂S with potassium sulfite, or potassium bisulfite or a mixture thereof (or sulfite rich potassium thiosulfate) to produce potassium thiosulfate may be used in special applications for H₂S recovery and removal from gas streams. Using potassium sulfite, or potassium bisulfite or a mixture thereof as a selective, non-regenerative absorption agent for H₂S may be used as a process alternative for amine treating H₂S containing streams. In many small and remote locations not having the required utilities and infrastructure to support a regenerative amine treating process operation, potassium sulfite, or potassium bisulfite or a mixture thereof may be imported or produced on site to be used as a non-regenerative H₂S recovery reagent producing potassium thiosulfate. This process step may also be used in large gas plants and refineries in place of amine units to off load amine treating capacity and the acid gas produced by amine treating going to sulfur recovery units and thus increase overall amine treating and sulfur recovery capacity.

In large sulfur recovery operations that are typically found in oil refineries and gas plants, this potassium thiosulfate process may be used to supplement or substitute sulfur recovery operations resulting in increased total sulfur recovery capacity or alternative sulfur recovery operations for the facility.

Sulfur bearing H₂S/Acid Gas may alternatively be diverted from the main Claus Sulfur Recovery units to an incinerator for combustion to form an SO₂ gas stream. This effectively off loads the main Claus SRU for more total sulfur recovery capacity for the facility. Also directing H₂S/Acid Gas to the T-3, H₂S Absorber off loads additional H₂S gas going to the Claus SRUs. Treating incinerated Claus off gas in the SO₂ absorption step of the process eliminates the need for other more process demanding regenerative Claus tail gas treating units such as SCOT units which

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typically recycle H₂S/Acid Gas back to the Claus SRU which reduces Claus SRU capacity.

In another embodiment (embodiment iii), this process step (step 4) to react potassium sulfite, or potassium bisulfite or a mixture thereof or sulfite rich potassium thiosulfate, is performed with potassium polysulfide.

In yet another embodiment (iv), potassium sulfide is used, while in embodiment (v), potassium bisulfide is used.

Any of these embodiments may be carried out in process equipment that promotes mixing of the reaction mixture. This is a liquid-liquid reaction which takes place much faster than with elemental sulfur which is a solid-liquid reaction. In this liquid-liquid reaction case, elevated reaction temperature and strong mixing is not required. The reaction pH is controlled to neutral or slightly alkaline with the addition of potassium hydroxide or potassium carbonate, stream (02C). If potassium carbonate is used or if any residual carbonate is present from the potassium sulfite, or potassium bisulfite or a mixture thereof produced, there will be CO₂ vented from the reactor in stream (07). The pH generally is between about 5 and about 9, preferably between about 6 and about 8.

The final step is recovering the potassium thiosulfate product, i.e. separating the potassium thiosulfate from the process to obtain a product that can be stored, transported and sold. This step of collecting the potassium thiosulfate, may optionally additionally comprise concentrating the potassium thiosulfate solution. If the potassium thiosulfate solution is concentrated, this is done preferably by boiling or evaporating excess water out of solution to produce a concentrated solution or dry potassium thiosulfate product, if required. The potassium thiosulfate solution is typically concentrated to about a 50% or slightly higher solution concentration having a total sulfur concentration of about 17% S using an evaporator or Solution Concentrator (E-4).

The degree of concentration required to produce potassium thiosulfate at about 17% S concentration depends on the amount of excess water that is present in the potassium sulfite, or potassium bisulfite or a mixture thereof/sulfite rich potassium thiosulfate feed obtained in step 3, and in the sulfur feed streams added in step 4 of the process. Elemental sulfur contains no water and can eliminate the need for the concentration step to produce concentrated potassium thiosulfate solution if the potassium sulfite, or potassium bisulfite or a mixture thereof feed to step three is sufficiently concentrated. H₂S gas or polysulfide solution feed to the third step does add water to the potassium thiosulfate produced and generally requires concentration in the final process step to remove excess water.

Although not typical, concentration of the potassium thiosulfate solution may be accomplished by limiting cooling and allowing the temperature in T-1 and T-2 to be sufficiently high to allow water to exit in the vent stack gas as water vapor. This allows for production of a concentrated potassium sulfite, or potassium bisulfite or a mixture thereof solution.

Additionally the potassium sulfite, or potassium bisulfite or a mixture thereof-SO₂ absorption solution in T-1 and T-2 may become potassium thiosulfate-SO₂ absorption solution if desired by allowing and controlling recycle of potassium thiosulfate between T-1, T-2 and T-3 or R-3 through streams (11, 12 & 15). This potassium thiosulfate-SO₂ absorption mode of operation transports potassium thiosulfate solution to the T-1 and T2 SO₂ gas absorption system to allow evaporation of excess water into the vent stack gas stream (06, 16). SO₂ absorption by the potassium thiosulfate solution in T-1, T-2 produces a sulfite rich potassium thiosulfate

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solution which recycles back to T-3 or R-3 for reaction of sulfite to produce additional potassium thiosulfate low in sulfite.

An additional benefit of utilizing potassium thiosulfate solution in T-1 and T-2 is lower sulfate formation caused by partial oxidation of the sulfite component in the potassium thiosulfate absorption solution by residual oxygen in the SO₂ combustion gas stream (01). Lower oxidation is realized from lower sulfite concentration in the potassium thiosulfate solution and possibly also from the potassium thiosulfate component in potassium thiosulfate acting as an oxidation inhibitor. Another benefit is the ability to redistribute alkalinity between step two and step three process solutions. Any excess alkalinity coming into step three may be redistributed to step two in stream (12) to where the bulk of alkalinity is required for SO₂ absorption and then recycled back to step three in stream (11).

Lower concentration potassium thiosulfate may hold some potassium sulfate in solution. However, concentrated potassium thiosulfate has a low tolerance for potassium sulfate in solution. After concentrating, the potassium thiosulfate solution may be cooled before it is sent to storage in stream (08). On cooling, any significant amount of potassium sulfate above its solubility limit of about 0.9% will crystallize and drop out of solution. The potassium sulfate crystals, if any, may be filtered out of the concentrated potassium thiosulfate solution and processed as a separate product if desired.

As previously described, production volume of potassium bisulfite and potassium thiosulfate may be increased by diverting or adding more sulfur containing feed streams to the SO₂ combustion gas equipment or incinerator to increase SO₂ production. One of the feed gas streams to the incinerator is from the unabsorbed gas exit T-3, stream (07). Excess H₂S gas to T-3 helps to produce potassium thiosulfate with low residual sulfite concentration and the excess H₂S in stream (07) adds to SO₂ combustion gas generation.

The present invention furthermore provides for the continuous production of potassium thiosulfate by (A) providing a sulfur dioxide containing gas stream (01) and potassium containing base (02) to at least one absorption tower (T-1, T-2), while absorbing the gas into an absorption solution containing sulfite and/or thiosulfate (10, 15), which is circulated over the absorption tower (T-1, T-2), and (B) removing part of the absorption solution for obtaining a potassium sulfite containing solution (11) for (C) reacting the potassium sulfite containing solution with sulfur, hydrogen sulfide, potassium sulfide, potassium bisulfide and/or potassium polysulfide (03) with the addition of further potassium base if required (02) to obtain potassium thiosulfate in a vessel (T-3, R-3), recovering potassium thiosulfate (09), and (D) optionally concentrating the potassium thiosulfate in a heat exchanger (E-4) to obtain concentrated potassium thiosulfate (08).

The present invention furthermore provides for a continuous production of potassium sulfite, or potassium bisulfite or a mixture thereof by (A) providing a sulfur dioxide containing gas stream (01) and potassium containing base (02) to at least one absorption tower (T-1, T-2), while absorbing the gas into an absorption solution containing sulfite (10, 15), which absorption solution is circulated over the absorption tower (T-1, T-2), and (B) removing part of the absorption solution for obtaining a potassium sulfite/potassium bisulfite containing solution (11) and (D) optionally concentrating the potassium sulfite/potassium bisulfite in a heat exchanger (E-4) to obtain concentrated potassium sulfite/bisulfite (08).

The embodiments and preferences described for the process, and as exemplified by the description of the drawings apply to the continuous process description provided in the former two paragraphs.

What is claimed:

1. A process for preparing potassium thiosulfate, comprising the following steps:

Step (1a): providing a potassium hydroxide or potassium carbonate solution for neutralizing acid forming components;

Step (1b): providing a SO₂ contacting solution, containing at least some potassium sulfite or potassium bisulfite or potassium thiosulfate;

Step (2): providing sulfur dioxide gas;

Step (3): reacting the solutions of steps (1a) and (1b) and the gas of step (2) to absorb at least a portion of the SO₂ gas and to form a reaction mixture comprising potassium sulfite, or potassium bisulfite, or mixtures of potassium sulfate and potassium bisulfite, or sulfite rich potassium thiosulfate;

Step (4): adding sulfur and/or hydrogen sulfide and/or potassium bisulfide and/or potassium sulfide and/or potassium bisulfate to the reaction mixture and optionally potassium hydroxide or potassium carbonate, reacting the reaction mixture under suitable conditions to form potassium thiosulfate; and

Step (5): recovering the potassium thiosulfate by separating the potassium thiosulfate from the process and optionally concentrating the potassium thiosulfate.

2. The process of claim 1, wherein in step (5) potassium thiosulfate is recovered that has a concentration of about 40 wt % or higher, without concentration step.

3. The process of claim 1, wherein the reaction is carried out at a temperature of up to about 121° C.

4. The process of claim 1, wherein in step (4) the reaction mixture is subjected to agitation and increased pressure.

5. The process of claim 1, wherein in step (5) potassium thiosulfate is recovered with an amount of products other than potassium thiosulfate and water of about 5 wt % or less.

6. The process of claim 5, wherein in step (5) potassium thiosulfate is recovered with an amount of products other than potassium thiosulfate and water of about 2 wt % or less.

7. The process of claim 1, wherein in step (5) a potassium thiosulfate is recovered with an amount of sulfate of about 1 wt % or less (measured as potassium sulfate).

8. The process of claim 1, wherein in step (5) a potassium thiosulfate is recovered with an amount of sodium of about 1 wt % or less.

9. The process according to claim 1, wherein the sulfur dioxide gas originates from burning sulfur with oxygen; sulfur dioxide from tail gas or incinerated tail gas, coke operation, or by converting hydrogen sulfide to sulfur dioxide.

10. The process according to claim 1, wherein SO₂ absorption efficiency is maintained by adding alkaline potassium hydroxide or potassium carbonate to maintain solution pH in a range of between about 5 and about 10.

11. The process according to claim 10, wherein SO₂ absorption efficiency is maintained by adding alkaline potas-

sium hydroxide or potassium carbonate to maintain solution pH in a range of between 7 and 9.

12. The process according to claim 1, wherein the SO₂ gas contains CO₂, and in step (3) the solutions of steps (1a) and (1b) are controlled to a pH of less than about 8.5.

13. The process according to claim 1, wherein the process is used as an SO₂ gas scrubbing and absorption system, as a Tail Gas Treating Unit (TGTU) or as a Flue Gas Desulfurization (FGD) system for treating and cleaning gas streams containing sulfur components before being discharged to atmosphere.

14. The process according to claim 1, wherein in step (4), sulfite from step (3) is reacted with the sulfur or sulfide containing compounds recited in step (4) to produce additional potassium thiosulfate.

15. The process according claim 1, wherein the process is a continuous process.

16. The process for the production of potassium thiosulfate according to claim 1, by

(A) providing a sulfur dioxide containing gas stream (01) and potassium containing base (02) to at least one absorption tower (T-1, T-2), while absorbing the gas into an absorption solution containing at least some sulfite, bisulfite, or thiosulfate (10, 15), which absorption solution is circulated over the absorption tower (T-1, T-2), and

(B) removing part of the absorption solution for obtaining a potassium sulfite containing solution (11) for

(C) reacting the potassium sulfite containing solution with Sulphur, hydrogen sulfide, polysulfide, sulfide and/or bisulfide (03) with the addition of further potassium base if required (02) to obtain potassium thiosulfate in a vessel (T-3, R-3), recovering potassium thiosulfate (09), and

(D) optionally concentrating the potassium thiosulfate in a heat exchanger (E-4) to obtain concentrated potassium thiosulfate (08).

17. The liquid potassium product obtained by a process according to claim 16, wherein the potassium product comprises thiosulfate in an amount of about 40-56 wt %, wherein the amount of products other than potassium thiosulfate and water is about 5 wt % or less.

18. The liquid potassium product of claim 16, wherein the amount of products other than potassium thiosulfate and water is about 2 wt % or less.

19. The liquid potassium product of claim 16, wherein the impurities comprise an amount of sulfate of about 1 wt % or less (measured as potassium sulfate).

20. The liquid potassium product according to claim 16, wherein the product has a storage stability of at least half a year or more, wherein storage stability means that the liquid remains clear with no crystals or deposition visible to the naked eye.

21. The liquid potassium product according to claim 16, which is a liquid fertilizer optionally used in combination with other fertilizers.

22. The process of claim 4, wherein the sulfur added in step (4) is molten sulfur and the reaction mixture is reacted at a temperature above about 121° C.

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