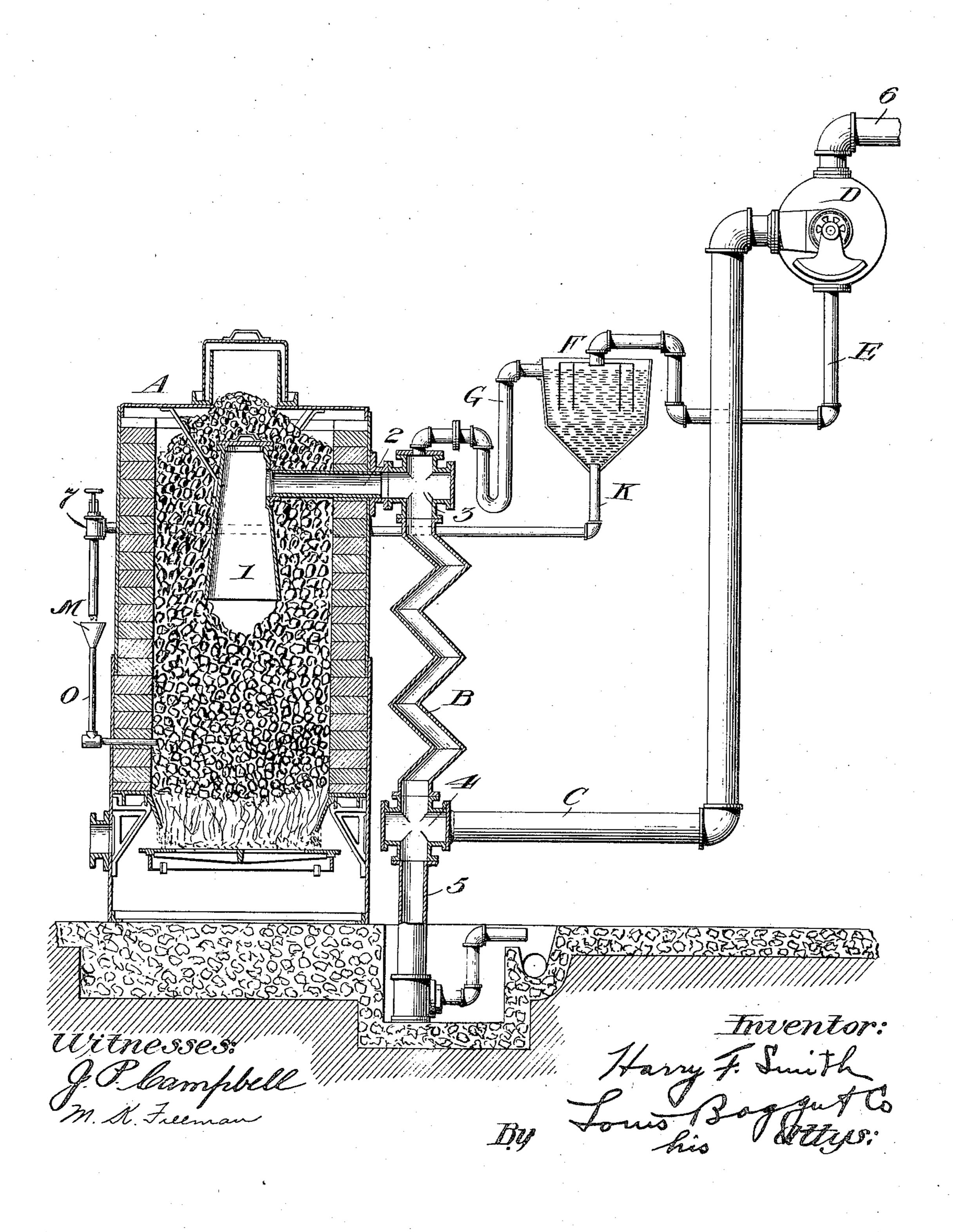
H. F. SMITH.

METHOD OF GENERATING PRODUCER GAS.

APPLICATION FILED AUG. 25, 1908.

928,808.

Patented July 20, 1909.



UNITED STATES PATENT OFFICE.

HARRY F. SMITH, OF LEXINGTON, OHIO.

METHOD OF GENERATING PRODUCER-GAS.

No. 928,808.

Specification of Letters Patent.

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Application filed August 25, 1908. Serial No. 450,176.

To all whom it may concern:

Be it known that I, Harry F. Smith, a citizen of the United States, residing at Lexington, in the county of Richland and State of Ohio, have invented certain new and useful Improvements in Methods of Generating Producer-Gas from Bituminous Coal, of which the following is a specification.

My invention relates to a method of generating producer gas from bituminous coal and particularly a process whereby the tar and volatile matters ordinarily condensable may be converted into fixed gases.

In the accompanying drawing I have shown a view partly in section of an apparatus which may be used in carrying out my invention, but I do not desire to be limited

to any specific construction.

A represents the producer, which is of the 20 general type of producer furnaces, but which is adapted to carry a deep bed of fuel. Supported from the top of the producer and in the center of the furnace is a tubular receptacle 1, from which a pipe 2 extends through 25. the side of the producer which carries the gas from the producer. A coupling 3 is connected to the pipe 2 and extending downwardly and connected to the coupling is a zig-zag pipe B for scrubbing and cooling the 30 gas. The gas as it passes from the furnace is subjected to a treatment of water and by the zig-zag formation of the pipe the gas is cooled by coming into contact with the water and at the same time the coarse dirt is 35 washed from the gas. A coupling 4 is connected to the pipe B and from this coupling a drain pipe 5 is connected, through which the dirty water passes to the sewer or drain. Pipe C is connected to the coupling 4 and conveys the gas to a tar extractor D, which may be of any approved form. The tar and the water associated with it are extracted from the gas and the clean gas will pass out from the extractor through the pipe 6. The 45 tar and water will pass out of the extractor D through a pipe E and will be conducted to a separator F. The tar, being heavier than the water, will go to the bottom of the separator, where it passes through a pipe K and 50 from this pipe it empties into a funnel M connected to a pipe O, the pipe O leading into the producer at a sufficient height above the grate to discharge the tar into the mass of incandescent coke that lies within the lower 55 part of the producer, and in contact with this

hot coke the tar is broken up, being then decomposed into fixed gases and discharged as such from the top of the producer. Any portion of the tar which might not be decomposed by this process is separated from 60 the gas again by the tar extractor D and returned to the fire in the manner above explained. The tar is admitted to the furnace through the pipe O by the operation of a regulating valve 7 connected to the pipe K. 65 A pipe G is connected to the separator F, which conveys the water from the separator to the coupling 3, to which the pipe is connected, and this water from the separator passes through the scrubber B for washing 70 and cooling the gas, thereby using the same water twice, in the tar extractor and the scrubber. The fuel is blasted with air or air and steam continuously, thus keeping the temperature of the fuel bed uniform, giving 75 a continuous and proper operating temperature.

The gas and water are thrown from side to side by the zig-zag scrubber B and in this way thoroughly mixed. The gas after being 80 cooled is treated to a second cleaning operation for removing the tar by the extractor D, where any condensable substances, such as tar, oils and the like, which are detrimental to the use of the gas are extracted. From 85 this extractor clean gas is passed to the gas tanks or any suitable receptacles for use. The tar extracted from the gas together with the water which may be associated with it, providing water is used in the tar 90 extractor, will pass through the pipe to a separator where the tar and water are separated, the water passing from the separator to the scrubber and the tar to the furnace. By this system I have provided means 95 whereby the gas can be thoroughly cleaned and the tar and other condensable substances are conveyed to the furnace after the gas and tar have been separated. In this manner not only a convenient means is provided for 100 disposing of the tar, but also for increasing the producer efficiency by converting into gas its thermal energy, and by this method the calorific intensity is also increased since the gas resulting from the decomposition of 105 the tar in contact with the hot coke consists almost entirely of gas of high calorific intensity, such as marsh gas and olefiant gas, and these constituents are very desirable in the producer gas for whatever purpose it 110

may be employed. The advantages of this method are immediately apparent for the reason that in most instances the tar is disposed of as a by-product and is never con-5 verted into fixed gas in the producer. In many instances and under certain conditions the disposition of a quantity of tar as a byproduct in this way is a difficult and expensive matter, and even could it be disposed of, 10 it is on account of its high heating value much more valuable as a gas producing agent than as a by-product for other uses, and the manner of returning the tar to the producer as outlined not only makes a convenient way 15 to dispose of the tar, but increases the producer efficiency by converting the tar into gas.

Having fully described my invention, what

I claim as new and desire to secure by Letters Patent is:—

A method for generating producer gas consisting in blasting the fuel with air and steam for obtaining the gas from the fuel, then cooling the gas, then extracting the tar and water from the gas, then separating the tar and water, and then discharging the tar into the incandescent fuel in the producer where it is converted into gas, and the water from the separator adapted to cool and wash the gas.

In testimony whereof I affix my signature, 33

in the presence of two witnesses.

HARRY F. SMITH.

Witnesses:

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A. B. Beverstock,

R. B. HUNTER.